Nitrogen Reduction Pilot Study at the Fairhaven, MA Water Pollution Control Facility



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### **Executive Summary**

The Fairhaven Water Pollution Control Facility (WPCF) on Arsene Street in Fairhaven, MA provides secondary wastewater treatment for the majority of the Town of Fairhaven prior to discharging the treated effluent to the Acushnet River. In 2014, this facility discharged a monthly average of 308 pounds per day (lbs/day) of total nitrogen (TN), equating to approximately 15 milligrams per liter (mg/L) at the facility's annual average daily flow of 3.1 million gallons per day (MGD). Under the new draft National Pollutant Discharge Elimination System (NPDES) permit, the monthly average effluent limit for TN will be reduced to 125 lbs/day, or 3 mg/L at 5 MGD, the design average daily flow for the WPCF. In order to consistently comply with the new lower TN limits, the Fairhaven WPCF needs to install additional nitrogen removal facilities and modify the current operation of the WPCF.

Based on a detailed evaluation conducted by Stantec (formerly FST) for the Fairhaven WPCF as part of a Phase 2 Wastewater Management Plan (WMP), converting the existing activated sludge process to a 4-stage Bardenpho process with BioMag<sup>™</sup> was found to constitute the most feasible alternative for nitrogen reduction. BioMag<sup>™</sup> is an enhanced biological process that utilizes magnetite as a ballast material to combine with the biological floc in the aeration basins. In order to confirm the ability of the 4-stage Bardenpho process with BioMag<sup>™</sup> to consistently reduce the TN concentration to less than 3 mg/L, the Town of Fairhaven applied for and received a grant from the Massachusetts Office of Coastal Zone Management, Buzzards Bay National Estuary Program to conduct a full-scale BioMag<sup>™</sup> pilot study at the Fairhaven WPCF.

A full-scale "modified" 4-stage Bardenpho process with BioMag<sup>™</sup> nutrient removal pilot study was conducted, with the entire flow for the plant handled in one aeration train. Since budget and time constraints made it impossible to modify one of the smaller existing secondary clarifiers to mimic a true 4-stage Bardenpho process, the pilot study's goal was to demonstrate the ability to achieve 5 mg/L TN in the final effluent, understanding that full-scale operation would have a second anoxic and reaeration process to polish from <5 mg/L to 3 mg/L TN.

Evoqua, the pilot plant vendor, set up a pilot trailer that housed the magnetite feed and recovery equipment and was located adjacent to the aeration train selected for the study. The Town rented a pump to provide internal recirculation through the aeration train, and return activated sludge (RAS) pumping rates were adjusted. The aeration system was turned off in the first aeration tank, and a mixer was installed to keep solids in suspension. From initial charge (magnetite addition) through plant stabilization, Evoqua took lead responsibility for the pilot plant's operation. During this phase, Evoqua trained the WPCF staff in the operation of the BioMag<sup>™</sup> system and the conduct of the test protocols so that they could take primary responsibility for operating the plant during the test phase. Evoqua also set up an Excel spreadsheet in which WPCF staff entered monitoring data, and coordinated with the staff about data collection using modified WPCF laboratory sheets and a trailer checklist. In the test phase,



Evoqua personnel maintained a presence on site and regularly monitored the pilot plant performance.

The pilot plant trailer arrived early in September 2015, magnetite addition began at the end of September 2015, process modifications were made to stabilize the system over the following month, the test phase began the third week of October 2015, supplemental carbon addition began in early November, and system parameters were optimized to try and demonstrate compliance with a 5 mg/L TN permit limit from mid-November through December 16, 2015, the final date of the pilot study.

The results of the pilot study demonstrated that operation of the modified 4-stage Bardenpho with BioMag<sup>™</sup> system would result in significantly lower effluent TN concentrations than the WPCF was discharging prior to the study. However, the pilot study did not consistently produce the required effluent TN concentration of 5 mg/L; the average TN concentration in the final effluent after supplemental carbon addition at 100 gallons per day (gpd) (the desired supplemental carbon dosage), was 6.3 mg/L. The shortfall in meeting this limit could be due to several factors, including the internal recycle and RAS pumping rates being lower than desired for optimum TN removal, the need to consistently maintain a higher magnetite to biosolids ratio, and/or increasing the supplemental carbon addition. We believe adjusting one or more of these factors would have led to achieving 5 mg/L TN in the final effluent TN value of 3 mg/L would be attained, satisfying the draft NPDES permit requirement for this parameter. This treatment technology is thus an effective means for significantly reducing nitrogen discharged to the plant's receiving water, the Acushnet River, and could be applied to other area WPCFs, depending on existing tankage, process layout and operation, and effluent TN requirements.

The pilot plant also achieved excellent total suspended solids (TSS) and 5-day biochemical oxygen demand (BOD<sub>5</sub>) removals, averaging 8 mg/L and 4 mg/L in the final effluent, respectively, over the course of the study.

Costs and energy use of this system are major issues, however, and should be investigated more thoroughly before proceeding with full-scale implementation. In 2014, the Phase 2 WMP estimated that the construction cost for the 4-stage Bardenpho with BioMag<sup>TM</sup> system would be about \$9.8 million. The additional operational costs are very significant as well, expected to exceed \$200,000 per year, and the increased energy requirements would greatly expand the carbon footprint of the Fairhaven WPCF. We note that the majority of the costs and energy requirements are inherent in the 4-stage Bardenpho process that would be a part of all the nitrogen reduction alternatives identified in the Phase 2 WMP for the Fairhaven WPCF.

Another issue encountered during the pilot study was damage to one of the final clarifier rake arms, believed to result from the magnetite sludge that is so effective in settling out solids and associated pollutants, and slightly heavier than normal secondary sludge. The rake arms were over 25 years old and in a deteriorated condition, making them susceptible to damage from the slightly heavier magnetite sludge.



INTRODUCTION

# **1.0 INTRODUCTION**

### 1.1 GENERAL

The Fairhaven, MA WPCF on Arsene Street is a secondary treatment plant, with a design capacity to process an average daily flow of 5.0 MGD and a peak hourly wet weather flow of 16 MGD; it is currently operating at an annual average daily flow of about 3.1 MGD. Following preliminary treatment, the liquid treatment train consists of two parallel trains, each with a primary clarifier, a three-chamber aeration tank and two final clarifiers. An ultraviolet irradiation system completes the liquid treatment process. Under present loading conditions, only one treatment train is normally placed in operation. Regarding sludge processing, primary sludge is sent to the onsite anaerobic digesters, waste activated sludge (WAS) is thickened by a gravity belt thickener, and the digested primary and thickened secondary sludges are transported offsite to a waste-to-energy facility where the sludge is incinerated. An onsite combined heat and power system uses the digester gas to generate electricity that offsets some of the plant's electrical use.

Secondary treatment at the WPCF is provided by a conventional activated sludge system, including two aeration trains, each with three aeration tanks, and two 45-foot diameter and two 75-foot diameter final settling tanks. Each aeration tank is equipped with fine bubble membrane diffusers and has an operational volume of 155,580 gallons. The 45-foot diameter settling tanks each have a volume of 119,000 gallons, and the 75-foot diameter settling tanks each have a volume of 429,600 gallons. Settled activated sludge is returned to the head of the aeration trains using seven RAS pumps, which provide an available total return flow rate of 9.7 MGD (with one large pump out of service).

Presently, the Fairhaven WPCF operates most of the time with two primary settling tanks, three aeration tanks (one aeration train) and two 75-foot diameter secondary settling tanks on-line. When flow rates are low, typically during July, August and September, only one primary and one 75-foot diameter secondary settling tank are on-line.

The final effluent discharges to the Acushnet River, also known as the New Bedford Inner Harbor, which has excessive nitrogen concentrations. The Massachusetts Department of Environmental Protection (MassDEP) has identified the Fairhaven WPCF as the major contributor of nitrogen to the New Bedford Inner Harbor in its Massachusetts Estuaries Project nitrogen modeling report for this water body.



INTRODUCTION

### 1.1.1 WATER QUALITY DATA

The following presents average water quality operating data for the Fairhaven WPCF in 2014:

Average Daily Flow (MGD):	3.1
Raw Influent TN mg/L:	29.1
lbs/day: Final Effluent TN	612
mg/L: Ibs/day:	15.1 308
Raw Influent TSS (mg/L): Final Effluent TSS (mg/L):	129 8.4
Raw Influent BOD5 (mg/L):	150
Final Effluent BOD₅ (mg/L):	6.6
Final Effluent Fecal Coliform (colony-forming-units per 100 milliliters [cfu/100 mL]):	10

The WPCF obtained a draft NPDES permit in 2010 from MassDEP and the U.S. Environmental Protection Agency (EPA). The draft NPDES permit requirements are listed in Table 1.

Parameter	Average Monthly	Maximum Daily
Flow	5.0 MGD	Report
BOD₅	30 mg/L	45 mg/L
TSS	30 mg/L	45 mg/L
рН	6.5 –	8.5
Fecal Coliform	88 cfu/100 mL	260 cfu/100 mL
Enterococci	35 cfu/100 mL	276 cfu/100 mL
Total Nitrogen	125 lbs/day	Report

### **Table 1 - Draft NPDES Permit Requirements**

This permit requires that the facility release less than 125 lbs/day TN on a monthly average basis, which equates to 3 mg/L at 5 MGD. The permit does not indicate that this is a seasonal limit, but other area WPCFs with a similar TN limit are only required to comply with this value from May to October. A copy of the draft NPDES permit is located in Appendix A. The current NPDES permit for the Fairhaven WPCF requires effluent monitoring for TN, but there are no TN limits.



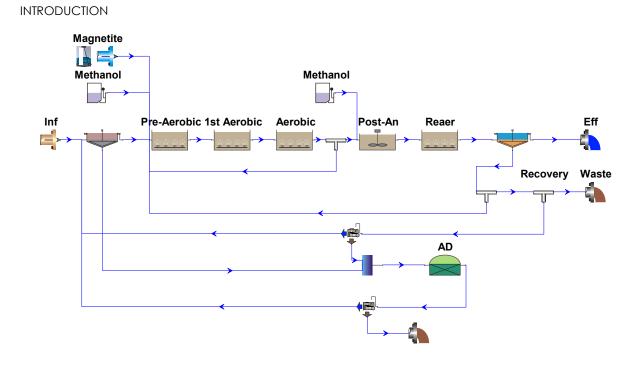
INTRODUCTION

### 1.1.2 PHASE 2 WASTEWATER MANAGEMENT PLAN RECOMMENDATIONS

Under the Phase 2 WMP completed in 2014, Stantec modeled several different options for reducing the final effluent TN discharge to within the new draft NPDES permit requirements. One of the alternatives investigated was a 4-Stage Bardenpho, or aerated anoxic process. In this arrangement, the first and third aeration tanks in each train would be set up as anoxic zones, with the second aeration basin and the smaller secondary clarifier used for aerobic zones. Recycle in the amount of 200 - 400% of the influent flow rate is returned from the end of the first aerobic zone to the start of the first anoxic zone. RAS from the secondary clarifiers, also in the amount of 200 - 400% of the influent flow rate, is returned to the first anoxic zone as well. Waste sludge would be thickened and sent along with primary sludge to the anaerobic digesters. Filtrate from the thickener is returned just downstream of the preliminary treatment facility. Modeling results indicated that the 4-stage Bardenpho process with methanol addition would result in TN levels in the plant effluent of approximately 4 or 5 mg/L, which exceeded the draft permit limit of 3 mg/L.

To further reduce the effluent TN content, the Phase 2 WMP recommended incorporating the BioMag<sup>™</sup> process into the 4-stage Bardenpho process. BioMag<sup>™</sup> is an enhanced biological process that utilizes magnetite as a ballast material to combine with the biological floc in the aeration basins. This combination of materials has a high specific gravity that rapidly settles out in the secondary clarifiers. This in turn enables the biological treatment system in the aeration tanks to operate at elevated mixed liquor solids concentrations, which can enable the processing of higher flows while also achieving enhanced suspended solids, nitrogen and phosphorus removal rates. When incorporating the BioMag<sup>™</sup> process into the 4-stage Bardenpho process, the first aeration tank would be a pre-aerobic/anoxic zone, the second and third aeration tanks would be aerobic zones, and the smaller secondary clarifier would be converted to create post-anoxic and reaeration zones. As shown in Figure 1, magnetite is added at the beginning of the first pre-aerobic tank where it is blended with RAS from the secondary clarifiers that is also combined with magnetite. Excess magnetite is recovered from the WAS by means of a magnetic drum separator and returned to the head of the process. Internal recycle in the amount of 200 - 400% of the influent flow rate is returned from the end of the aerobic zone to the start of the pre-aerobic zone. Methanol is also added as a carbon food source to facilitate the denitrification process.







The results of the modeling indicated that with incorporation of the 4-stage Bardenpho and BioMag<sup>™</sup> processes, including supplemental carbon addition, the WPCF would be capable of reducing the final effluent TN level to less than the permit required 3 mg/L. Previous studies have confirmed this achievement.<sup>1</sup> As stated earlier, Stantec modeling results indicated the final effluent TN level would be 4 or 5 mg/L without the benefit of the BioMag<sup>™</sup> process.

Following the recommendations of the Phase 2 WMP, the Town of Fairhaven applied for and received a grant from the Massachusetts Office of Coastal Zone Management, Buzzards Bay National Estuary Program to conduct a full-scale BioMag<sup>™</sup> pilot study to evaluate the effectiveness of the process to meet the draft NPDES permit limit for TN. This report describes the pilot study, the results achieved, and the applicability of using this technology in the future at the Fairhaven WPCF and other area WPCFs in an effort to reduce nitrogen loadings to meet future NPDES requirements and significantly reduce nitrogen concentrations in receiving waters.

# 1.2 PURPOSE AND SCOPE

The primary objective of this pilot study was to demonstrate that converting the existing activated sludge process at the Fairhaven WPCF to a 4-Stage Bardenpho process with BioMag<sup>™</sup> would allow the plant to effectively maximize its treatment capacity and reliably achieve compliance with the proposed TN permit limits. The effluent TN was expected to be 3 mg/L with full-scale implementation of the process. However, since budget and time constraints made it impossible to modify one of the smaller existing secondary clarifiers to mimic a true 4-stage



### PILOT STUDY

Bardenpho process, the pilot study's goal was to demonstrate the ability to achieve 5 mg/L TN, understanding that full-scale operation would have a second anoxic and reaeration process to polish from <5 mg/L to 3 mg/L TN in the final effluent. Final effluent phosphorus levels would also be reduced with implementation of the "modified" 4-Stage Bardenpho process with BioMag<sup>™</sup>, but this nutrient was not monitored during the pilot study because there is no phosphorus limit in the draft NPDES permit.

# 2.0 PILOT STUDY

# 2.1 NARRATIVE SUMMARY OF PILOT STUDY PROCESS

A full-scale "modified" 4-stage Bardenpho process with BioMag<sup>™</sup> nutrient reduction pilot study was conducted, with the entire flow for the plant handled in one aeration train. Primary effluent flowed by gravity to the first aeration tank, and from there to the second and third aeration tanks in a plug flow mode. Each aeration tank is 40 ft x 40 ft x 13 ft deep, for a combined volume of 0.47 million gallons (MG) - more than enough volume for the modified 4-stage Bardenpho with BioMag<sup>™</sup> system established for this study. The target mixed liquor concentration was approximately 5,600 mg/L. The first zone (first aeration tank) was converted into an anoxic zone by turning the air off, and a mixer was installed to keep the solids in suspension. The second zone (second aeration tank) was aerated anoxic, and the third zone was aerobic. The Town rented an internal recirculation pump to pump 200 - 400% of the flow capacity from the last to the first aeration tank to effectively achieve the required TN levels (Figure 2).



Figure 2 - Internal Recirculation Pump Rented by Town



#### PILOT STUDY

Mixed liquor from the aerobic zone flowed by gravity to one of the existing secondary clarifiers. RAS pumps transported RAS from the secondary clarifiers in the range of 200 - 400% of the flow capacity to the first aeration tank. Secondary effluent flowed by gravity through existing piping to the existing disinfection system.

The BioMag<sup>™</sup> trailer housed the magnetite feed and recovery equipment and was located adjacent to the first two aeration tanks of the train that was in operation for the pilot study. The equipment was similar to that used in previous full-scale BioMag<sup>™</sup> pilot studies; the trailer at the Fairhaven WPCF is shown in Figure 3.



Figure 3 – BioMag™ Pilot Plant Trailer



#### PILOT STUDY

A pump located in the aeration tank effluent channel diverted a 100-gpm slipstream of the mixed liquor flow to the magnetite feed/ballast mix tank set up adjacent to the BioMag<sup>™</sup> trailer. An automated feed system metered dry magnetite into the well-mixed ballast mix tank, where the magnetite was enmeshed in the biological floc (Figures 4 and 5). Ballasted mixed liquor was then pumped from the magnetite feed tank back to the first aeration tank. It took approximately three weeks to charge the mixed liquor with the initial dose of magnetite.



Figure 4 - Automated Magnetite Feed System



PILOT STUDY



Figure 5 - Ballast Mix Tank

Another RAS slipstream was diverted, on the order of 10 - 20 gpm, to waste excess ballasted sludge to the magnetite recovery system using a pump located in the RAS chamber ahead of the first aeration tank. The waste sludge flowed through an in-line shear mill, and then onto the magnetic recovery drum, both of which were housed in the BioMag<sup>™</sup> trailer (Figure 6). The recovered magnetite was dropped into the ballast mix tank. The waste biological solids were pumped from the bottom of the recovery drum to the first aeration tank in the off-line aeration train, where they flowed by gravity through a tank drain to the overflow primary settling tank, and were then pumped to the gravity belt thickener. The magnetite feed/recovery system had a high-level shutoff switch to prevent an inadvertent tank overflow.



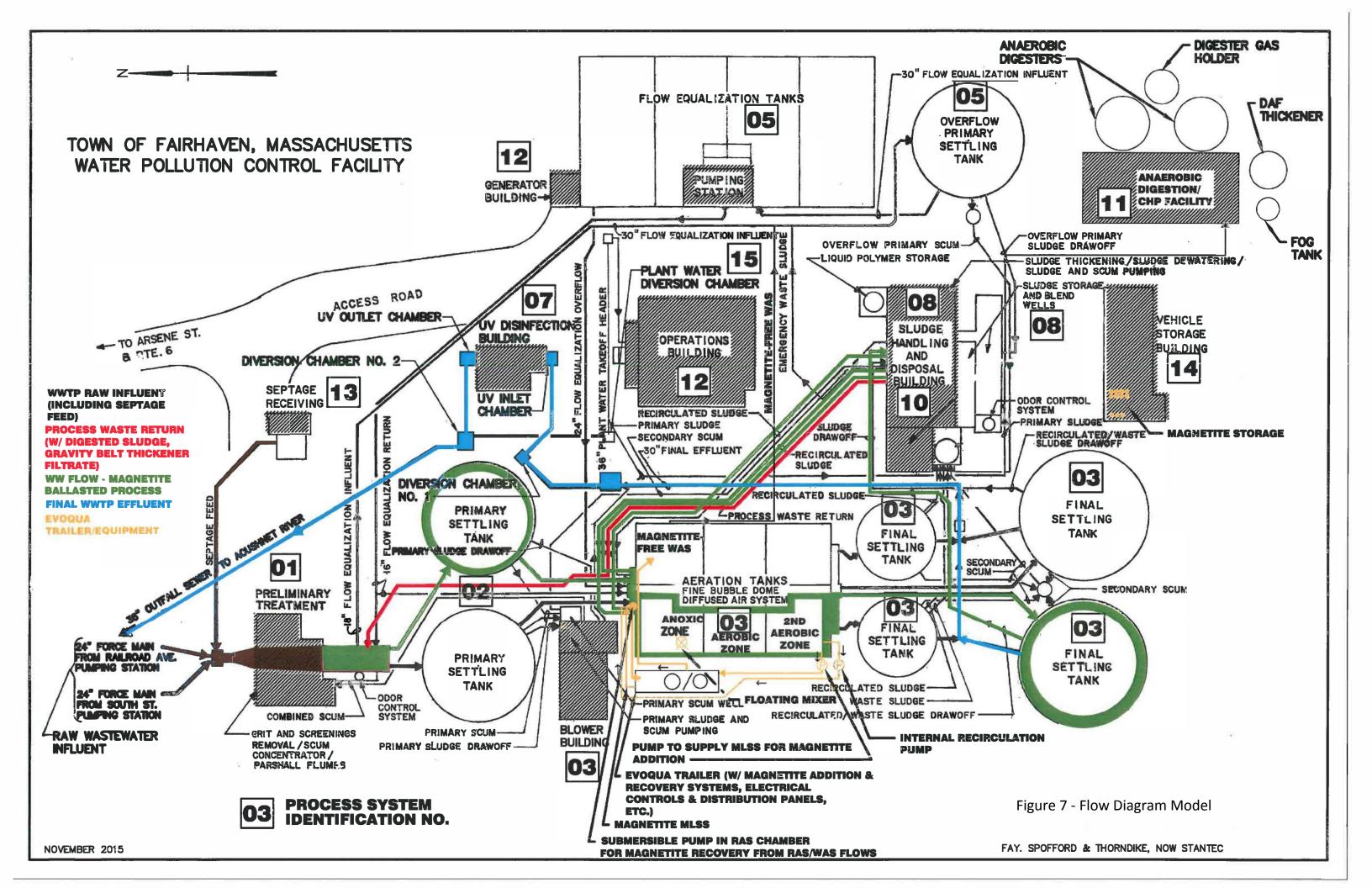
PILOT STUDY



Figure 6 - Shear Mill (Foreground) and Magnetic Recovery Drum (Background)

Figure 7 presents a schematic layout/process flow diagram of the Fairhaven WPCF, including the BioMag™ pilot study components described previously.





PILOT STUDY

### 2.2 PILOT PLANT PERFORMANCE PARAMETERS

Table 2 presents the main parameters assumed for the pilot plant operation.

	Primary Effluent Characteristics	Required Performance Final Effluent	Measure
Flow	3 MGD		
TKN	42 mg/L		
TN		5.0 mg/L	Average Monthly
TSS	62 mg/L	<30 mg/L	Average Monthly
BOD	142 mg/L	<30 mg/L	Average Monthly

#### Table 2 - Pilot Plant Performance Parameters

# 2.3 PROJECT SCHEDULE

Table 3 presents the schedule for the BioMag<sup>™</sup> pilot study. This timeframe represented a "warmweather" operation, with plant influent wastewater temperatures varying from 20.6 degrees Centigrade in early October 2015, to 14.5 degrees Centigrade on the last day of the pilot study, December 16, 2015.

Phase	Date
1. Begin Mobilization	September 8, 2015
2. Begin Charging	September 28, 2015
3. Begin Testing	Upon achievement of stable operation, October 22, 2015
4. MicroC Addition @ 35 gal/day	November 8, 2015
5. MicroC Addition @ 70 gal/day	November 9, 2015
6. MicroC Addition @ 100 gal/day	November 12, 2015
7. Last day of pilot operation	December 16, 2015

Table 3 -	Pilot Study	y Schedule
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PILOT STUDY

# 2.4 PILOT OPERATIONS

From initial charge (magnetite addition) through plant stabilization, Evoqua, the pilot plant vendor, took lead responsibility for the pilot plant's operation. During this time, Evoqua also trained the WPCF staff in the operation of the BioMag<sup>™</sup> system and the conduct of the test protocols so that they could take primary responsibility for operating the plant during the test phase. During the test phase, Evoqua personnel maintained a presence on site and regularly monitored the performance of the pilot plant and provided assistance and counsel as necessary.

### 2.4.1 Training

Town personnel and a Stantec intern providing weekday and weekend sampling and monitoring, respectively, were trained by Evoqua on sample collection and logging, as well as magnetite analysis, at the beginning of the project during pilot plant startup. Appendix B contains a copy of the training sign-in sheets.

Topics covered by the Town personnel training included BioMag<sup>™</sup> basics of operation, ballasted treatment process, process flows, sampling locations, procedures and methods, trailer operations and alarming, troubleshooting alarms, targets for the project and system adjustments to achieve them. Topics covered by the Stantec intern training included wastewater treatment process and components, pilot plant components, environmental safety and health, emergency awareness, sludge blanket level measurement, and dissolved oxygen (DO), pH, temperature and oxidation reduction potential (ORP) meter measurements and recording.

# 2.5 ANALYTICAL TESTING

In addition to their normal duties for operating and maintaining the Fairhaven WPCF, town staff was tasked with taking the daily readings, conducting a routine walkthrough of the trailer, recording data, and recording the data in an Evoqua-supplied Excel file that was pertinent to the pilot study. Evoqua Process Engineers supplied guidance to town staff to make adjustments to the biological, ballasted, and chemical feed components of the system. This included routine inspections and adjustments of the BioMag<sup>™</sup> test equipment, daily sampling rounds, chemical feed adjustments, and laboratory analyses. BioMag<sup>™</sup> system monitoring included the following:

- Raw influent flow rate
- Primary effluent and final effluent BOD, TSS and VSS
- Final effluent ultraviolet intensity and percent transmittance
- Raw influent, primary effluent, final effluent and thickener filtrate nitrite (NO<sub>2</sub>-N), nitrate (NO<sub>3</sub>-N), ammonia (NH<sub>3</sub>-N), total Kjeldahl nitrogen (TKN) and TN (by certified laboratory)
- Daily readings with Hach TNT vials for NH<sub>3</sub>-N, NO<sub>3</sub>-N and TN (by WPCF laboratory)



#### PILOT STUDY

- Primary effluent temperature
- Acidity (pH) in the primary effluent, aeration tanks (zones) 1, 2, 3 and final effluent
- Alkalinity in the raw influent, primary effluent and final effluent
- DO and ORP in zones 1, 2 and 3
- MLSS, MLVSS, magnetite and MLSS biological concentration in zones 1, 2 and 3
- 5-minute and 30-minute settle-o-meter, and sludge volume index (SVI) in zone 3
- Magnetite:biosolids ratio in zone 3
- RAS flow rate
- TSS, magnetite and biological solids concentration in the RAS
- Internal wastewater recycle speed
- Secondary clarifier sludge blanket level
- Polymer dial speed, level and feed rate (when applicable)
- Magnetic drum speed and shear mill current and speed
- WAS flow and TSS, magnetite and biological solids concentration and mass to and from magnetic drum
- Percent recovery of magnetite and biological solids from magnetic drum
- Pounds of TSS, magnetite and biological solids, and magnetite:biosolids ratio in zones 1, 2 and 3, final clarifier, and total plant inventory
- Target and actual solids retention time (SRT)
- Target WAS mass, concentration and flow rate
- Supplemental carbon (MicroC) feed rate

All sample collection and analyses, except for non-test kit nitrogen and some alkalinity analyses, were completed by town staff (and the Stantec intern on the weekend) in accordance with the collection, sampling and analytical procedures as detailed in the previously submitted Quality Assurance Project Plan (QAPP). All nitrogen analyses, and some alkalinity analyses, were completed by an outside certified laboratory, Microbac.

Appendix C contains a copy of the Excel spreadsheet set up by Evoqua personnel that shows the results of the parameters that were monitored, excluding MicroC, which was added as described in Section 3.4 - Nitrogen Data. We highlighted a few of the results in this spreadsheet that look "questionable", but kept them in the spreadsheet because the backup data support the results. We note there are some missing data in this spreadsheet during the first week of October 2015 as the systems were starting up, in the final week of the pilot study in December 2015 when the flow to the magnetite recovery drum was not recorded, and in the final two weeks of December 2015 following the end of the pilot study when the systems were shutting down.

Appendix D includes the pilot trailer checklist for readings taken by town personnel and the Stantec intern for items such as sludge blanket height, operation of magnetite feed, magnetic recovery drum, polymer feed, Kady (shear) mill, internal recycle pump, and air compressor and dryer, various control readings, and DO, pH, ORP and temperature in zones 1, 2 and 3.



#### OPERATING DATA AND ANALYSIS

Appendices E and F contain back-up Fairhaven WPCF laboratory data sheets for BOD and solids analyses, respectively, completed by town personnel. The solids backup sheets also contain temperature, pH and nitrogen data, with the nitrogen data determined by Hach TNT vials in the WPCF laboratory; we did not include this nitrogen data in Appendix C or in our later review of nitrogen results, relying instead on the nitrogen data from Microbac. Also, the pH data for the aeration tanks shown in the spreadsheet in Appendix C originates from the trailer checklist, and not the values shown on the solids backup sheets. Appendix G contains the laboratory reports completed by Microbac.

During the last few weeks of the pilot study, the company supplying MicroC provided a Nitratax probe made by Hach that gave real-time values and trends of combined NO<sub>2</sub>-N and NO<sub>3</sub>-N (NOX) concentrations leaving zone 1. This proved helpful in determining some of the limiting factors within the pilot system.

### 2.6 PILOT OPERATIONS AND STAFFING

Evoqua provided a Process Engineer to commission, train, provide technical support, and assist with an Operations Report. Fairhaven WPCF staff handled pilot operations and testing once the pilot plant was stabilized.

# 3.0 OPERATING DATA AND ANALYSIS

This report section presents and discusses the results of the full-scale BioMag™ trial. The demonstration began in early September 2015. The system experienced difficulties in the first few weeks of the trial until the "bugs" were eventually worked out, and steady state operation began in mid-October 2015. The early challenges were primarily due to two factors. First, the temporary pump layout had issues with entraining air and trapping it in the temporary hoses. This effect was exaggerated due to the shallow sump areas housing pumps along with the use of flexible hoses. Though the hose had an air relief point close to the pump, there was not enough time for the air to separate to the top of the pipe and escape. The air that continued downstream of the air relief then became trapped in the lines, eventually slowing and stopping flows to the trailer. To combat this, all the lines were pitched and additional air relief points were installed. The second major challenge revolved around filament growth. With all of the biological changes to the existing system including water temperature, rapidly increasing the SRT, achieving complete nitrification, gaining de-nitrification, changing the air configuration, adding a new mixing regime in the first cell, and stopping chemicals used to help reduce the septicity of the influent, the plant grew multiple filaments and ultimately an unhealthy biology. A third party was consulted to gain a better understanding. Jeffery MacDonald, M.S., of MacDonald Environmental Services based in Oak Creek, Wisconsin, reviewed the mixed liquor sample and reported a high level of Microthrix Parvicella along with other filaments. He also noted a lack of higher organisms. His independent report is incorporated as Appendix H. As a result of this report, the plant chlorinated the RAS to target the filament population.

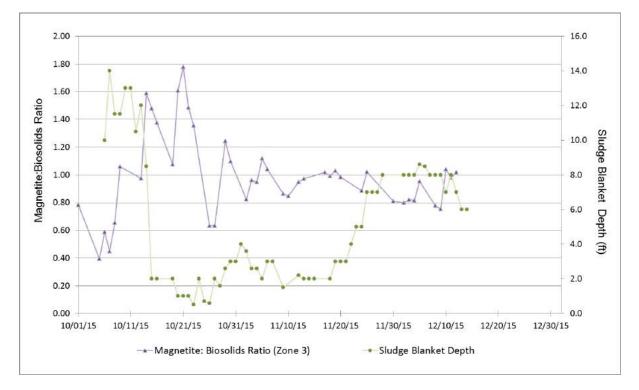


Once the contributory factors were identified and addressed, the system was able to achieve a steady state of performance effectively and consistently, as detailed below. Pilot operations continued through December 16, 2015, and final pilot study samples were obtained on the morning of December 17, 2015. This report presents additional data through December 31, 2015 that reflects some of the study's impacts, as the major changes following December 16 were cessation of supplemental carbon addition, elimination of internal wastewater recirculation and no further magnetite addition to the WAS. Magnetite removal from the WAS did occur through the end of December 2015.

### 3.1 MAGNETITE RATIO

Stantec

When looking at the stability of the BioMag<sup>™</sup> system, the magnetite ratio is a key parameter. Magnetite at a ratio between 1:1 and 1.5:1, meaning 1 gram of magnetite per 1 gram of MLSS or higher, was ideal for the flows and loadings during the Fairhaven pilot. This correlation is seen in Figure 8, which shows the sludge blanket height in the final clarifier compared to the magnetite to biosolids ratio in zone 3 over the course of the trial. At the beginning of the pilot study, with lower ratios (<1:1), the blanket stability struggled, but once "charged" with magnetite in excess of the 1:1 ratio, the blanket was able to consistently maintain a very low level. In the last month of the pilot study, the blanket depth increased several feet when the ratio dropped below 1:1, and then decreased the last week when the 1:1 ratio was again achieved.



### Figure 8 – Magnetite:Biosolids Ratio vs. Sludge Blanket Depth

### 3.2 TSS DATA

Once the target magnetite ratio is achieved, the solids are much heavier and will have increased settling velocities, leading to low TSS in the effluent. The primary effluent and final effluent TSS compared to the daily influent flow for the pilot study are shown in Figure 9. The dashed lines for the TSS data represent the 2-day moving average. The pilot study achieved permit compliance success in this category with an average of 8 mg/L TSS in the final effluent over the duration of the study. The draft NPDES permit has a monthly average limit of 30 mg/L. Figure 9 also indicates that the final effluent TSS remained low even as flows increased in the last week of the pilot study and through the end of December.

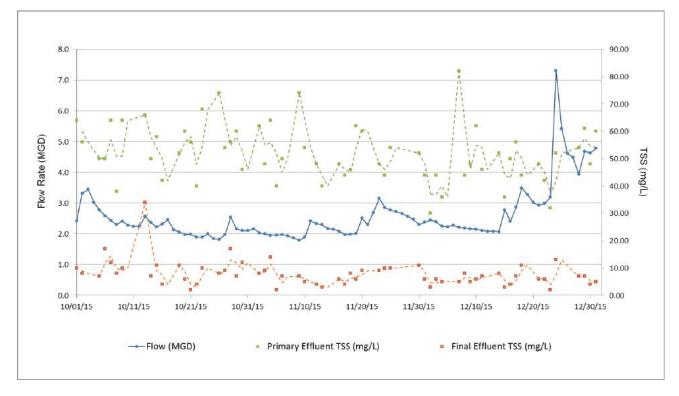


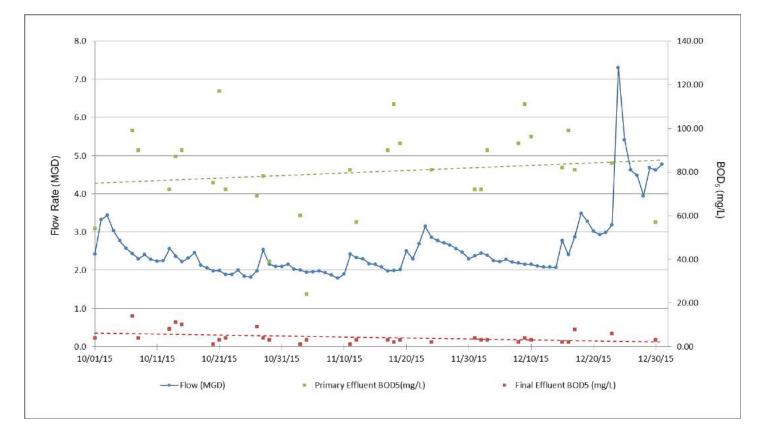
Figure 9 - Flow vs. Primary Effluent and Final Effluent TSS

An unintended consequence of the slightly heavier magnetite sludge, as compared to normal secondary sludge, is that it was likely the cause of damage to one of the 75-foot diameter final clarifier rake arms. The clarifier mechanisms were over 25 years old and in a deteriorated condition. When a portion of the metal rake arm broke several weeks into the pilot study, the final clarifier had to be taken down to repair the rake arm. The flow was diverted to the other 75-foot diameter secondary clarifier during the repair, and then transferred back again. The Town is currently designing replacement of the equipment in all of the WPCF's clarifiers.



### 3.3 BOD DATA

Final effluent BOD was another critical parameter monitored during the pilot study with a monthly average limit of 30 mg/L in the draft permit. The pilot study was able to reach compliance in this category with an average of 4 mg/L over the course of the study. The final effluent BOD decreased during the course of the pilot study despite the growing gap between the linear trend lines shown below in Figure 10, with the primary effluent gaining strength and the final effluent seeing more of a reduction.





### 3.4 NITROGEN DATA

TN removal, the main objective of this pilot study, is more difficult to achieve than the other tested parameters due to its complex nature and ideal removal requirements. The primary effluent at the WPCF has a low carbon-to-nitrogen ratio because much of the BOD is removed in the primary clarifiers (~50% removal during the pilot), while the vast majority of the nitrogen (95%) is retained in the primary effluent, leaving a carbon deficiency for TN removal. Consequently, while the raw influent has a more desirable ratio of 4.5:1 BOD to TN, the secondary treatment



#### OPERATING DATA AND ANALYSIS

system is limited by a poor ratio of 2.7:1, making supplemental carbon addition necessary for efficient TN removal. Recognizing early on that the biological treatment system would be limited by the primary effluent carbon-to-nitrogen ratio, a plan to use MicroC to boost the influent carbon strength was implemented, simulating less BOD removal in the primary clarifiers and a more desirable BOD to TN ratio at the introduction to the aeration tanks.

Prior to implementing MicroC addition, the TN performance was baselined without change to the primary clarifiers or any chemical additions. After this was completed, MicroC addition was started. MicroC was introduced at 35 gpd on November 8, and increased to 70 gpd on November 9, 85 gpd on November 11, and finally 100 gpd on November 12. Figure 11 below shows how the change in MicroC addition affected the final effluent TN levels by providing a better carbon-to-nitrogen ratio and promoting better overall TN removal. After running the MicroC at 100 gpd for a few days, and in an effort to keep pilot costs down (MicroC costs approximately \$6 per gallon), it was agreed by all parties involved in the study to only feed supplemental carbon just prior to and on sampling days. Town staff turned the carbon pump on Sunday morning and left it in operation until the carbon supply ran out, as explained below;

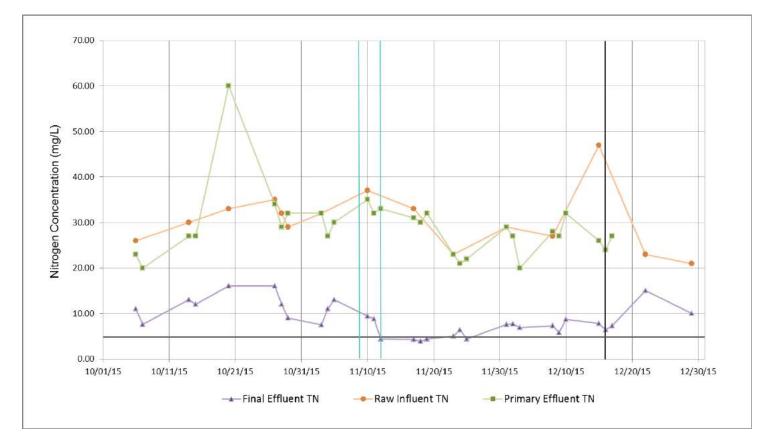


Figure 11 - Raw Influent, Primary Effluent and Final Effluent Total Nitrogen



#### OPERATING DATA AND ANALYSIS

24-hour composite samples were normally collected from Tuesday morning though Thursday morning. However, the Town was also trying to work within the budgetary constraints of using no more than one tote of MicroC a week, which only held 330 gallons. This resulted in less MicroC being applied prior to the last day of sampling (Thursday). The final effluent TN results for the Thursdays with reduced MicroC addition were not noticeably higher than the days with the full 100-gpd application rate, indicating that MicroC was still present in significant quantities in the RAS and internal recycle stream. We also note that during the Thanksgiving holiday week, MicroC was not turned on prior to the samples taken on November 23, 2015. In addition, the Phase 2 WMP recommended 230 gpd of MicroC addition for the 5-MGD design flow, which equates to about 110 gpd of MicroC used for the pilot study may have been on the low side, but was the amount the Town could manage with existing resources.

### 3.4.1 Sampling Results

The nitrogen sampling data through December 10, 2015 included 24-hour composite samples that were analyzed for NH<sub>3</sub>-N and TKN, and grab samples that were analyzed for NO<sub>3</sub>–N and NO<sub>2</sub>-N. In accordance with the QAPP, the testing should have been conducted on composite samples for NO<sub>2</sub>-N and NO<sub>3</sub>-N. The inadvertent sampling error was discovered on December 10, 2015, and all samples taken thereafter for NO<sub>2</sub>-N and NO<sub>3</sub>-N were composites. The certified laboratory conducting the nitrogen analyses, Microbac, was also able to determine the combined NO<sub>3</sub>-N and NO<sub>2</sub>-N (NOX) concentration from remaining composite samples used for testing NH<sub>3</sub>-N and TKN at the laboratory between December 1 and 10, 2015. Composite samples obtained for nitrogen analyses throughout the study were preserved with sulfuric acid, and the certified laboratory explained that it would need a non-preserved sample to analyze for NO<sub>3</sub>–N and NO<sub>2</sub>-N individually, so all NO<sub>3</sub>-N and NO<sub>2</sub>-N anal NO<sub>2</sub>-N analyses in December 2015 were a combination of the two parameters.

Figure 11 on the previous page illustrates the TN concentrations throughout the treatment process, including raw influent, primary effluent and final effluent concentrations. The first blue line represents when MicroC addition to the system was started at 70 gpd (November 9, 2015), and the second blue line represents when MicroC addition was boosted to 100 gpd (November 12, 2015). The black vertical line represents the finish date of the pilot study - December 16, 2015. The horizontal black line represents the pilot study final effluent TN goal of 5 mg/L. As can be seen from the graph, final effluent TN concentrations stabilized after introduction of MicroC at 100 gpd, even getting down to levels below 5 mg/L. The low final effluent TN levels were not maintained throughout the period with 100-gpd MicroC addition, however, averaging 6.3 mg/L from November 15 – December 17, 2015 (The December 17 samples were obtained in the morning, having the benefit of the MicroC addition and the modified 4-stage Bardenpho operation throughout the previous day.). Once the pilot study was completed on December 16, 2015, Figure 11 shows that the final effluent TN levels started to increase again, reaching 15 mg/L and 10 mg/L in the two samples taken December 22 and 29, 2015, respectively.



Figure 12 shows the final effluent concentrations of NO3-N, NO2-N, TKN and TN. The vertical blue and black lines are the same as those in Figure 11. As explained previously, the final effluent TKN and combined NO3-N+NO2-N (NOX) analyses were conducted on composite samples, while the individual final effluent NO2-N and final effluent NO3-N analyses were conducted on grab samples. Of the TN components shown, Figure 11 indicates that the major constituent was NO3-N, and when this parameter was reduced to <4 mg/L in the final effluent, TN stayed at or below 5 mg/L, the target goal for the pilot study. NO2-N levels were largely insignificant, especially following MicroC addition. The latter two statements would bear more weight if the study had included composite samples for these individual parameters, but we believe composite sample analyses would yield the same conclusions. Also, it appears that the composite samples analyzed for NOX starting on December 1, 2015 had higher concentrations through the end of the pilot study than the combination of the results for the grab samples analyzed for NO2-N and NO3-N individually from November 10 – 25, 2015. Again, we put more faith in the composite sample results, but achieving the goal of <5mg/L final effluent TN in mid-to-late November may have resulted in relaxing some of the parameters, such as the magnetite to biosolids ratio, which varied between 0.8 and 1.0 from November 10, 2015 through the end of the study (Figure 8).

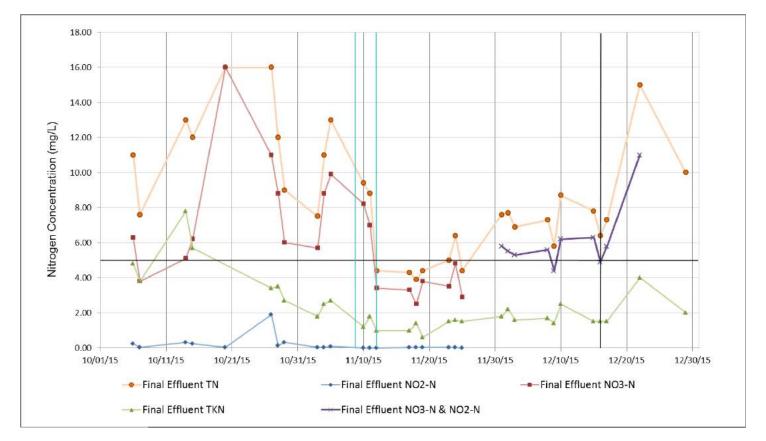


Figure 12 - Final Effluent Nitrogen



#### OPERATING DATA AND ANALYSIS

Keeping the magnetite to biosolids ratio at 1.0, increasing the MicroC addition beyond 100 gpd, and/or altering other factors discussed below, might have boosted the system performance in the direction of the <5 mg/L goal.

A Nitratax probe manufactured by Hach was installed on November 30, 2015 at the tail end of the anoxic cell (zone 1) before discharging into the aerobic zones, to provide real-time NOX levels in the system. The data provided by this probe was helpful in determining a limiting factor in the pilot performance, which was insufficient internal recycle, as discussed in the following section.

### 3.4.2 Internal and RAS Recycle Rates

During the pilot study, it was determined that as the influent flow goes up the internal recycle ratio decreases, and the NOX removal rate decreases because the internal recycle flow is constant and limited to the maximum capacity of the pump. To further explain the recycle rate shortfall, originally the pilot was slated to run side-by-side with one train being BioMag<sup>TM</sup> and the other running as a conventional activated sludge system. This plan was not used, as the flows to the plant were not high enough to split the flow and still demonstrate the pilot study's capabilities. The pump was specified to provide 3,000 gpm, and on-site flow measurement of this pump showed that it was pumping approximately 3,200 gpm of internal recycle, equivalent to twice the incoming average daily flow (2.0Q) during the pilot study (October 1 – December 16, 2015). Using Nitratax probe data, a comparison of real-time NOX levels leaving zone 1 with internal recycle ratios showed that NOX concentrations were on the order of 1 - 3 mg/L with recycle ratios around 2.8 - 3.8Q, but inched back up to 4 - 6 mg/L with recycle ratios of 1.6 - 2Q. This indicates that internal recycle flows on the order of 3 - 4Q would produce lower final effluent TN results.

In addition to the internal recycle, RAS was also pumped from the secondary clarifiers to the first aeration tank. Average RAS flow from October 6 to December 13, 2015 was approximately 1,833 gpm, or 1.15Q for the entire pilot study. The original intent of the pilot study was to pump 2 – 4Q RAS to the first aeration tank, so a higher RAS rate would likely have been more beneficial during the pilot study for achieving nitrogen reduction.

### 3.4.3 Impact of Thickener Filtrate on Influent Nitrogen Loading

Filtrate from the Gravity Belt Thickener (GBT) at the Fairhaven WPCF, which thickens WAS, is sent back to the headworks of the plant, downstream of the location where influent samples are taken. During the pilot study, the filtrate flow was sampled on three dates (a composite sample composed of grab samples taken over the course of the GBT operation on each date), and the additional nitrogen loading to the headworks was calculated based on the results of the sample analysis. As can be seen from Table 4 below, the GBT filtrate TN loading to the plant headworks



#### OPERATING DATA AND ANALYSIS

	12/1/2015	12/8/2015	12/15/2015
Thickener Filtrate Total Flow (gpd)	13,200	15,400	33,200
Thickener Filtrate TN Conc. (mg/L)	530	190	240
Thickener Filtrate TN Loading (lbs.)	58.4	24.4	66.5
Raw Influent Flow Rate (MGD)	2.4	2.2	2.8
Raw Influent TN Conc. (mg/L)	29	27	47
Raw Influent TN Loading (lbs.)	581	496	1098
Ratio of Filtrate TN/(Raw Influent + Filtrate TN)	9.1%	4.7%	5.7%

### Table 4 – Gravity Belt Thickener Filtrate TN Loadings

can be significant, contributing about 5 – 10 percent additional TN loading to the plant headworks.

# 3.5 OPERATING COSTS

Compared to the current operation of the Fairhaven WPCF, the modified 4-stage Bardenpho with BioMag<sup>TM</sup> pilot study required significant additional electrical use to maintain pumping requirements and to operate the various processes associated with magnetite addition and recovery. Looking at the months of pilot study operation in 2015 compared to the same months in 2014, Table 5 below indicates the electricity consumed by the WPCF more than doubled in October, and increased by more than a factor of four in November and December. The December increase in particular is stunning, since the internal recirculation pump was removed December 17, 2015. As a gross approximation of the electrical cost increase associated with full-scale implementation of this study, we could apply the average of the cost difference for October and November in 2014 vs. 2015 ((\$23,166.83 - \$11,716.70 + \$24,131.63 - \$6,398.25)/2 = \$14,591.76) over six months, assuming the new permit would only have a TN limit of 3 mg/L from May – October. The draft permit did not specify a seasonal TN limitation, but this has been the case for other area WPCFs that have received final NPDES permits in the last few years. This cost



#### PILOT PLANT OPEN HOUSE

		2014			2015	
	October	November	December	October	November	December
Usage (KWH)	89,000	44,220	37,640	184,180	195,920	161,760
Cost	\$11,716.70	\$6,398.25	\$5,122.20	\$23,166.83	\$24,131.63	\$20,776.51

### Table 5 - Electrical Consumption Comparison

is  $6 \times 14,591.76 = 87,550$ , and would be even higher with increased internal recycle and/or RAS pumping rates and a complete 4-stage Bardenpho process.

Besides the increased electrical consumption, the addition of MicroC to the BioMag<sup>™</sup> system is another significant O&M cost that would be borne from the operation of the system. During the pilot study, MicroC was added at 100 gpd to achieve the desired effluent TN concentrations. At a cost of approximately \$6 per gallon, the annual cost of MicroC addition, if added every day at 100 gpd for six months, would be about \$109,200. If a higher rate of 110 gpd were needed, as indicated in the Phase 2 WMP, the annual cost would be about \$120,100. To offset this cost, the Town investigated obtaining a waste carbon source from a local winery to use instead of MicroC. This alternative was not pursued for the pilot study, but would be worthwhile to investigate if the 4-stage Bardenpho process, with or without BioMag<sup>™</sup>, is chosen for implementation at the Fairhaven WPCF in the future.

The cost of magnetite is another operational expense to take into account. A rough estimate of this cost for the Fairhaven WPCF for six months is \$10,000, plus freight and trucking. Combining this cost with those for MicroC at 100 gpd and additional electrical requirements yields an additional annual operating cost for the Fairhaven WPCF of about \$207,000 for a six-month operation of a 4-stage Bardenpho with BioMag<sup>TM</sup> system. We caution that this cost is very preliminary, and does not include sufficient electrical backup information, or other costs associated with increasing internal recycle and RAS pumping rates to improve nitrogen removal, additional labor, increased pump maintenance, possible polymer addition, etc.

# 4.0 PILOT PLANT OPEN HOUSE

On December 16, 2015, the final day of pilot plant operation, the Town of Fairhaven held an open house at the Fairhaven WPCF to explain and demonstrate the operation of the pilot plant to town, state and federal officials who were invited to the open house. Several representatives from Evoqua, Stantec and the Fairhaven WPCF were on hand to talk about the various



SUMMARY AND RECOMMENDATIONS

components of the modified 4-stage Bardenpho with BioMag<sup>™</sup> system, and conduct a walkthrough of the pilot trailer and the modified aeration tanks and pumping facilities. Invited attendees included officials from EPA Region 1, MassDEP, and the Town of Fairhaven Executive Secretary.

# 5.0 SUMMARY AND RECOMMENDATIONS

### 5.1 SUMMARY

The pilot study at the Fairhaven WPCF demonstrated that operation of the modified 4-stage Bardenpho with BioMag<sup>TM</sup> system resulted in significantly lower effluent TN concentrations than the WPCF was discharging prior to the study. However, the pilot study did not consistently produce the required effluent TN concentration of 5 mg/L; the average TN concentration in the effluent after MicroC addition at 100 gpd was 6.3 mg/L.

The shortfall in achieving the effluent TN value could be due to several factors, including the internal recycle and RAS pumping rates being lower than desired for optimum TN removal throughout the system. Another factor is that in the beginning of the pilot study the samples for NO<sub>3</sub>-N and NO<sub>2</sub>-N were analyzed using grab samples in lieu of composite samples as originally intended. The results of the grab sample analyses yielded lower concentrations than the composite samples (conducted subsequently), and indicated that the system was operating optimally. If the higher concentrations were originally recorded, operation of the BioMag<sup>TM</sup> system might have been altered further to achieve the lower effluent nitrogen levels required. These alterations might have included maintaining a consistent magnetite to biosolids ratio of 1:1, or increasing the MicroC addition from 100 gpd to 110 gpd, as the latter dose was indicated in the Phase 2 WMP. We believe that adjustment of one or more of these factors would have led to achieving a final effluent TN of 5 mg/L, and with modifications to the existing smaller final clarifier to provide further polishing, a final effluent TN value of 3 mg/l would be attained, satisfying the draft NPDES permit requirement for this parameter. We also believe this treatment technology is an effective means for significantly reducing the amount of nitrogen discharged to the plant's receiving water, the Acushnet River, and could be applied to other area WPCFs, depending on existing tankage, process layout and operation, and effluent TN requirements.

The pilot study easily met the TSS and BOD requirements of the new draft NPDES permit.

Costs and energy use of this system are major issues, however, and should be investigated more thoroughly. In 2014, the Phase 2 WMP estimated that the construction cost for the 4-stage Bardenpho with BioMag<sup>TM</sup> system would be about \$9.8 million. The additional operating costs are very significant as well, roughly estimated from this study to exceed \$200,000/year for a sixmonth operation, and the increased energy requirements would greatly expand the carbon footprint of the Fairhaven WPCF. There may be alternative waste carbon sources to replace



#### FUNDING ACKNOWLEDGEMENT

MicroC, but there is no ready replacement for the internal recycle and significantly higher RAS pumping requirements associated with a 4-stage Bardenpho system.

One of the final clarifier rake arms was also damaged during the pilot study, likely as a result of the magnetite sludge that is effective in settling out solids and associated pollutants, and is slightly heavier than normal secondary sludge. The rake arms were over 25 years old and in a deteriorated condition, making them susceptible to damage from the slightly heavier magnetite sludge.

### 5.2 **RECOMMENDATIONS**

The results of the pilot study, given certain adjustments, showed that the 4-stage Bardenpho with BioMag<sup>TM</sup> process is an effective option for the Town to consider for meeting future NPDES permit limits for TN at the Fairhaven WPCF. However, the cost to build and operate this system is too great for the Town to manage at this time. The Town would like to investigate alternative processes that would be less expensive and energy-intensive, and would produce a lighter sludge with less impact on the WPCF's aging facilities. This investigation should involve the other processes recommended in the Phase 2 WMP – membrane bioreactor and denitrification filter. Both of these systems require working in conjunction with the 4-stage Bardenpho process to achieve sufficient nitrogen removal, and the Phase 2 WMP estimated that the operating costs would be comparable to or greater than the current study's alternative, but the sludge would be lighter. Our recommendation is to first identify where these systems are in place, what the results and associated costs have been, and if there are any concerns. We also recommend looking into other innovative options for nitrogen reduction that may not be fully proven, but have a more sustainable approach. A pilot study may follow the above investigations depending on the applicability for Fairhaven and the need to test the performance with Fairhaven's wastewater.

# 6.0 FUNDING ACKNOWLEDGEMENT

This project has been funded wholly or in part by the United States Environmental Protection Agency under assistance agreement CE-96185701 to the Massachusetts Executive Office of Energy and Environmental Affairs Buzzards Bay National Estuary Program. The contents of this document do not necessarily reflect the views and policies of the Environmental Protection Agency, nor does the EPA endorse trade names or recommend the use of commercial products mentioned in this document.

# 7.0 **REFERENCES**

1. Durson, D., and Jimenez, J. (2014), Getting More Out of Activated Sludge Plants by Using a BioMag Process, Florida Water Resources Journal, 67 (4), 62-66.



# APPENDIX A

# DRAFT NPDES PERMIT

### NPDES Permit No. MA0100765 Page 1 of 13

# AUTHORIZATION TO DISCHARGE UNDER THE NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM

In compliance with the provisions of the Federal Clean Water Act as amended, (33 U.S.C. §§1251 <u>et seq</u>.; the "CWA"), and the Massachusetts Clean Waters Act, as amended, (M.G.L. Chap. 21, §§26-53),

### Town of Fairhaven

is authorized to discharge from the facility located at

### Fairhaven Wastewater Pollution Control Facility Arsene Street Fairhaven, MA 02719

to receiving water named

Acushnet River (New Bedford Inner Harbor; Buzzards Bay Watershed; State Code 95-42)

in accordance with effluent limitations, monitoring requirements and other conditions set forth herein.

This permit shall become effective on (See \*\* below)

This permit and the authorization to discharge expire at midnight, five (5) years from the effective date.

This permit supersedes the permit issued on March 4, 2003.

This permit consists of 13 pages in Part I including effluent limitations and monitoring requirements, Part II including Standard Conditions and Definitions, and Attachments A (Toxicity Protocol) and B (Summary of Report Submittals).

Signed this day of

Director

Office of Ecosystem Protection Environmental Protection Agency Boston, MA Director

Division of Watershed Management Department of Environmental Protection Commonwealth of Massachusetts Boston, MA

\*\* This permit will become effective on the date of signature if no comments are received during public notice. If comments are received during public notice, this permit will become effective no sooner than 30 days after signature.

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PARTI

number 001 to the Acushnet River. Such discharges shall be limited and monitored as specified below.	met River. Such di	scharges shall be	shall be limited and monitored as specified below.	tored as specifie	d below.		
EFFLUENT CHARACTERISTIC			EFFLUENT LIMITS	STIMI		MONITORING REQUIREMENTS <sup>3</sup>	EQUIREMENTS <sup>3</sup>
PARAMETER	AVERAGE	AVERAGE WEEKLY	AVERAGE MONTHLY	AVERAGE WEEKLY	MAXIMUM DAILY	MEASUREMENT FREQUENCY	SAMPLE <sup>3</sup> TYPE
FLOW <sup>2</sup>	****	*****	5.0 MGD	*****	Report MGD	CONTINUOUS	RECORDER
FLOW <sup>2</sup>	*****	*****	Report MGD	*****	******	CONTINUOUS	RECORDER
BOD <sub>5</sub> <sup>4</sup>	1252 lbs/Day 569 kg/Day	1878 lbs/Day 854 kg/Day	30 mg/l	45 mg/l	Report mg/l	3/WEEK	24-HOUR COMPOSITE <sup>5</sup>
TSS <sup>4</sup>	1252 lbs/Day 569 kg/Day	1878 lbs/Day 854 kg/Day	30 mg/l	45 mg/l	Report mg/l	3/WEEK	24-HOUR COMPOSITE <sup>5</sup>
pH RANGE <sup>1</sup>	6.5 - 8.5	SU (SEE PERM	6.5 - 8.5 SU (SEE PERMIT PAGE 5 OF 13, PARAGRAPH I.A.1.b.)	3, PARAGRAPI	HI.A.1.b.)	1/DAY	GRAB
FECAL COLIFORM <sup>1,6</sup>	****	***	88 cfu/100 ml	***	260 cfu/100ml	2/WEEK	GRAB
ENTEROCOCCI 6	****	****	35 cfu/100 ml	****	276 cfu/100ml	2/Week	GRAB
TOTAL NITROGEN ( TKN + NITRATE + NITRITE ) <sup>4</sup>	125 lbs/day 57 kg/day	****	Report mg/l	****	Report mg/l	3/WEEK	24-HOUR COMPOSITE 5
WHOLE EFFLUENT TOXICITY 7, 8, 9, 10	Acute $LC_{50} \ge 100\%$ Chronic C-NOEC $\ge 12.2\%$	so ≥ 100% 3C ≥ 12.2%				2/YEAR	24-HOUR COMPOSITE <sup>5</sup>

Sampling Location: All effluent sampling shall be conducted at the outlet of the ultraviolet disinfection system.

Footnotes:

- 1. Required for State Certification.
- 2. Report annual average, monthly average, and the maximum daily flow. The limit is an annual average, which shall be reported as a rolling average. The value will be calculated as the arithmetic mean of the monthly average flow for the reporting month and the monthly average flows of the previous eleven months.
- 3. All required effluent samples shall be collected at the point specified on page 2. Any change in sampling location must be reviewed and approved in writing by EPA and MassDEP.

A routine sampling program shall be developed in which samples are taken at the same location, same time and same days of the week each month. Occasional deviations from the routine sampling program are allowed, but the reason for the deviation shall be documented in correspondence appended to the applicable discharge monitoring report.

All samples shall be tested using the analytical methods found in 40 CFR §136, or alternative methods approved by EPA in accordance with the procedures in 40 CFR §136.

- 4. Sampling required for influent and effluent.
- 5. 24-hour composite samples will consist of at least twenty four (24) grab samples taken during one consecutive 24 hour period, either collected at equal intervals and combined proportional to flow or continuously collected proportionally to flow.
- 6. The monthly average limits for fecal coliform and enterococci are expressed as a geometric mean.
- 7. The permittee shall conduct chronic (and modified acute) toxicity tests two times per year. The chronic test may be used to calculate the acute LC<sub>50</sub> at the 48 hour exposure interval. The permittee shall test the Inland silverside and Sea urchin. Toxicity test samples shall be collected during months of March and September. The test results shall be submitted by the last day of the month following the completion of the test. The results are due April 30 and October 31 respectively. The tests must be performed in accordance with test procedures and protocols specified in Attachment A of this permit.

NPDES Permit No. MA0100765 Page 4 of 13

Test Dates	Submit Results By:	Test Species	Acute Limit LC <sub>50</sub>	Chronic Limit C-NOEC
March and September	April 30 and October 31	Inland silverside and Sea urchin	≥ 100%	≥ 12.2%

After submitting **two years** and a **minimum** of **four** consecutive sets of WET test results, all of which demonstrate compliance with the WET permit limits, the permittee may request a reduction in the WET testing requirements. The permittee is required to continue testing at the frequency specified in the permit until notice is received by certified mail from the EPA that the WET testing requirement has been changed.

- 8. The LC<sub>50</sub> is the concentration of effluent which causes mortality to 50% of the test organisms. Therefore, a 100% limit means that a sample of 100% effluent (no dilution) shall cause no more than a 50% mortality rate.
- 9. C-NOEC (chronic-no observed effect concentration) is defined as the highest concentration of toxicant or effluent to which organisms are exposed in a life cycle or partial life cycle test which causes no adverse effect on growth, survival, or reproduction at a specific time of observation as determined from hypothesis testing where the test results exhibit a linear dose-response relationship. However, where the test results do not exhibit a linear dose-response relationship, the permittee must report the lowest concentration where there is no observable effect. The "12.2% or greater" limit is defined as a sample which is composed of 12.2% (or greater) effluent, the remainder being dilution water.
- 10. The permittee will submit a map or GIS coordinates of the receiving water sampling point with the first toxicity test under this permit If toxicity test(s) using receiving water as diluent show the receiving water to be toxic or unreliable, the permittee shall either follow procedures outlined in Attachment A (Toxicity Test Procedure and Protocol) Section IV., DILUTION WATER in order to obtain an individual approval for use of an alternate dilution water, or the permittee shall follow the <u>Self-Implementing Alternative Dilution Water Guidance</u> which may be used to obtain automatic approval of an alternate dilution water, including the appropriate species for use with that water. This guidance is found in Attachment G of <u>NPDES Program Instructions for the Discharge Monitoring Report Forms (DMRs)</u> which is sent to all permittees with their annual set of DMRs and

### NPDES Permit No. MA0100765 Page 5 of 13

may also be found on the EPA, Region I web site at

http://www.epa.gov/region01/enforcementandassistance/dmr.html. If this guidance is revoked, the permittee shall revert to obtaining individual approval as outlined in Attachment A. Any modification or revocation to this guidance will be transmitted to the permittees as part of the annual DMR instruction package. However, at any time, the permittee may choose to contact EPA-New England directly using the approach outlined in Attachment A.

Part I.A.1. (Continued)

- a. The discharge shall not cause a violation of the water quality standards of the receiving waters.
- b. The pH of the effluent shall not be less than 6.5 or greater than 8.5 at any time.
- c. The discharge shall not cause objectionable discoloration of the receiving waters.
- d. The effluent shall not contain a visible oil sheen, foam, or floating solids at any time.
- e. The permittee's treatment facility shall maintain a minimum of 85 percent removal of both total suspended solids and biochemical oxygen demand. The percent removal shall be based on monthly average values.
- f. The results of sampling for any parameter done in accordance with EPA approved methods above its required frequency must also be reported.
- g. If a future TMDL for the Acushnet River is completed and approved during the term of the permit, EPA may either modify or reissue the permit as necessary to incorporate any nitrogen limits mandated by the TMDL.
- 2. All POTWs must provide adequate notice to the Director of the following:
  - a. Any new introduction of pollutants into the POTW from an indirect discharger which would be subject to section 301 or 306 of the Clean Water Act if it were directly discharging those pollutants; and
  - b. Any substantial change in the volume or character of pollutants being introduced into that POTW by a source introducing pollutants into the POTW at the time of issuance of the permit.
  - c. For purposes of this paragraph, adequate notice shall include information on:

#### NPDES Permit No. MA0100765 Page 6 of 13

- (1) The quantity and quality of effluent introduced into the POTW; and
- (2) Any anticipated impact of the change on the quantity or quality of effluent to be discharged from the POTW.
- 3. Prohibitions Concerning Interference and Pass Through:
  - a. Pollutants introduced into POTW's by a non-domestic source (user) shall not pass through the POTW or interfere with the operation or performance of the works.

#### 4. Toxics Control

- a. The permittee shall not discharge any pollutant or combination of pollutants in toxic amounts.
- b. Any toxic components of the effluent shall not result in any demonstrable harm to aquatic life or violate any state or federal water quality standard which has been or may be promulgated. Upon promulgation of any such standard, this permit may be revised or amended in accordance with such standards.
- 5. Numerical Effluent Limitations for Toxicants

EPA or MassDEP may use the results of the toxicity tests and chemical analyses conducted pursuant to this permit, as well as national water quality criteria developed pursuant to Section 304(a)(1) of the Clean Water Act (CWA), state water quality criteria, and any other appropriate information or data, to develop numerical effluent limitations for any pollutants, including but not limited to those pollutants listed in Appendix D of 40 CFR Part 122.

#### **B. PRETREATMENT**

Within 120 days of the effective date of the permit, the permittee shall submit the results of an industrial user survey including identification of industrial users and the character and volume of pollutants contributed to the Publicly Owned Treatment Works (POTW) by the industrial users. The industrial user survey shall as a minimum include the following:

(i) Industries discharging wastes which are or may be in the future subject to local limitations or the national prohibited discharge standards found in 40 CFR Part 403.5; and

(ii) Industries discharging wastewater from processes in one or more primary industry categories (See Appendix A to 40 CFR Part 122 or Appendix C of 40 CFR Part 403).

#### C. UNAUTHORIZED DISCHARGES

The permittee is authorized to discharge only in accordance with the terms and conditions of this permit and only from the outfall listed in Part I A.1.of this permit. Discharges of wastewater from any other point sources, including sanitary sewer overflows (SSOs), are not authorized by this permit and shall be reported in accordance with Section D.1.e. (1) of the General Requirements of this permit (Twenty-four hour reporting).

Notification of SSOs to MassDEP shall be made on its SSO Reporting Form (which includes DEP Regional Office telephone numbers). The reporting form and instruction for its completion may be found on-line at <u>http://www.mass.gov/dep/water/approvals/surffms.htm#sso</u>.

Bypasses of treatment units are not authorized. If during peak flow there are emergency bypasses of any treatment unit, the permittee shall take hourly grab samples of the final effluent and test for fecal coliform and enterococci. Each incident shall be documented in a report that includes the monitoring results, and the date, time, duration of bypass and volume by passed. This report shall be attached to the monthly DMR.

#### D. OPERATION AND MAINTENANCE OF THE SEWER SYSTEM

Operation and maintenance of the sewer system shall be in compliance with the General Requirements of Part II and the following terms and conditions:

1. Maintenance Staff

The permittee shall provide an adequate staff to carry out the operation, maintenance, repair, and testing functions required to ensure compliance with the terms and conditions of this permit.

2. Preventative Maintenance Program

The permittee shall maintain an ongoing preventative maintenance program to prevent overflows and bypasses caused by malfunctions or failures of the sewer system infrastructure. The program shall include an inspection program designed to identify all potential and actual unauthorized discharges.

3. Infiltration/Inflow Control Plan:

The permittee shall update its plan to control infiltration and inflow (I/I) to the separate sewer system. The plan shall be submitted to EPA and MassDEP within six months of the effective date of this permit (see page 1 of this permit for the effective date) and shall describe the permittee's program for preventing infiltration/inflow related effluent limit violations, and all unauthorized discharges of wastewater, including overflows and

by-passes due to excessive infiltration/inflow.

The plan shall include:

- An ongoing program to identify and remove sources of infiltration and inflow. The program shall include the necessary funding level and the source(s) of funding.
- An inflow identification and control program that focuses on the disconnection and redirection of illegal sump pumps and roof down spouts. Priority should be given to removal of public and private inflow sources that are upstream from, and potentially contribute to, known areas of sewer system backups and/or overflows.
- Identification and prioritization of areas that will provide increased aquifer recharge as the result of reduction/elimination of infiltration and inflow to the system.
- An educational public outreach program for all aspects of I/I control, particularly private inflow.

Reporting Requirements:

A summary report of all actions taken to minimize I/I during the previous calendar year shall be submitted to EPA and MassDEP annually, by March 31. The summary report shall, at a minimum, include:

- A map and a description of inspection and maintenance activities conducted and corrective actions taken during the previous year.
- Expenditures for any infiltration/inflow related maintenance activities and corrective actions taken during the previous year.
- A map with areas identified for I/I-related investigation/action in the coming year.
- A calculation of the annual average I/I and the maximum month I/I for the reporting year.
- A report of any infiltration/inflow related corrective actions taken as a result of unauthorized discharges reported pursuant to 314 CMR 3.19(20) and reported pursuant to the <u>Unauthorized Discharges</u> section of this permit.

4. Alternate Power Source

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In order to maintain compliance with the terms and conditions of this permit, the permittee shall continue to provide an alternative power source with which to sufficiently operate its treatment works (as defined at 40 CFR §122.2).

#### E. SLUDGE CONDITIONS

- The permittee shall comply with all existing federal and state laws and regulations that apply to sewage sludge use and disposal practices, including EPA regulations promulgated at 40 CFR Part 503, which prescribe "Standards for the Use or Disposal of Sewage Sludge" pursuant to Section 405(d) of the CWA, 33 U.S.C. § 1345(d).
- 2. If both state and federal requirements apply to the permittee's sludge use and/or disposal practices, the permittee shall comply with the more stringent of the applicable requirements.
- The requirements and technical standards of 40 CFR Part 503 apply to the following sludge use or disposal practices.
  - a. Land application the use of sewage sludge to condition or fertilize the soil
  - b. Surface disposal the placement of sewage sludge in a sludge only landfill
  - c. Sewage sludge incineration in a sludge only incinerator
- 4. The requirements of 40 CFR Part 503 do not apply to facilities which dispose of sludge in a municipal solid waste landfill. 40 CFR § 503.4. These requirements also do not apply to facilities which do not use or dispose of sewage sludge during the life of the permit but rather treat the sludge (e.g. lagoons, reed beds), or are otherwise excluded under 40 CFR § 503.6.
- 5. The 40 CFR. Part 503 requirements including the following elements:
  - General requirements
  - Pollutant limitations
  - Operational Standards (pathogen reduction requirements and vector attraction reduction requirements)
  - Management practices
  - Record keeping
  - Monitoring
  - Reporting

Which of the 40 C.F.R. Part 503 requirements apply to the permittee will depend upon the use or disposal practice followed and upon the quality of material produced by a facility. The EPA Region 1 Guidance document, "EPA Region 1 - NPDES Permit Sludge Compliance Guidance" (November 4, 1999), may be used by the permittee to

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assist it in determining the applicable requirements.<sup>1</sup>

6. The sludge shall be monitored for pollutant concentrations (all Part 503 methods) and pathogen vector attraction reduction (land application and surface disposal) at the following frequency. This frequency is based upon the volume of sewage sludge generated at the facility in dry metric tons per year

less than 290	1/ year
290 to less than 1,500	1 /quarter
1,500 to less than 15,000	6 /year
15,000 +	1 /month

Sampling of the sewage sludge shall use the procedures detailed in 40 CFR 503.8.

- 7. Under 40 CFR § 503.9(r), the permittee is a "person who prepares sewage sludge" because it "is ... the person who generates sewage sludge during the treatment of domestic sewage in a treatment works ...." If the permittee contracts with *another* "person who prepares sewage sludge" under 40 CFR § 503.9(r) i.e., with "a person who derives a material from sewage sludge" for use or disposal of the sludge, then compliance with Part 503 requirements is the responsibility of the contractor engaged for that purpose. If the permittee does not engage a "person who prepares sewage sludge," as defined in 40 CFR § 503.9(r), for use or disposal, then the permittee remains responsible to ensure that the applicable requirements in Part 503 are met. 40 CFR §503.7. If the ultimate use or disposal method is land application, the permittee is responsible for providing the person receiving the sludge with notice and necessary information to comply with the requirements of 40 CFR Part 503 Subpart B.
- 8. The permittee shall submit an annual report containing the information specified in the 40 CFR Part 503 requirements (§ 503.18 (land application), § 503.28 (surface disposal), or § 503.48 (incineration)) by **February 19** (see also "EPA Region 1 NPDES Permit Sludge Compliance Guidance"). Reports shall be submitted to the address contained in the reporting section of the permit. If the permittee engages a contractor or contractors for sludge preparation and ultimate use or disposal, the annual report need contain only the following information:
  - Name and address of contractor(s) responsible for sludge preparation, use or disposal
  - Quantity of sludge (in dry metric tons) from the POTW that is transferred to the sludge contractor(s), and the method(s) by which the contractor will prepare and use or dispose of the sewage sludge.

<sup>1</sup> This guidance document is available upon request from EPA Region 1 and may also be found at: http://www.epa.gov/region1/npdes/permits/generic/sludgeguidance.pdf

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#### F. MONITORING AND REPORTING

1. For a period of one year from the effective date of the permit, the permittee may either submit monitoring data and other reports to EPA in hard copy form, or report electronically using NetDMR, a web-based tool that allows permittees to electronically submit discharge monitoring reports (DMRs) and other required reports via a secure internet connection. Beginning no later than one year after the effective date of the permit, the permittee shall begin reporting using NetDMR, unless the facility is able to demonstrate a reasonable basis that precludes the use of NetDMR for submitting all DMRs and reports. Specific requirements regarding submittal of data and reports in hard copy form and for submittal using NetDMR are described below:

#### a. Submittal of Reports Using NetDMR

NetDMR is accessed from: http://www.epa.gov/netdmr. Within one year of the effective date of the Permit, the permittee shall begin submitting DMRs and reports required under this permit electronically to EPA using NetDMR, unless the facility is able to demonstrate a reasonable basis, such as technical or administrative infeasibility, that precludes the use of NetDMR for submitting DMRs and reports ("opt out request").

DMRs shall be submitted electronically to EPA no later than the 15th day of the month following the completed reporting period. All reports required under the permit shall be submitted to EPA, including the MassDEP Monthly Operations and Maintenance Report, as an electronic attachment to the DMR. Once a permittee begins submitting reports using NetDMR, it will no longer be required to submit hard copies of DMRs or other reports to EPA and will no longer be required to submit hard copies of DMRs to MassDEP. However, permittees shall continue to send hard copies of reports other than DMRs (including Monthly Operation and Maintenance Reports) to MassDEP until further notice from MassDEP.

#### b. Submittal of NetDMR Opt Out Requests

Opt out requests must be submitted in writing to EPA for written approval at least sixty (60) days prior to the date a facility would be required under the Permit to begin using NetDMR. This demonstration shall be valid for twelve (12) months from the date of EPA approval and shall thereupon expire. At such time, DMRs and reports shall be submitted electronically to EPA unless the permittee submits a renewed opt out request and such request is approved by EPA. All opt out requests should be sent to the following addresses:

<u>Attn: NetDMR Coordinator</u> U.S. Environmental Protection Agency, Water Technical Unit 5 Post Office Square, Suite 100 (OES04-4) Boston, MA 02109-3912

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#### And

#### Massachusetts Department of Environmental Protection Surface Water Discharge Permit Program 627 Main Street, 2<sup>nd</sup> Floor Worcester, Massachusetts 01608

c. Submittal of Reports in Hard Copy Form

Hard copy DMR submittals shall be completed and postmarked no later than the 15<sup>th</sup> day of the month following the completed reporting period. MassDEP Monthly Operation and Maintenance Reports shall be submitted as an attachment to the DMRs. Signed and dated originals of the DMRs, and all other reports required herein, shall be submitted to the appropriate State addresses and to the EPA address listed below:

#### U.S. Environmental Protection Agency Water Technical Unit 5 Post Office Square, Suite 100 (OES04-4) Boston, MA 02109-3912

The State Agency addresses are:

#### Massachusetts Department of Environmental Protection Southeast Regional Office - Bureau of Resource Protection 20 Riverside Drive Lakeville, MA 02347

And

Massachusetts Department of Environmental Protection Surface Water Discharge Permit Program 627 Main Street, 2<sup>nd</sup> Floor Worcester, Massachusetts 01608

Signed and dated Industrial Pretreatment Program Reports should be sent to:

U.S. Environmental Protection Agency Office of Ecosystem Protection 5 Post Office Square, Suite 100 (OEP06-03) Boston, MA 02109-3912 Attn. Justin Pimpare

And

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#### Massachusetts Department of Environmental Protection Bureau of Waste Prevention Industrial Wastewater Program 1 Winter Street Boston, MA 02108

#### G. STATE PERMIT CONDITIONS

This Discharge Permit is issued jointly by the U. S. Environmental Protection Agency (EPA) and the Massachusetts Department of Environmental Protection (MassDEP) under Federal and State law, respectively. As such, all the terms and conditions of this Permit are hereby incorporated into and constitute a discharge permit issued by the Commissioner of the MassDEP pursuant to M.G.L. Chap.21, §43.

Each Agency shall have the independent right to enforce the terms and conditions of this Permit. Any modification, suspension or revocation of this permit shall be effective only with respect to the Agency taking such action, and shall not affect the validity or status of this Permit as issued by the other Agency, unless and until each Agency has concurred in writing with such modification, suspension or revocation. In the event any portion of this Permit is declared, invalid, illegal or otherwise issued in violation of State law such permit shall remain in full force and effect under Federal law as an NPDES Permit issued by the U.S. Environmental Protection Agency. In the event this Permit is declared invalid, illegal or otherwise issued in violation of Federal law, this Permit shall remain in full force and effect under State law as a Permit issued by the Commonwealth of Massachusetts.

#### Attachment B

#### **Summary of Required Report Submittals\***

Required Report	Date Due	Submitted By:	Submitted To: ** (see bottom of page for key)
Discharge Monitoring Report (DMR)	Monthly, postmarked by the 15 <sup>th</sup> of the month following the monitoring month (e.g. the March DMR is due by April 15 <sup>th</sup> .	Town of Fairhaven	1, 2, 3
Whole Effluent Toxicity (WET)Test Report (Part I.A.1)	April 30 and October 31 of each year	Town of Fairhaven	1, 2, 3
Pretreatment: Industrial User Survey (Part I.B.b.)	Within 120 days of permit effective date	Town of Fairhaven	1, 2, 4
I/I Control Plan (Part I.D.2)	Within 6 months of permit effective date	Town of Fairhaven	1,2
I/I Annual Report (Part I.D.2)	March 31 each year	Town of Fairhaven	1,2
Annual Sludge Report (Part I.E.8.)	February 19 each year	Town of Fairhaven	1,2

\*This Table is a summary of reports required to be submitted under this NPDES permit as an aid to the permittee. If there are any discrepancies between the permit and this summary, the permittee shall follow the permit requirements.

\*\*The addresses are for the submittal of hard copies. When the permittee begins reporting using NetDMR, submittal of hard copies of many of the required reports will not be necessary. See permit conditions for details.

- Environmental Protection Agency Water Technical Unit
   5 Post Office Square, Suite 100 (OES04-4) Boston, Massachusetts 02109-3912
- Massachusetts Department of Environmental Protection Bureau of Resource Protection Southeast Regional Office 20 Riverside Drive Lakeville, MA 02347
- Massachusetts Department of Environmental Protection Division of Watershed Management Surface Water Discharge Permit Program 627 Main Street, 2nd Floor Worcester, Massachusetts 01608
- 4. EPA New England Attn: Justin Pimpare One Congress Street Suite 1100 - CMU Boston, MA 02114

#### UNITED STATES ENVIRONMENTAL PROTECTION AGENCY EPA NEW ENGLAND OFFICE 5 POST OFFICE SQUARE, SUITE 100 BOSTON, MASSACHUSETTS 02109-3912

#### FACT SHEET

#### DRAFT NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM (NPDES) PERMIT TO DISCHARGE TO WATERS OF THE UNITED STATES.

#### NPDES PERMIT NO.: MA0100765

NAME AND ADDRESS OF APPLICANT:

William Fitzgerald, Supervisor Fairhaven Water Pollution Control Facility Arsene Street Fairhaven, MA 02719

#### NAME AND ADDRESS OF FACILITY WHERE DISCHARGE OCCURS:

Fairhaven Water Pollution Control Facility Arsene Street Fairhaven, MA 02719

# RECEIVING WATER: Acushnet River (New Bedford Inner Harbor), Buzzards Bay Watershed (MA 95-42).

CLASSIFICATION: SB

I. Proposed Action, Type of Facility, and Discharge Location.

The above named applicant has requested that the U.S. Environmental Protection Agency (EPA) re-issue its NPDES permit to discharge into the designated receiving water. **Attachment A** shows the locations of the outfall and the wastewater treatment facility. The facility is engaged in collection and treatment of domestic wastewater. The discharge is from a secondary wastewater treatment facility.

The Town of Fairhaven owns and operates a 5 million gallon per day (MGD) activated sludge wastewater treatment facility. Wastewater treatment includes preliminary, primary and secondary processes. Final effluent is disinfected using ultraviolet rays and is discharged to the Acushnet River. Sludge is sent off-site to Woonsocket, RI for incineration.

The segment of the Acushnet River receiving the Fairhaven discharge (New Bedford Inner

Harbor) is classified as SB. The designated uses for SB waters include: habitat for fish, other aquatic life, and wildlife, and for primary and secondary contact recreation, and shall have consistently good aesthetic value. Where designated, SB waters shall be suitable for shellfish harvesting with depuration.

The Massachusetts Year 2008 Integrated List of Waters lists the receiving water (New Bedford Inner Harbor, Coggeshall Street Bridge to hurricane barrier, Fairhaven/New Bedford) as a Category 5 water, not achieving water quality standards and requiring a total maximum daily load (TMDL). The water is listed for priority organics, metals, nutrients, organic enrichment/low DO, pathogens, oil and grease, taste, odor and color, and objectionable deposits.

II. Description of Discharge.

A quantitative description of the discharge in terms of significant effluent parameters, based on Discharge Monitoring Reports (DMRs) from January 2006 to February 2008, is shown on **Attachment B**.

III. Limitations and Conditions.

The effluent limitations and the monitoring requirements may be found in the draft NPDES permit.

IV. Permit Basis and Explanation of Effluent Limitation Derivation

EPA is required to consider technology and water quality requirements when developing permit effluent limits. Technology-based treatment requirements represent the minimum level of control that must be imposed under Section 402 and 301(b) of the Act. Section 301(b)1)(B) requires that Publicly Owned Treatment Works achieve limits based on secondary treatment. Secondary treatment is defined at 40 CFR Section 133.102.

EPA regulations require NPDES permits to contain effluent limits more stringent than technology-based limits where more stringent limits are necessary to maintain or achieve federal or state water quality standards.

Under Section 301(b)(1)(C) of the CWA, discharges are subject to effluent limitations based on water quality standards. The Massachusetts Surface Water Quality Standards include requirements for the regulation and control of toxic constituents and also require that EPA criteria, established pursuant to Section 304(a) of the CWA, shall be used unless site specific criteria is established.

The permit must limit any pollutant or pollutant parameter (conventional, non-conventional, toxic and whole effluent toxicity) that is or may be discharged at a level that caused, has reasonable potential to cause, or contributes to an excursion above any water quality criterion. An excursion occurs if the projected or actual in-stream concentrations exceed the applicable criterion. In determining reasonable potential, EPA considers existing controls on point and

non-point sources of pollution, variability to toxicity and where appropriate, the dilution of the effluent in the receiving water.

A permit may not be renewed, reissued or modified with less stringent limitations or conditions than those contained in the pervious permit unless in compliance with the anti-backsliding requirements of the CWA.

EPA's anti-backsliding provisions are found in Section 402(o) and 303(d)(4) of the CWA, and in 40 CFR 122.44(l), restrict the relaxation of permit limits, standards, and conditions. Anti-backsliding provisions require that limits in the reissued permit must be at least as stringent as those of the previous permit, unless specific conditions are met.

#### A. Conventional Pollutants

Under Section 301(b)(1)(B) of the CWA, POTWs must have achieved effluent limitations based upon secondary treatment by July 1, 1977. The secondary treatment requirements are set forth at 40 CFR Part 133. The regulations describe the secondary treatment requirements for biochemical oxygen demand (BOD), total suspended solids (TSS), and pH. The "Average Monthly" and "Average Weekly" BOD and TSS limitations are based on the requirements of 40 CFR 133.102. Numerical limitations for pH and fecal coliform requirements are based on state certification requirements under Section 401(a)(1) of the CWA, as described in 40 CFR 124.53.

Monitoring frequency for BOD and TSS have been increased from 1/week to 3/week and monitoring frequency for bacteria has been increased from 1/week to 2/week to conform with requirements of similar wastewater treatment facilities.

New monitoring requirements and effluent limitations for enterococci are included in the draft permit based on water quality criteria recently adopted by MassDEP and approved by EPA.

- **B.** Non-Conventional Pollutants
- 1. Toxics

#### a. Whole Effluent Toxicity

EPA's *Technical Support Document for Water Quality-based Toxics Control*, EPA/505/2-90-001, March 1991, recommends using an "integrated strategy" containing both pollutant (chemical) specific approaches and whole effluent (biological) toxicity approaches to control toxic pollutants in effluent discharges entering the nation's waterways. EPA-New England adopted this "integrated strategy" on July 1, 1991, for use in permit development and issuance. These approaches are designed to protect aquatic life and human health. Pollutant-specific approaches such as those in the Gold Book and State regulations address individual chemicals, whereas, the whole effluent toxicity (WET) approach evaluates interactions between pollutants thus rendering an "overall" or "aggregate" toxicity assessment of the effluent. Furthermore, WET measures the "additive" and/or "antagonistic" effects of individual chemical pollutants which pollutant specific approaches do not,

thus the need for both approaches. In addition, the presence of an unknown toxic pollutant can be discovered and addressed through this process.

Under Section 301(b)(1)(C) of the CWA, discharges are subject to effluent limitations based on water quality standards. The Massachusetts Surface Water Quality Standards (314 CMR 4.00), include the narrative statement that "All surface waters shall be free from pollutants in concentrations and combinations that are toxic to humans, aquatic life or wildlife." 314 CMR 4.05(5)(e).

Federal NPDES regulations at 40 CFR §122.44(d)(1)(v) require whole effluent toxicity limits in a permit when a discharge has a "reasonable potential" to cause or contribute to an excursion above the State's narrative criterion for toxicity. WET tests of the Fairhaven WPCF's effluent show consistent compliance with effluent limitations, however the low dilution ratio (1:7.2) calculated for the discharge contributes to a "reasonable potential" that the discharge could cause an excursion of the no toxics provision in the State's regulations. Inclusion of the whole effluent toxicity limit in the Draft Permit will ensure compliance with the State's narrative water quality criterion of "no toxics in toxic amounts".

Moreover, the Massachusetts Department of Environmental Protection's Division of Watershed Management's toxics policy requires whole effluent toxicity testing for all major dischargers such as the Fairhaven POTW (Implementation Policy for the Control of Toxic Pollutants in Surface Waters, MassDEP 1990).

Therefore, based on the potential for toxicity from domestic contributions, the low level of dilution, water quality standards and in accordance with EPA and MassDEP regulation and policy, the draft permit includes acute and chronic effluent toxicity limitation and monitoring requirements. (See, e.g., "Policy for the Development of Water Quality-Based Permit Limitations for Toxic Pollutants: 50 Fed. Reg. 30,784 (July 24, 1985); see also, EPA's <u>Technical Support Document for Water Quality-Based Toxic Control</u>). The principal advantages of biological techniques are: (1) the effects of complex discharges of many known and unknown constituents can be measured only by biological analyses; (2) bioavailability of pollutants after discharge is best measured by toxicity testing; and (3) pollutants for which there are inadequate chemical analytical methods or criteria can be addressed.

The type of test (acute and/or chronic) and the effluent limitations are based on available dilution. The Draft Permit requires the permittee to perform acute toxicity tests twice per year using Inland Silverside and Sea Urchin and contains an LC50 limit of 100% effluent concentration. The LC50 is defined as the concentration of toxicant, or in this draft permit, as the percentage of effluent lethal to 50% of the test organisms during a specific length of time.

The Draft Permit also requires chronic tests twice per year using Inland Silverside and Sea Urchin and contains a Chronic-No Observed Effect Concentration (C-NOEC) limit of 14 percent. C-NOEC is defined as the highest concentration to which test organisms are exposed in a life cycle or partial life cycle test, which causes no adverse effect on growth, survival or reproduction during a specific time of observation. The C-NOEC limit was calculated as follows;

Chronic NOEC Limit Calculation:

$$\frac{1.0*100}{8.2} = 12.2\%$$

As a condition of this permit, the testing requirements may be reduced by a certified letter from the EPA. This permit provision anticipates that the permittee may wish to request a reduction in WET testing. After four consecutive WET tests, demonstrating compliance with the permit limits for whole effluent toxicity, the permittee may submit a written request to the EPA seeking a review of the toxicity test results. The EPA will review the test results and pertinent information to make a determination. The permittee is required to continue testing at the frequency and species specified in the permit until the permit is either formally modified or until the permittee receives a certified letter from the EPA indicating a change in the permit conditions.

#### b. Chlorine

In April 2004, the Town of Fairhaven completed construction of an ultraviolet light (U/V) disinfection system and has ceased using chlorine as a disinfectant. Accordingly, limitations and monitoring requirements for total residual chlorine have been removed from the permit.

#### c. Metals

Certain metals like copper, lead, cadmium and zinc can be toxic to aquatic life. EPA has evaluated (see below) the reasonable potential of toxicity on the concentration of metals in the effluent. Based on this evaluation EPA has determined that there is no reasonable potential for adverse impact on the aquatic life and no need to monitor and limit these metals.

Calculation of reasonable potential for copper, lead, zinc and cadmium:

All effluent metals data are taken from the Toxicity Test Reports from the period March 2004 to March 2008.

Total allowable Receiving Water Concentration, C = Criteria (Tot. Rec.) x Dilution Factor/Conversion Factor

EPA 2002 National Recommended Water Quality Criteria for salt water and the dilution factor of 8.2 [calculated dilution ratio is 7.2:1 based on EPA approved UM Model with a discharge from a single 36 inches diameter port oriented at 90 degrees; dilution factor = (7.2 + 1)/1 = 8.2] are used to calculate effluent limits.

Copper:	Chronic	$C = 3.1 \times 8.2 / 0.83 = 30.6 \text{ ug/l}$ which is greater than the
		monthly average effluent concentration range of 10 - 20
		ug/l. So, reasonable potential does not exist.

	Acute	$C = 4.8 \times 8.2 / 0.83 = 47.4 \text{ ug/l}$ which is greater than the maximum effluent concentration of 20 ug/l. So, reasonable potential does not exist.
Lead:	Chronic	$C = 8.1 \times 8.2 / 0.951 = 69.8 \text{ ug/l}$ which is greater than the monthly average effluent concentration range of 2.7 - 10 ug/l. So, reasonable potential does not exist.
	Acute	$C = 210 \ge 8.2 / 0.951 = 1811 \le 10 \le 10 \le 10 \le 10 \le 10 \le 10 \le 10$
Zinc:	Chronic	C = 81 x8.2 /0.946 = 702 ug/l which is far greater than the monthly average effluent concentration range of 12 - 50 ug/l. So, reasonable potential does not exist.
	Acute	$C = 90 \times 8.2 / 0.946 = 780 \text{ ug/l}$ which is far greater than the maximum effluent concentration of 50 ug/l. So, reasonable potential does not exist.
Cadmium:	Chronic	C = 9.3 x 8.2 /0.994 =76.7 ug/l which is greater than the monthly average effluent concentration of 0.5 -10 ug/l. So, reasonable potential does not exist.
	Acute	$C = 42 \times 8.2 / .994 = 346 \text{ ug/l}$ which is far greater than the maximum effluent concentration of 10 ug/l. So, reasonable potential does not exist.

#### 2. Nutrients

#### a. Nitrogen

As described earlier, the receiving water is listed as impaired due to, among other things, nutrients, organic enrichment/low DO, taste, odor and color, and objectionable deposits. Numerous studies, as summarized below, have identified nitrogen enrichment as causing or contributing to these impairments. Excessive nitrogen causes algae blooms that deplete dissolved oxygen, causes visible color and turbidity, and ultimately decay causing objectionable odors and oxygen demanding sediments.

The current permit required the Town to evaluate and implement optimization of nitrogen removal processes at the WPCF. In November 2004, the Town completed a Draft Nitrogen Removal Optimization Study which evaluated influent nitrogen loadings and control options, and also evaluated the practicable extent to which nitrogen removal at the existing treatment facility could be further optimized. The study found that during the period from July 2000 to July

2004, the total nitrogen (TN) concentration in the treatment plant influent ranged from 11 to 53 mg/l with an average concentration of 29 mg/l. For the same period, TN in the effluent ranged between 5 to 22 mg/l with an average concentration of 13 mg/l. This translates to an average removal efficiency of 55%. The study concluded that with some operational changes, this efficiency could be improved to 70%. At an influent concentration of 29 mg/l and a removal rate of 70 %, the resulting effluent concentration would be about 9 mg/l.

Recent discharge monitoring reports (DMRs) for the months of January 2006 to February 2008 show an average effluent TN concentration of 15.3 mg/l, suggesting that the operational changes were not implemented.

#### Past Studies

The final Buzzards Bay Comprehensive Conservation and Management Plan dated August 1991, identified nitrogen loading as one of the most serious problems threatening many embayments around Buzzards Bay.

In 1994, the Buzzards Bay Project published a draft report titled "A Buzzards Bay Embayment Sub-watershed Evaluation: Establishing Priorities for Nitrogen Management Action". This report highlighted the major sources of nitrogen to New Bedford Inner Harbor and all other Buzzards Bay embayments. The report identified the Fairhaven wastewater treatment plant as the major source of nitrogen to the Inner Harbor.

On March 6, 1998 a refined evaluation of nitrogen loading and water quality of New Bedford Inner Harbor (Acushnet River) as it relates to the Fairhaven wastewater treatment facility was completed by the Buzzards Bay Project. The report concluded that the Fairhaven wastewater plant is the single largest source of nitrogen to the estuary.

On July 28, 2000, another report by the Buzzards Bay Project titled "A Preliminary Evaluation of Nitrogen Loading and Water Quality of New Bedford Inner Harbor (Acushnet River) as it relates to the Fairhaven Wastewater Treatment Facility", further refined the nitrogen loadings and again concluded that the Fairhaven wastewater plant is the single largest source of nitrogen.

MassDEP has completed a report (dated December 2008) entitled "Massachusetts Estuaries Project – Linked Watershed-Embayment Model to Determine Critical Nitrogen Loading Thresholds for the New Bedford Inner Harbor Embayment System, New Bedford, MA." The report documents nitrogen-caused impacts on the Acushnet River - New Bedford Inner Harbor embayment system from its headwaters to the hurricane barrier in New Bedford. The report uses historic sources as well as data collected for the study, quantifies sources of nitrogen to the receiving waters, summarizes hydrodynamic and water quality models developed to analyze the impacts of nitrogen loads, establishes a target nitrogen concentration necessary to achieve water quality standards, and using the water quality model evaluates scenarios for achieving the nitrogen target. In determining the nitrogen threshold for the embayment, the study focused on habitat parameters (particularly infauna<sup>1</sup> since eelgrass has not grown in the receiving waters for at least 50 years), sediment characteristics, and nutrient-related water quality information (particularly dissolved oxygen, chlorophyll  $a^2$  and macroalgae).

Benthic animal populations are influenced by dissolved oxygen and sediment quality. Low organic matter loading and high dissolved oxygen (DO) concentrations generally support healthy habitat and high organic matter loading and low DO do not support healthy habitat. Depletion of oxygen may occur only infrequently yet may have severe effect on system health. High chlorophyll *a* indicates large amounts of algae in the receiving water, which can cause large diurnal swings in dissolved oxygen as the algae produce oxygen during daylight hours and consume it during hours of darkness. Algae blooms also reduce sunlight penetration into the water column, generate high sediment oxygen demands as it dies and decays, and cause odors and visual impairments.

The study found impairment of infaunal <u>habitat</u> quality due to oxygen depletion, the magnitude of daily oxygen excursions, and organic matter enrichment from phytoplankton production (chlorophyll *a* level) at all monitoring locations. These impacts are indicative of nutrient enriched waters, specifically moderate to high nitrogen loading rates.. The study concluded that nitrogen enrichment is related to the dissolved oxygen depletion. Additionally, due to the increased phytoplankton production, the dissolved oxygen levels can rise significantly during daylight hours, due to photosynthesis, to concentrations above atmospheric equilibration. Oxygen levels above atmospheric equilibration is indicative of enriched nitrogen and associated organic matter. All monitoring locations showed periodic oxygen depletions below 5 mg/l and generally less than 4 mg/l.

The upper basin has a moderately impaired benthic habitat due to macroalgal accumulation, high chlorophyll <u>a</u> levels, frequent depletions of DO, and a preponderance of stress tolerant species.

The middle basin is a depositional area with sediments consisting of organic rich mud. The middle basin has moderate to high chlorophyll levels, frequent DO depletions and a moderately impaired infaunal community.

The lower basin is slightly to moderately impaired by nitrogen enrichment with significant impairment in localized areas of physical disturbance or altered flushing. The lower basin experiences moderate oxygen depletions and elevated chlorophyll  $\underline{a}$  levels.

<sup>1</sup> Infauna are benthic animals that live in the substrate of a body of water, especially in a soft sea bottom. Infauna usually construct tubes or burrows and are commonly found in deeper and subtidal waters. Clams, tubeworms, and burrowing crabs are infaunal animals.

<sup>2</sup> Chlorophyll is the green pigment found in all plants. Chlorophyll *a* is measured to estimate the abundance of phytoplankton in the water. More chlorophyll a indicates that there are more phytoplankton present. Most chlorophyll a is found near the surface of the water because there is less light at depth. Chlorophyll a concentrations are often highest just below the surface, not at the surface of the water.

In general, the data indicate a gradient in oxygen depletion and chlorophyll a levels from the upper to the lower basins. Consistent with the estuarine response to over-enrichment from nitrogen, the extent of bottom water oxygen depletion parallels the levels of phytoplankton biomass.

Limit Derivation:

The "Massachusetts Estuaries Project – Linked Watershed-Embayment Model to Determine Critical Nitrogen Loading Thresholds for the New Bedford Inner Harbor Embayment System, New Bedford, MA" report developed a loading scenario which would achieve the target total nitrogen concentration of 0.5 mg/l at the most highly impacted "sentinel" location at the head of the middle basin of the Acushnet River (see figure VIII-I) of the report.

The water quality model was first run assuming the elimination of loads from CSOs and the elimination of the Fairhaven WPCF discharge. Under this scenario, the desired nitrogen target of 0.5 mg/l was not achieved. A 13 percent reduction of loads from septic tank discharges was then added, resulting in attainment of the desired target. The estimated loads under this scenario were:

Current total nitrogen load = 310 kg/day (sum of loads from Fairhaven WPCF, New Bedford CSOs, septic, runoff, and fertilizer)

- CSO load eliminated = 25.7 kg/day reduction

- Fairhaven TN load is eliminated = 39236 kg/year = 107.5 kg/day reduction

- 13 percent of septic load eliminated = 11.4 kg/day reduction

Load meeting target TN concentration = 310 kg/day - 107.5 kg/day - 25.7 kg/day - 11.4 kg/day = 165.4 kg/day

The analysis shows that a TN load of about 165 kg/day is necessary to achieve the target concentration at the sentinel location. The Fairhaven treatment plant currently discharges about 256 lbs/day (116 kg/day) of TN (calculated 2006-2007 average load based on a flow of 1.99 MGD and 15.43 mg/l, which is somewhat greater than the 107.5 kg/day used for the study estimate). The treatment plant discharge of TN therefore has the reasonable potential to cause or contribute to the exceedance of the target concentration given that the current discharge represents about 37 percent of the current loading and 70 percent of the loading that will achieve the target concentration.

Regulations at 40 CFR Part 122.44(d)(1) require that effluent limitations must be included for any pollutant discharge at a level that has the reasonable potential to cause, or contribute to an excursion above any State water quality standard.

Additional scenarios evaluated in the Massachusetts Estuaries Project (MEP) report included the

Fairhaven treatment plant discharging at 3.0 mg/l total nitrogen and various levels of CSO remediation and septic system elimination (see page 173-176). These scenarios provide the necessary detail to determine the extent of CSO remediation and septic system elimination that will need to be accomplished in addition to reducing the Fairhaven treatment plant loading to the limit of technology (3.0 mg/l total nitrogen). Given the magnitude of the overall load reduction necessary to achieve the target load (about 165 kg/day) a high level of removal at Fairhaven, as well as high levels of removal from CSO and septic tank sources are necessary.

A TMDL has not been completed for this receiving water, but the information discussed above shows the reasonable potential for nitrogen discharges from the Fairhaven WPCF to cause or contribute to exceedances of water quality standards and shows that a total nitrogen effluent limit of 3 mg/l at the facility design flow of 5 MGD (coupled with significant reductions in other sources of nitrogen) is necessary to attain water quality standards. Accordingly, EPA and MassDEP have included a monthly average limitation of 57 kg/day (125 lbs/day), which corresponds to treatment plant flow of 5.0 MGD and an effluent concentration of 3 mg/l TN.

The draft permit requires total nitrogen monitoring three times per week. Following completion of the TMDL, EPA will either modify or reissue the permit as necessary to incorporate the nitrogen limits mandated by the TMDL.

C. Other Monitoring Requirements

The effluent monitoring requirements have been specified in accordance with 40 CFR 122.41(j), 122.44(i) and 122.48 to yield data representative of the discharge.

#### D. Pretreatment Program

Pollutants introduced into POTW's by a nondomestic source (user) shall not pass through the POTW or interfere with the operation or performance of the works.

The permittee will perform an Industrial User Survey as stated in the draft permit.

#### E. Sludge

In February 1993, the Environmental Protection Agency (EPA) promulgated standards for the use and disposal of sewage sludge. The regulations were promulgated under the authority of section 405(d) of the Clean Water Act (CWA). Section 405(d) of the CWA requires that sludge conditions be included in all municipal permits. The sludge conditions in the draft permit satisfy this requirement.

F. Essential Fish Habitat Determination (EFH)

Under the 1996 Amendments (PL 104-267) to the Magnuson-Stevens Fishery Conservation and Management Act (16 U.S.C.§1801 <u>et seq</u>.(1998)), EPA is required to consult with NMFS if EPA's action or proposed actions that it funds, permits, or undertakes, may adversely impact any

essential fish habitat.16 U.S.C.§1855(b). The Amendments broadly define essential fish habitat as: waters and substrate necessary to fish for spawning, breeding, feeding, or growth to maturity. 16 U.S.C.§1802(10). Adversely impact means any impact which reduces the quality and/or quantity of EFH. 50C.F.R.§600.910(a). Adverse effects may include direct (e.g., contamination or physical disruption), indirect (e.g., loss of prey, reduction in species' fecundity), site-specific or habitat-wide impacts, including individual, cumulative, or synergistic consequences of actions.

Essential fish habitat is only designated for fish species for which federal Fisheries Management Plans exist. 16 U.S.C§1855(b)(1)(A). EFH designations for New England were approved by the U.S. Department of Commerce on March 3, 1999.

Attachment C is the list of 16 managed species that are believed to be present during one or more life-stage within EFH Area, which encompasses the existing discharge site. No "habitat areas of particular concern", as defined under §600.815(a)(9) of the Magnuson-Stevens Act, have been designated for this site. Although EFH has been designated for this general location, EPA has concluded that this activity is not likely to adversely affect EFH or its associated species for the following reasons:

- This is a re-issuance of an existing permit;
- The quantity of discharge from the WWTF is 5.0 mgd monthly average; Effluent receives as a minimum secondary treatment using activated sludge processes;
- Effluent is discharged into the Acushnet River (New Bedford Inner Harbor) with an estimated dilution ratio of 7.2:1;
- Use of chlorine has been discontinued due to installation of a new Ultra Violet (U/V) ray system to disinfect fecal coliform;
- A new monthly average total nitrogen limit of 125 lbs/day is established in the draft permit;
- Acute and chronic toxicity tests will be conducted on Inland Silverside and Sea urchin two times per year;
- The permit will prohibit any violation of state water quality standards.

Accordingly, EPA has determined that a formal EFH consultation with NMFS is not required. If adverse impacts to EFH are detected as a result of this permit action, NMFS will be notified and an EFH consultation will be promptly initiated.

#### G. Endangered Species

Section 7(a) of the Endangered Species Act of 1973, as amended (ESA) grants authority to and imposes requirements upon Federal agencies regarding endangered or threatened species of fish, wildlife, or plants ("listed species") and habitat of such species that has been designated as critical (a "critical habitat"). The ESA requires every Federal agency, in consultation with and with the assistance of the Secretary of Interior, to insure that any action it authorizes, funds, or carries out, in the United States or upon the high seas, is not likely to jeopardize the continued existence of any listed species or result in the destruction or adverse modification of critical

habitat. The United States Fish and Wildlife Service (USFWS) typically administers Section 7 consultations for bird, terrestrial, and freshwater aquatic species. The National Marine Fisheries Service (NMFS) typically administers Section 7 consultations for marine species and anadromous fish.

EPA has reviewed the federal endangered or threatened species of fish and wildlife to see if any listed species might potentially be impacted by the re-issuance of this NPDES permit. The review has focused primarily on Bristol County since the discharge is into the Buzzards Bay. Sea Turtles (Green, Kemp's Ridley Leatherback) are listed as endangered species and Sea Turtles (Green and Loggerhead) are listed as threatened species. Based on the conditions in the permit, which are as, or more stringent than in the present permit, EPA has determined that there will be no adverse effects on these species (see section F, EFH for a discussion of the pertinent permit conditions).

EPA is coordinating a review of this finding with NMFS and/or USFWS through the Draft Permit and Fact Sheet and consultation under Section 7 of the ESA with NMFS and/or USFWS is not required. If adverse impacts are detected as a result of this permit action, NMFS and/or USFWS will be notified and a consultation will be promptly initiated.

#### H. Anti-degradation

This draft permit is being reissued with an allowable wasteload identical to the current permit with the same parameter coverage and no change in outfall location. The State of Massachusetts has indicated that there will be no lowering of water quality and no loss of existing water uses and that no additional anti-degradation review is warranted.

#### V. State Certification Requirements.

The staff of the Massachusetts Department of Environmental Protection has reviewed the draft permit. EPA has requested permit certification by the State pursuant to 40 CFR 124.53 and expects that the draft permit will be certified.

#### VI. Public Comment Period, and Procedures for Final Decision

All persons, including applicants, who believe any condition of the draft permit is inappropriate must raise all issues and submit all available arguments and all supporting material for the arguments in full by the close of the public comment period, to the U.S. EPA, MA NPDES Municipal Permit Branch 5, Post Office Square , Suite 100 (OEP 6-4), Boston, Massachusetts 02109-3912. Any person, prior to such date, may submit a request in writing for a public hearing to consider the draft permit to EPA and the State Agency. Such requests shall state the nature of the issues proposed to be raised in the hearing. A public hearing may be held after at least thirty days public notice whenever the Regional Administrator finds that response to this notice indicates significant public interest. In reaching a final decision on the draft permit the Regional Administrator will respond to all significant comments and make these responses available to the public at EPA's Boston office.

Following the close of the comment period, and after a public hearing, if such hearing is held, the Regional Administrator will issue a final permit decision and forward a copy of the final decision to the applicant and each person who has submitted written comments or requested notice.

#### VII. Monitoring and Reporting

The effluent monitoring requirements have been established to yield data representative of the discharge under authority of Section 308 (a) of the CWA in accordance with 40 CFR §§122.41 (j), 122.44 (l), and 122.48.

The Draft Permit includes new provisions related to Discharge Monitoring Report (DMR) submittals to EPA and the State. The Draft Permit requires that, no later than one year after the effective date of the permit, the permittee submit all monitoring data and other reports required by the permit to EPA using NetDMR, unless the permittee is able to demonstrate a reasonable basis, such as technical or administrative infeasibility, that precludes the use of NetDMR for submitting DMRs and reports ("opt out request").

In the interim (until one year from the effective date of the permit), the permittee may either submit monitoring data and other reports to EPA in hard copy form, or report electronically using NetDMR.

NetDMR is a national web-based tool for regulated Clean Water Act permittees to submit discharge monitoring reports (DMRs) electronically via a secure Internet application to U.S. EPA through the Environmental Information Exchange Network. NetDMR allows participants to discontinue mailing in hard copy forms under 40 CFR 122.41 and 403.12. NetDMR is accessed from the following url: <u>http://www.epa.gov/netdmr</u> Further information about NetDMR, including contacts for EPA Region 1, is provided on this website.

The Draft Permit requires the permittee to report monitoring results obtained during each calendar month using NetDMR no later than the 15th day of the month following the completed reporting period. All reports required under the permit shall be submitted to EPA as an electronic attachment to the DMR. Once a permittee begins submitting reports using NetDMR, it will no longer be required to submit hard copies of DMRs or other reports to EPA and will no longer be required to submit hard copies of DMRs to MassDEP. However, permittees must continue to send hard copies of reports other than DMRs to MassDEP until further notice from MassDEP.

The Draft Permit also includes an "opt out" requests process. Permittees who believe they can not use NetDMR due to technical or administrative infeasibilities, or other logical reasons, must demonstrate the reasonable basis that precludes the use of NetDMR. These permittees must submit the justification, in writing, to EPA at least sixty (60) days prior to the date the facility would otherwise be required to begin using NetDMR. Opt outs become effective upon the date of written approval by EPA and are valid for twelve (12) months from the date of EPA approval. The opt outs

expire at the end of this twelve (12) month period. Upon expiration, the permittee must submit DMRs and reports to EPA using NetDMR, unless the permittee submits a renewed opt out request 60 days prior to expiration of its opt out, and such a request is approved by EPA.

Until electronic reporting using NetDMR begins, or for those permittees that receive written approval from EPA to continue to submit hard copies of DMRs, the Draft Permit requires that submittal of DMRs and other reports required by the permit continue in hard copy format.

VIII. EPA Contact

Additional information concerning the draft permit may be obtained between the hours of 9:00 a.m. and 5:00 p.m., Monday through Friday, excluding holidays from:

Suprokash Sarker, P.E. Municipal Permits Branch Environmental Protection Agency 5 Post Office Square, Suite 100 (OEP 6-4) Boston, MA 02109-3912 Telephone: (617) 918-1693 E-Mail: sarker.soupy@epa.gov

Date

Stephen Perkins, Director Office of Ecosystem Protection U.S. Environmental Protection Agency

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY OFFICE OF ECOSYSTEM PROTECTION REGION I BOSTON, MASSACHUSETTS 02203

JOINT PUBLIC NOTICE OF A DRAFT NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM (NPDES) PERMIT TO DISCHARGE INTO THE WATERS OF THE UNITED STATES UNDER SECTION 301 AND 402 OF THE CLEAN WATER ACT (THE "ACT"), AS AMENDED, AND REQUEST FOR STATE CERTIFICATION UNDER SECTION 401 OF THE ACT.

DATE OF NOTICE: July 8, 2010

PERMIT NUMBER: MA0100765

PUBLIC NOTICE NUMBER: MA-020-10

NAME AND MAILING ADDRESS OF APPLICANT:

Fairhaven Water Pollution Control Facility Arsene Street Fairhaven, Massachusetts 02719

NAME AND ADDRESS OF THE FACILITY WHERE DISCHARGE OCCURS:

Fairhaven Water Pollution Control Facility Arsene Street Fairhaven, Massachusetts 02719

RECEIVING WATER: Acushnet River (New Bedford Inner Harbor)

RECEIVING WATER CLASSIFICATION: Class SB

PREPARATION OF THE DRAFT PERMIT:

The U.S. Environmental Protection Agency, (EPA) and the Massachusetts Department of Environmental Protection (MassDEP) have cooperated in the development of a permit for the above identified facility. The effluent limits and permit conditions imposed have been drafted to assure that State Water Quality Standards and provisions of the Clean Water Act will be met. EPA has formally requested that the State certify this draft permit pursuant to Section 401 of the Clean Water Act and expects that the draft permit will be certified.

#### INFORMATION ABOUT THE DRAFT PERMIT:

A fact sheet or a statement of basis (describing the type of facility; type and quantity of wastes; a brief summary of the basis for the draft permit conditions; and significant factual, legal and policy questions considered in preparing the draft permit) may be obtained at no cost at

http://www.epa.gov/region1/npdes/draft\_permits\_listing\_ma.html or by writing or calling EPA's contact person named below:

Suprokash Sarker US EPA 5 Post Office Square Suite 100 Mail Code – OEP06-1 Boston, MA 02109-3912 Telephone: (617) 918-1693

The administrative record containing all documents relating to this draft permit is on file and may be inspected at the EPA Boston office mentioned above between 9:00 a.m. and 5:00 p.m., Monday through Friday, except holidays.

#### PUBLIC COMMENT AND REQUEST FOR PUBLIC HEARING:

All persons, including applicants, who believe any condition of this draft permit is inappropriate, must raise all issues and submit all available arguments and all supporting material for their arguments in full by **August 6, 2010**, to the U.S. EPA, 5 Post Office Square, Suite 100, (OEP 06-1) Boston, Massachusetts 02109-3912. Any person, prior to such date, may submit a request in writing to EPA and the State Agency for a public hearing to consider this draft permit. Such requests shall state the nature of the issues proposed to be raised in the hearing. A public hearing may be held after at least thirty days public notice whenever the Regional Administrator finds that response to this notice indicates significant public interest. In reaching a final decision on this draft permit the Regional Administrator will respond to all significant comments and make the responses available to the public at EPA's Boston office.

#### FINAL PERMIT DECISION:

Following the close of the comment period, and after a public hearing, if such hearing is held, the Regional Administrator will issue a final permit decision and forward a copy of the final decision to the applicant and each person who has submitted written comments or requested notice.

Glenn Haas, Director DIVISION OF WATERSHED MANAGEMENT MASSACHUSETTS DEPARTMENT OF ENVIRONMENTAL PROTECTION Stephen Perkins, Director OFFICE OF ECOSYSTEM PROTECTION ENVIRONMENTAL PROTECTION AGENCY

## APPENDIX B

## TRAINING SHEETS

### Nitrogen Reduction Pilot Study at the Fairhaven, MA WPCF

**Evoqua Training Record** 

#### Training Date and Time

September 28th & 29th, 10 am - 2 pm

#### **Training Location**

Fairhaven, MA WPCF, BioMag Trailer (on-site)

#### Trainer Name, Title, Signature

Matthew Vareika, Pr	rocess Engineer, BioMag & CoMag Processes Motther Vareile
Personnel Trained - Rene Robillard	Name, Title, Signature Assistant Superintendent Blue Voullas
Linda Schick	Superintendent Nanda & Sanck
Kyle Winderlick	Maintenance Craftsman White Mindulick
Raymond Paczosa	Electrician
Joseph Bonneau	Maintenance Craftsman Joe Bonneau
Joseph Frates	Mechanic Joep Frates
Victor Oliveira	Maintenance Craftsman
Matt Manzone	Maintenance Craftsman Muthur Manag
Doug Pinard	Operator Dan MM
Robert Gomes	Operator Roberto Blomme
Dana Hathaway	Maintenance Craftsman Jona Howing used
	· ( )

#### **Topics Covered**

BioMag basics of operation, ballasted treatment process, process flows, sampling locations/ procedures/methods, trailer operations and alarming, troubleshooting alarms, targets for the project and system adjustments to achieve them.

## Nitrogen Reduction Pilot Study at the Fairhaven, MA WPCF

## Evoqua Training Record

Training Date and Time Sc.pt 29, 2015 1-2:30 PM	
Training Location	
Fairbauch, MA WHITE	
Trainer Name, Title, Signature Matthew Vareika , Process (	Engineer Actul Aland
Personnel Trained - Name, Title, Signature Jake Spinetto intern	le pà
opics Covered Wastewater treatment proces Rilot plant components Environmental health & safety to Emergency awareness Sludge blanket level measurement	raining
D.O., pH; temperatures ORP mete	r measurement & recording
aining Record Location airhaven, MA WPCF	

## APPENDIX C

PILOT STUDY MASTER DATA SHEET

## Questionable Data

					Ra	w In	fluer	nt								Ρ	rimar	y Eff	lue	nt									Fir	nal E	Efflu	ent					
Date	Day		рН	BOD <sub>5</sub>	Alkalinity	NO3-N	NO2 - N	NO3 & NO2 - N	NH3-N	TKN	ΤN	рН	Temp	BOD <sub>5</sub>	TSS	VSS	Alkalinity	NH3-N	TKN	NO3 & NO2 - N	NO3-N	NO2 - N	TN	рН	UV	UV Trans	BOD <sub>5</sub>	TSS	% TSS Reduction	VSS	NH3-N	TKN	NO3 & NO2 - N		NO2 - N	TN	Alkalinity
		MGD	SU	mg/L	mg/L as CaCO₃	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	°C	mg/L	mg/L	mg/L	mg/L as CaCO3	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	MW/c m²	%	mg/L	mg/L	%	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L as CaCO3
10/01/15	1	2.4	7.1	99								6.9	20.4	54	64	64								6.7	16.2	70	4	10	84	10						· · · · ·	
10/02/15	2	3.3	7.1									6.5	20.6		56	56								6.7	9.1	72		8	86	7							
10/03/15	3	3.4																						6.7	18.5	74											
10/04/15	4	3.0																						6.6	19.3	75											
10/05/15	5	2.8	7.1									6.8	19.7		50	50								6.6	18.5	74		7	86	5							
10/06/15	6	2.6	7.1			0.24	0.23		18	25	26	6.9	19.8		50	42		17	23		<0.050	0.03	23	6.7	19.8	76		17	66	12	2.4	4.8		6.3	0.24	11	
10/07/15	7	2.4	7.1	126								6.8	19.5	99	64	64		16	20		0.053	0.042	20	6.8	119.8	76	14	12	81	12	2.1	3.8		3.8	0.033	7.6	113
10/08/15	8	2.3	7.1	186								6.7	19.5	90	38	38								6.7	19.2	75	4	8	79	8							70
10/09/15	9	2.4	7.1									7	19.5		64	64								6.7	18.5	74		10	84	10							
10/10/15	10	2.3																						6.8	13.9	67											
10/11/15	11	2.2																						6.8	16.7	71											
10/12/15	12	2.3																						6.8	27.8	84											
10/13/15	13	2.6	7.1	192								7	19.2	72	66	33								6.8	14.7	67	8	34	48	28							140
10/14/15	14	2.4	7	204		<0.050	0.19		18	30	30	6.9	19.1	87	50	46		20	27		<0.050	0.078	27	6.7	7.3	69	11	7	86	7	6.1	7.8		5.1	0.31	13	80
10/15/15	15	2.2	7.1	204								6.9	18.9	90	58	58		20	27		<0.050	0.041	27	6.6	6.6	70	10	11	81	11	4.0	5.7		6.2	0.24	12	
10/16/15	16	2.3	7.2									7	19.2		42	42								6.6	7.6	74		4	90	4							
10/17/15	17	2.5																						6.6	7.6	74											
10/18/15	18	2.1																						6.7	7.6	74											
10/19/15	19	2.1	7.2									7	18.6		52	42								6.7	7.1	72		11	79	7							63
10/20/15	20	2.0	7.2	129		<0.050	0.043		25	33	33	6.8	18.4	75	60	56		24	60		<0.050	0.051	60	6.6	7.6	74	1	6	90	6	0.32	<2.0		16	0.035	16	
10/21/15	21	2.0	7	132								6.9	18.9	117	56	56								6.6	7.1	72	3	2	96	2							62
10/22/15	22	1.9	7.2	126								6.8	18.4	72	40	40								6.7	15.7	69	4	4	90	4						· · · ·	
10/23/15	23	1.9	7.3									6.9	18.4		68	68								6.6	6.6	70		10	85	10							
10/24/15	24	2.0																						6.7	6.6	70											
10/25/15	25	1.8																						6.8	16.6	70											
10/26/15	26	1.8	7.1									7	18.3		74	62								6.8	16.2	70		8	89	8							
10/27/15	27	2.0	7.2	84		< 0.050	0.066		28	35	35	7	18.1	69	54	52		28	33		0.59	0.38	34	6.7	13.4	64	9	9	83	9	2.1	3.4		11	1.9	16	61
10/28/15	28	2.5	7.2	120	180	< 0.050	0.024		26	32	32	7.1	18	78	56	56	160	25	29		<0.050	0.024	29	6.7	6.4	69	4	17	70	14	0.49	3.5		8.8	0.13	12	71
10/29/15	29	2.2	7.1	72	110	< 0.050	0.043		20	29	29	7	17.9	39	60	56	120	25	32		<0.050	0.049	32	6.6	8.1	65	3	7	88	7	0.33	2.7		6.0	0.31	9.0	56
10/30/15	30	2.1	7.1									6.9	17.8		46	46								6.7	15.7	69		12	74	12							
10/31/15	31	2.1																						6.7	17.9	73											

				Z	one #1						Z	one #2								Zon	e #3					
Date	Day	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	Magnetite:Bi	5 Min Settle	30 Min Settle	SVI
		mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	osolids Ratio	mL/L	mL/L	mL/g
10/01/15	1	2820	1320	1280	1540	6.6	0.6		2180	1280	1050	1130	6.4	2.0		2460	1400	1080	1380		3.4		0.78	800	300	214
10/02/15	2	7700	4180	3700	4000	6.5	1.4		1740	900	750	990				1560		700	860				0.81			
10/03/15	3																									
10/04/15	4																									
10/05/15	5	8280	4020	2500	5780	6.6	1.4		2600	1460	720	1880	6.7	2.6		2620	1520	740	1880		4.6		0.39	900	520	342
10/06/15	6	3720	1920	1400	2320	6.8	0.7		3140	1640	1100	2040	6.6	1.7		3080	1620	1140	1940	6.6	3.5		0.59	900	550	340
10/07/15	7	4720	2700	1830	2890	6.9	0.5	-144.0	3680	2100	1310	2370	6.7	0.4	-127.9	4620	2580	1430	3190	6.6	4.3	-130.2	0.45	910	690	267
10/08/15	8	5360	2720	2300	3060	6.9	0.2	-147.2	4300	2220	1870	2430	6.8	0.7	-145.5	4300	2220	1860	2440	6.7	4.0	-132.5	0.76	960	700	315
10/09/15	9	4100	2040	1960	2140	6.9	0.5	-176.1	3600	1820	1730	1870	6.8	0.3	-154.0	3520	1800	1810	1710	6.7	0.3	-173.2	1.06	940	670	372
10/10/15	10					6.9	0.3	388.9					6.8	0.3	421.6					6.7	0.2	416.9		930	540	
10/11/15	11					6.9	0.4	405.0					6.8	0.3	571.9					6.7	0.3	562.4		930	700	
10/12/15	12					6.8	0.2						6.9	0.9						6.8	1.4			920	520	
10/13/15	13	5420	2500	2770	2650	6.9	0.2	-216.0	3220	1580	1620	1600	6.6	1.4	-147.9	3120	1500	1600	1520	6.7	2.6	-108.3	1.05	800	280	187
10/14/15	14	10540	4200	6290	4250	6.8	0.1	-243.7	5240	2060	3280	1960	6.6	2.5	-141.7	3520	1520	2160	1360	6.6	0.6	-148.0	1.59	520	220	145
10/15/15	15	6720	2760	3850	2870	6.8	0.2	-175.7	5160	2140	3280	1880	6.6	1.8	-144.3	3820	1620	2280	1540	6.7	0.3	-163.5	1.48	450	200	123
10/16/15	16	14200	5980	8140	6060	6.7	0.1	-71.9	4300	2220	2500	1800	6.7	1.6	-101.9	4040	2040	2340	1700	6.5	2.8	-102.9	1.38	420	180	88
10/17/15	17 18																									
10/18/15		10590	4360	6130	4450	6.8	0.2	164.0	4480	1900	2630	1850	6.6	1 /	-470.0	4480	1900	2320	2160	6.6	21	170.0	1.07	250	200	105
10/19/15 10/20/15	19 20	10580 7780	3300	4750	3030	6.6	0.2 0.5	-164.0 -125.4	4480	1900	2030	1630	6.6 6.5	1.4 1.7	-470.0	4480	1900	2540	1580	6.6 6.4	3.1 3.7	-179.0 -87.2	1.61	350 340	200 200	105 115
10/20/13	20	5180	2200	3460	1720	6.9	0.3	-125.4	4420	2000	2920	1630	6.7	0.9	-116.0	5000	2180	3200	1380	6.6	1.4	-166.7	1.01	340	190	87
10/21/15	21	9440	4200	5320	4120	6.8	0.2	-190.8	4500	2100	2320	1700	6.7	0.6	-306.9	4720	2130	2820	1900	6.6	1.4	-174.9	1.48	330	190	89
10/22/15	22	4420	1960	2760	1660	6.8	0.2	-142.8	7860	3300	4630	3230	6.7	0.6	-134.4	4520	1960	2600	1900	6.5	0.8	-129.6	1.48	350	200	102
10/23/15	23		1000	2,00	1000	7.5	0.4	-79.0	, 000			5250	7.5	0.0	-95.0	1020		2000	1920	7.5	0.0	-70.0	1.55	370	200	
10/25/15	25					7.4	0.4	-80.0					7.4	0.1	-48.0					7.4	0.2	-66.0		380	200	
10/26/15	26	4160	1820	2450	1710	6.9	0.1	-277.8	4820	2200	4270	550	6.8	0.6	-108.9	4200	1960	1630	2570	6.7	1.0	-91.2	0.63	370	220	112
10/27/15	27	1940	1000	830	1110	7.0	0.3	-128.7	2100	1140	820	1280	6.9	3.2	-104.4	1520	840	590	930	6.8	4.6	-139.6	0.63	160	100	119
10/28/15	28	4400	2120	2230	2170	7.2	0.2	-221.0	5800	2780	3050	2750	6.7	1.3	-204.0	4580	2200	2230	2350	6.6	3.3	-140.0	0.95			
10/29/15	29	3700	1860	2650	1050	6.8	0.4	-129.6	6140	2960	3290	2850	6.6	1.7	-134.5	4420	2300	2450	1970	6.5	3.1	-124.6	1.24	360	200	87
10/30/15	30	5340	2760	2800	2540	6.9	0.5	189.3	8180	4080	4240	3940	6.6	0.9	-126.1	5140	2620	2690	2450	6.5	2.5	-104.4	1.10			
10/31/15	31					6.8	0.4	-239.0					6.6	1.3	-89.7					6.6	3.8	-137.6				

		RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4		٦	Thickene	er Filtrat	e		Internal Recycle (RFR)	Clarifier	Clarifier		lymer	
Date	Day	Flow	Flow	TSS	TSS	Magnetite SS	Magnetite SS	Biological SS	Biological SS	NH3-N	TKN	NO3-N	NO2 & NO3 - N	NO2 - N	TN	Speed	3 Blanket	4 Blanket	Pump Dial Speed	Level	Polymer Feed Rate
		GPM	GPM	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	Hz	FT	FT	#	inches in barrel	gpd
10/01/15	1	700																		30	0
10/02/15	2	500		11720		4970		6,750												30	0
10/03/15	3	500																		30	0
10/04/15	4	500																		30	0
10/05/15	5	650		9340		3240		6,100												30	0
10/06/15	6	1100		8160		3200		4,960								55	10.0			30	0
10/07/15	7	1600		7080		2850		4,230									14.0			30	0
10/08/15	8	1750		6800		2650		4,150								30	11.5			30	0
10/09/15	9	750		6940		3150		3,790								30	13.0			30	0
10/10/15	10															25	13.0			30	0
10/11/15	11															25	13.0			30	0
10/12/15	12															25	10.5			30	0
10/13/15	13	1750		5980		3250		2,730								25	12.5			30	0
10/14/15	14	1750		5940		3720		2,220								25	8.5			30	0
10/15/15	15	1750		8480		5500		2,980								25	2.0			30	0
10/16/15	16	1750		10260		5960		4,300								25	2.0			30	0
10/17/15	17																			30	0
10/18/15	18																			30	0
10/19/15	19	1700		8840		5160		3,680								40	2.0			30	0
10/20/15	20	1700		12380	ļ	7300		5,080	ļ			ļ				45	1.0			30	0
10/21/15		864		10180		6600		3,580								45	1.0			30	0
10/22/15	22	1100		11100		6800		4,300								55	1.0			30	0
10/23/15	23			8020		4800		3,220								60	0.5			30	0
10/24/15	24															60	2.0			30	0
10/25/15	25															60	0.8			30	0
10/26/15	26	2029		9900		5730		4,170								60	0.5			30	0
10/27/15	27	1767	20.47		40.40		<b>5</b> 000									60	2.0	4.5		30	0
10/28/15	28		2847		10440		5330		5,110							60		1.5		30	0
10/29/15	29	2000	2874		13220		7260		5,960									2.5		30	0
10/30/15	30	2809			11800		6250		5,550							<u> </u>		3.0		30	0
10/31/15	31	2519														60		3.0		30	0

		Eq	uip. D	ata				Ma	TO Ig Drum								OM Drum					Drum overy
Date	Day	Mag Drum Speed	Shear Mill Current	Shear Mill Speed	F	low	TSS	Mag	Bio	TSS	Mag	Bio	F	low	TSS	Mag	Bio	TSS	Mag	Bio	Mag	Bio
		Hz	Amps	Hz	gpm	Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	gpm	85% Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	%	%
10/01/15	1																					
10/02/15	2						11,720	4,970	6,750													1
10/03/15	3																					1
10/04/15	4																					
10/05/15	5						9,340	3,240	6,100													
10/06/15	6		30	38	20		8,160	3,200	4,960				17		5720	740	4,980					
10/07/15	7						7,080	2,850	4,230													
10/08/15	8		30	38	40	60,289	6,800	2,650	4,150	3,419	1,332	2,087	34	51,246	4700	950	3,750	2,009	406	1,603	70	77
10/09/15	9		30	37	40	54,894	6,940	3,150	3,790	3,177	1,442	1,735	34	46,660	4360	860	3,500	1,697	335	1,362	77	78
10/10/15	10		28	37	42	62,334							36	52,984								
10/11/15	11		29	37	41	74,757							35	63,543								ļ
10/12/15	12				42	44,178							35	37,551								ļ
10/13/15	13		30	37	40	71,112	5,980	3,250	2,730	3,547	1,927	1,619	34	60,445	3240	630	2,610	1,633	318	1,316	84	81
10/14/15	14		30		40	47,699	5,940	3,720	2,220	2,363	1,480	883	34	40,544	3060	640	2,420	1,035	216	818	85	93
10/15/15	15		30		33	26,155	8,480	5,500	2,980	1,850	1,200	650	28	22,232	2380	660	1,720	441	122	319	90	49
10/16/15	16		30		19	26,546	10,260	5,960	4,300	2,271	1,319	952	16	22,564	3800	610	3,190	715	115	600	91	63
10/17/15	17					26,546								22,564								
10/18/15	18					26,546								22,564								
10/19/15	19	60	30	32	19	29,000	8,840	5,160	3,680	2,138	1,248	890	16	24,650	4720	680	4,040	970	140	831	89	93
10/20/15	20	60	30	37	21	30,689	12,380	7,300	5,080	3,169	1,868	1,300	18	26,086	5200	1010	4,190	1,131	220	912	88	70
10/21/15	21	60	30	37	21	31,072	10,180	6,600	3,580	2,638	1,710	928	18	26,411	6180	950	5,230	1,361	209	1,152	88	124
10/22/15	22	60		27	21	24,980	11,100	6,800	4,300	2,312	1,417	896	18	21,233	5540	1020	4,520	981	181	800	87	89
10/23/15	23	60	20	37	18	26,000	8,020	4,800	3,220	1,739	1,041	698	15	22,100	4640	690	3,950	855	127	728	88	104
10/24/15	24 25	60 60	30 30	37 37	18 18	26,000 27,735							15 15	22,100 23,575								!
10/25/15 10/26/15	25	60	50	37	18	26,091	9,900	5,730	4,170	2,154	1,247	907	15	23,575	5540	630	4,910	1,025	117	908	91	100
10/26/15	20	60		37	10	0	9,900	3,750	4,170	2,134	1,247	507	10	0	8040	1630	6,410	0	0	908	91	100
10/27/15	27	60		50		20,834	10,440	5,330	5,110	1,814	926	888		17,709	0040	1030	0,+10	0	0	0		!
10/28/15	20	60	31	38	18	9,071	13,220	7,260	5,960	1,000	549	451	15	7,710	6420	690	5,730	413	44	368	92	82
10/30/15	30	60	31	38	10	3,589	11,800	6,250	5,550	353	187	166	16	3,051	0120	0.50	3,730			500	52	
10/31/15	31	60		38		-6	,000	0,200	2,550					-5								<u>/</u>

Date	Day		Reacti	on Tank			Clar	ifier			TOTAL IN	IVENTOR	Y	Target SRT		Targe	t Waste		Actual SRT
		TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	days	lbs/d	Concentration Y (RAS)	Gallons at Concentration Y	Flow Rate gpm	days
10/01/15	1	9,643	4,233	5,409	0.8									11					
10/02/15	2	6,115	2,744	3,371	0.8									11		6,750			
10/03/15	3													11					
10/04/15	4													11					
10/05/15	5	10,270	2,901	7,369	0.4									11		6,100			
10/06/15	6	12,073	4,469	7,604	0.6	17,813	6,923	10,890	0.6	29,886	11,392	18,494	0.6	11	1,681	4,960	40,644	28	
10/07/15	7	18,109	5,605	12,504	0.4	24,141	9,165	14,976	0.6	42,251	14,771	27,480	0.5	11	2,498	4,230	70,813	49	
10/08/15	8	16,855	7,291	9,564	0.8	18,901	7,560	11,341	0.7	35,756	14,851	20,905	0.7	11	1,900	4,150	54,909	38	12
10/09/15	9	13,798	7,095	6,703	1.1	20,770	9,681	11,089	0.9	34,567	16,775	17,792	0.9	11	1,617	3,790	51,171	36	11
10/10/15	10													11					
10/11/15	11													11					
10/12/15	12													11					
10/13/15	13	12,230	6,272	5,958	1.1	17,308	9,297	8,011	1.2	29,538	15,568	13,969	1.1	11	1,270	2,730	55,775	39	7
10/14/15	14	13,798	8,467	5,331	1.6	12,019	7,493	4,527	1.7	25,817	15,959	9,858	1.6	11	896	2,220	48,401	34	10
10/15/15	15	14,974	8,937	6,036	1.5	3,816	2,439	1,377	1.8	18,790	11,376	7,414	1.5	11	674	2,980	27,118	19	14
10/16/15	16	15,836	9,172	6,664	1.4	4,510	2,619	1,891	1.4	20,346	11,791	8,555	1.4	11	778	4,300	21,687	15	13
10/17/15	17													11					
10/18/15	18													11					
10/19/15	19	17,561	9,094	8,467	1.1	4,069	2,321	1,748	1.3	21,630	11,415	10,215	1.1	11	929	3,680	30,257	21	10
10/20/15	20	16,150	9,956	6,193	1.6	2,652	1,574	1,078	1.5	18,801	11,530	7,271	1.6	11	661	5,080	15,602	11	7
10/21/15	21	19,599	12,543	7,056	1.8	2,329	1,506	823	1.8	21,928	14,049	7,878	1.8	11	716	3,580	23,988	17	/
10/22/15	22	18,501	11,054	7,448	1.5	2,472	1,508	964	1.6	20,973	12,562	8,412	1.5	11	765	4,300	21,323	15	10
10/23/15	23	17,717	10,191	7,526	1.4	944	560	384	1.5	18,661	10,752	7,910	1.4	11	719	3,220	26,776	19	9
10/24/15	24													11					<u> </u> ]
10/25/15 10/26/15	25 26	16,463	6,389	10,074	0.6	1,102	601	501	1.2	17,565	6,990	10,575	0.7	11 11	961	4,170	27,642	19	10
10/26/15	20	5,958	2,313	3,645	0.6	1,102	001	301	1.2	17,505	0,990	10,373	0.7	11	501	4,170	27,042	19	10
10/27/15	27	17,953	8,741	9,212	0.8	3,507	1,775	1,731	1.0	21,459	10,516	10,943	1.0	11	995	5,110	23,342	16	<u> </u> ]
10/28/13	28	17,335	9,604	7,722	1.2	7,084	3,895	3,188	1.0	21,439	13,499	10,943	1.0	11	993	5,960	19,954	10	22
10/23/15	30	20,148	10,544	9,604	1.2	7,084	4,184	3,188	1.2	24,403	14,729	13,336	1.2	11	1,212	5,550	26,192	14	
10/31/15	31	20,170	10,077	5,004	***	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	·,±0+	5,752		20,000	1,725	10,000		11		3,330	20,192	10	<u> </u>
10/21/12	71	<u> </u>						1						11					

## Questionable Data

					Ra	w In	fluen	t								Ρ	rimar	y Eff	lue	nt									Fi	nal I	Efflu	ient					
Date	Day		рН	BOD <sub>5</sub>	Alkalinity	NO3-N	NO2 - N	NO3 & NO2 - N	NH3-N	TKN	TN	рН	Temp	BOD₅	TSS	VSS	Alkalinity	NH3-N	TKN	NO3 & NO2 - N	NO3-N	NO2 - N	TN	рН	UV T	UV rans	BOD <sub>5</sub>	TSS	% TSS Reduction	VSS	NH3-N	TKN	NO3 & NO2 - N	NO3- N	NO2 - N	TN	Alkalinity
		MGD	SU	mg/L	mg/L as CaCO₃	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	°C	mg/L	mg/L	mg/L	mg/L as CaCO3	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	MW/c m <sup>2</sup>	%	mg/L	mg/L	%	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L as CaCO3
11/01/15	32	2.2																							17.3	72											
11/02/15	33	2.0	7.1									6.9	17.4		62	56								6.8	7.1	72		8	87	8							71
11/03/15	34	2.0	7.1	72		<0.050	0.043		24	32	32	6.9	17.7	60	48	48		26	32		<0.050	0.051	32	6.7	7.8	71	1	9	81	9	0.61	1.8		5.7	0.021	7.5	
11/04/15	35			129								6.9	17.4	24	64	64		22	27		<0.050	0.031	27	6.6		71	3	14	78	14	0.15	2.5		8.8	0.021	11	33
11/05/15	36		7.3									7	17.3		40	40		25	30		<0.050	0.048	30	6.6	6.7	66		2	95	2	0.87	2.7		9.9	0.079	13	
11/06/15	37	2.0	7.2									7	17.5		50	50								6.6		70		7	86	7							78
11/07/15	38	1.9											_											6.6		71											
11/08/15	39	1.9																						6.7		71											
11/09/15	40	1.8	7.2									7	17.4		74	68								6.7		70		7	91	7							75
11/10/15	41	1.9	7.1		170	<0.050	0.036		28	37	37	7	17.5		54	42	180	28	35		<0.050	0.050	35	6.7		70		5	91	3	0.20	1.2		8.2	0.018	9.4	67
11/11/15	42	2.4		84										81				23	32		<0.050	0.023	32	6.6	7.1	72	1				0.45	1.8		7.0	0.015	8.8	
11/12/15	43	2.3	7.2	147								7	17	57	48	48		25	33		0.059	0.025	33	6.7	7.6	74	3	4	92	4	0.16	1.0		3.4	0.012	4.4	
11/13/15	44	2.3	7.1									7	16.9		40	40								6.7	7.1	72		3	93	3							48
11/14/15	45	2.2																						6.7	7.6	74											
11/15/15	46	2.2																						6.7	6.8	44											
11/16/15	47	2.1	7.2									7.1			48	48								6.7	6.8	71		6	88	6							56
11/17/15	48	2.0		144		<0.050	0.054		23	33	33	7.1	16.7	90	44	44		24	31		<0.050	0.024	31	6.7		72	3	4	91	4	0.32	0.98		3.3	0.02	4.3	
11/18/15	49	2.0		180								7.1	16.5	111	46	46		25	30		<0.050	0.30	30	6.7	6.8	71	2	8	83	8	0.15	1.4		2.5	0.029	3.9	56
11/19/15		2.0		174								7		93		62		25	32		<0.050	0.029	32	6.7	7.1	72	2.8		90		0.40	0.61		3.8	0.03	4.4	
11/20/15			7.2									7	16.1		60	60		ļ							8.8			9	85	9							
11/21/15		2.3																								75											
11/22/15	53	2.7				0.51									40							0.40		6.8		75			~ ~ ~						0.00-		
11/23/15	54	3.2				0.51	0.18		17	22	23		4		48	48		15	22		1.1	0.19	1	6.6		76		9	81	9	0.40	1.5		3.5	0.035	5.0	57
11/24/15	55			96					<u> </u>			6.9	15.6	81	44	44		16	20		0.70	0.16	21	6.6		74	2	10	77	10	0.87	1.6		4.8	0.021	6.4	
11/25/15			7.2									7			54	50		16	22		0.37	0.16	22	6.7	9.7	76		10	81	10	0.29	1.5		2.9	0.018	4.4	
11/26/15		2.7																					+		7.9												
11/27/15 11/28/15	58	2.7 2.6																								75 78											
11/28/15	59 60	2.6						<u> </u>	+									+					+			78 77											
11/29/15	61		7.1									7.1			52	38							+		7.6			11	79	9							56

				z	one #1						z	one #2								Zon	e #3					
Date	Day	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	Magnetite:Bi	5 Min Settle	30 Min Settle	SVI
		mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	osolids Ratio	mL/L	mL/L	mL/g
11/01/15	32					6.8	0.4	-193.7					6.6	1.3	-103.9					6.5	3.7	-125.8		680	360	
11/02/15	33	4660	2480	2180	2480	6.9	0.4	-217.7	6940	3560	2940	4000	6.8	0.6	-146.7	4920.0	2560.0	2220	2700	6.7	1.9	-133.8	0.82	650	300	117
11/03/15	34	8140	4300	3600	4540	6.8	0.2	-219.5	6180	3120	3200	2980	6.7	0.9	-295.9	5200.0	2660.0	2550	2650	6.6	2.8	-107.3	0.96	490	300	113
11/04/15	35	8920	4980	3530	5390	6.8	0.3	-147.7	6960	3660	3300	3660	6.7	0.7	-116.1	5180.0	2740.0	2520	2660	6.6	1.8	-89.2	0.95	480	280	102
11/05/15	36	7880	4080	3520	4360	6.8	0.2	-126.7	9500	4560	4780	4720	6.7	0.4	-129.1	5360.0	2520.0	2830	2530	6.6	0.9	-132.9	1.12	470	280	111
11/06/15	37	7180	3800	3030	4150	6.8	0.6	-141.4	7080	3480	3590	3490	6.7	1.0	-131.1	4940.0	2340.0	2520	2420	6.6	2.0	-104.5	1.04	480	270	115
11/07/15	38					6.8	0.3	-140.3					6.6	0.8	-141.2					6.5	2.6	-132.8		510	260	
11/08/15	39					7.1	0.4	-98.7					6.7	0.7	-126.7					6.6	2.6	-129.6		490	270	
11/09/15	40	6460	3360	2740	3720	6.9	0.7	-244.8	12600	6180	5560	7040	6.8	0.7	242.9	4380.0	2140.0	2030	2350	6.6	1.2	-171.1	0.86	400	220	103
11/10/15	41	8080	4420	2840	5240	6.9	0.3	-121.0	7940	4020	3510	4430	6.8	1.1	-116.6	4360.0	2120.0	2000	2360	6.6	1.8	-118.1	0.85	420	250	118
11/11/15	42																									
11/12/15	43	3980	2140	2200	1780	6.9	0.4	-92.9	6640	3520	3050	3590	6.8	0.7	15.3	4480.0	2400.0	2180	2300	6.6	2.1	-207.1	0.95	420	250	104
11/13/15	44	4260	2220	2250	2010	6.8	0.4	-131.7	13220	7260	5650	7570	6.7	0.8	-138.8	4140.0	2100.0	2040	2100	6.5	1.4	-114.6	0.97	390	230	110
11/14/15	45					6.7	0.3	-89.6					6.6	1.0	-253.4					6.5	3.0	-205.7				
11/15/15	46					7.2	0.3	-56.0					6.9	0.8	-116.3					6.7	1.9	-106.2			<b> </b>	
11/16/15	47	4600	2500	2360	2240	6.9	0.4	-110.6	5620	3000	2820	2800	6.7	1.4	-79.3	4240.0	2280.0	2200	2040	6.6	2.3	5.2	1.08	450	270	118
11/17/15	48	4840	2520	2350	2490	6.9	0.4	-64.0	5660	2940	2720	2940	6.8	0.6	-231.7	4400.0	2240.0	2220	2180	6.6	2.4	129.2	1.02	490	280	125
11/18/15	49 50	5100 5520	2740 3160	2560 2720	2540 2800	6.9 7.0	0.5	-31.8 -120.9	6680 7400	3600 4160	3200 3720	3480 3680	6.8 6.8	1.4 1.2	-36.5 -134.4	4740.0	2560.0 3100.0	2360	2380 2660	6.7	2.7 3.6	-31.0	0.99 1.03	510 550	300	117 103
11/19/15 11/20/15	50 51	5020	2740	2720	2800	6.9	0.4	-120.9	5120	2780	2600	2520	6.7	2.2	-134.4	5400.0 4940.0	2640.0	2740 2450	2660	6.7 6.5	4.3	-116.0 -110.0	0.98	500	320 300	103
11/20/15	52	3020	2740	2380	2440	6.7	0.4	-44.1	5120	2780	2000	2320	6.6	0.6	-53.6	4940.0	2040.0	2430	2490	6.5	3.2	-121.5	0.38	700	410	114
11/22/15	53					6.9	0.3	-155.7					6.7	0.8	-74.5					6.5	3.1	-109.7		820	450	
11/22/15	54	4340	2340	2000	2340	6.9	0.4	101.9	4380	2320	2050	2330	6.7	0.9	72.3	4060.0	2160.0	1960	2100	6.6	2.5	-7.9	0.93	520	300	139
11/24/15	55	4320	2200	2180	2140	6.9	0.4	89.9	6340	3360	2800	3540	6.7	1.2	70.6	4320.0	2200.0	2030	2290	6.6	4.1	145.2	0.89	530	300	136
11/25/15	56	4360	2380	2030	2330	7.0	0.3	133.4	5040	2740	2250	2790	6.8	1.6	2.0	3960.0	2100.0	2000	1960	6.6	3.2	-53.4	1.02	550	330	157
11/26/15	57					6.9	0.4	-107.4					6.7	1.2	-68.3					6.6	3.1	-77.3		550	320	
11/27/15	58					6.9	0.4	-120.6					6.7	1.2	-71.2					6.7	3.1	-48.9		890	550	
11/28/15	59					6.7	0.5	-136.5					6.7	1.6	-131.2					6.6	4.3	-126.5		900	580	
11/29/15	60					7.0	0.6	-103.0					6.8	1.5	-27.9					6.7	5.2	-113.7		900	570	
11/30/15	61	4160	2300	1850	2310	7.0	0.2	99.7	4640	2520	1830	2810	6.8	3.7	-139.2	4020.0	2180.0	1800	2220	6.7	5.7	100.3	0.81	800	340	156

		RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4		٦	Thicken	er Filtrat	e		Internal Recycle (RFR)	Clarifier	Clarifier	Рс	olymer	
Date	Day	Flow	Flow	TSS	TSS	Magnetite SS	Magnetite SS	Biological SS	Biological SS	NH3-N	TKN	NO3-N	NO2 & NO3 - N	NO2 - N	TN	Speed	3 Blanket	4 Blanket	Pump Dial Speed	Level	Polymer Feed Rate
		GPM	GPM	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	Hz	FT	FT	#	inches in barrel	gpd
11/01/15	32															60		4.0		30	0
11/02/15	33		1415		10680		4660		6,020							60		3.5		29	1.80
11/03/15	34		1389		11720		6040		5,680							60		2.5		29	0
11/04/15	35		1358		11780		6000		5,780							60		2.5		29	0
11/05/15	36		1361		8700		5600		3,100							60		2.0		29	0
11/06/15	37		1378		7300		3800		3,500							60		2.5		29	0
11/07/15	38		1343													60		3.0		29	0
11/08/15	39		1301													60				29	0
11/09/15	40		1963		9780		4560		5,220							60		1.5		29	0
11/10/15	41		1960		8100		3860		4,240							60				29	0
11/11/15	42		1954													60				29	0
11/12/15	43		1939		9240		4490		4,750							60		2.2		29	0
11/13/15	44		1939		5820		3300		2,520							60		2.0		29	0
11/14/15	45		1955													60		2.0		29	0
11/15/15	46		1961													60		2.0		29	0
11/16/15	47		1958		9900		5000		4,900							60				29	0
11/17/15	48		1949		8840		4050		4,790							60				29	0
11/18/15	49		1947		11200		5210		5,990							60		2.0		29	0
11/19/15	50		1947		12800		6400		6,400							60		3.0		29	0
11/20/15	51		1938		12300		6180		6,120			-				60		3.0		29	0
11/21/15	52		1938													60		3.0		29	0
11/22/15	53		1932		10020		4840		F 190							60 60		4.0		29 29	0
11/23/15 11/24/15	54		1932 1934		10020 5560		4840 5430		5,180 130							60		5.0 5.0		29	0
11/24/15	55 56		1934		10260		4580		5,680							60		7.0		29	0
11/25/15	57		1940		10200		400		5,000							60		7.0		29	0
11/20/13	58		1939													60		7.0		29	0
11/28/15	59		1941													60		8.0		29	0
11/29/15	60		1942													60		8.0		29	0
11/30/15	61		1948		10060		4250		5,810											29	0

		Equ	uip. Da	ata				Ma	TO g Drum		-						OM Drum	_				Drum overy
Date	Day	Mag Drum Speed	Shear Mill Current	Shear Mill Speed	1	Flow	TSS	Mag	Bio	TSS	Mag	Bio	F	low	TSS	Mag	Bio	TSS	Mag	Bio	Mag	Bio
		Hz	Amps	Hz	gpm	Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	gpm	85% Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	%	%
11/01/15	32			38		6,615								5,623								
11/02/15	33		32	38	39	31,984	10,680	4,660	6,020	2,849	1,243	1,606	33	27,186								
11/03/15	34		31	38	24	32,684	11,720	6,040	5,680	3,195	1,646	1,548	20	27,781								
11/04/15	35		32	38	24	28,500	11,780	6,000	5,780	2,800	1,426	1,374	20	24,225	6300	850	5,450	1,273	172	1,101	88	80
11/05/15	36		29	38	24	10,260	8,700	5,600	3,100	744	479	265	20	8,721	5420	750	4,670	394	55	340	89	128
11/06/15	37		32	38	22	21,953	7,300	3,800	3,500	1,337	696	641	19	18,660	5300	560	4,740	825	87	738	87	115
11/07/15	38		32	38	19	59,719							16	50,761								
11/08/15	39		31	38	25	36,899							21	31,364								
11/09/15	40		31	38	19	35,120	9,780	4,560	5,220	2,865	1,336	1,529	16	29,852	4820	430	4,390	1,200	107	1,093	92	71
11/10/15	41		31	38	18	22,381	8,100	3,860	4,240	1,512	720	791	16	19,024	4660	350	4,310	739	56	684	92	86
11/11/15	42					22,381								19,024								
11/12/15	43		31	38	15	22,890	9,240	4,490	4,750	1,764	857	907	12	19,457	5100	480	4,620	828	78	750	91	83
11/13/15	44		32	38	13	17,271	5,820	3,300	2,520	838	475	363	11	14,680	5360	480	4,880	656	59	597	88	165
11/14/15	45		31	38	14	16,970							12	14,425								
11/15/15	46		31	38	14	31,922							12	27,134								
11/16/15	47				17	25,284	9,900	5,000	4,900	2,088	1,054	1,033	14	21,491	5660	480	5,180	1,014	86	928	92	90
11/17/15	48				14	17,148	8,840	4,050	4,790	1,264	579	685	12	14,576	5420	450	4,970	659	55	604	91	88
11/18/15	49		31	38	14	19,947	11,200	5,210	5,990	1,863	867	996	12	16,955	5320	380	4,940	752	54	699	94	70
11/19/15	50		30	38	15	20,202	12,800	6,400	6,400	2,157	1,078	1,078	13	17,172	5980	490	5,490	856	70	786	93	73
11/20/15	51		31	38	14	17,604	12,300	6,180	6,120	1,806	907	899	12	14,963	6640	630	6,010	829	79	750	91	83
11/21/15	52		31	38	14	20,100							12	17,085								
11/22/15	53 54		31	38	14	23,854	10.020	1 0 1 0	E 100	2,330	1 1 2 5	1 204	12	20,276	5880	400	E 400	1 160	70	1 000	02	00
11/23/15 11/24/15	54 55		31 31	38 38	20 22	27,878 28,617	10,020 5,560	4,840 5,430	5,180 130	2,330	1,125 1,296	1,204 31	17 19	23,696 24,324	5880	400 480	5,480 5,160	1,162 1,144	79 97	1,083 1,047	93 92	90 3,374
11/24/15	55		31	38	13	16,285	10,260	5,430 4,580	5,680	1,327	622	771	19	13,842	5940	360	5,180	686	42	644	92	3,374 84
11/25/15	50		31	38	13	16,285	10,200	4,300	3,000	1,222	022	//1	11	13,842	5940	300	5,360	000	42	044	33	04
11/27/15	57		31	38	13	17,928							11	15,239								
11/28/15	59		32	38	12	97,953							11	83,260								
11/29/15	60		32	38	13	1,369							11	1,163								
11/30/15	61				33	1,369	10,060	4,250	5,810	115	49	66	28	1,163	5080	660	4,420	49	6	43	87	65

Date	Day		Reacti	on Tank			Clar	rifier			TOTAL IN	IVENTOR	Υ	Target SRT		Targe	t Waste		Actual SRT
		TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	days	lbs/d	Concentration Y (RAS)	Gallons at Concentration Y	Flow Rate gpm	days
11/01/15	32													11					
11/02/15	33	19,285	8,702	10,583	0.8	8,446	3,709	4,737	0.8	27,731	12,411	15,320	0.8	11	1,393	6,020	27,740	19	
11/03/15	34	20,383	9,995	10,387	1.0	6,574	3,358	3,216	1.0	26,957	13,354	13,603	1.0	11	1,237	5,680	26,106	18	
11/04/15	35	20,305	9,878	10,427	0.9	6,597	3,333	3,264	1.0	26,902	13,211	13,691	1.0	11	1,245	5,780	25,819	18	10
11/05/15	36	21,010	11,093	9,917	1.1	4,180	2,576	1,603	1.6	25,190	13,670	11,520	1.2	11	1,047	3,100	40,508	28	31
11/06/15	37	19,364	9,878	9,486	1.0	4,485	2,323	2,162	1.1	23,849	12,201	11,648	1.0	11	1,059	3,500	36,277	25	14
11/07/15	38	,	,	,		,	,	,		,		,		11	,	,	,		
11/08/15	39													11					
11/09/15	40	17,169	7,957	9,212	0.9	3,297	1,536	1,762	0.9	20,466	9,493	10,973	0.9	11	998	5,220	22,914	16	9
11/10/15	41	17,090	7,840	9,251	0.8									11		4,240			
11/11/15	42													11					
11/12/15	43	17,561	8,545	9,016	0.9	4,638	2,254	2,384	0.9	22,199	10,800	11,399	0.9	11	1,036	4,750	26,159	18	14
11/13/15	44	16,228	7,996	8,232	1.0	2,898	1,587	1,311	1.2	19,126	9,583	9,543	1.0	11	868	2,520	41,277	29	15
11/14/15	45													11					
11/15/15	46													11					
11/16/15	47	16,620	8,624	7,996	1.1									11		4,900			
11/17/15	48	17,247	8,702	8,545	1.0									11		4,790			
11/18/15	49	18,580	9,251	9,329	1.0	4,984	2,347	2,637	0.9	23,564	11,598	11,966	1.0	11	1,088	5,990	21,775	15	14
11/19/15	50	21,167	10,740	10,427	1.0	8,539	4,281	4,259	1.0	29,706	15,021	14,685	1.0	11	1,335	6,400	25,012	17	17
11/20/15	51	19,364	9,604	9,760	1.0	8,137	4,080	4,058	1.0	27,501	13,683	13,818	1.0	11	1,256	6,120	24,611	17	15
11/21/15	52				ļļ									11					
11/22/15	53													11					
11/23/15	54	15,914	7,683	8,232	0.9		-					40.5		11		5,180			
11/24/15	55	16,934	7,957	8,976	0.9	7,089	5,918	1,171	5.1	24,022	13,875	10,147	1.4	11	922	130	850,807	591	8
11/25/15	56	15,522	7,840	7,683	1.0	15,734	7,173	8,561	0.8	31,257	15,013	16,244	0.9	11	1,477	5,680	31,173	22	19
11/26/15	57				<u>↓                                    </u>									11					
11/27/15	58				┼───┨									11					
11/28/15 11/29/15	59 60				+									11 11					
11/29/15	61	15,758	7,056	8,702	0.8									11		5,810			
11/30/13	10	13,730	7,050	0,702	0.0									11		3,010			

## Questionable Data

					Rav	w In	flue	nt								Pri	mary	Efflu	uent	t									Fir	nal E	fflu	ent					
Date	Day		рН	BOD <sub>5</sub>	Alkalinity	NO3-N	NO2 - N	NO3 & NO2 - N	NH3-N	I TKN	TN	рН	Temp	BOD <sub>5</sub>	TSS	VSS	Alkalinity	NH3-N	TKN	NO3 & NO2 - N	NO3- N	NO2 - N	TN	рН	UV	UV Trans	BOD <sub>5</sub>	TSS	% TSS Reduction	VSS	NH3-N	TKN	NO3 & NO2 - N		NO2 - N	TN	Alkalinity
		MGD	SU	mg/L	mg/L as CaCO₃	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	°C	mg/L	mg/L	mg/L	mg/L as CaCO3	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	SU	MW/c m²	%	mg/L	mg/L	%	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L as CaCO3
12/01/15	62	2.4	7.1	144				<0.050	23	29	29	7.1	15.2	72	44	44		22	29	<0.050			29	6.7	7.9	75	4	6	86	6	0.57	1.8	5.8			7.6	52
12/02/15	63	2.5	7.1	156					1			7.1	15.4	72	30	30		21	27	<0.050	1		27	6.8	8.1	76	3	3	90	3	1.1	2.2	5.5	1		7.7	
12/03/15	64	2.4	7.2	126								7	15	90	44	44		14	20	0.42			20	6.7	7.6	74	3	6	86	6	0.44	1.6	5.3			6.9	
12/04/15	65	2.3	7.2									7	15.1		36	36								6.6	7.9	75		5	86	5						1	
12/05/15	66	2.2																						6.5	7.3	73											
12/06/15	67	2.3																						6.7	7.9	75										í'	
12/07/15	68	2.2	7.1									6.9	14.8		82	68								6.8	8.4	73		5	94	5						ļ '	71
12/08/15	69	2.2	7.1	306				0.6	19	26	27	6.9	14.7	93	44	44		22	28	<0.050			28	6.7	7.3	73	2	8	82	8	0.48	1.7	5.6			7.3	
12/09/15	70	2.2	7.1	504								7	14.6	111	48	48		22	27	<0.050			27	6.7	8.7	74	4	5	90	5	0.19	1.4	4.4			5.8	
12/10/15	71	2.2	7.2	156								7	14.6	96	62	66		24	32	<0.050			32	6.7	7.6	74	3	6	90	12	0.96	2.5	6.2			8.7	
12/11/15	72	2.1	7.2									7	14.6		46	46								6.6	7.9	75		7	85	7						<b></b> '	
12/12/15	73	2.1																						6.6	7.3	73										<b></b> '	
12/13/15	74	2.1																						6.7	7.1	72										<b></b> '	
12/14/15	75	2.1	7.2									7.1	14.8		52	52								6.8	6.8	71		8	85	8						ļ'	56
12/15/15	76	2.8	7.1	174				0.95	36	46	47	7	14.6	87	36	36		24	26	<0.050			26	6.7	16.3	76	2	3	92	3	0.74	1.5	6.3			7.8	
12/16/15	77	2.4	7.2	180								7	14.5	99	50	50		20	24	0.095			24	_	41.4	77	2	4	92	4	0.47	1.5	4.9			6.4	
12/17/15	78	2.9	7.2	105								7	14.5	81	56	56		20	27	<0.050			27	-	8.5	77	7.9	7	88	7	0.34	1.5	5.8			7.3	
12/18/15	79	3.5	7.0									6.9	14.4		44									6.7	11.5	73		11	75							í'	
12/19/15	80	3.3																						6.9	7.3	73										í'	
12/20/15	81	3.0																						6.8	17.6	92										ļ'	
12/21/15	82	2.9	7.1									6.9			48									6.8	9.7	77		6	88							í'	
12/22/15	83	3.0		102				0.050	17	23	23	6.9		84	42									_	7.9		6	6	86		4.1	4.0	11			15	
12/23/15	84	3.2											14.1		32	ļ			ļ						10.1			2	94							·'	
12/24/15	85	7.3	6.9									6.7	13.7		52									-	17.5			13	75							<b> </b> '	
12/25/15	86	5.4																						_	25.6											<b> </b> '	
12/26/15	87	4.6																	ļ						21.8											·'	<b>↓</b> ]
12/27/15	88	4.5			ļ														<u> </u>	ļ					34.2									L		·'	<u> </u>
12/28/15	89		7.0		ļ								13.8		54				<u> </u>	ļ				_	44.7			7	87					L		·'	<u> </u>
12/29/15	90	4.7	7.0		ļ			0.45		21	21	6.9			61				<u> </u>	ļ				-	48.6	80		7	89			2.0	8.0	L		10	<u> </u>
12/30/15	91	4.6		66	ļ			ļ	<u> </u>				13.7	57	48	<u> </u>		<u> </u>	<u> </u>	ļ			<u> </u>		53	83	3.2	4	92					<u> </u>		·'	
12/31/15	92	4.8	6.8									6.8	13.5		60									6.7	51	82		5	92							<u> </u>	

				Z	one #1						Z	one #2								Zon	e <b>#3</b>					
Date	Day	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	MLSS - TSS	MLSS - VSS	MLSS - Magnetite	MLSS - Biological	рН	DO	ORP	Magnetite:Bi	5 Min Settle	30 Min Settle	SVI
		mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	mg/L	mg/L	mg/L	mg/L	SU	mg/L	mV	osolids Ratio	mL/L	mL/L	mL/g
12/01/15	62	4280	2520	1980	2300	7.0	0.3	-18.1	4680	2700	1560	3120	6.8	1.7	-88.9	4280	2420	1900	2380	6.7	2.8	-73.7	0.80	800	450	186
12/02/15	63	4460	2700	1850	2610	6.9	0.4	-97.2	4820	2920	2120	2700	6.7	0.9	-113.9	4040	2440	1820	2220	6.6	2.6	-96.9	0.82	780	400	164
12/03/15	64	5160	2960	2260	2900	6.9	0.4	-126.3	4760	2680	2280	2480	6.8	1.4	-141.8	4720	2680	2120	2600	6.7	3.6	-119.5	0.82	790	400	149
12/04/15	65	4680	2620	2130	2550	6.8	0.4	-51.4	4060	2240	2010	2050	6.7	2.5	-152.8	4220	2300	2060	2160	6.6	2.9	72.2	0.95	650	400	174
12/05/15	66					6.9	0.4	-76.3					6.8	2.1	-145.7					6.6	3.0	-74.9		880	490	
12/06/15	67					6.8	0.4	-25.1					6.6	2.6	-43.1					6.6	3.6	-104.1		890	520	
12/07/15	68	4340	2360	2030	2310	6.9	0.2	-146.5	5720	3100	2630	3090	6.7	1.5	-98.3	4120	1020	1800	2320	6.7	3.1	-102.3	0.78	800	420	412
12/08/15	69	4760	2940	2120	2640	7.0	0.3	-29.0	7340	4300	3050	4290	6.8	1.7	-32.3	4680	2840	2010	2670	6.7	2.5	-4.3	0.75	800	350	123
12/09/15	70	4700	2700	2130	2570	7.0	0.3	29.8	6520	3640	2800	3720	6.8	0.8	-270.9	4160	2300	2120	2040	6.7	1.7	71.6	1.04	860	440	191
12/10/15	71	4380	2540	2040	2340	6.9	0.3	-145.6	5840	3300	2650	3190	6.8	1.6	-141.0	4160	2400	2060	2100	6.7	2.3	-86.1	0.98	820	440	183
12/11/15	72	6760	4120	2720	4040	6.9	0.3	-123.5	4920	2960	2290	2630	6.7	1.8	-138.1	4640	2760	2340	2300	6.6	4.1	-108.5	1.02	650	350	127
12/12/15	73					6.8	0.9	290.5					6.6	1.2	-13.3					6.6	3.9	72.1				
12/13/15	74					6.8	0.4	-87.9					6.7	1.4	-90.0					6.6	5.4	-88.9		880	470	
12/14/15	75	7260	4240	2560	4700	6.9	0.4	-114.2	5660	3220	2260	3400	6.8	0.9	-142.7	5020	2760	2160	2860	6.7	1.9	-115.2	0.76			
12/15/15	76	4540	2620	2290	2250	6.9	0.4	-105.9	5600	3180	2820	2780	6.8	0.7	-124.6	5080	2880	2220	2860	6.6	1.9	-137.1	0.78			
12/16/15	77	5230	3100	2350	2880	7.0	0.4	52.7	5820	1820	2550	3270	6.8	1.0	-124.8	5280	3060	2320	2960	6.7	2.0	20.5	0.78			
12/17/15	78	4960	2960	2450	2510				6080	3580	2830	3250				4800	2800	2220	2580				0.86			
12/18/15	79																									
12/19/15	80																									
12/20/15	81																									
12/21/15	82	5760							6540							5080										
12/22/15	83	2940							3940							5540										
12/23/15	84	3840							6160							5020										
12/24/15	85	3100							2940							2680										
12/25/15	86																									
12/26/15	87																									
12/27/15	88																									
12/28/15	89	4500							5700							3920										
12/29/15	90								3080							3320										
12/30/15	91								3040							2440										
12/31/15	92								3200							2740										

		RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4	RAS 3	RAS 4		1	Thickene	er Filtrat	e		Internal Recycle (RFR)	Clarifier	Clarifier		lymer	
Date	Day	Flow	Flow	TSS	TSS	Magnetite SS	Magnetite SS	Biological SS	Biological SS	NH3-N	TKN	NO3-N	NO2 & NO3 - N	NO2 - N	TN	Speed	3 Blanket	4 Blanket	Pump Dial Speed	Level	Polymer Feed Rate
		GPM	GPM	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	Hz	FT	FT	#	inches in barrel	gpd
12/01/15	62		1949		8580		3890		4,690	110	530	0.48	0.7	0.22	530			8.0	677.0	28	1.80
12/02/15	63		1942		8840		3290		5,550									8.0	677.0	28	0
12/03/15	64		1942		9780		4430		5,350									8.0	677.0	28	0
12/04/15	65		1951		6620		3250		3,370									8.6	677.0	28	0
12/05/15	66		1953															8.5	677.0	27	1.80
12/06/15	67		1949															8.0	677.0	26	1.80
12/07/15	68		1947		9200		4050		5,150									8.0	677.0	28	-3.60
12/08/15	69		1946		10000		4290		5,710	110	170		23		190			8.0	677.0	27	1.80
12/09/15	70		1899		9480		4250		5,230									7.0	677.0	27	0
12/10/15	71		1949		9980		4530		5,450									8.0	677.0	24	5.40
12/11/15	72		1954		9960		4700		5,260									7.0		24	0
12/12/15	73		1927															6.0		24	0
12/13/15	74		1922															6.0		24	0
12/14/15	75				9580		4200		5,380									5.0		27	-5.40
12/15/15	76				11680		5350		6,330	150	210		33		240			3.0	677.0	22	8.99
12/16/15	77				11080		4730		6,350									2.5	702.0	20	3.60
12/17/15	78				18000		7490		10,510												
12/18/15	79				19460																
12/19/15	80																				
12/20/15	81																				
12/21/15	82			1980	24920																
12/22/15	83			2140	13840																
12/23/15	84			4200	12380																
12/24/15	85			4200	16600																
12/25/15	86																				
12/26/15	87																				
12/27/15	88																				
12/28/15	89			7000					ļ												ļ]
12/29/15	90			7600	9220																
12/30/15	91			8860	21940																
12/31/15	92			9200	14300																

		Eq	uip. Da	ata				Ma	TO Ig Drum								OM Drum					Drum overy
Date	Day	Mag Drum Speed	Shear Mill Current	Shear Mill Speed	FI	ow	TSS	Mag	Bio	TSS	Mag	Bio	F	low	TSS	Mag	Bio	TSS	Mag	Bio	Mag	Bio
		Hz	Amps	Hz	gpm	Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	gpm	85% Metered Flow GPD	mg/L	mg/L	mg/L	LBS	LBS	LBS	%	%
12/01/15	62	60	31	38	15	12,285	8,580	3,890	4,690	879	399	481	13	10,442	5400	380	5,020	470	33	437	92	91
12/02/15	63	60	31	38	15	24,417	8,840	3,290	5,550	1,800	670	1,130	13	20,754	5140	320	4,820	890	55	834	92	74
12/03/15	64	60	31	38	17	25,769	9,780	4,430	5,350	2,102	952	1,150	14	21,904	5220	520	4,700	954	95	859	90	75
12/04/15	65	60	31	38	17	31,815	6,620	3,250	3,370	1,757	862	894	14	27,043	5200	440	4,760	1,173	99	1,074	88	120
12/05/15	66	60	31	38	15	8,998							13	7,648								
12/06/15	67	60	32	38	15	24,176							13	20,550								
12/07/15	68	60	31	38	16	24,034	9,200	4,050	5,150	1,844	812	1,032	14	20,429	5260	300	4,960	896	51	845	94	82
12/08/15	69	60	31	38	17	27,358	10,000	4,290	5,710	2,282	979	1,303	14	23,254	5220	490	4,730	1,012	95	917	90	70
12/09/15	70	60	32	38	22	29,435	9,480	4,250	5,230	2,327	1,043	1,284	19	25,020	5600	650	4,950	1,169	136	1,033	87	80
12/10/15	71	60	31	38	19	25,590	9,980	4,530	5,450	2,130	967	1,163	16	21,752	5380	540	4,840	976	98	878	90	75
12/11/15	72	60	31	38	20	24,464	9,960	4,700	5,260	2,032	959	1,073	17	20,794	5260	560	4,700	912	97	815	90	76
12/12/15	73	60	32	38	21	26,718							18	22,710								
12/13/15	74	60	32	38	16								14									
12/14/15	75		31	38	18		9,580	4,200	5,380				15		5380	360	5,020					
12/15/15	76		31	38	15		11,680	5,350	6,330				13		5980	800	5,180					
12/16/15	77		31	36	14		11,080	4,730	6,350				12		5660	730	4,930					
12/17/15	78						18,000	7,490	10,510						8680	1250	7,430					
12/18/15	79						19,460								5280							
12/19/15	80																					
12/20/15	81																					
12/21/15	82						13,450															
12/22/15	83						7,990															
12/23/15	84						8,290															
12/24/15	85						10,400															
12/25/15	86																					
12/26/15	87																					
12/27/15	88																					
12/28/15	89						7,000															
12/29/15	90						8,410															
12/30/15	91						15,400															
12/31/15	92						11,750															

Date	Day		Reacti	on Tank			Clar	rifier			TOTAL IN	IVENTOR	Y	Target SRT		Targe	et Waste		Actual SRT
		TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	TSS LBS	Magnetite LBS	Biological LBS	Magnetite:Bi osolids Ratio	days	lbs/d	Concentration Y (RAS)	Gallons at Concentration Y	Flow Rate gpm	days
12/01/15	62	16,777	7,448	9,329	0.8	15,749	7,111	8,638	0.8	32,526	14,558	17,968	0.8	11	1,633	4,690	41,760	29	32
12/02/15	63	15,836	7,134	8,702	0.8	15,955	6,170	9,784	0.6	31,791	13,304	18,486	0.7	11	1,681	5,550	36,308	25	21
12/03/15	64	18,501	8,310	10,191	0.8	17,835	8,065	9,770	0.8	36,337	16,375	19,961	0.8	11	1,815	5,350	40,670	28	20
12/04/15	65	16,542	8,075	8,467	1.0	13,787	6,759	7,028	1.0	30,329	14,834	15,495	1.0	11	1,409	3,370	50,118	35	13
12/05/15	66													11					
12/06/15	67													11					
12/07/15	68	16,150	7,056	9,094	0.8	16,542	7,272	9,270	0.8	32,692	14,328	18,364	0.8	11	1,669	5,150	38,869	27	20
12/08/15	69	18,345	7,879	10,466	0.8	18,129	7,779	10,350	0.8	36,474	15,658	20,816	0.8	11	1,892	5,710	39,737	28	20
12/09/15	70	16,306	8,310	7,996	1.0	14,860	6,826	8,034	0.8	31,167	15,136	16,031	0.9	11	1,457	5,230	33,411	23	14
12/10/15	71	16,306	8,075	8,232	1.0	17,718	8,168	9,549	0.9	34,024	16,243	17,781	0.9	11	1,616	5,450	35,563	25	18
12/11/15	72	18,188	9,172	9,016	1.0	15,786	7,546	8,240	0.9	33,974	16,718	17,255	1.0	11	1,569	5,260	35,759	25	18
12/12/15	73													11					
12/13/15	74													11					
12/14/15	75	19,677	8,467	11,211	0.8	11,101	4,848	6,253	0.8	30,778	13,315	17,464	0.8	11	1,588	5,380	35,383	25	
12/15/15	76	19,913	8,702	11,211	0.8	7,834	3,559	4,275	0.8	27,747	12,261	15,486	0.8	11	1,408	6,330	26,667	19	
12/16/15	77	20,697	9,094	11,603	0.8	6,299	2,704	3,595	0.8	26,995	11,798	15,197	0.8	11	1,382	6,350	26,088	18	
12/17/15	78	18,815	8,702	10,113	0.9											10,510			
12/18/15	79																		
12/19/15	80																		
12/20/15	81																		
12/21/15	82	19,913											ļ						
12/22/15	83	21,716											ļ						
12/23/15	84	19,677											ļ						
12/24/15	85	10,505											ļ						
12/25/15	86																		
12/26/15	87				<b>↓</b>														
12/27/15	88	45.000			<b>├</b> ──── <b>│</b>														
12/28/15	89	15,366																	
12/29/15	90	13,014																	
12/30/15	91	9,564			├────┨								┼───┤						
12/31/15	92	10,740																	

## APPENDIX D

PILOT STUDY TRAILER CHECKLIST

	_	K.E.	K. W. K. K.	, , , , , , , , , , , , , , , , , , ,			
	1	Tuesday	Wednesday	Thursday	Thursday	Saturday	Sunday
Date	12-14-15	2-2-81	C1-11-121		1		
Time	11:05	10:55	11:00				
Slindra hlanket heirtht († of Sliidge)	ý		1				
		l r					
5 min settleometer	220	640	640				
10 min settleometer	540	500	490				
15 min setileometer	4. 7	044	430				1
20 min settleometer	430	400	390				
25 min settleometer	390	370	360				
30 min settleometer	360	350	340				
Madnetite.Feed	and Kara	and a state of the second s					
		//	~ ~ ~				
Green Light: ON	1	~	7				
Weight Ib	1172	2487	1173				
<b>Air Drýér</b> , ar sá sata a strait di késet é sa staráita.	alitati Xarata		starting and start a sta				
	~ ~	~~	7				
Green Light: ON	7	7	7				
Pressurized gauge reading (>80 psi)	110	110	115				
Mag Drum : set of the set of the set of the set		and the second					
	ζ,	11	V /	-			
No sludge build up (if wiper is on)	$\checkmark$	$\overline{\mathbf{A}}$	<u>\</u>				
Kadv Milk Terrare							•
	18	27	14				
Oil is clear	MIKV	PU KV	MILKV				
Amos	31/	31'	 M				
Speed (Hz)	38	38	, n N				

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1. 19**00** - 1. 1. 1.

Discharge Water flowrate (gDm)	50 0	1,0	1,3	
Mixing water flowrate (gpm)	0AF	0.7	1, 2	
Polymer pump speed knob (0-999)	с Но	677	702	
Running position (H/O/A)	off	Ĥ	ţ,	
Discharge Pressure <30 psi (or adjust water valve down)	JJa	5	37	
Drum Liquid Height (inches)	37"	23."	*0E	
	0 AU	(NO	NO	
DDM Mixer: ON/OFF (also check breaker (MX3))	(VV)	0N	02	
Mix Tank Agitator: ON/OFF	ON	ØN	04)	
Wasting Pump: ON/OFF	ON	60	NO	
RAS Feed Pump: ON/OFF	on	00	20	
WAS Discharge Pump: ON/OFF	0N	ON	01	
Mag Drum: ON/OFF	ON	ON	NO NO	
Kady Mill: ON/OFF	NQ	0N	0~	
RAS Discharge Pump: ON/OFF (also check	,, ···			
breaker (RDP 1))	ew *:	22		
Stinger Power: UN/UFF	<u>cv</u>	22		
Air Compressor (1999) and the second s		and the second		
	$\wedge$	/ /	>	
Green Light lit	· ·	>	>	
Pressure <100 psi	1/5	125	120	
Rain for Rent Pump topy of Property and the release	a the Article	and the second second		
Running		//		
Amps	//	//		
Hertz	>			
Notes and a second s	~			
Alarms?	1) /A	$\Delta I / \Delta$	× / / ×	
Tripped Breakers?	. chat	1/1		

Cell 1	12/14/15	12/11/15 12/12/12/12/12	"12/14/15"
DO (mg/L)	0.4	6.4	0,4
Hq	6.9	6.9	2.0
ORP	-114.2	-105,9	52,7
Temperature C	1515	15.3	14.9
	0.9	0,7	//0
Hd	513	6,8	6.8
ORP	-142.7	1.124.6	-124.8
Temperature C	1516	15,3	15.0
Cell 3 agreed and the structure of the s			
DO (mg/L)	1.7	1.9	2,0
Hd	612	6.6	6eT
ORP	-115.2	-137,1	20.5
Temperature C	15,6	15,4	/ <i>5</i> ,/

		-3					
i Participanti andreanti andreanti andreanti andreanti andreanti andreanti andreanti andreanti andreanti andrea	K.W.	K, W,	K, W, K, W, Trischaul Wednacdaul	Thursday	K, W. Fridav	Saturday	€. Sundav
		12-8-15	12-9-15	12-10-15	12-11-15	12-12-15	12-13-15
Time	11:15	11:05	11:15	1:00	11:20	8:50	5.00
Sludge blanket height (ft of Sludge)		ž	1	<b>`</b> &			¢,
		· · · · · · · · · · · · · · · · · · ·					
5 min settleometer	800	800	860	820	650		880
10 min settleometer	650	650	680	1090	500		770
15 min setlleometer	5.50	570	580	590	450		650
20 min settleometer	500	500	520	520	400		580
25 min settleometer	450	450	480	480	360		540
30 min settleometer	. 420	350	440	440	350		270
Magnetite Feed States and the states		and the second second	Star Land				
120 V: ON	~ ~			2	/>	>	2
Green Light: ON	~	~	>	/	í/	7	>
Weight Ib	1595	177	2559	2005	1531	1238	الكلاا
Air Diversity of the second							
			1	A	~		N /
Green Light: ON	>	ر ا	i	~	$\sim$	7	>
Pressurized gauge reading (>80 psi)	115	120	105	110	105	// 8	115
Mag.Drum with a state of the st							
Rotating		11	1/	1	~ ~	7	>
No sludge build up (if wiper is on)		2	/	>	>	Ż	>
Kadv Million and the second state of the secon							
Flowrate (gpm)	16	61	22	19	20	21	183
Oil is clear	MIKU	21	2 f	ii.	MILKY	MilKY	milky
Amps	3/	Зİ	32	Э <u>(</u>	3/ (	32	
Speed (Hz)	38	38	i		38	38	3S
Flow Totalizer (gallons)	7611762	7635796	7663154	7692589	7718179		776361

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Mixing water flowrate (gpm)       .         Polymer pump speed knob (0-999)       .         Running position (H/O/A)       .         Running position (H/O/A)       .         Discharge Pressure <30 psi (or adjust water valve down)       .         Discharge Pressure <30 psi (or adjust water valve down)       .         Drum Liquid Height (inches)       .         System Control Light: ON/OFF       .         System Control Light: ON/OFF       .         Mix Tank Agitator: ON/OFF       .		• 8				5
A)         A)         A           A)         A)         A           A)         Bit (or adjust water valve         A           Pies)         A         A           NOFF         A         A           N/OFF         A         A           DFF         O/         A	= # m [e]				1	щo
A) H PSi (or adjust water valve 77 hes) A8 N/OFF A33) CA OFF 04	# m #	67	5 130-	1	{	ci j
psi (or adjust water valve	m <sup>E</sup>	- <i>t+</i> -	0	þ	0	0 HO
hes) 28 N/OFF / o check breaker (MX3)) C/		11		1	ţ	JJ.
N/OFF V/OFF		2 2 2 2 2	34"	11	344	, ne
N/OFF o check breaker (MX3)) DFF					1207	
·	~	· / /			~	>
	ON	NS NS	20	NO	020	
	οŇ	S	00	20	02	\ \ 
Wasting Pump: ON/OFF	00	NO	NO	DN	NO	>
RAS Feed Pump: ON/OFF	0N	0N	NO	00	NO	>
p: ON/OFF	8 N	EN	NO	NON	01	<u>\</u>
Mag Drum: ON/OFF	00	00	00/	No	21	<u>`</u>
Kady Mill: ON/OFF	08	DN	DN	Ne	NO	$^{\prime}$
RAS Discharge Pump: ON/OFF (also check OV)	DA)	047	Ael .	0N	NO	<i>\</i>
Stinger Power: ON/OFF	NO	00	001	0N	NO	
Air compressor when the second s						
Test Blow Down						
Green Light lit				>		7
Pressure <100 psi $/\mathcal{ZO}$	110	115	120	120	115	105
Rain for Rent Pump						
Running V/	\/ 	//	]			
Amps	//			1/		
Hertz			~	Ń	/	2
		1/1	01/0	1/12	0///	
Tripped Breakers? / / / / / /	N/11-	11/11	10/2	1/N	16/11	

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Bioreactor Cell 1	12/1/5	12/15	12/9/15	12/10/15	1/1/2		13/15/15
DO (mg/L)	0,2	0.3	0,3	0.3	0,3	0.9	0.42
рн	6.9	2:0	7,0	6.9	6.9	6.8	6.79
ORP	-146,5	0'62-	29.8	- 145.6	-123.5	290.5	-67.9
Temperature C	15,5	124	15:2	15.3	15.5	15:0	16.0
Cell 2							
DO (mg/L)	1,5	1.1	0.5	1.6	1:8	1.2	1,37
pH	6.7	6.8	6.8	8.9	6.7	ورو	6.70
ORP	-98,3	5'72-	270.9	-141.0	1.28.1-	-/3,3	-40

DO (mg/L)	l'm	2,5	1.7	1. 1. 1.	4,1	39	5,4 ब
pH	6:7	6.7	6.7	6.7	6.6	6.6	6.64
ORP	-/02,3	14. is	71.6	- 26.1	-108,5	72.1	- 68.0
Temperature C	125	, Y, Y,	2	10 1	1 22 1	くく	15 0

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Temperature C

mt (ft.of. Sludge)		.K.w, Theday St	Х. Э.		_	5	ν, V
<b>je blanket he</b> eter reading o settleometer n settleomete		Tuesday (1)	<b>7. 8</b> 0 22 22 24 24		_		
je blanket hel leter reading ( settleometer n settleomete			Wednesday		Friday 🔄	Saturday	Sunday
<b>je blanket height (ft of Sludge)</b> eter reading on MLSS cell 3 settleometer n settleometer	<u></u>	12-1-15	12-2-151	12-3-15	12-4-15	12-5-15	12-6-15
<b>je blanket height (ft of Sludge)</b> leter reading on MLSS cell 3 settleometer n settleometer		11:15	02:11	11:00	11:20	8	5.00
TSS meter reading on MLSS cell 3 5 min settleometer 10 min settleometer			E Stores		\$ 19 St 8 St 1	8.8	
					·		
	0	800	780	790	650	650	S.
	0	680	020	690	600	740	<u> %00</u>
15 min setleometer	550	530	550	500	540	690	720
	00	520	490	450	470	(KC)	0740
	410	984	430	430	440	550	570
	420	450	400	400	400	490	1 536
			· · //	1	>	×	<u>}</u>
Green Light: ON		$\sim$	Ņ	>	7	>	
	3024	1475	1089	1762	135	7522	11.0
			「「「「「「「「」」」」				
						$V_{\prime}$	$\overline{\langle}$
SWILL: UN				~	>	<u> </u>	>
ge reading (>80 psi)	115	110	115	105	110	211	110
		11	1		>	>	
No studge build up (if wiper is on)			1	>	>	>	-
				· "我 一次会社 年後			
l `	<u>%</u>	, <i>5</i> ,	15	17	17	۲. ۲	ه. <del>د</del> ا
	لا	12	21			~	
	0.0 31400	m		η	- 6	31.5	، آ <sup>ي</sup>
(Hz)	38.0 HZ	38 HZ	38 42	_	2 X 4		i
izer (gailons)	14 2046	×44 ×44 747 4302		17521004	2119461	_	21125125E

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Discharge water flowfate (gpm)	デ ン	1,5	11	11	₹£	AN 1.6	<u>۲</u>
	1-0	1.1	11	11	21	1,0	, , ,
(666-0	12 %	677	11	11	11	477	iu 7-7
	/	Hend	Hanl	Hand	Hank	Mand	hund
Discharge Pressure <30 psi (or adjust water valve down)	>	0 M	0 m	0 M	30	30	30
n Liquīd Height (inches)	ř 29."	28''	28"	38 "	28"	`۲۴'	ي م
Controls							
System Control Light: ON/OFF	>	$\overline{\ }$			N		>
DDM Mixer: ON/OFF (also check breaker (MX3))	>	NO	ÓN	DN	au	25	00
Mix Tank Agitator: ON/OFF	>	62	00	00	00	c o	Й
Wasting Pump: ON/OFF	~	00	CN	NO	ŝ	¢,	\$
RAS Feed Pump: ON/OFF	>	62	υN	20	0N N	ر م	ΨC
WAS Discharge Pump: ON/OFF	>	0N	02	20	00	00	00
Mag Drum: ON/OFF	7	20	60	20	0 8	01	5
Kady Mill: ON/OFF	0-5-6	00	02	0N	96 S	\$	00
RAS Discharge Pump: ON/OFF (also check breaker (RDP 1))	>	QN)	20	0×	ΰŇ	Ve	00
Stinger Power: ON/OFF	Ā	02	02	01	0N N	SG -	02
Alt Compressor							
Test Blow Down	2	ν,	<, <	/ /	۲ ۲	/>	> ) 
Green Light lit	~			>	$\mathbf{\mathcal{T}}$	۲.	× 
Pressure <100 psi	011 /	120	021	011	125		
Rain for Rent Pump			* Scrylech	. K Surgiced			
Running	~	Υ.	>	<i>``</i> >	<u>``</u>	<u> </u>	>
Amps	2	/	1/	V/	11	\ \	~~
Hertz	د	Λ.	$\overline{}$	>	>	>	>
Notes							
Alarms?	<u>N NA</u>	A1/A	A//A	1 1/0	×1 /0	NIA	A1.
Tripped Breakers?	NM N	1.1.1	11/11	41101	1/1/	v t al	2

a/c	0.4%	6.54	1 22.5		2.62	4.43	1.57-	15.5				-17.1-	15 51	5.5
12/5	O. Ý	6.90	16.3			6.75	2.321-	15, 7				0 74	1 4 7	15.7
1. Alexandre 1. Al	0.4	6.82	-51.4 1555		ر م	6.73	- 153,8	1		6 C	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	0.20	۰ I	15,5
12/3 12/3	0,4	6:94	-126.3 15.9		1.43	6.78	-14% 8	1. 1			1997	- 119.5	16,0	16.0
2/12	10°4	2-	-97,2		0.9	6.74	-113,9	1506		2.13	$u \sim$	6.76-	15.1	7 9
1/2/	0,3	6.97	-18.1 15.6		1,65	6.79	-88.9	K576		2.76	6,65	- 73,7	15.7	1.01
	0.2	ر. در ا	14.1		13.7	1 (1)	C1 581-	15.7		1   So 1		100.3	15.7	
Bioreactor Cell 1									Cell3					
Bioreactor Cell 1	DO (mg/L)	PH	perature C	cell 2	DO (mg/L)	pH	ORP	Temperature C	celt3	DO (mg/L)	рН	ORP	Temperature C	
		<u></u> L`	-121	ಿಷ್		<u></u>	<u>.~1</u>	<u></u> -	ي <b>ې</b> يد:				<b> </b>	1

特許 とうかがた 変化 たいかくちかい たいけいしょう イント・バント しょうけい しゅうけん しょうしん しゅうしゅう しゅうしゅう しゅうしん しゅうしゅう しゅうしゅう かいせい かいしょう		いたのためというないというない			第二日 日本 日本 日本 日本 日本		「「「「「「「「「「」」」」」」
D0 (mg/L)	ŝ	2,76	2,63	1,0 1,0 1,0	5.4	3.01	2.1.1
Hd	RC.	6.65	61.2	6.66	2.2		(, C)
ORP	100.3	- 73,7	6'96-	-119,5	27.2	0 74-1	-1.2.3-
Temperature C	15.7	15.7	15.2	16,0	12.5	1 4. 7	15 51
	-						
	-						
	•						
				L			

ŀ	、、、、、、、、、、、 、、Friday、「、Saturday、「	11-27-15 11-26-15 11	5:00 5:00 5:00				\$10 \$10	39¢ 730 740 750	660 650	590 620	320 550 570			1951 1201 1205 1195	「たたい」の準備やなどを続けるなどのです。ためでは、おけ									11	31.5 31.5 31.5	35	236 564 73656 13656
	K, W, S.S.	11-25-15	11-26-15		······································	550	460	410	380	350	330			1883					120				13	•	31	38	1
	K, w. Tuesday	11-24-15	11:15			530	430	370	350	310	300		,\ 	1869				>	- 110		$\overline{)}$	>	<u>н</u>	11	m	38	2011000
	$\langle \chi,\omega_{i} \rangle$	11123	11:45			520	410	360	055	310	. 300		, , , , ,	2762			> -		1115				30	MIIKU	- / Y	200	
•				Strates Mankat heidett (If of Sludge)	Trss mater reading on MLSS cell 3		10 min settleometer	15 min catlanmater	10 min cottleometer	25 min settleometer	30 min settleometer		120 V: ON	Green ugn:: UN Weight Ib		All Dryet was the second se	Switch: ON	Green Light: ON	Pressurized gauge reading (>80 psi)	Mac Delum second se	Rotating	No sludge build up (if wiper is on)	Nady Will grave of some second and a second s			Suead (H2)	

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Bioreactor							
Cell f	Novi	ta	~~X	Thurs	Ľ,	44	27 2
DO (mg/L)	0.4	0,4	0,3	0.39	5-0 0	0,53	0,56
PH	6.9	6,9	7:0	5	6.9	C-22	6.96
ORP	101.9	89,9	133,4	-167.4	-120.6	1	-103 0
Temperature C	15,6	15.4	15:7	1°.1	16.3		15.5
Cell 2							
DO (mg/L)	0,9	1,2	1.6	91 · 5		1.55	1,47
pH	6.7	6.7	6.8	\$	6.7	C-7 I	6.75
ORP	73.3	70,6	3.0	-68.3	- 71. 2	-131.2	- 27. 9
l'emperature C	1516	15,5	15,8	к. 3 1	16.4	lí. 3	11-

uu (mg/ L)	19	4	ry m	рл Г.	3.09	4 26	S AG
На	6,6	6.6	la b	3	0.0	1,4	
ORP	- 7.9	145.2	1 23 -		1/2 4		۲ م م م
Temperature C	15,7	15.5	1.5.8		لر. بر ازر. بر	1 - 1 1 1 1	- 11
					,		
	· .						
							-

		51 -171		11-19-15		24 - 2 - 1 2 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2	11-20-15
	ノニシン				1		
	C/01/1	05.C	11:15	00:11	$1 \sim$	3.40	
Shint and Monthly H. M. Shint and							
TEC	1 S						
נייין בייון בפתוונג חון ואראא רבוו א	120	160		- (m)			ų Į
5 min settieometer		770	4/8 5/0	650	500	100	84C
10 min settleometer	26.0	390	360410	450	420	630	40 ¢
15 min setlleometer	220	350	340.300	400	350	Ste	610
20 min settleometer	1 2,00	088	340	360	330	495	540
25 min settleometer	280	000	3/0	350	310	0 <b>h</b> h	005
30 min settleometer	120	280	300	320	300	2 7	03h
Magnetite Feed		- NA					
	2			<u> </u>	1	>	$\geq$
Green Light: ON	2					Ń	
Weight Ib	1097	2955	1687	1230	1123	1040	1095
Alf Dryer		「日本のない」の言語では、					
Switch: ON		1	1	7.			>
Green Light: ON		~	<u> </u>	$\overline{V}$	~	V –	
Pressurized gauge reading (>80 psi)	2	1	100	100	105	105	130
Nag Drum and the second second second second							
Rotating	7	5	V .	1/	~~	¥	>
No sludge build up (if wiper is on)	2			Ś	>	>	>
Kady Mill	の時代のためのないである。						
Flowrate (gpm)	12	14	14	15	14	2000 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	13.8
Oil is clear	MI/Ky	Milke	$\wedge \chi (H)$	MILKU	MILKY	<i>Cleudy</i>	Clevely
Amps	/		31 '		3/ ′	_ ≫1≁	31.5
Speed (Hz)			3842	l '	SE	\$\$	38
Flow Totalizer (gallons)	H132481	シバンしい	7174913	7194860	7215062	7232666	12252766

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Polymer Feed Pump				18			
הוארומוצב אמרבו ווסאומרב (צחווו)			1. 	044	0 4 1	22	C 7 7 2 A
iviixing water flowrate (gpm)		-	o 本	of t	0 1 U	5	450
Polymer pump speed knob (0-999)			0 79	0 <del>11</del>	0 1 1 0	(f.	110
Running position (H/O/A)			L off	0.ft	5f0	ur K	900
Discharge Pressure <30 psi (or adjust water valve down)			d da	He .	4	纺	4 Z
Drum Liquid Height (inches)	29"	39"	39"	165	294	i Be	29.1
Controls							
System Control Light: ON/OFF	7	7	20	N0	NO NO	>	
DDM Mixer: ON/OFF (also check breaker (MX3))	2	7	NO	NO	NG	>	
Mix Tank Agitator: ON/OFF	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	2	00	00	00	Ń	
Wasting Pump: ON/OFF		~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	(10)	50	00	Ń	
RAS Feed Pump: ON/OFF	2	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	00	en.	00	2	
WAS Discharge Pump: ON/OFF	$\overline{\ }$	1	00	20	NO		>
Mag Drum: ON/OFF	2	//	20	~ 0	00	>	, , ,
Kady Mill: ON/OFF	2	2	50 20	20	20		>
RAS Discharge Pump: ON/OFF (also check breaker (RDP 1))	>	~	0m	20	NO		>
Stinger Power: ON/OFF	2		on	ØN	00	>	
Air.Compressor							2011年1月1日日本部に1911年1月1日日本部に1911年1月1日日本部に1911日日本部に1911日本第二月10日本第二月11月11日本第二月11月11日本第二月11月11月11月1月11月1月1月1月1月1月1月1月1月1月1月1月1
Test Blow Down	7	1		, ,	\ \	>	>
Green Light lit	2	1	· / /			×	
Pressure <100 psi	7			120	125	\$	100
Rain for, Rent Pump							になった。「「「「「「「「「」」」」」
Running	5	5	//	11	056	~	
Amps			//	//	Being		
Hertz			/		Scruced	~	
Notes :							
Alarmsr	2		NZA	A/N	6/N	Q V	2,
Tripped Breakers?	١	>	×/م م	N/A	1/4	e va	م ج

Ŧ								
Bioreactor Cell 1								
DO (mg/L)	0.4	10	کرہ	0,4	7	\$ }	0.33	
pH	6.0	(0.9	6.9	7.0	0	6.7	5.85	
ORP	- 110.6	- (04.0	- 21.8	0 001-	2/. X		- 155 -	
Temperature C	(7.3		1617	16.8	17.0	- C - O	16.5	
Cell2								
DO (mg/L)	.4		1, 4	1. 2				
pH	6.7	5,2	6, 8	1. K	5,7	e «	۵ ۲ ۵	
ORP	-75.3	-23.(.)	-36, 5	-124.4	-184.8	-53.6	1 1 1	
Temperature C	17.3	11.9	16.3	17.0	17:0	۲. ع		
	an sana basar ya in ta taka wang							
DO (mg/L)	ی ک	b't	2.7	2	4,3	8 1 2 2	× 11	
pH	6.6	6.6	6.7	1				
					6.3	<b>小</b> 海	د.2	

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**Temperature C** 

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) U Monday Date ///-9-/5		Tuesday         Wednesday         Thursday         Friday         Saturday           1:00pm         11/13         11/13         11/14           1:000         11/13         11/14         8:00 A.M.	y Thursday	Friday 11/13 1/2M	Saturday 11/14 8:00 A.M	Sunday N/\S Stop & M
Strate hanket heidhf (H of Shudde)			20			
TSS meter reading on MLSS cell 3			×	X		4 1
5 min settleometer	400		926	390	035	8
10 min settleometer	1 310		330	3/0	350	
15 min setlleometer	280		296	280	8 M	0
20 min settleometer	žč Š	-	260		120	
25 min settieometer	07 C		228	240	0	2 4 4 C 4 4
30 min settleometer	240		350	120	2	× 
			>		>	, ,
Green Light: ON			>		ž>	>,
Weight Ib	1,097141	10 85	0500	1955		224
			~		2	>
Green Light: ON		~	>		>	- and
Pressurized gauge reading (>80 psi)	100 ps 1	100051	100651	20,251	100 101	10¢ 5%
					「おん」というないないないで、ないない	
Rotating		7	>		>;	>
No sludge build up (if wiper is on)	7	<u> </u>			<i>3</i>	2
Kady Million and a second s			行いていたので、			
Flowrate (gpm)	19.25pm	18.4	4	13.0	»[-	· · · · · · · · · · · · · · · · · · ·
Oil is clear	1	cloudy	Claudy	CLOUDY	C louchy	
Amps		31.0 '	31-4	32	_	M X
Speed (Hz)	38	38	38712	38 42		
Flow Totalizer (gallons)	6963546 (	6998666	6 LC 194	0 7866318	17583554	9 7185 553

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	<u>95" 29" 29" 29" 29"</u>	
Polymer Feed Pump Discharge Water flowrate (gpm) Mixing water flowrate (gpm) Polymer pump speed knob (0-999)	si (or adjust water valve es) <b>39</b> <sup>11</sup> <b>39</b> <sup>11</sup>	Rain for, Rent Pump Running Amps Hertz Notes Notes Tripped Breakers?

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Bioreactor Cell 1					
DO (mg/L)	0.7 0.3	<u>۲</u> ٥	0.4		24
þH	6.9 6.9	6.9	10.8	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	
ORP	0.101- 3.44.8 - 121.0	-12.4	-131.7		-56.0
Temperature C	0.81	17.5	17.4	1 1 1 1	0 C.
DO (mg/L)	0.7 11				
Hď	0.8	× ,		~ ~ ~ {	
ORP	242.9 -116.6		120 0	7	
Temperature C	281 6.61	17.6	17.50	13.3	
Cell3				日本に対応していた。	
D0 (mg/L)	<u>  3.1 1.5  </u>	6	17/	~~~	<b>•</b>
Hq	6.6 6.6				* * *
ORP	1.211 - 1.101 -	12.00-	- 112 6		3 2 1
Tamparatura					

1						
	<u>د.</u>	5	ñ	14	10 10 10 10	~ % `
PH	6.6	0.9		200	200	8
	1714-	- 118.1	12.01 -	- 119 6		
emperature C	/8.0	19.2	- 121-			۲ . ۴
					\$	× •• *
-						
	÷ *					
	-					
-						
				-		
			-			

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Sunday Sunday Sunday Sunday Si Si S
37.5 Saturday Stores St
K.W. J. R.W. J. K.W. J. K. J.
K, W,
K, W, Wednesday T, Wednesday T, Wednesday T, 11/1/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/15/11/11
6773 6 2 2 4 4 6 2 4 4 9 6 7 7 6 7 7 6 7 6 7 7 6 7 6 7 7 6 7 7 6 7 7 6 7 7 6 7 7 6 7 7 6 7 7 6 7 7 7 6 7 7 7 6 7 7 7 7 6 7
Monday 13-15 24 13-15 24 100 1-10 100 100 100
Date     111-2       Time     111-2       Fine settleometer     10-0       Sind ge blanket height (ft of Sludge)     3       Sin settleometer     10-0       Sin settleometer     10-0       Somin settleometer     100       Somin settleometer     100       Somin settleometer     100       Magnetitis Feed     Magnetitis (>80 psi)       Mag Drum     No       No sludge build up (if wiper is on)     10       No sludge build up (if wiper is on)     10       I is clear     Amps       Amps     Speed (Hz)       Flow Totalizer (gallons)     5peed (Hz)

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		S Y S Y	كردما	Thurs	Fri Sta	SAT	SUN
	-1-	1,7	0 89	550	940	95 C	
Ulscharge water How are level	Ð	1,2	e ff	440	tto t	AS C	040
MIXING Water HUW are (Sprin)	0 Ò	0	off	090	055	173	37.5
Polynier partic speed with the set	530	Hand	s F	f f	0#+	440	
Discharge Pressure <30 psi {or adjust water valve		+ F	77	Jira	d र र	550	A de
		20		:00	.≈ • 0 • 0		م <sup>د</sup>
Liquid Height (inches)	297	29	27	- / 20	16		
	and the second second second						
	1.1				0 45		
System Control Light: ON/OFF	20	Nor >	No -	220	2.2	>	>
DDM Mixer: ON/OFF (also check breaker (MX3))	GN	N0/ 2	2				>
Mix Tank Agitator: ON/OFF	ક	10×	<u>o</u> v	NO V	2 3 0		<u> </u>
Wasting Pump: ON/OFF	on l	V.0V	0~	0%	~~~		
RAS Feed Pump; ON/OFF	CN	100	ON	× ×	000		
WAS Discharge Pump: ON/OFF	SC	00	SN SN	2	22	_ _ _	
Mad Drim: DN/OFF	20	0N	0N	e N	62	,   	
Kadv Mill: ON/OFF	No	90	NO	NO	3		
RAS Discharge Pump: ON/OFF (also check	GN	61	DN	80	RO	>	>
breaker (RDP 1))	(YO	0N	0 NO	NO	NO		>
Stinger Power: UN/Urr	)					•	- - - - -
1	Terstad	Υ,	/	>	× > -+		
Green Light lit	۲	>	>	>	)   		120
Pressure <100 psi	125	115	02/	120	2		
Kain tor Kent Pump and Automatication and	>				>	>	
Kunning	1623	165	167	167	7/		
Amps Hertz	(00HC	60 HZ	2H 09	10 42	60 HZ		
Notes: Provide the second s				0/1	1 20	0.4	<u>av</u>
Alarms?		22	202	× 0/2	NO	ŝ	1 A. A
Tripped Breakers?	20	NC					

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Bioreactor Call A	Won	27	لمعم	ĴŅÚ	Et.	Set	s.m
DO (mg/L)	0.4	, o	0,2	0,2	1 o . K	د د ۲	0.34
μų	6.0]	6.8	6.9	6, 8	6,8	6.8	7.06
ORP	101	-219.5	-147,7	-126.7	1/1/-	-140.3	- 95.7
Temperature C	18.3	18,2	18,3	18.0	18,6	1.S. I	15.4
Cell 2							
DO (mg/l)	04	0.9	0.7	0,4	01	0 0 2	0.74
На	L. 8	6.7	6.7	6,7	6.7	<u>6.57</u>	6.67
ORP	くっわー	-295.9	-116.1	-129,1	-131,1	-141. 2	- 126.7
Temperature C	18.4	18,3	18,3	18,0	1806	15.7	٤, ک
Cell 3 March 19 March							
DO (mg/L)	4	2.8	1.8	0.9	2.0		3.57
pH	L.7	6.6	616	616	6,6	e. 45	(z. 5 8
ORP	-133.8	-107.3	-89.2	-132,9	-104,5	-132. 8	ر ایک ط. ز
Temperature C	18.4	18,3	18.3	1221	18,6	15.7	19.7

	Р Т	K. W.	NN	X E	Х З	<b>۲</b> ,۲	<i>د</i> رز
	Monday	Tuesday	2	Thursday	Friday	Saturday	Sunday
	10/30	Te/01	86101	10129	10/30	101.31	22 8 8
Time	8:20	11:10	10:05	11:10		ž: ò S	6:46
) Sludge blanket height (ff of Sludge)	<b>6 .</b> "	'n		, 2, 6		, <b>t</b>	
	×	×	×	×	×	×	.×
5 min settleometer	370	160	400	360	944	530	680
10 min settleometer	3 80	120	3/0	300	350	410	072
15 min setlleometer	260	110	280	260	310	360	470
20 min settleometer	240	100	250	340	290	320	430
25 min settleometer	2 20	100	042	042	270	300	340
30 min settleometer	220	100	230	OFE	250	350	340
Maghétte Feed ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) (							
	2		×	17	12	>	>
Green Light: ON	7	det o	X	>	>	>	~
Weight Ib	1092	off	0201	2088	1140	101	1108
Är Örjersen helten des en de staat de se							
Switch: ON	>		2	12	<i>'</i> , <i>'</i> ,	>	)
Green Light: ON	>	>	7	>	~	/	<u> </u>
Pressurized gauge reading (>80 psi)	180	120	115	115	120	180	105
<b>ฟิสต์ มีที่มีท</b> างคราม และสี่มีคราม เป็นสู่สั		an a		an de service de la constante d La constante de la constante de	an an Annaichean Annaichean an Annaichean A	an an an an an an Angles. An an	and a second
Rotating		1,	×	< ^ >	//	~	\ \
No sludge build up (if wiper is on)	7	~	×	7	>		>
			a tanàn ang ana dia di				
Flowrate (gpm)	19.4	0	X	HJ5 81	19 GPH	0	0
Dil is clear	A Public Card	cloadu	cloudy		Ĵ	Cleandry	Claudy
Amps	V. 0 V	, 0	X	31		0	0
speed (Hz)	76.9	37,5	×	38	38	376	328
-low Totalizer (gallons)	65656901	HHH1019	1020 Hdd	JL WEEL ?	67313	6734938	1 -6 734 45 Q
				1202 1-12 SO 7(		58	و
Flowrate (gpm) Oil is clear Amps Speed (Hz) Flow Totalizer (gallons)		cleady 2718 6701444	270 tr XX		14 90 23 1 31 ( ( )		60 336 67393

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Polymer Feed Pump						DD DD	14.
Discharge Water flowrate (gpm)		+	>	200 Q	100	3	+ t-t
Mixing water flowrate (gpm)	A C	ŧξ	< >	100	DEC	et.	. PP
Polymer pump speed knob (0-999)	C X C	014	() ()	20-	250	-140	4
Running position (H/O/A)	1 10	++0	<		Z1 1		
Discharge Pressure <30 psi (or adjust water valve	ð	9 27 0	×	offe	off	044	44
down) Denem   Ionuid Height (inches)	33	" OF	30 "	30 "	30,'	304	3o"
חומוו הואמות וובופור לוויגיובה)				and the second secon			
Controls							
System Control Light: ON/OFF	>		7	>	>	>	>
DDM Mixer: ON/OFF (also check breaker (MX3))	~ .	<u> </u>	7	>		>\`	>\`
Miv Tank Agitator: ON/OFF		>	7	, , ,		>	<b>`</b>
Wasting Pump: ON/OFF		949	X		>	>	7;
PAS Food Dumn. ON/OFF	>	ON,	2	`>	>	>	> \`
WAS Discharge Dump: ON/OFF	330	450	×	./	>	>	>`
Mag Drim - ON/OFF	40		×	>	>	>	
Kody Mill- ON/DEF	50	540	X	offo	Z	Stopped	Stappe 4
RAS Discharge Pump: ON/OFF (also check	4	· / ·	>	>	>	>	>
breaker (RDP 1)) Seinonna Dowarn ON (OFF	120	75-0 V 5-0	×			>	7
Stillger Fower, Stry OL							
Air compressor and the second s							
Test Blow Down	· · ·		7		>		>>
Green Light fit	>		7	>	>	>	
Pressure <100 psi	WS PS!	115	110	115	110	125	ater
	>		>	Servicz	et o	>	<u> </u>
Amos	N(0) &	160	100	515125	120	120.4	167
Hertz	2	ZH 09	09)	55 54/66	0 + +	0 2	60
		Nove	NA	N/A	NIA	N/A	N/A
Alartitis ? Trinned Breakers?		ΙŻ	NA	N/A	NIA	N/A	N/A
			•••				

Bioreactor Cell 1	0/2C	10/27	10 LS	10/39	10/30	10/31	mhhs
DO (mg/L)	0.1	0.3	0,2	0,4	0,5	0.36	0.42
PH	(o. f	7.0	ч. л	6.8	6.9	6.84	4.81
ORP	- 277.8	-128.7	186-	-129.6	189,3	- 139	~ 113.7
Temperature C	185	18:1	18.2	18.6	18,0	17. 9	18:0
		20	0	1 ; 7	0 (	1 2 6	-
	70		۸ -		<u> </u>		
рН	le.8	6.9	67	6.6	6,6	6.62	6. 61
ORP	- 108.9	1 401-	うねで!	-134,5	-126,1	- \$9.7	- 102-9
Temperature C	19.5	181	1.81	18.6	131	1.8.1	1.2.1
Cell 3 States of the second							
DO (mg/L)	0:1	4,6	ы 19 19	M, V	رو م	3.81	3. 72

\$ 341 -(و. 5 ۲ ا ک<sup>ر</sup> کام ا 6-56 -137.6 16,1 -104,4 18,2 Ŋ -124,6 18.7 5 0.0 140 ĝ ۱ -139. 6.8 18 2.18-18.U 5.3 pH ORP Temperature C

Jake Sunday (0/25 0.75	2380 2380 2380 2380 2380 2380	7701	V V V leudy Cloudy 30.9 30.49 66216366476018
The ke Saturday (0/24	3000 2000 2000 2000 2000	776177	
Rene Friday 0.5	2260 2260 2200 2200 2200		2 10 10 10 10 10 10 10 10 10 10 10 10 10
K, W, Thursday 10/28	330 330 320 320 320 190	5/1	1- 0- 0- 0- 0- 0- 0- 0- 0- 0- 0- 0- 0- 0-
K.W. Wednesday 10 240	330 330 330 230 230 230 230 230 230 230		30 30
K, W, Tuesday 10 /30	270 270 270 270 270 270	1085	30 31
	3200 3200 310	2010 2010 2010 2010 2010 2010 2010 2010	>> 6> 20 E
	Sludge blanket height (ft of Sludge) TSS meter reading on MLSS cell 3 5 min settleometer 10 min settleometer 20 min settleometer 25 min settleometer	30 min settleometer Magnetite Feed 120 V: ON Green Light: ON Weight Ib Weight Ib Switch: ON Green Light: ON Dressurized gauge reading (>80 psi)	

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Polymer Feed Pump Toward Structure Control of the	OFF	OFF	<del>dto</del>	<del></del>	off.	off	00 CC
Discharge Water flowrate (gpm)	×	8	8	8	×	×	
Mixing water flowrate (gpm)	×	۶	7	8	×	< >	<, ''
Polymer pump speed knob (0-999)	×	*	7	~	×	< >	< ×
Running position (H/O/A)	×	×	7	×	×	< (	(
Discharge Pressure <30 psi {or adjust water valve							
down)	×	×	ž	X	×	×	×
Drum Liquid Height (inches)	×	×	X	X	30"	30 "	30″
Controls to the state of a strengthene to the state of the							
System Control Light: ON/OFF	7	, , ,				7	<u> </u>
DDM Mixer: ON/OFF (also check breaker (MX3))	7	~	\` \`		2	7	
Mix Tank Agitator: ON/OFF	7	/	Υ.		2	7	7
Wasting Pump: ON/OFF	7	>	~		>	2	7
KAS Feed Pump: ON/OFF	۲	>	>	``	7	>	7
WAS Discharge Pump: ON/OFF	7	>	)		2	7	7
Mag Drum: ON/OFF	7	>	, ,	>	>	2	7
Kady Mill: ON/OFF	7	>	>	<u> </u>	7	7	2
KAS UISCHARGE PUMp: ON/OFF (ziso check breaker (RDP 1))	7	>	>		7	7	
Stinger Power: ON/OFF	7		>	Ń	7	7	. 7
Air Compressor							
Test Blow Down	7		<u> </u>		>		
Green Light lit	>		>		>		
Pressure <100 psi	001	130	110	110	115	110	011
Rain for Rent Pump							
Running	7						
Amps	83	97	79	137	1100	100	ja A
Hertz	40	ЪЧ	45	55	60	60	60
Notes		· · · ·					
Alarms?	none	NONE	NONE	JONE	NONE	1000	0 VOV
Tripped Breakers?	DONE	NONE	Nove	NONE	None	Neve	NOV

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Bioreactór (					Kene		
cell 1 states and state	mon	Tucs	ww	Thurs	7	SAT	542 542
DO (mg/l)	0.2	0.5	5.0	0.2	0.35	o. Å	0.38
pH	ه. 8	6. k	6.9	6,8	6.9	7.5	ר, יי
ORP	- 164	-125.4	61911-	-190.8	- 142.8	1 0 0	-80
Temperature C	18.4	18.9	2061	19,3	19.0	16.1	18.3
		-					
DO (mg/L)	1.4	1.7	0.9	0.6	0.62	o 1 ]	1.
pH	و و	6.5	6.7	6.7	6.0	7.5	7.43
ORP	047-	213612	- 116.0	-306,9	- 134.4	۔ <del>م</del> ک	1 40
Temperature C	18.5	18.9	18.1	19.2	19.0	2.11	18.4
Cell 3 - Province - Pr							
DO (mg/l)	3, (	3.7	1.4	1,0	0.83	Ľ,	724
pH	و، لا	6.7	616	6.6	6.5	7.5	7,43
ORP	- 174	-87.2	- 166.7	-174,9	-129.6	-70	99-
Temperature C	18.5	18.9	19.2	19,3	19.0	87	18.5

			K.w.	K, W,	K.W.		
	Monday	Triesday	Wednesday	Thursday	Friday	Saturday	Sunday
	(manala)		10/14/15	10/15/15	21/11/21		
Time			10:450	5	11:05		
Sludge blanket height (ft of Sludge)			9'	.ع ر	1		
TSS meter reading on MLSS cell 3/2222/2402 )							
5 min settlaometer			520	450	390		
10 min settleometer			400	350	300		
15 min setlleometer			330	280	250		-
20 min settleometer			280	240	230		
25 min settleometer			240	310	200		
30 min settleometer			220	200	190		
	-						
Magnetite Feed							
120 V: ON			040	550	off		
Green Light: ON			off	o££	990		
Weight Ib			}				
Air Drver							
Switch: ON			, ,	>	>		
Green Light: ON			>	>	>	-	
Pressurized gauge reading (>80 psi)			130	118	115		
Mac Drum							
Rotating			>	>	>		
No sludge build up (if wiper is on)			>	>	>		
Kady Mill			,	(			
Flowrate (gpm)			38 504	<u> </u>	H& 63H		
Oil is clear				×,	> -		
Amps				0 50	0++		
Speed (Hz)			37 42	044	10++		

	WED.	TAKOS		
Flow Totalizer (galions)	6316445	(365821	6396917	
Polymer Feed Pump				-
Discharge Water flowrate (gpm)	¢ţţ	ەرر	0	
Mixing water flowrate (gpm)	\$ <del>1</del>	θf	• /	
Polymer pump speed knob (0-999)	999	999	<u> 999</u>	
Running position (H/O/A)	off	045	e ff	
Discharge Pressure <30 psi (or adjust water valve downi	Jt O	950	ų	
Drum Liquid Height (inches)	EMPAN	EMPY	30"	
		-		
Controls		1		
System Control Light: ON/OFF	<u>۲.</u>		·/·	
DDM Mixer: ON/OFF (also check breaker (MX3))		Z	, / /	
Mix Tank Agitator: ON/OFF	>	>	>	
Wasting Pump: ON/OFF		Ń		
RAS Feed Pump: ON/OFF	×	>	>	
WAS Discharge Pump: ON/OFF	< <u>``</u>		, , ,	
Mag Drum: ON/OFF	<u>&gt;</u>	>	>	
Kady Milt: ON/OFF		offo	>	
RAS Discharge Pump: ON/OFF (also check breaker (RDP 1))	<b>`</b>	ζ	<.	
Stinger Power: ON/OFF	<b>&gt;</b>	>	>	
Note any alarms:				
Note any tripped breakers:				
Rain for Rent Pump			~	an a
Running		$\geq$	>	
Amps	54,4	54.9	55	
Hertz	25.0	25.0	25	

			•	7.
			,	
	WED.		Thurs	Fri
Bioreactor				
Cell 1		-		
DO (mg/L)	0,1	0,2	r <b>r</b>	0.1
	6.8	_	<i>S</i> e	6,7
ORP	6-243.9	7 -17517	5:7	-71.9
Temperature C	19:9	[	<u>}</u>	19:5
Cell 2				
DO (mg/l)	<u>ک کے ا</u>		Ň	1.6
DH	6.6	6,6	-	6.7
ORP	L'1H1-	$\neg$	-144.3	-101.9
Temperature C	19.9	9 19,5		12,4
Cell 3				
DO (mg/L)	0.6		5.3	2.8
Ha	616		617	6.3
ORP	9+1-	}	فظرحم	-102,9
Termoaratture C	16.8		7,4	19,4

	K.W. Turk John		00.11	Kone / Todd	K.W.	Jak C	Jake	
· · ·	- Winday	Tuesday	Wednesday	Thursday	- 1	Saturday	Sunday	Monday
Date		10/6/15	10/1/15	10/8/15	10/9/15	toxio/is	10/11/02	10/12/15
Tìme	8:20	B: SDAR	9:35hm	8:32MM	8:2014	7:05AM	N835:7	M214:1
							ţ	
Sludge blanket height (ft of Sludge)	13, 21	10.	Bullfing	//	/3 ′	×,	+3. S.	<b>ح-0</b>
TSS meter reading on MLSS cell 3 (WEEKEND)			>			\$\$ 507 C	41.10	
5 min settleometer		900	010	960	940	930	430	920
10 min settleometer	520	030	088	900	8 >0	520	8	850
15 min setlleometer	430	750	920	950	830	830	630	- 06L
20 min settleometer	360	670	780	810	<u> 58 0</u>	750	740	700
25 min settleometer	320	600	ohl	770	740	640	246	Q .9
30 min settleometer	280	550	690	002.	630	240	200	520
Magnetite Feed					-			
120 V: ON	off	>	OFFIONE	7	7	¥	>	<i>,</i> ,
Green Light: ON	<del>JJ</del> Q	<	10000	7	$\geq$	>	2	2
Weight Ib	EMPYY	2657	1843	1092	2310	2		1087
				,				
Air Dryer	/							Ŋ
Switch: ON	ν,	>	>	2	>	>	7	•
Green Light: ON ~	7	>		7	>	>	7.	
Pressurized gauge reading (>80 psi)	11.5	2103 pst	7120	Z110 psz	15011	110 053	100	1 0 <b>1</b> 0 1
Rotating	\ \ \	>	>	7	/ /	>	>	2
No sludge build up (if wiper is on)	>	<u> </u>	>	>	>	>		7
Kady Mill		I	16		¢ . :			ند م ۲
Flowrate (gpm)	38 9.P. M.	20 3.P.M.	0 K 1	55:0	41.4	4.4 1		41. e
Oil is clear	>	>	LAN.	. X				
Amps	Ľ	30 AMPS		×11.14ml		36.1	49.3	0 4114
Speed (Hz)	37 42	38 #2		3842	37 HZ	36.9Hz	36.9	0 H E
Toth LizeR -	A425	290 339	590 5399 5923572 595	× 5958823	1116107	5 005, 25 7	6136339	62 <sup>1</sup> 109 <sub>6</sub>

	tucs ie/13							
Polymer Feed Pump			<b>6</b> 7			-		- -
Discharge Water flowrate (gpm)				~d6C./	1.7 904	51	551 <b>1</b> 55	1 0
MIXINg water riowrate (gpm)				wiec.	12/ 5/21	ן   	<i>1</i> ////	
Polymer pump speed knob (0-999)	824	$\checkmark$	1.21 1	a/ 2/	300	197	147	824
Running position (H/O/A)	off	$\langle$	W1/10~	14mD	Kann	Hand	Hancel	T
Discharge Pressure <30 psi (or adjust water valve down)	0	<		29	Ч	کلا	30	33
Drum Liquid Height (inches)	¢		××-	2612	×	8	7	ž.
Controls	1		,	1	,		-	
System Control Light: ON/OFF	<u> </u>	>	>	7	ν,	X		7
DDM Mixer: ON/OFF (also check breaker (MX3))	. >	>	>`	~	<u>``</u>	$\searrow$		7
Mix Tank Agitator: ON/OFF		>		>'	>	>		7
Wasting Pump: ON/OFF		>	0 FF	>	<u> </u>	2	~	OFF
RAS Feed Pump: ON/OFF	>	7	2	>	,  </td <td>server and the server ser</td> <td></td> <td>7,</td>	server and the server ser		7,
WAS Discharge Pump: ON/OFF	>	>	OFF		Υ.	N.	Ň	<b>`</b> .
Mag Drum: ON/OFF	>	>	7	、	<i>\</i> ,		7	7
Kady Mill: ON/OFF	>	2	OFF	>	<u>, , , , , , , , , , , , , , , , , , , </u>	~	7	054
RAS Discharge Pump: ON/OFF (also check headed and also check headed and a second and a second and a second and a second		>	>		$\overline{\ }$	~ /	2	7
Stinger Power: ON/OFF		>	055	320	00		2	>
	>			-		: · ·		
							*	
Note any alarms:								
Note any tripped breakers:						- - - -		
Rain for Rent Pump			/		、			
Running	>		UK L		$\overline{}$	>		7
	<b>در</b> ا	135 AMPS	XAVX	54.5AM	5 96.2 ANDS	VI hs	54. K.	<del>4</del> .4
	25	55 HERT2	D ml	25.0	45,0'	XS AX	as H2	25

•

•

	<b></b>	<b></b>	0.23	6.80	1		ŀ	[	0.89	6-87		69.3"	1		1.43	6.75	1	- 69.0°F	1	off						
· .			. 37	<u>ر</u> ، ط	4 42-5	19.85			ま	6-8	5.17.5	14 . A.V.	\$	ः २	. 26	6.7	+175	45 R 8	E		WAS. 0.95	WAS 0.56			WAS 0.63	
			. 33	¢. 4	365. q	X 0. 6			. 25	2	421-6	14.96			0. Jà	6.7	616.9	14.45	WAS. D.	2.85	O WA		WAS		WAS	
			0,5	6.9	- 1-941-	20,3			0,3	6.8	-154.0	20.3		-	0,3	6.5	-1>3.2	2013	RAS. 3.20	RAS. 0	1 43 1.86 KAS-2.60 M	<i>دا رتی کو</i> ر	A3 L <sup>a</sup> ua (NAS		45 3.25	
			0.2	6.9	- 147.2	19.4			2.0	6.0	-145.5	0.00			4.0	6.7	-133.5	20.1	A3.1.14	A3 1.43	31.86	13/18/ E	λ L <sup>44</sup>	A3 4. PSG	A31.60 RAS 3.25	
			0.50	6.0	- 144	- 19.6			0.4	6.7	127.9	19.9			4.3	6.0	-130.2	20.0	A2. 1.10	ົ	A.1.87 4	AZ 1.73 6	AN 1. 139 A	A1 1.0 5Y A	421.621	
			0.70	6.8					1.7	6.6					3.45	6.6			1. 1.40	1. 1.83	AI. 2.30 A	811.96 A		ני נאן	2.25	
K.W. Tues 10/2/15			0,2	613	-216	20.0			1.4	606	- 147.9	19.9			2,6	6.7	-108,3	19.9	×	4	A	9 <del>5</del> 9	4 I	Al	<i>H</i> 2	
																			10/0/15	11/15	51/8/01	19/15	10/10/15	511119	21/21/01	
						c						c						J	MAANA Fite 10/61						-	
	Bioreactor	Cell 1	DO (mg/L)	pH	ORP	Temperature C		Cell 2	DO (mg/L)	РН	ORP	Temperature C		Cell 3	DO (mg/L)	рН	ORP	Temperature C	MAG	0						

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## APPENDIX E

WPCF LAB BOD BACKUP SHEETS

Bate - 1/4/16 Time - 10:55



			FI	VE DA	AY B.	0.D.								
•			Sa	ample	d- /∂	1291	15	•						
				-			12/3							
	<b></b>	r	г		r	r	<u> </u>	915				r	<u>r</u>	
SOTTLE NUMBER	110	111	112	113	114	115	116	114	118	119	120	121	122	123
SAMPLE				~		n /							r	
	DI	1(1K	F٦			V								
A. ML OF SAMPLE ADDED TO DILUTION WATER		<u>}</u>	<u> </u>	<u> </u>					[				<b>-</b>	
	0	0	5	10	15	20	5	10	15	20	100	150	200	250
3. DILUTION FACTOR VOLUME OF BOTTLE						<u> </u>	-			-			ļ	- 0.
MG OF SAMPLE	0	0	60	30	20	15	60	30	20	15	3	2	1.5	1.2
. DO MG/L OF #1			[ [ ]							<u> </u>			<u> </u>	
. DO NOTE OF AL	9.4	9.4	9.4	9.2	9.3	9.2	9.4	9.2	9.2	9.2	9.2	9.1	9.0	.8.9
). DO MG/L OF #1	<u> ''</u>	· ·	/ /		12		11	10		100	1.0~	1.7	110	.0.7
E. DEP. AFTER 5 DAYS .	0,11	0.7	0.1	7.0	19	10	8.0	-711	1.1	6.1	81	211	1.8	6.2
	1.9	112	1.0	1.0	00	5'8	013	1.4	6.7	5.7	0"	7.9	00	
F. BOD (MG/L) = D X B				- <b>1</b> .2	20	111	0.9	1.9	2.9	20	1.1	1.7	j.2	2.7
$\frac{1}{2} \frac{1}{2} \frac{1}$	0	0.1	lid	0.3	3.5	7.7	0.9	1.1	011		1.1	1.1	0.4	Ļ
G. RAW - FINAL = BOD REMOV	AL MO	;/L			(	4.4	)		(	3.8	)		• (	(2:7)
H. BOD MG/L REMOVAL G X 10	<u>)0</u> =	7 RE	MOVED	)										

BOD MG/L RAW CHECKED SEAL DATE

NAME

LB

12/31/15 200- 414 × 15 = 66 mg/L 1/1/14 Pri-3.8 × 15 = 37 mg/L 1/2/14 EEE- 2.7×1.2 = 3.2 mg/2 1/3/14

Bate - 12/29/15

BOTTLE NUMBER

DILUTION WATER

**B. DILUTION FACTOR** 

. MG OF SAMPLE

C. DO MG/L OF #1

D. DO MG/L OF #1

SAMPLE

Time - 10:00

51

TEMP 190

FIVE DAY 8.0.D. Sampled - 12/23/15 DATE 12/24/15 140 Blank A. ML OF SAMPLE ADDED TO z, 250 2,5 250 5 5 4 5 5 10 10 10 10 O 0 VOLUME OF BOTTLE 60 60 30 30 60 60 30 30 1.2 0 0 1.0 12 1.0 8,98.8888898.98.98.888.87.57.5 24 9.0 8.98.9 7.1 5.4 5.6 7.8 7.8 6.5 6.6 1.2 1.4 9.0 8.9 7.1 E. DEP. AFTER 5 DAYS 1.0 0.9 F. BOD (MG/L) = D X B

- G. RAW FINAL = BOD REMOVAL MG/L
- H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

(No Gaud)

NAME

Dipletion to Low

DATE 12/25 12/26 12/28

8ff-

Row.

Pri-

CHECKED SEAL

Bate - 12/28/15 Time - 1:30



					AY B.( ad- /0	2/2:		5 13/1	5					
BOTTLE NUMBER	163	164.	16.5	166	168	169	171	172	173	175	176	138	179	180
SAMPLE	Bl	ank	R		V	$\mathbf{V}^{l}$		P	R		E	ΞF	=F	<b>—</b>
A. ML OF SAMPLE ADDED TO DILUTION WATER									10		100	150	200	250
B. DILUTION FACTOR VOLUME OF_BOTTLE	0	0	5	5	10	10	5	5		10				<u>~~Q</u>
. MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	3	2	.15	1.2
C. DO MG/L OF #1 D. DO MG/L OF #1	8,9	8,9	8,8	8.8	8,7	8:7	8,9	8.9	8.8	8,8	8,6	8.4	8.2	8.1
E. DEP. AFTER 5 DAYS	8.9	8.8	7.3	71	5.3	5.4	7.9	8.0	6.0	6.1	6.5	5.4	4.4	3.5
F. BOD (MG/L) = D X B	0	0.1	1.5	1:4	3.4	3.3	1.0	019	2.8	2.7	1.1	3.0	3.8	4.4
G. RAW - FINAL = BOD REMOV	AL MC	;/L	L	(		.4 ,	)	(	2	.8 /	5	7	3.8	5
H. BOD MG/L REMOVAL G X 10	j0 ≖	% REM	MOVED	,										

DATE NAME CHECKED SEAL 12/24 10 Row D. 3.4×30 = 102 mg/c 12/25 12/26 Pri- 2.8 × 30 = 84 mg/c. 12/23 ŀŊP EEE- 3,8×1.5 = 6 mg/k-

Bate - 12/23/15 Time - 11:30

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те**м**р /%

1

, ,			FI Sa	VE D <i>i</i> mple	АҮВ. d− /	2/1	»./1. 12/1	5  18/1	5			-	•	
BOTTLE NUMBER	<b></b> .		112	<u>)13</u>	114	115	116	118	)19	121	122	123	124	125
A. ML OF SAMPLE ADDED TO DILUTION WATER	· BI8	ank 1	R			V			F-{		E		<b> </b>	
<b>B. DILUTION FACTOR</b>	8	0	6	5	10	10	5	5	10	10	250	250	2)5	2)5
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1 D. DO MG/L OF #1	8.9	<u>9.1</u>	9.0	9.0	<u>8.</u> 9	9.0	9.1	9.1	9.0	9.0	28	<u>).</u> 8	<u>&gt;.</u> >	7.)
E. DEP. AFTER 5 DAYS	8,2	9.0	7,3	7,3	5,3	5,6	8,0	7.9	6,3	6,3	1.2	1,2	0.8	0,7
F. BOD (MG/L) = D X B	7،	]./	1,7	117	3,6	314	1.1	1,2	2,7	2,7	6.6	6,6	6.19	7,0
G. RAW - FINAL = BOD REMOV	AL MO	;/L		(	3,	5)		(	2	.7 J	( 61	6)	t	
H. BOD MG/L REMOVAL G X 10 BOD MG/L RAW	<u>0</u> =	z rei	MOVED								-			

CHECKED SEAL	DATE	NAME
	12/19	-7D
Row 3.5 × 30 = 105 Mg/L	12/20	JB
Pri-2,7 × 30 = 81 Mg/L	12/21	VO
	1.0	VO
BEE-6.6×1.2=7.9 Mg/L	12/22	-

Bate - 12/22/15 Time - 1:20

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7

ТЕМР 19

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•			FI Sa	VE DA umple	AY B. d- 1	0.D.  2/1 Date	6-[1= 12]	e 15/1	5					
								_					[	1
BOTTLE NUMBER	140	141	142	143	144	145	146	143	148	149	156	153	158	159
SAMPLE	Bla	ank	R	Δ	<b>V</b>	V		P	R		E	ΞF	— F	<b>—</b>
A. ML OF SAMPLE ADDED TO DILUTION WATER		ļ										-	<u> </u>	
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	250	250	275	2)5
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1														
D. DO MG/L OF #1	9.2	9.2	9.0	9.0	8.9	8,9	9.1	<u>9.1</u>	9.0	9.0	<i>9. j.</i>	9.1	9.1	9.1
E. DEP. AFTER 5 DAYS	9.1	9.0	6.1	5.9	2.9	3.8	<u>7.4</u>	7.6	5.8	5.5	<u>2.1</u>	23	6.9	7.1
F. BOD (MG/L) = D X B	,1	.2	2.9	3.1	6.0	5.1	1.7	1.5	<b>3</b> .2	<b>3</b> .3	2.0	1:8	2.2	2.0
G. RAW - FINAL = BOD REMOV	AL MG	:/L (	3.	0)				(	3.	3)	)	l	[ 2.	()
H. BOD MG/L REMOVAL G X 10 BOD MG/L RAW	<u>0</u> =	% REN	NOVED											

CHECKED SEAL	DATE	NAME
1	mo/ 12/18	JB
Row- Gox 3.0 =	180 mo/ 12/18 180 mo/ 12/18 99 ms/ 12/19	53
	no MIS/L in lap	JB
Pri- 30 X 3.3 =	999 1 12100	10
	2 11/2 12/21	10
355- 1+2.1=	d IL	

Bate - 12/21/15

Time - 1:30

,

ТЕМР 19

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			FL Sa	VE DA	AY 8. d- /	2/13	5/1-	5  16/	1					
BOTTLE NUMBER			[					/6/	15				[	
SAMPLE	<u>763</u> Bla		/65 R	165	/68	169 <b>\</b> /	17/	/72 D	<u>123</u>	175	176 176	/78 	/ <i>79</i> — •	180
A. ML OF SAMPLE ADDED TO DILUTION WATER						•						®   	■ 	 
B. DILUTION FACTOR VOLUME OF BOTTLE	0	0	5	5	10	10	5	5	10	10	250	250	275	2)4
MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1	9.0	a .	90	00	09	o g	9	9.0	69	09	09	90	90	9.0
D. DO MG/L OF #1														L.
E. DEP. AFTER 5 DAYS	9.0	<u>9.0</u>	6.1	6.Z	2.6	2.6	7.7	z.7	6.0	6.1	<u>7.0</u>	6.9	7.0	/. c
F. BOD (MG/L) = D X B	ø	ø			6.3	6.3	1.3	1.3			1.9	2.1	2.0	2.0
<pre>G. RAW - FINAL = BOD REMOV H. BOD MG/L REMOVAL G X 10</pre>			~	9)	)			l	2	. 9 ,	1 2	.Q /	, ,	

CHECKED SEAL	DATE	NAME
	ms/2 12/13	VO
Row- 60 x 2.9 = 1>4		JB
Pri-30 x2.9 = 8>	mp/ 12/18	JB
Pri-30 X J.9 = 07	72 12/19	
EEE- 1.2 × 2.0= 2 m	10/2 12/20	TB
	1010-	

Bate - 12/16/15 Time - 11:15

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ТЕМР /9°С-

•			FI Sa	VE DA ample	d→ /	2/10	45 121	1,, 1,	5					
BOTTLE NUMBER	110	111	112	1/3	114	115	116	118	119	121	122	123	124	125
SAMPLE	Bla	ank	R	Α	V	V		Ρ	R		E	ΞF	F	
A. ML OF SAMPLE ADDED TO DILUTION WATER		<u> </u>							<b></b>					
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	250	250	2)5	2)
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1														
D. DO MG/L OF #1	9.0	9.0	8.9	8.9	8.8	8,8	8.9	8.9	<u>8.7</u>	8.8	8.3	8.3	<u>8.3</u>	8,.
E. DEP. AFTER 5 DAYS	8.9	8.9	6.4	6.3	3.8	3.6	7.4	7.4	5.5	5.3	5.6	5.9	5.3	5.
F. BOD (MG/L) = D X B	.1		2.5	2.6	5.0	5.2	1.5	1.5	3.2	3.1	2.3	<i>a.</i> 4	2:6	2.0
G. RAW - FINAL = BOD REMO	VAL MO	1		.6 )	<del>)</del>	L	<u> </u>	J		2	72	6	, ,	
H. BOD MG/L REMOVAL G X 1 BOD MG/L RAW	<u>00</u> =	Z RE	MOVEI	)								•		

checked seal	ms ]	DATE 12/12/15	name V O
Raw- 60 X2.6 =	156 /L	12/13	VO
Pri- 30 X3.2=	96 mg/L	12/14	VO
255- 1.2 × 2.6=	3 mg/L	12/15	VD

Bace - 12/15/15

Time - 1:30

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TEMP /9

Too much Deplection on Raw

					AY 8.		liz							
			Sa	amp 1 e	:d- /	2/9/ Date		Jec						
	r	,	F	<b>r</b>	γ <u> </u>		/ <i>}//</i>	и <i>1.5</i> т	<b>r</b>	·	<b></b>	<del>،</del>	<u></u>	r
BOTTLE NUMBER	140	141	142	143	144	145	146	1415	148	149	156	153	158	159
SAMPLE	RI	ank			V						L	╤┎		_
A. ML OF SAMPLE ADDED TO		אווג ⊷	רו		\ V	<b>V</b>				. <b>B</b>		╺ <u>╺</u> ╺╸╹ ╷────	∎ 	<b></b>
DILUTION WATER					****							Ì		
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	250	250	225	29:
<u>VOLUME OF BOTTLE</u> MC OF SAMPLE	0	D	60	100	30	30	60	10	30	30	1.2	12	1.0	1.0
C. DO MG/L OF #1	10			00						<u> </u>	1	1	1.0	/
•	9,0	9.0	8,9	8,9	8,7	8;7	8.9	9,0	8,9	8.8	8.7	8.7	8,7	8.7
D. DO MG/L OF #1			<u>:</u>   			<u></u>   								
E. DEP. AFTER 5 DAYS	9.0	9.0	0.5	0.5	0.1	0.1	7.0	23	5.2	5.2	5.1	5.4	5.1	5.
						0	. 0	1.5		26	36	2 2	21	
F. BOD (MG/L) = D X B	.0	ø	8.4	8.4	8,0	8.6	1.7	1.7	<u> </u>			173	L	3.6
C. RAW - FINAL = BOD REMO	VAL MO	;/L						(	3	. 5 /	,	(	<b>'</b> 3.	6
H. BOD MG/L REMOVAL G X 1 BOD MG/L RAW	<u>00</u> =	% RE	MOVED	ļ										

CHECKED SEAL	DATE	NAME
7	DATE 12/11	VD
Row- 60 × 8.4 = 504	12/12	VO
Pri- 30×3.) = 111	12/13	VO
	12/14	VO
BEE- BX3.6 = 4	10/117	

Bate - 12/14/15

SAMPLE

Tíme 🗝 1:15

FIVE DAY B.O.D. Sampled- 12/8-11.5 DATE 12/9/15 BOTTLE NUMBER CU 1 169 68 79 166 Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 5 5 3 Ò 0 5 10 10 250 295 10 D 2.50 123 8. DILUTION FACTOR VOLUME OF BOTTLE . MG OF SAMPLE 60 30 30 1.2 1.2 60 60 30 30 60 1.0 1.0 Ò 0 C. DO MG/L OF #1 9.3 9.3 8.9 8.9 9.1 9.29.0 9.0 9.29.2 9.2 9.2 9.191 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 414.004 0.6 7.6 7.6 5.9 5.9 7.0 7.27.1 7.0 9.2 9.1 .1 8.3 8.5 1.5 1.6 F. BOD  $(MC/L) = D \times B$ 2 3.1 3.1 50 5.1 2.2 20 3 G. RAW - FINAL = BOD REMOVAL MG/L 5 H. BOD MG/L REMOVAL G X 100 = % REMOVED

TEMP

19

BOD MG/L RAW

CHECKED SEAL	DATE	NAME
	mel, 12/10	K.w.
Row- 5, / X 00 =	300 12 12/11	VO
CHECKED SEAL Row- 5. / X60 = Pri- 3. / X30 =	93 mg/2 12/12	VÒ
BEE- 2,2 × 1.0 =	2 ms/ 12/13	10

too much

Bate - 12/9/15 Time - 11:50

TEMP

19

FIVE DAY B.O.D. Sampled- 12/3/15 DATE 12/4/15 **BOTTLE NUMBER** 12.2 SAMPLE Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 5 5 5 5 10 10 10 0 0 260 250 D 22522 **B. DILUTION FACTOR** VOLUME OF BOTTLE 30 60 . MG OF SAMPLE 30 60 30 30 1.2 1.2 1.0 60 60 0 0 1.0 C. DO MG/L OF #1 8,9 8,9 8,9 8,9 8.5 8.5 8.5 8.5 8.9 8.9 8.9 9.0 8.9 9.1 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 5.8 5.8 5.9 9.0 8.9 6.8 6.8 4.1 4.3 7.4 7.6 5.9 6.0 5.7 1330 1.5 29 2.8 2.5 4.8 2.3 F. BOD (MG/L) = D X B4.6 3 G. RAW - FINAL = BOD REMOVAL MG/L H. BOD MG/L REMOVAL G X 100 = Z REMOVED

CHECKED SEAL	DATE	NAME
	mg/, 12/5	K.W,
Row- 60 x 2.1	= 126 12/6	KW,
Pri- 30 × 3.0	$= 126 \frac{m_{S/L}}{12/5}$ $= 90 \frac{m_{S/L}}{12/5}$	VO
zee- 1.2 x2.8	= 3 ms/L 12/8	VO

Bate - 12/8/15 Time - 11:35

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TEMP 19

					Y B.		,						•	
Sampled- 12/2/15														
						DATE	121:	3/1 <i>5</i>						
	[		[	[`	<u>_</u>	[		· · · · ·	[				<b>[</b> ]	. ]
BOTTLE NUMBER	140	141	142	143	144	145	146	143	148	149	156	157	158	159
Sample	Bla	ank	<b>'</b>			•				_ <b>x, _ x _ </b>	F	<b> F</b>		
A. ML OF SAMPLE ADDED TO DILUTION WATER								L			<b></b>	<b>F</b>	•	÷
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	250	290	235	<u>2)5</u>
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF ∦1												:		
D. DO MG/L OF #1	8.9	8,9	<u>8.9</u>	8.9	8.8	8,8	8.8	8.9	8.8	8,8	8.3	88	8.8	8.8
E. DEP. AFTER 5 DAYS	8.8	8.8	6.3	6.4	3.5	3.5	7.6	<u>7. 7</u>	6.5	6.4	6.2	6.3	6.2	6.2
F. BOD (MG/L) = D X B	.1	.1	2.6	2.5	53	5, 3	1.2	1.2	2.3	2.4	2.5	2.5	2. <b>6</b> *	2.6
G. RAW - FINAL = BOD REMOVAL MG/L $(2.6)$ $(2.4)$ $(2.6)$														
H. BOD MG/L REMOVAL G X 10	<u>o</u> =	% REM	10ved											

Row- 60 × 2.6 = 156  $\frac{ms}{L}$  12/4 Pri- 30 × 2.4 =  $\frac{32}{L}$  12/5 Ref. 1 × 2.6 =  $\frac{ms}{L}$  12/5 Ref. 1 × 2.6 =  $\frac{ms}{L}$  12/5 NAME VO K.W. KIW, 10

Bate - 12/17/15 Time - 1:20

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TEMP 19 °

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•					AY B. ad- ∕	alı.	1.5 12	2	 15					
BOTTLE NUMBER	163	164	165	166	168	169	171	172	173	175	1.76	178	179	18
SAMPLE	· ·		R	•		· ·		P	R	· <b>I</b>	F	<b>=</b> F	<b>—</b> F	
A. ML OF SAMPLE ADDED TO DILUTION WATER						-	I	•   **** ****	• • }	、 ■ [		P		<u>+</u>
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	250	250	235	23
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1														
D, DO MG/L OF #1	8.9	8.9	8.8	8.8	8.3	8.7	8,\$	8.9	8,8	8.8	8.4	8.4	8.3	8.4
E. DEP. AFTER 5 DAYS	8.8	<u>8.</u> 8	6.3	6.5	3.1	3.1	7.6	7.6	6.4	6.4	50	5.2	5.0	5.
F. BOD (MG/L) = D X B	.1	1.1	2.5	2.3	5.6	5.6	1.3	1.3	2.4	2.4			3.3	3.
G. RAW - FINAL = BOD REM	OVAL MG	/L	(2.	47				(	2.	4)	13	.37	) ,	
H. BOD MC/L REMOVAL G X	100 =	% REI	MOVED	•										

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CHECKED SEAL		DATE	NAME
	ปปม	MOL 12/3	VO
Row 2.4 × 60 =	• 7 3	my/12/4	VO
Pri-2.4 ×30 =	72	1110) 12/5 1/2 12/6	K.W.
255- 3.3×1.2=	4	12 12/6	K.W.

Bate - 11/30/15

Time - 1:50

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18

111		mple			4. 1 11	. 1	<i>c</i>					
111			1		·	/	2					, <b></b> _
	112	//3	114	11.5	116	118	119	121	122	123	124	1.
ink	R	Δ	V	V				<u> </u>	F	<b></b> F	<b>T</b> F	
	• •	. <b>.</b>		-		• • • • • • • • • • • • •		-		•	• }	⊢
0	5	5	10	10	5	5	10	10	250	250	2)5	2
		60	źp	30	60		20	30	12	12	10	
	60	00	30		00	00	50	<u> </u>	7.0-	7.0		ŕ
9.3	9.3	9.3	9.Z	9.2	9.3	9.3	9.2	9.2	9.2	93	9.2	9
9.2	3.6	>6	6.0	6.1	8.0	8.0	6.5	6.6	7.3	5.4	21	2
.)	1.5	7.3	3.2	3.1	1.3	1.3	2.5	2.6	1.9	1.9	2.1	2
/L	<u> </u>	(			<del>}</del>	(	2,	57	<b>,</b>	(	2.	7
	0 9 <u>.3</u> <u>9.2</u> .1 1L	0 60 9 <u>.</u> 3 9.3 9.2 9.6 .1 1.7	0 60 60 9.3 9.3 9.3 9.2 7.6 2.6 .1 1.5 7.5 1L	0 60 60 30 9.3 9.3 9.3 9.2 9.2 7.6 7.6 6.6 .1 1.7 1.7 3.2 12 3.	0 60 60 30 30 9.3 9.3 9.3 9.2 9.2 9.2 7.6 7.6 6.6 6.1 .1 1.7 1.7 3.2 3.1 1L 3.2 1	0 60 60 30 30 60 9.3 9.3 9.3 9.2 9.2 9.3 9.2 7.6 7.6 6.6 6.1 8.0 .1 1.7 1.7 3.2 3.1 1.3 12 (3.2)	0 60 60 30 30 60 60 9.3 9.3 9.3 9.2 9.2 9.3 9.3 9.2 7.6 7.6 6.6 6.1 8.0 8.0 .1 1.7 1.7 3.2 3.1 1.3 1.3 12 (3.2)	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$				

CHECKED SEAL DATE NAME Row- 30 × 3.2 = 96  $\frac{m_9}{L}$   $\frac{m_9}{L}$   $\frac{m_2}{2}$   $\frac{m_9}{L}$   $\frac{m_2}{2}$   $\frac{m_9}{2}$   $\frac{m_9}{L}$   $\frac{m_9}{2}$   $\frac{m_9}{L}$   $\frac{m_9}{2}$   $\frac{m_9}{2}$   $\frac{m_9}{2}$   $\frac{m_9}{2}$   $\frac{m_9}{2}$  Date - 11/2.5 Time - 11:5.5

SAMPLE

FIVE DAY B.O.D. Sampled- 11/1.9./1.5 DATE 11/20/15 BOTTLE NUMBER 68 Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 5 5 10 10 5 10 250 250 2)5 2 0 5 10 0 **B. DILUTION FACTOR** VOLUME OF BOTTLE MG OF SAMPLE 60 30 1.0 1.0 60 30 1.2 1.2 30 60 30 0 O 60 C. DO MG/L OF #1 8.5 8.4 8.4 8.5 8.5 8.4 8.3 8.4 8.4 8.3 8.4 G.6 8.4 8.5 D. DO MG/L OF #1 5,55,8 1.9 2.4 7.1 5.3 5.3 6.1 6.4 6.2 6.3 E. DEP. AFTER 5 DAYS 8,6 8,6 7,1 Ũ 6.56.0 1,4 2.32.02; 3.1 2.92.7 F. BOD (MG/L) = D X B14 13,0 G. RAW - FINAL = BOD REMOVAL MG/L 129 3

TEMP

180

H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

CHECKED SEAL	DATE	NAME
<b>`</b>	11/21	RNP
200-2.9×60= 174 1/2	11/22	ĹŊĹ
Pri-3,1×30 = 93 Hall	11/23	νO
285-2,3×1,2=2,8 Hg/L	11/24	10

Bate - 11/24/15

Time - 11:20

•				VE D# ample	NY Β. d→	nh	8.  11.	15  191	1.5					
BOTTLE NUMBER	140	141	142	143	144	145	146	143	148	149	156	157	158	159
SAMPLE	Bla	ank	R			· 		P	R		E	ĒF	<b>— F</b>	
A. ML OF SAMPLE ADDED TO DILUTION WATER				,						· · ·				
B. DILUTION FACTOR VOLUME OF BOTTLE	0	0	5	5	10	10	5	5	10	10	260	250	275	225
. MG OF SAMPLE	0	0	80	80	30	30	60	60	30	30	1.2	1.2	1.0	1.0
C. DO MG/L OF #1														
D. DO MG/L OF #1	8.5	8.1	8.6	8,6	8.5	85	8.6	86	<u>8.5</u>	8.5	8.8	8.9	8.9	8.9
E. DEP. AFTER 5 DAYS	8.7	8.3	5.6	5.6	1,5	2.3	7.1	<u>7.1</u>	5.0	4.5	6.4	6.3	6.6	<u>6. 6</u>
F. BOD (MG/L) = D X B	0	0	3.0	3.0	Þ.Q	6.2	1.5	1.5	3.5	5.8	2.4	2.2	2.3	2.3
G. RAW - FINAL = BOD REMOV	AL MC	5/L (	3.	0)	1	L	. <u> </u>	(	3.		)	(	2.	3)
H. BOD MG/L REMOVAL G X 10 BOD MG/L RAW	= 00	% RE1	MOVED	×,				_						

CHECKED SEAL Row-  $60 \times 3.0 = 180$  Pri-  $30 \times 3.0 = 111$  DATE ms/L = 11/20 ms/L = 11/21 ms/L = 11/22CHECKED SEAL NAME VO EEE-1×23 = 2 ms/2 11/23 10

Date - 11/23/15 Time - 3:35

ТЕМР *19* 

FIVE DAY B.O.D. Sampled- 11/13/15 DATE 11/18/15														
BOTTLE NUMBER	110	111	112	11.3	114						122	123	)24	125
SAMPLE	Bla	ank	R	Ά	V	V		P	R		E	ĒF	- F	
A. ML OF SAMPLE ADDED TO DILUTION WATER						[				<u> </u>				<u> </u>
8. DILUTION FACTOR VOLUME OF BOTTLE	0	0	5	5	10	10	5	5	10	10	250	250	275	225
MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	1.2	1.2	10	1.0
C. DO MG/L OF ∦1		Q \	0 5	01	07	07	86	06	91	01	0.	a 1	9.1	9.2
D. DO MG/L OF #1	ſ					_							· · · ·	
E. DEP. AFTER 5 DAYS	8.5	<u>8. &gt;</u>	6.3	6.2	3.5	3.5	<u>7.1</u>	<u>5.1</u>	5.4	5.5	6.4	6.4	6.0	6',3
F. BOD (MG/L) = D X B	a	s	2.2	2.3	4,8	4.8	1.5	1.5	3.0	2.9	2.3	2.>	3.1	2.9
G. RAW - FINAL = BOD REMO	VAL MG	/L	•	(	4.	8 >	\$	1	3.	0,	)	7	3	0)
H. BOD MG/L REMOVAL G X 1 BOD MG/L RAW	= 00	% RE1	NOVED											

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CHECKED SEAL	DATE	NAME
3	11 mol 11/19	VO
$R_{SW-} = 30 \times 7.0 = 77$	1 mg/ 11/20	VD
Pri- 30 x 3.0 = \$	10 1/2 11/21	RIP
CHECKED SEAL Row- $30 \times 4.8 = 14$ Pri- $30 \times 3.0 = 9$ Eff- $3.0 \times 1.0 =$	3 11/22	LYP

Bate - 11/18/15

Time - /1:20

FIVE DAY B.O.D. Sampled- 11/12-115 DATE 11/13/15 BOTTLE NUMBER 68 SAMPLE Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 20 Ô 20 10 10 10 20 20 Ò 200 200 250 250 0 8. DILUTION FACTOR VOLUME OF BOTTLE MG OF SAMPLE 1.5 1.5 30 15 15 1.2 30 30 15 15 30 1.2 Ô 0 C. DO MG/L OF #1 9.0 9.0 9.0 9.0 9.1 9.0 8.9 9090 9.0 9.0 89 9.0 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 4.3 0.5 0.4 7.3 9.3 5.2 うじ 6.96 8.939 52 e, 8.9 1,N 1.8 F. BOD  $(MG/L) = D \times B$ 4.5 8.5 3.8 1 8.6 15.1 ۶, 3 2.0 20 9 4 G. RAW - FINAL = BOD REMOVAL MG/L

H. BOD MG/L REMOVAL C X 100 = Z REMOVED BOD MG/L RAW

CHECKED SEAL	Mal 11/14/1	NAME
Row- 30x 4.9=	DATE Mg/ 11/14/1 147 /L 11/15 57 mg/ 11/15 3 mg/ 11/16 3 mg/ 11/15	JB
Prin 15 X 3.8=	37 1L 11/16	VD
BEE- 1.5 X2.1=	3 1/ 1/13	Vo

Date - 11/13/15 тем Time -12:10 Failed Not enocuph Depli FIVE DAY B.O.D. 11/17. Depletion Sampled-DATE 11/12 EFF ΰN BOTTLE NUMBER 145)46 40 SAMPLE Blank A. ML OF SAMPLE ADDED TO DILUTION WATER Ø 0 20 20 10 10 20 20 200 10 b 200 250 23 8. DILUTION FACTOR VOLUME OF BOTTLE MG OF SAMPLE 0 0 15 30 30 15 30 30 15 15 1.5 1.5 1.2 1.2 C. DO MC/L OF #1 9.4 9.3 9.3 9.3 9.4 9.3 3 3 9 93 94 Q 2 2 7 2 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 6.3 .9 8.5 8.6 8.9 8.5 6.366 0.8 0.4 1.4 9.2 9.2 6.6 ッ \$ 5 8,4 5 8.4 2.3 F. BOD (MG/L) = D X B 8.8 25 7 8 2 G. RAW - FINAL = BOD REMOVAL MG/L H. BOD MG/L REMOVAL G X 100 = Z REMOVED BOD MG/L RAW

CHECKED SEAL	DATE ,	NAME
1	mg/ 11/13	VO
20w- 30 x 2,8 =	84 mg/ 11/13 11/14	TB
Pri- 30x2.72	81 mig/2 11/15	TB
	1 mg/ 11/16	VO
EES- 1.5x.8=	1 74	

11/10/15 Bate -

Time - 1:20

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•	·				AY 8.	u 14.		s115					·	
BOTTLE NUMBER	110	111	112	113	114	115	116	118	119	121	122	123	124	129
SAMPLE		ank	R	Δ		<u>\</u>		$\mathbf{P}$		• <b>•</b>	F			
A. ML OF SAMPLE ADDED TO DILUTION WATER	-	411N						•		. ■ 	│ <b>┖</b> ╸ │ │	━━• ■   	-	
8. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	150	150	200	20
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	2.0	2.0	1.5	1.5
C. DO MG/L OF #1														
D. DO MG/L OF #1	8.5	8.6	8.5	<u>8.5</u>	8.4	8.4	8.4	8.4	8.3	8.3	8.6	8.8	8.7	8.
E. DEP. AFTER 5 DAYS	8.5	8.5	28	7.9	4.0	4.2	8.0	8.0	7.6	7.5	8.0	8.0	6.9	6.
F. BOD (MG/L) = D X B	2	./	0.3	0:6	4.4	4.2	.4	.4	.)	.8	.6	.8	2.0	2.0
G. RAW - FINAL = BOD REM	OVAL MG	;/L	,	. (	4.	3 /	}			8 /	)		(2	0
H. BOD MG/L REMOVAL G X	100 =	Z REI	NOVED	1										

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CHECKED SEAL	DATE	NAME
Row- 30 × 4.3 =	129 11/2 11/6	VO
	24 11/2 11/3	VO
Pri- 30x.8 =	1.118	VO
eee- 1.5×2.0=	3 mg/2 11/8	VO

Bate - 11/9/15

Time - 1:30

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TEMP 200

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Failed Not enough at EFF

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BOTTLE NUMBER	163	164.	165	166	/68	169	171	172	173		176	178	179	180
SAMPLE A. ML OF SAMPLE ADDED TO	Bla	ank	R	A	V	V		Ρ	R		E	ΞF	<b>=</b> F	
DILUTION WATER	0	0	5	سى	10	10	5	5	10	10	150	150	200	200
B. DILUTION FACTOR VOLUME OF BOTTLE MG OF SAMPLE	.0	_0			- <i>k</i>	-							1.5	
C. DO MG/L OF #1														
D. DO MG/L OF #1	9,1	<u>9.1</u>	9.3	9.3	9.3	9.3	<u> 9.9</u>	7.7	7.5	7.3	9.2	7.a	7.1	<u>9.1</u>
E. DEP. AFTER 5 DAYS	2.1	2.1	8.2	8.2	6.7	69	8.5	8.6	7.3	7.3	8.4	8.4	8.3	8.1
F. BOD (MC/L) = D X B	æ	a	1.1	1:1	2.4	2.4	.9	.8	20	2,0	.8	.8	:8	1.0
G. RAW - FINAL → BOD REMOV	AL MG	./L	•	- (	2.4	4)	)	(	2	.0 /	)	(		7)

H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

CHECKED SEAL	, DATE	NAME
	Mo/1 1/5	VO
2000- 30x 2,4 =	72	10
Prin 30×2.0=	DATE 11/2 11/5 11/6 60 11/2 11/3	VO
		VO
REE- ,9X/,5 =	· 1 <sup>mg/</sup> 11/8	

Bate - 11/4/15 Time - 11:45

BOD MG/L RAW

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• •		FIVE D Sample	AY B.O.D. ad- 101 DATE	29/1.5 10/301	1.5		
BOTTLE NUMBER	140 141	142 143	144 145	146 145	148 149	156 157 159	3 159
SAMPLE	Blank	RA		P	RI	EF	F
A. ML OF SAMPLE ADDED TO DILUTION WATER							-
B. DILUTION FACTOR	00	55	10 10	5 5	10 10	150 150 200	» <u>200</u>
VOLUME OF BOTTLE MG OF SAMPLE	00	60 60	30 30	60 60	30 30	20201	51.3
C. DO MG/L OF #1							
D. DO MG/L OF #L	8.7 8.7	8. 8. 5	8. 7 8.7	8.) 8.8	8.6 8.6	8.6 8.6 8.2	5 8.5
E. DEP. AFTER 5 DAYS	8.7 8.1	28 28	6.2 6.5	8.28.4	31 23	7.17.06.	5 6.4
F. BOD (MG/L) = D X B		.9 :9	2.5 2.2	.5 .4	1.21.3	1.5 1.6 2.	0 2.1
G. RAW - FINAL = BOD REM	OVAL MG/L	<b></b>	(2.4)	)	( 1.3 /	دً]	<u>ν</u> , γ
H. BOD MG/L REMOVAL G X	100 = % RE	MOVED					

DATE RESULT SEAL RESULT 30 X 2.4 =  $72 \frac{m_9}{L} \frac{10/3}{10/3}$ Pri-30 X 1.3 =  $39 \frac{m_6}{L} \frac{11/2}{11/3}$ RESULT 5 X 2.1 =  $3 \frac{m_6}{L} \frac{11/3}{11/3}$ NAME K.W. 20 VO

11/3/15 Date -

Time - 12:00

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FIVE DAY B.O.D. Sampled- 10/28/15														
	DATE 10/29/15													
BOTTLE NUMBER	110	111.	112	113	114	115	116	118	119	121	122	123	124	125
SAMPLE		ink						$\mathbf{P}$	R	<u> </u>	F	<b>F</b>	— F	
A. ML OF SAMPLE ADDED TO DILUTION WATER								•		••••••	<b></b>	<b>—</b> •		
B. DILUTION FACTOR VOLUME OF BOTTLE	0	0	5	5	10	10	5	5	10	10	150	150	200,	2000
. MG OF SAMPLE	0	0	60	60	: 30	30	60	60	30	30	20	20	1.5	1.6
C. DO MG/L OF #1	0.7	03	a .,	00	0.0	o'a	12 -		0.0	00	0-7	0.1	aı	¢ц
D. DO MG/L OF #1	<u>9.3</u>	7.9	7.3	7.3	7.a	7.2	7.5	7.3	7. a	<u>7. 2</u>	9.5	7.4	7.4	<u>7.7</u>
E. DEP. AFTER 5 DAYS .	9.34	<u>9.3</u>	73	7.4	3.8	3.8	8.3	8.3	6.7	6.6	<u> </u>	7.5	6.3	6.7
F, BOD $(MG/L) = D \times B$	ø	ø	2.0	1.9	5. <u>4</u>	5.4	1.0	1.0	2.5	2.6	1.8	1.9	a:}	2.3
G. RAW - FINAL = BOD REMOV	AL MG	/L	2	0)	)				( 2.	6)	1		( 2.	37
H. BOD MG/L REMOVAL G X 10 BOD MG/L RAW	<u>- 00</u>	Z REN	HOVED	I										

CHECKED SEAL DATE NAME Row 60 x 2.0 = 120  $\frac{mg}{L} \frac{10/30}{10/31}$  K.W. Pri- 30 x 2.6 = 38  $\frac{mg}{L} \frac{10/31}{11/1}$  K.W. EFE-  $\frac{1.5x2.7}{10} = \frac{4}{100} \frac{mg}{L} \frac{11/2}{100}$ 

Bate - 11/2/15 Time - 1:30

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TEMP ø 19

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•			FI Sa	VE D# ample	AY 8. d- /	0 /2	10/2 10/2	15 28/1	ی ا					
BOTTLE NUMBER	/63	164	165	166	168	169	171	172	173	175	176	178	179	180
SAMPLE	Bla	ank	R	Δ	V	V			R		F	_ _ F	=1	
A. ML OF SAMPLE ADDED TO DILUTION WATER	1					•				· •	<b></b>	•	-	<b>†</b>
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	150	.150	200	20
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	20	2.0	1.5	1.
C. DO MG/L OF #1						•								
D. DO MG/L OF #1	9.0	9.0	9.1	9.1	9.0	9.0	9.3	9.2	9.1	<u>9.1</u>	8.8	8.8	8.9	8.
E. DEP. AFTER 5 DAYS	9.0	9.0	8.0	<u>7.9</u>	6.2	6.3	8.4	8.a	6.8	6.9	4.2	4.6	2.5	2.
F. BOD (MG/L) = D X B	e	ø	1.1	1.2	2.8	2.5	•9	1.0	2.3	2.2	4.6	4.2	6.4	6.
G. RAW - FINAL = BOD REMO	OVAL MG	/L	•	l	<i>a</i> .	8 /	)	(	2.	3 /	)( 4	.4)	) ,	
H. BOD MG/L REMOVAL G X I	100 =	2 RE1	MOVED											

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BOD MG/L RAW

CHECKED SEAL	DATE	NAME
	011 MS/L 10/29	VO
200- 30×2.8=	87 10/30	10
Pri- 30 × 2.3 =	84 <sup>m5/L</sup> 10/29 69 <sup>m9/L</sup> 10/30 9 <sup>m9/L</sup> 10/31 9 <sup>m9/L</sup> 11/1	K.W.
355-20×4.45	9 mg/2 11/1	K.W.

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Date - 10/28/15 Time - 11:10

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•			FI Sa	VE DA imple	AY B. d-	10/01	122/1 10 k	.5 23./)	5				•	
BOTTLE NUMBER	140	141	142	143	144	145	146	143	148	140	156	15>	158	159
SAMPLE	Bla	ank						P	R	· <b>·</b>	F	— F	— F	
A. ML OF SAMPLE ADDED TO DILUTION WATER			• •			-					-		-	<u> </u>
<b>B. DILUTION FACTOR</b>	0	0	5	5	10	10	5	5	10	10	100	100	150	15
VOLUME OF BOTTLE . MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	3,0	3.0	2.0	2.0
C. DO MG/L OF ∦1														
D. DO MG/L OF #1	8.1	8.	8.0	8.0	80	80	8.1	8.1	<u> </u>	8.0	<u>7.9</u>	<u>う.9</u>	28	2.
E. DEP. AFTER 5 DAYS	. 8.1	8.1	5.9	5.9	2.1	3.0	7.2	7.3	5.6	5.5	6.0	6.0	5.8	5.8
F. BOD (MG/L) - D X 8			2.1	2.1	5.9	6.0	.9	.8	23	2.5	1.9	1.9	à.0	2.0
G. RAW - FINAL = BOD REMO	VAL MG	;/L (	2.	1)	;		• • • •	(	2.	4)			[2]	.0
H. <u>BOD MG/L REMOVAL G X 1</u> BOD MG/L RAW	00 =	Z REI	MOVED											

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CHECKED SEAL	DATE	NAME
	mo/ 10/24/15	VO
15w- 60 X 2.1 =	120 1 10/25/15	$K, \omega$
Pri- 30 X 2.4 =	72 10/26/15	K.W.
EES- 2.0 X2.0 =	126 mol 10/24/15 126 10/25/15 72 ms/L 10/25/15 4 ms/L 10/25/15	10

Bate - 10/27/15 Time - 11:17

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TEMP 190

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•					AY B.	10/2	10/	s     aa	5					
BOTTLE NUMBER	110	111	112	11.3	114	115	116	#8	119	121	102	123	124	125
SAMPLE	Bla	ank	1 <u></u>	_					R	· <b>I</b>	F	<b>—</b> F	<b>—</b> F	
A. ML OF SAMPLE ADDED TO DILUTION WATER										┟╌╌╌				
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	100	100	150	150
VOLUME OF SOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	3.0	3.0	2.0	2.0
C. DO MG/L OF #1				<u>-</u>										
D, DO MG/L OF #1	8.6	8.6	8.5	8.5	8.4	8.4	8.5	8.5	8.5	8.4	8.4	8.[	8,0	8.0
E. DEP. AFTER 5 DAYS	8.5	8.5	6.4	6.3	3.0	3.4	7.0	7.0	4.6	4.6	<u>7.5</u>	7.5	6.5	6. 3
F. BOD (MG/L) = D X B	۱, ا	.7	2.1	2:2	5.4	50	1.5	1.5	3.9	3.8	.9	.6	1.3	1.3
G. RAW - FINAL = BOD REMOV	AL MO	:/L (	2.	21	ŧ		-	(	3.	91	)		[ 1	3)
H. BOD MG/L REMOVAL G X 10		% RE1												

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CHECKED SEAL	DATE / /	NAME
	mal 10/23/15	VO
250- 60 x 2.2 =	132 1/2 10/24/15	VO
- <b>A</b>	ms/, 10/25/15	K.W.
rri- 30 x 3.7 -	3 ms/L 10/26/15	K.W.
EEE- 20 X 1.3 =	3 m3/L	

Bate - 10/26/15

Time - 12:10

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TEMP 190

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FIVE DAY B.O.D. Sampled- 10/20/4.5														
DATE 10/21/13														
BOTTLE NUMBER	163	104	16.5	166	168	169	171	172	173	175	176	178	179	180
SAMPLE		ank	R	A		V		P	R		E	ΞF	=F	
A. ML OF SAMPLE ADDED TO DILUTION WATER				<del>ان</del>						· '		['	<b></b>	<b> </b> i
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	100	100	150	150
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	3.0	3.0	2.0	2.0
C. DO MG/L OF #1	~ A	00	00	00	2 K	o'h	al	o K	21		0-	97	79	7.9
D. DO MG/L OF #1	[			4. Q.	8.7									
E. DEP. AFTER 5 DAYS	8,9	8.9	7,2	7,3	4,4	4.7	7,7	7,8	6.1	6.2	8.0	8,1	7,6	7,4
F. BOD (MG/L) = D X B	Ø	Ø	1.6	1.6	4,3	4,0	1.0	0,9	2.5	2.4	0,3	0,2	0,3	0,5
G. RAW - FINAL = BOD REMOV	AL MG	/L		(	(43)	)	_	(	2,5	)			· (	(0,5)
H. BOD MG/L REMOVAL G X 10 BOD MG/L RAW	0 =	Z REN	MOVED	J										

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CHECKED SEAL	DATE	NAME
r	10/22/15	VO
Row- 4,3×30 = 129 Mg/L	10/23/15	VO
Pri 2,5 × 30 = 75 Mg/L	10/24/15	VO
	10/25/15	K.W.
ESE-0.5x2.0=1 Mg/L		

Date - 10/21/15

Time - 1:20

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TEMP

201

•					AY B. .d- /0	0/15	75 10  ,	Iolis	5					
BOTTLE NUMBER	110	,,,,	112	113	114	115	116	118	119	121	1.22	123	124	1.25
SAMPLE	· Bla	I		Δ							F		<u> </u>	
A. ML OF SAMPLE ADDED TO DILUTION WATER				· •				• 		. ■ 		■	╸	<u> </u>
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	100	100	150	15
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30				20	
C. DO MG/L OF #1		<u> </u>		····										
D. DO MG/L OF #1	9.0	9.0	8.9	8.9	<u>88</u>	8.8	8.9	8.8	8.7	8.>	28	28	8.2	8.2
E. DEP. AFTER 5 DAYS	8.9	8.9	5,5	5.5	1.9	2.0	ええ	7.1	5.7	5.8	4.6	4.6	6.2	6.2
F. BOD (MG/L) = D X B	· [	.1	3.4	3:4	<b>F</b> .9	6.8	1.5	1.3	3.0	2.9	3.2	<i>3.</i> 2	2.0	2.0
G. RAW - FINAL = BOD REMO	VAL MO	L		L.,		<u></u>		(			3	· · · · · · · · · · · · · · · · · · ·	),	<b>L</b>
H. BOD MG/L REMOVAL G X 1	<u>00</u> =	<b>Z</b> RE1	MOVED	I										

CHECKED SEAL	DATE	NAME
	ms/ 10/17	VO
Row- 60 x 3.4 =	204 1 10/18	VO
Pri- 30 x 3.0 =	204 mg/ 10/12 10/18 90 mg/L 10/19	VO
BEE- 30 X3.2 =	10 mg/L 10/20	VÒ

Bate - 10/20/15

Time - 11:35

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100 100 150

30 3.0 3.0 20 2.0

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6.4

3.9

58

FIVE DAY B.O.D, Sampled- 10/14/15. DATE 10/15/15

145 146

5

30 80 60

1.6

1.6

10

895558222273236059

6

10

30

2.8

2

2.9

10

8.9 8.9 8.8 8.8 8 5 8.5 8.3 8.3

3,6

BOTTLE NUMBER

SAMPLE

- A. ML OF SAMPLE ADDED TO DILUTION WATER
- B. DILUTION FACTOR VOLUME OF BOTTLE MG OF SAMPLE
- C. DO MG/L OF #1
- D. DO MG/L OF #1
- E. DEP. AFTER 5 DAYS
- F. BOD (MG/L) = D X B
- G. RAW FINAL = BOD REMOVAL MG/L ( 3
- H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

CHECKED SEAL	DATE	NAME
2000 60×34-	204 "15/ 10/16	VO
- 13	87 mg/ 10/13 10/18 11 MH/2 10/19	VO
Pri. 30 X 8.15	10/18	VD
Eff- 3 X 3.6=	11 10/19	VO

Blank

0

0

9.0 9.0

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0

8.9

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60 60

10

30

9.0 8.9 8.9

326.76.7

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9.0

Bace - 10/19/15 Time - 1:15

TEMP

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FIVE DAY B.O.D. Sampled- 10/13/7.5 . DATE 10 /14/15 BOTTLE NUMBER 163 SAMPLE Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 5 5 5 10 10 10 5 10 100 100 150 0 Ò **B. DILUTION FACTOR** VOLUME OF BOTTLE 60 MG OF SAMPLE 0 60 30 30 60 303020 0 60 30 30 2.0 C. DO MG/L OF #1 8.8 8.8 8.9 8.9 8.8 8.7 8.6 8.6 8.3 8.3 9.0 8.9 8.9 9.0 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 58 786464626.24.446 8.9 8.9 53 5.3 01 2.1 F. BOD (MG/L) = D X B 1.1 1.1 2.1 2.3 2.4 2.4 39 6. 5 6. 7 .1 3.2 3.2 G. RAW - FINAL = BOD REMOVAL MG/L H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

CHECKED SEAL	DATE	NAME
Row 60× 3.2 = 192	10/15	VO
dev- 60 x 5.00 - 19 x	10/16	VO
Pri- 30 x2.4= 72	10/17	レロ
EEE- 2.0 X3.8 = 8	10/18	V۵
EEE- 2.0 A.2. 6		

Bate - 10/14/15 Time - 11:45

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•			FIN Se	VE DA Imple	.YB.( d→ /	D.D. <b>G</b> /8 DATE	ti 5	1/13	<b>,</b>			۰		
BOTTLE NUMBER	)10	117.	112	113	114	115	116	118	119	121	127	123	124	125
SAMPLE	Bla	ank	R	Δ	V	V			R	1	F		<b>=</b> F	÷
A. ML OF SAMPLE ADDED TO DILUTION WATER					• •					-		••••		
B. DILUTION FACTOR	0	0	5	5	10	10	5	5	10	10	150	150	200	200
VOLUME OF BOTTLE MG OF SAMPLE	0	0	60	60	30	30	60	60	30	30	2.0	2.0	1.5	1.5
C. DO MG/L OF #1														
D. DO MG/L OF #1	8.8	8.8	8.5	8.3	8.6	8.6	8.5	8.5	8,5	8.6	7.5	2.2	24	<u>7.5</u>
E. DEP. AFTER 5 DAYS	8.8	8.8	5.5	5.8	2.0	2.0	7.4	7.4	5.5	5.6	5.3	5.3	4.8	4.9
F. BOD (MG/L) = D X B	0					6.6	1		}			l		1
G. RAW - FINAL = BOD REMOV	AL MO	G/L	(3	. 1 -	)				3,	01	)	(	2.	6)
H. BOD MG/L REMOVAL G X 10	<u>)0</u> =	% RE	MOVEI	)										

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BOD MG/L RAW

CHECKED SEAL	DATE	NAME
	186 mg/2 10/10	JB
Kaw- 60 X 3.1:	90 ms/L 10/12	JB
Pri- 30 × 3.0 :		JB
BEE- 1.5 X 2.6 =	4 ms/ 10/13	vo

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Bate - 10/13/15 Time - 11:05

FIVE DAY B.O.D. Sampled- 10 17 15 DATE 10/8/15 BOTTLE NUMBER WO 156 SAMPLE Blank A. ML OF SAMPLE ADDED TO DILUTION WATER 5 5 5 5 150 150 200 200 0 Ø 10 10 10 10 B. DILUTION FACTOR VOLUME OF BOTTLE 60 30 60 60 30 30 60 30 2.0 2.0 0 О 1.5 1.5 C. DO MC/L OF #1 9.39.1 9.2 9.01 92 9.0 97 9.0 9.019.0 7979 7.4 D. DO MG/L OF #1 E. DEP. AFTER 5 DAYS 497575585907020.2 4.3 20 1.7 F. BOD (MG/L) = D X B4.1 1.7 3 .3 2.2 3 G. RAW - FINAL = BOD REMOVAL MG/L H. BOD MG/L REMOVAL G X 100 = % REMOVED BOD MG/L RAW

CHECKED SEAL		DATE	NAME
Row- 30 x 4.2 =	126 mg	1/2 10/9 1/2 10/10 1/2 10/11	JB
Pri-30 × 3,3 :			-JB
BEE- 2.0 x 7.2 2	14 m	0/2 10/12	JB

TEMP

Date - 10/3/15

Time - 11:20

TEMP 200 FIVE DAY B.O.D. 10/1/15. Sampled-DATE 10/2/15 68 169 172 76 178 180 Blank A. ML OF SAMPLE ADDED TO 5 5 5 lo 10 6 10 150 150 200 200 D 10 O

60

30

30

1.0 1.8 1.8 20 2.0 2.4

2002.0 1.5

1. 3

5,0

50

60 30

30 60

899.07.57.5585.78.08.17.27.25.85.9

9.19.19.19.19.19.09.09.09.19.09.078

3.23.3 1.0

**B. DILUTION FACTOR** VOLUME OF BOTTLE MG OF SAMPLE

DILUTION WATER

C. DO MG/L OF #1

BOTTLE NUMBER

SAMPLE

- D. DO MG/L OF #1
- E. DEP. AFTER 5 DAYS
- F. BOD (MG/L)  $\simeq$  D X B
- G. RAW FINAL = BOD REMOVAL MG/L
- H. BOD MG/L REMOVAL G X 100 = 7 REMOVED BOD MG/L RAW

CHECKED SEAL DATE NAME Row 30 × 3.3 = 99  $\frac{m_{9}}{L}$  10/3 Pri- 30 × 1.8 = 54  $\frac{m_{9}}{L}$  10/4 BEE- 1.5 × 2.4 = 4  $\frac{m_{9}}{L}$  10/6

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60

1.6

1:6

## APPENDIX F

WPCF LAB SOLIDS BACKUP SHEETS

	-		SET	TTLE	OME	TER	3		FAIRHA	ΈN.	CONT	ROL DAT		G						: 12/3.1. RA 15' 1		ļ
	8:	28		:			SAMPLES	, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	INF 50	<u>A</u> 3	5ml	PRI 50	EFF	100 1	F3 100	F 4	100	R.J	init.	R4 5m1	9, 97 C	7
νE		55C	\$\$	V S	sśc		CRUCIBLE		21.4387	21	6228	21, 7172	$\mathcal{U}_{j} \mathcal{G}$	731	16;5807	22	0318	2(37	44	21, 3201	K, LISI	
U	1000	2.2				L.	WT. + SAMPL	Е — —		1 1			Ĺ	·					1		. •	
5	470						CRUCIBLE						يز رما		1. 1800	22	1310	212	806	21, 2484	21,259.	1
0	360					 	WT.	·				21/1142	<u>، د ر</u> کمه	205	16;5000		5008	104	160	10715	10160	Ţ
15	320		:				. DIFFERENC		-0052		0137	10030	- 00	-	7	ľ	8	92	00	14,300	3200	2
20	290	· ·				ļ	PRE-FURNA		. 104		2,740	60				<u> </u> .		· · · · · · · · · · · · · · · · · · ·				
Z5 '	270		ļ					( <del>*</del> * *		1								· .			•	
30	260		<b>_</b>				WT. + SAMP					· ,.	<b>.</b>							· ·		
10	240	2	<u> .                                    </u>				WT. POST		1	ł				· .	•				<u>.</u>			
50	220		╀┅┯━		ļ	.	DIFFEREN		_ <u> </u> -		<b></b>	•									1.	
60 1 7	210		1	2	3		VOLATILE														_	
. من مرد	أمعري	Ê	•	-	Ũ		PRE-FURNA				•			نسر	·		.8	9	200	14,300	3,20	O
	<u>/ 2.7</u> 3 4	$\frac{C}{R}$	. 2	2	3 4		VOLATILE		.104		2740	. 60	ن ا	5-	7	<u> </u>	· 3	· "		11,500		
~		RSC	• •				FIXED SOLI	DS ·								<u></u>			, 	<u> </u>		
· · · · · · · · · · · · · · · · · · ·	<u>13.0</u> 13111		1	2	3 4				BACTER	A		•	міс		RGANISH	Ą.				*NOT	ES .	
1147	14111	Q I		• •			SAMPLE		LONIES		#/1	00ml			ROUP	<del>.</del> .						
2	3 Ai	A	1	2	3 4	-   -			*				- 4 4 4	OFRO	olds:			•		INF. TEL	œ/3	7.:
1.16	37.2								· · · · · · · · · · · · · · · · · · ·							5	1.			al ph	· 6	., l
	RESI		<sub>-</sub> C	L <sub>2</sub>										, <b>.</b>	· <u> </u>			tt				
. דו אוד	E F	LOW	1	EV	ΞL_			<b> </b>		_ -	., 		-/ E	AGEL	LATES	(Ď.	2			A2 ph		.4
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						-	OUT:						W	ORMS	5'	S	,	•			total	
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			SETTL	EOMET	ER		FAIRHAN	ΈN	CONT	ROL DAT	TA LOG	INITL					: 12/3.0		
	9:	05	:	<u> </u>	SAMPLES	•	INF 50	A3	5ml	PRI 50	EFF 100	F3 100	F4	100	R3	_ <u>5m1</u>	R4 5m1	hiz_	15m1
AE		550	SSV	Issc	CRUCIBLE		21 2600	19	4217	21 2829	22.0316	21, - 2494	21,	6104	21,7	590	21, 8639	21,	44,87
]	1000	2.0			WT. + SAMP	LÉ	· ·	1	, , , , , , , , , , , , , , , , , , , ,				ĺ						
i	410	>.			CRUCIBLE		l -		•				. 	1.000	21	7147	9,7549	21	4335
)	320				WT.	·	1				12,0312	21,2476	1.	000%		443	0,1097		0157
5	270			<b></b> ])	DIFFERENC	•	10014	14	0132 440	-0074 48	4	8		4. G		860			,040
2	250			┼┉╍┉┥┟			.28		440	70			<u>† .</u>			<u>.                                    </u>		1	
5.	230	· · ·		┼──┤╿	CRUCIBLE WT. + SAMP	νĽΕ <sup><sup>66</sup> – Γ</sup>	. 	Ì			]						•		•
<u>ן</u> ס	<u>720</u> 200			┛	WT. POST	<b>min</b>	-				<u> </u> .		Į		1		•	-	•
0	200		_ <u> ·</u>		FURNACE								_		<u> </u>		<u></u>		
<u> </u>	190		-		DIFFEREN	CE	-								1			.	
2	3	Ą	1 2	3	VOLATILE	-	 	.				· ·				·			
2.0	3 4	ċ			PRE-FURNA		.28	.	2,440	48	4	8		:6	1.8	- 86 C	21.94	0	3,040
		1.51	1. 2	3 4	VOLATILE	<u></u>	. ~ 0	<i>"</i>	x,770						<u> </u>	• •			
	19.6	······································		3 4	FIXED SOLI		BACTERI					ORGANISN	l		~	·	+NO	 TE C	-
RII	7/14	ğ	1 2 3:00		SAMPLE		LONIES	Ĥ	#/10			ROUP					- HIQ		• <u>•</u> •••••••
2	3 A.			3 4	<u> </u>			_				ري	• :				INF. TE	мр	/3
57. J	7.0	ÎD		5.0 6.4						•	AMOEB	oids		,			•		
	RES	IDUA	L CL 2							<u>·</u>	<u></u>			<u>.</u>	<u> </u>		Al ph	. <sup>-</sup> -	<i>6</i> .
пме	F	FLOW	LEV	ΈL		·			**				15	<u>۶ </u>		•	A2 ph	-	-61
;	1	plant				-			<u> </u>		L FLVOFI	LATES	مرجب	·   .		i l		TAC	
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	SET	TLEOME	TER	FAIRHAV	EN CON	ROL DA	TA LOG				E: 12/29	
9:1	4	; .	SAMPLES	INF 10	A3 5ml	PRI 160	EFF 100	F3 100	F4 100	R3 5m1	R4 5m1	A2 15m1
ME SSV	SSC SS	v ssc	CRUCIBLE	21, 5774	21, 2647	21, 4398	22,0314	19; 4248	21, 2813	21, 29.74	21, 6557	21,7683
0 1000		·	WT. + SAMPLE									
5 670			CRUCIBLE	.	• • • •			· 1/1-20	2. 32.2	21 2594	71 6096	21 7539
10 520			WT	21,5727		21:4337	12,0307	17.7277	1, 2802	10380	21,6096	10154
5 440	·		DIFFERENCE PRE-FURNACE	10047	3320	10061	, 0007 . 7	10009.	1.1	7600	-	3,080
0 390				. 94	3.300		1					
25 350			CRUCIBLE	1 ·								
30 <u>370</u>			WT. POST	~			· ·		ł			
10 300 50 270	├ <u></u>		FURNACE				· · ·		· ·			<u></u>
50 260			DIFFERENCE	-					1	· .		
	<u> </u>	2 3	VOLATILE		-1	· .		· · ·	· .	·		
12024		1	PRE-FURNACE	Cil			;	9	111	7.600	9,220	3,080
12/ 3 4	R 1. 2	34	VOLATILE	.94	3,320	. 61	.7.	1 /		1.000	-1,000	- <u>), 2 a</u>
	č		FIXED SOLIDS				<u> .</u>				· ]	 
17114114		3 4	COLIFORM	the second day of the				RGANISM	<u>.</u> . ] .		• <b>*</b> NOT	ES ,
	ě		SAMPLE CO	LONIES	#/!	0000						
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		<u>· 2</u> EVEL				·····		•	~		AZ ph	- 6.3
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	<u>auc</u>						· · ·		-	· · · · · · · · · · · · · · · · · · ·	SEPI	ACE .
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			START:				CILIATE				Rocheste	
—Ч	z S.						ROTIFER	4 1 1 1 1			•	
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			UUT:				WORMS	ß	2			total
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·		· T01	TAL NITROGEN-	NITRAI	E— .	NITRITI	<u>f</u> unk ,		LINITI-			

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	ILEU	METE	R		FAIRHAVEN C	ONTROL	DATA LO	ÓĠ				.s: 4	9	DATE	19.12	$\alpha \in \mathbb{R}^{+}$
Time	9	30		310	SAMPLES - VOLUME	INF 50	PRI 50	EFFI/cc	F3 100	F4/22	R3 5	R4 5	A1 5	A2 5	12:12 A3 5	
Time	SSV	SSC	SSV	SSC	CRUCIBLE	19,427	21,2658	21, 2597	22,0324	21,5746	21.3155	21.71.29	21 4589	21 1.221	31 772-	
0	1000	4			WT. + SAMPLE	19 4250	21,2481	21 2590	22021	2/ 5721	2/ 22-5	21 7700	2,1000	2. 1	21700	
5	900		;		CRUCIBLE WT.	· 0047	10037	10007	10009	10009	10350			10285		
10	800					84	54	7	9	9	7,000		4500	5700	3920	
15	700			!	DIFFERENCE PRE-			· .						7		
20 25	620 550						<u> </u>				[					
30	500				CRUCIBLE WT. + SAMPLE	*	'									
40	440	· · · · ·			WT. POST									•	ļļ	
50	400				FURNANCE								an a			
60	370				DIFFERENCE		1	•								
		-			VOLATILE						a statu				- <u>1</u>	
- 123	A	1	2	3	PRE-FURNACE									· ·	· ·	
3.04.5 3.0	T C				VOLATILE FIXED SOLIDS			········		· · · · · · · · · · · · · · · · · · ·		1.14	18. J			
1-234	R	1	2 3	4	FIXED SULIDS		1 1									
	S			· I	COLIFORM	BACTERI	A		, I				_			
5.5 8.0	c	• .			SAMPLE	COLON		100mL		%Rer	noval	84-	7		X 100	= 929
1 2 3 4	D	1	23	4	ß	0				06 0	D	چر احد ا	t 84-	<u>c</u> 4		10 00
•	ō				100	0				%P <b>r</b> 11	пагу ке		07-	<u>74</u>	X 1	00 = 35 Z
1234	B	1	2 3	4	. 150		<u> </u>			lb/da	y RAW 8	3.34 x 🕫	4 x 3	~~~ z C	-79-7 <b>-</b> 1	= 92 % 00 = 35 %
		. '	2 0	4	·	1/250	× <u>r</u>					~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~			6,130	-
¥ '	D I						) i Z			i in/da	IV PRIX	<b>34 Y S 1</b>	ィモマ	9 -	ITCL.	
¥ '	D O							3.44		],	<i>iy</i> i <i>i</i> . 0.	J + A /	-	-	1129	
5.0 6.9 6.9	0				CTADT.			100	n:[ ]	lb/da	ay PRI. 8. ay EFF. 8	.34 x 7	× 3.	9 ,	7,75 Ģ 727	
5.3 6.9 6.9	ō				START: //:00			.49	n:[]	lb/da	ay EFF. 8	.34 x 7	× 3.;	9 = 15,	227	
5.3 6.9 6.9 INF.	0 NOTE TEMF	13	40		11;00			1100	p <i>n</i> [	/ lb/da MLSS	ay EFF. 8 5 8.34 x .	.34 x 7 467 x 3	× 3.; 3920	9 = 15,	77 767	
5.3 6.9 6.9 INF.		13.	7 200		FINISH: 11:17			7.44	pr://	/ lb/da MLSS	ay EFF. 8 5 8.34 x .	.34 x 7 467 x 3	× 3.; 3920 = 12	9 ,	227 267	
5.3 6.9 6.9 INF.	O NOTE TEMF A1 pH	: 13. : 6	00 kg		FINISH: 11:17			5.44 1700	pr#] )	MLSS SVI_ CF_	ay EFF. 8 5 8.34 × . <u>1000 ×</u> 3 3,	.34 x 7 467 x 3	× 3.; 3920 =/2 =/3		227 267	
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5.3 6.9 6.9 INF.	O TEMF A1 pH A2 pH	: 13. : 6	A Z Z		FINISH: 11:17				pru] )	/ Ib/da MLSS SVI _ CF SA	ay EFF. 8 5 8.34 × . <u>1000 ×</u> 3 3,	.34 x 7 467 x 3 500 920 920 920 920 920 920 920 920 920 9	× 3.; 3920 =/2 =/3		227 267 : !/ml	

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	SET	TLEC	MET	ER		li fai	RHAVEN C		ΠΔΤΔ Ι	0Ġ			INITIAL	e. 1/	10	DATE			
1.			2		2.0	SAMPLE	S - VOLUM	UNFL 50	PRILSO	EFFLing	F3lico	F4 140						24115	<u> </u>
	Time		_		V SSC	CR	UCIBLE	1 195	1	1	10000	1 - 100	1015	17415	14113	1/2/3	17012	╉┈┈╬╼	<b>_</b>
	0	1000					SAMPLE												1
-	5	380						<u>19.4294</u>	21.7855	21.4370	21.6132	21.7202	21.772	22.1162	21.59/2	21.2757	21264	<u>‡ /</u>	
	10	300		_		CRUC	IBLE WT.	194200	0000	in unes						•	21. 250	1 /	
	15	270		+		זפיפות	ENCE PRE	0032	21.2827	21 +357	21.649	21.7/70	21,2562	22.038	21.3737	21,261	24	<u> </u>	_
	.20	240		- <u> </u>	1		RNÁCE	64	52	·.09.13 13	13	.0032	1000	1082	1.0155	0147	,0134.		•
	25	220					UCIBLE	10.7	172		<u> </u>	- 52	7,200	16600	13/00	129 <i>4 0</i>	2630	<u> </u>	-
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ļ	50	200			1	FUF	NANÇE												
	60	190	۱ <u>.</u>			E .	ERENCE ·		[	· · · · ·				k			<u> </u>  · ·		
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1	23	A	1	. 2	3		URNACE									1	<u>.</u>		
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40	2020 234	C	ļ		<u></u>	FIXE	SOLIDS			<u> </u>				· .	<b>н</b> .	-	<u> </u>	1. /	
F .	<b>x</b> 3 4	R	11	<b>?</b> :	3 4						, <sup>1</sup>			N.2					_
	3,0	S C										%Ror	noval	64 -	13		v 10	n = 80	%
1	2 3 4	D	1	2	3 4	<u> </u>	MPLE	COLON		(100mL		701361	10441	<u>o / _ /</u>	<u> </u>		^	0- 0 /	
l.'	- • 1	ō	'	~ .	Ŭ. T			<u>-</u>				%Prir	nary Rei	moval	(4	52	x	10= <i>80,</i> 100= /	9%
		в				,				·····				<b>.</b>	64	4 ·			/-
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0.6	5 8 5 8	0				ľ				· · · · ·		, by ue	iy Fixi. 0.	.5 ~ ~ 5 /	~x /·		5,165		
												lb/da	y EFF. 8	.34 x / j	3 × 7.	3 =	791		
• *-,						START:									-				
÷	I											MLSS	58.34 x .	.467 x 🎗	630	= 10	; 733		
•		NOTE		-		FINISH:				-		51/1	1000 -	210	- >	g ml/	-		
		TEM										341	26	210	/	0 11/2	5		
		<u>A1 pl</u>		-		OUT:								80				,	
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	TLEO	17	<u>K</u>		FAIRHAVEN C	ONTROL	DATA L	DG	•		INITIAL	.s: K.	$\mathcal{W}_{-}$	DATE:	12 12	311	5
Time			ssv		SAMPLES - VOLUME	IN- 50	PRI <i>50</i>	EFF/00	F3 /10	F4 100	R3 5	R4 5	A1 5	A2 5	A3 5		
			<u> 33</u>	550		21.28:2	20.6036	19,1000	19,5582	16,5818	21,5125	19,4882	20,9949	19 1972	17.7/09	1	
0	1000	340			WT. + SAMPLE				•	i .			[ , , , , ,		111001	(	
	890				CRUCIBLE WT	A1 0000								1.			
	780 680		<u> </u>			21,2825	20,6020 .0076 .32	17.0998	19,5575	16.5813	21,4915	19,4263	20,987	17.545	17.7358		
	600	<u> </u>	┍━━━┼╸		DIFFERENCE PRE- FURNACE	74	27	,0002	10007	.0005	,021	10619	:0192	,0308	,0251	.(	
	540				CRUCIBLE			<u> </u>	7	، ف	4,200	12,380	3,840	6,160	5,020	}	
	490		. 1		WT. + SAMPLE						<b>.</b>					Ĩ	
	420				WT. POST	-		····		<u> </u>			l				}
	380				FURNANCE												
60 ,	350	·			DIFFERENCE									l <u>.</u>		/	
123	- A (				VOLATILE	•	- I			· · ·					- <u>1</u> 2	- 1	
1 2 3	A T	1 ·	2	3	PRE-FURNACE	74	32	2	7	ز سی	4 26	10	2015	1.110		<del>{</del>	
2.5 4.0 3.0	ċ				VOLATILE FIXED SOLIDS	11.			1	<u> </u>	7,200	12,580	5×70	6,160	5,030	$\rightarrow$	1
2,5 4,0 3,0 4-2-3 4	Ř	1 2	2 3	4	FIXED SULIDS									·		į	
	S		-	i ir							•	- A.A.					
	-					ACTER	Δ										
2,75 10,0					COLIFORM E SAMPLE			:  00ml		%Ren	noval	74 – J	٤		x 100	1= 93	770
7,75 10,0 1 2 3 4	C  · D	1 2	2 3	4		COLON		: 100mL							x 100		
<u>7,8 10,0</u> 1 2 3 4	C D O	1 2	3	4	SAMPLE			00mL									
	C D O B							00ml.		%Prin	hary Ren	noval <u>7</u>	7 <u>4</u> 74	32	×1	ئ= 00	
	C D O B	1 2		4	SAMPLE			: 00ml.	•	%Prin lb/da	bary Ren y RAW 8	noval <u>7</u> .34 x 7	7 <u>4</u> 74 1 × 3.	32 19 =	×1 196°	ئ= 00	
1 2 3 4	C D O B A D							00mL	•	%Prin lb/da	bary Ren y RAW 8	noval <u>7</u> .34 x 7	7 <u>4</u> 74 1 × 3.	32	×1 196°	ئ= 00	
1234	C D O B A D							00ml.	•	%Prin Ib/da Ib/da	nary Ren y RAW 8 y PRI. 8.3	noval <u>7</u> .34 x 7 34 x <i>3</i> =	74 <u>-</u> 74 74 74 74 74 74 74 74 74 74 74 74 74	32 19 = 19 =	×1  96* 85!	ئ= 00	
1234	C D O B A D			4	SAMPLE			00ml.	•	%Prin lb/da lb/da lb/da	hary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3	noval <u>7</u> .34x 7 34x 32 34x ス	74 - 74 1 × 3. 2 × 3. × 3.1	32 19 = 19 = 19 = 5	x1  96* 85  ;3	ئ= 00	
1 2 3 4 0,2 5,5 6,7	C D B A D O	1 2		4	COLIFORM E SAMPLE			00ml.	•	%Prin lb/da lb/da lb/da	hary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3	noval <u>7</u> .34x 7 34x 32 34x ス	74 - 74 1 × 3. 2 × 3. × 3.1	32 19 = 19 = 19 = 5	x1  96* 85  ;3	ئ= 00	
1 2 3 4 2,2 5,5 6,7	C D B A D O O	12	3	4	SAMPLE				•	%Prin lb/da lb/da lb/da MLSS	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4	noval <u>7</u> .34 x 7 34 x <i>3</i> 34 x ス 467 x <i>5</i>	74 <u>-</u> 74 4 × 3. 2 × 3. × 3.1 ;020 =	32 19 = 19 = 19 = 3 19,55		ئ= 00	
1 2 3 4 2,2 5,5 6,7	C D D D D D O O E M P: C C D D D D D D D D D D D D D D D D D	1 2	3	4	SAMPLE START: FINISH:			00ml.		%Prin lb/da lb/da lb/da MLSS	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4	noval <u>7</u> .34 x 7 34 x <i>3</i> 34 x ス 467 x <i>5</i>	74 <u>-</u> 74 74 74 74 74 74 74 74 74 74 74 74 74	32 19 = 19 = 19 = 3 19,55		ئ= 00	
1 2 3 4 0,2 5,5 6,7	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START:			00ml.	•	%Prin lb/da lb/da lb/da MLSS SVI	nary Ren y RAW 8 y PRI. 8.: y EFF. 8.: 8.34 x .4 1000 x 4 57 c3	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 /90	74 <u>-</u> 74 74 2 × 3. 2 × 3. 3 ×	32 19 = 19 = 19 = 1 19 = 5 7 ml/g		ئ= 00	
1 2 3 4 0,2 5,5 6,7	C D D D D D O O E M P: C C D D D D D D D D D D D D D D D D D	1 2	3	4	SAMPLE START: FINISH:				•	%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8. 8.34 x 4 5.000  x 4 5.000   x 4 5.00000 x 4 5.0000 x 4 5.00000  x 4 5.00000 x 4 5.00000 x 4 5.000000000000000000000000000000000000	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. × 3. ; 020 = -= 98 -= 1,6	32 19 = 19 = 19 = 3 19,55 7 ml/g 73 mg/l	x1  96 85  53 2	ئ= 00	
1 2 3 4 0,2 5,5 6,7 INF. 7	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START: FINISH:			00ml.	•	%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8. 8.34 x 4 5.000  x 4 5.000   x 4 5.00000 x 4 5.0000 x 4 5.00000  x 4 5.00000 x 4 5.00000 x 4 5.000000000000000000000000000000000000	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. × 3. ; 020 = -= 98 -= 1,6	32 19 = 19 = 19 = 3 19,55 7 ml/g 73 mg/l	x1  96 85  53 2	ئ= 00	
	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START: FINISH:			00ml.	•	%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4 5, 6 5, 6 3	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. 2 × 3. 3 × 3. 2 ×	32 19 = 19 = 19 = 3 19,55 7 ml/g 73 mg/l	x1  96 85  53 2	ئ= 00	
1 2 3 4 0,2 5,5 6,7	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START: FINISH:				•	%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4 5, 6 5, 6 3	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. 2 × 3. 3 × 3. 2 ×	32 19 = 19 = 19 = 1 19 = 5 7 ml/g	x1  96 85  53 2	ئ= 00	
1 2 3 4 0,2 5,5 6,7	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START: FINISH:			00ml.		%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4 5, 6 5, 6 3	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. 2 × 3. 3 × 3. 2 ×	32 19 = 19 = 19 = 3 19,55 7 ml/g 73 mg/l	x1  96 85  53 2	ئ= 00	
1 2 3 4 2,2 5,5 6,7 INF. 7	C D O B A D O O E MP: 1 pH:	1 2	3	4	SAMPLE START: FINISH:			00ml.	•	%Prin lb/da lb/da lb/da MLSS SVI CF	nary Ren y RAW 8 y PRI. 8.3 y EFF. 8.3 8.34 x 4 5, 6 5, 6 3	noval <u>7</u> .34 x 7 34 x 3 34 x 2 467 x 5 <u>190</u> 20	74 <u>-</u> 74 74 2 × 3. × 3. ; 020 = -= 98 -= 1,6	32 19 = 19 = 19 = 3 19,55 7 ml/g 73 mg/l	x1  96 85  53 2	ئ= 00	

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•	•									•			•			
SI	ETTLEO		ER		FAIRHAVEN C	ONTROL	DATA L	OG			INITIAL	e. 1.	10			· · · · · · · · · · · · · · · · · · ·
Time		10	<u> </u>		SAMPLES - VOLUME	INF 50	PRISO	EFF 100	F3 /00	F4 100	R3 5			DATE:	1212	2115
	SSV	SSC	SSV	SSC	CRUCIBLE			<u> </u>		<u></u> _						<u>├</u>
0	1000	71			WT. + SAMPLE	16.5846	20.6041	19,4268	21 1.26	o Linza	10 100	. in	- 1 AOL			
5 10	850 750		i		CRUCIBLE WT.	16 5813		19:4262						1.	4	
15	650				DIFFERENCE PRE	.0033	,0021	.0006	0007	0010	0107	04917	047	19,1000	20 975	
20 25	570				FURNACE	66	42	6	2	10	2140	139.40	2940	3940	1540	
30	480			 		-					<u> </u>				7.97	
40	4.30				WT. + SAMPLE WT. POST	 	<u>_</u>				-		· ·			
50	B90				FURNANCE			·								
60	370				DIFFERENCE						·			<u> </u>		
					VOLATILE											· ·
123	A	1	2	3	PRE-FURNACE									1		· · · · · · · · · · · · · · · · · · ·
3.5 5.03	5 c				VOLATILE					•						
1234	4 R	1.	2 3	4	FIXED SOLIDS								· · ·			
, -		•	÷ V	_ ī	COLIFORM	ACTED			r e			19				
1.5	d c l	•			SAMPLE	COLON		: 100mL		%Ren	oval	66 .	- 6		v 100	= 91%
1 2 3 4	4 D ]	1 ;	2 3	4		00201	10 77									
•.	0			-						%Prin	nary Ren	noval	6 - 4	12	X 1	.00 = 36%
1234	<u>B</u>   A	1 2	2 3	4	· · · · · · · · · · · · · · · · · · ·					lb/day	V RAW S	34 x ~	66		1141	.00 = 36% 16/dar
1.207			డ ప	4	· · · ·				•							1
092761	5 0									lb/da	y PRI. 8.3	34 x 4/	ストス	,99 = 1,	047	16/day
· ·						···· , ···	<u></u>			lb/da	v EFF. 8.	34 x <i>L</i>	xad	79 = 1-	50 15	Ider
, the					START:											· 7
· ·	NOTES			ļ	FINISH:		-				· ·			= 21		
INF	A1 pH	14.								. svi_1	1000 x	480	_= 8	⟩ ml/g		
	A2 pH A3 pH	6	ź		OUT:					CF	ۍ کې <u>4 کې کې</u> 3. ۲	40 5	_= /5	> ml/g 8.3mg/l,	/ml	
<u>-</u>		<u>. i e, f</u>	<u> </u>							SA8	3.34 x .4	67 x 554	<u>#0</u> =(	2/0	ays )	
. •		• .			· ·					٤	3.34x <i>4</i> 2	2×2.9	29			

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SET	TLEO		R	· · · ·	FAIRHAVEN C	ONTROL		OG .			INITIAI	_s: v	0	DATE		
Time		30			SAMPLES - VOLUME	INF 50	PRISO	EFF 10	F3 100	F4 100	R3 5				12 12/ A31 C	75
0	SSV  1000		SSV	ssc	CRUCIBLE	1	i i	i i	i i		1 ·			·		
5 10	<u>860</u> 150				CRUCIBLE WT.	16.5864 16,5813		1	1	1	•	1	1	•		
15	650	,			DIFFERENCE PRE	,0047	,0000	21 4914	20006	20.995/	217171	19.0996	19,5651	21.2826	20 6021	
and the second se	570					94	48	6	6	>	1980	24920	5760	6540	5080	
30	470		<u>.</u>		WT. + SAMPLE		•				-					
50	410 370				WT. POST FURNANCE						·					
	250				DIFFERENCE VOLATILE											·····
123	A T	1	2	3	PRE-FURNACE VOLATILE											
54.730	C R	1	2 3	4	FIXED SOLIDS											
1.5 20.	s C	1			COLIFORM E SAMPLE			: 100mL	r r	%Ren	noval	94	-6		x 100	= 94%
234	D O B	1 ;	23	. 4	<u> </u>	2/50				%Prin	nary Rer	noval{	94 <u>94</u> 	48	x 1	= 94% 00=49
234	Ā	1 :	2 3	4	. 100	2/10			•	lb/da	y RAW 8	8.34 x 94	412	93 =	229	>
> 3.26.5						·				ib/da	y PRI. 8.	34 x 48	X 2.9	33 =	1173	
					CTADE:					lb/da	y EFF. 8.	34 x 6	x 2.4	73 =	1466	
[]	NOTES		—		START: 1:00									: 197		
INF.	TEMP A1 pH	14.			FINISH:					.SVI	1000 x . 49	5080	_= jo8	.09 mi∕g		
	A1 pH A2 pH A3 pH	6.6			OUT: 12:45									33 mg/l		
<u> </u>	<u>va hu</u>	. <b>16. 5</b>						<b>^</b>		SA	<u>3.34 x .4</u>	<u>67 x 5 c 8</u>	0 =	170	AYS	
		• .			-					:	B.34x 42	3 X				

 ${\bf t}_{1}{\bf t}_{1}$ 

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. SETTLEOMET	ER			ROL DA	and the second sec	يببانسه						12/18	
9:05 :	SAMPLES '	INF 50	A3 5ml	PRI <b>50</b>	EFF 100	F3	$[\ge]$	F4	100	<u>R3</u>	_5ml	R4 5m1	<u>A7 5mĩ</u>
ME SSV SSC SSV SSC	CRUCIBLE		•				) •			\			
0 1000	WT. + SAMPLE						)	21.5	364	ļ	(	21.3482	17.7619
5 740.	CRUCIBLE	22.0386	21.782.4	19.5594	21.4362	1 /		•	57.56		)	21,2509	17, 735
10 590	WT	22.0339	217564	19:55)2 .0022	21.4357	┼─┼	· · · · · ·	01.0	003		f	,0973	.0264
15 490	DIFFERENCE PRE-FURNACE	.004>	5200	1 .	11	$  \rangle$			8	÷		19460	5280
20 430	CRUCIBLE		3	-1-1			1		<u></u>				<b>!</b> .
25 400 · · · · · · · · · · · · · · · · · ·	WT. + SAMPLE		1		1		} .	· ·			•		
30 <b>3</b> 70 40 <b>3</b> 40	WT. POST	-						۱.			•		:
50 330	FURNACE		<u> </u>			·   ·	<u>  · · ·</u>			<u>  · ·  </u>	<b>\</b>	<u></u>	
50 <b>300</b>	DIFFERENCE	ľ			ļ						1.		ŀ .
1 2 3 A 1 2 3	VOLATILE		·			_ <b>_</b>	-				}		· · ·
0 3.0 3.0 c	PRE-FURNAGE						1		•	1. 1	(	• "	
12 × 4 R 1. 2 3 4			· <b> </b>				+				7.		·
$\frac{10.0 \text{ C}}{112113114 \text{ D}}$	FIXED SOLIDS	BACTERI	۵.	 •	MICRO	ORG	ANISH	4	•		· · · ·	+NOT	FS
1174/174/174 0 1 2 3 4		LONIES		lm00		ROUP							
2 3 12 4 2 3 4		•	<u> </u>		4							INF. TER	<u>e. 14</u> .4
2 3 A A 1 2 3 4 4 4 4 7 2 0					AMOEB	UIDS	ે પ્રિડે		•			Ål ph	6.9
RESIDUAL CL Z									·	<u> </u>		мі рі	6.6
TIME FLOW LEVEL		· · · · · · · · · · · · · · · · · · ·			_]. _] FLAGE		FS (	(D.)				A2. ph	
: plant		· · · · · · · · · · · ·	<u></u>			, ,	-)	. من ا	¦ .		. 1	SEP	CAGE
			^`		FREE	:	•	۲.	1			Fairbave	<u>n</u>
				·	SWIMM		r	-+ *			•		•
		· · · · · · · · · · · · · · · · · · ·		•	CILIATE			~	<u> .</u>			Mattapoi	sett-
·····		·····			STALK	ED	12.	~	, .	•		Marion-	
:	START:			;	CILIATE	<u>∃S </u> ]	<u>5</u> ~	$\sim$	· [ ·		· · ·	Rochests	•r-
4vg_ H 2 S	FINISH:			•	ROTIFE	RS	\$Q2				-	{ .	• •
	\			· .				002	-		······	Acushne	·
	OUT:		•		WORM	S'	A	S		•			total
	<u>]]</u>	·	·		<u></u>							. <b>ل</b>	•
· IOL	M. NITROGEN-	NITRAI	)E— .	.NITRIT	E-*		ALKA	MWY.	LI~				

21. 286) Al 5ml <u>21. 2618</u> .0249

1980

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I Removal 94 - 11 x 100 - 88% 2 Primary Removal 94 - 44 x 100 - 53% 16/day RAW 8.34 x 94×3.49=236 16/day PRI. 8.34 x 44 x 3.49 = 1281 1b/day EVN. 8.34 x 11 × 3.49 = 320 MLSS. 8-34 x -467 x 5200 = 20253 SVL 1000 m 370 = 7/ ml/g CF <u>5200</u> - 1)33 mg/1/ml SA 18.34 x .467 x 5200 8.34 x 44 x 349 16 DAYS

SE	TTLEO	METE	R		FAIRHAVEN C								16		12.11	
т	9	40	·		SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3 🗙	F4 100	R3)>	< R4 4	A1 5	A2 5	A3 5	WAS 5
Time	SŚV	Śsc	ss∨	SSC	CRUCIBLE				- 1							
0	1000				WT. + SAMPLE	21.6149	17.7382	19.4265		21,2621		19.64	421.7419	19.5969	22.0573	21.534>
5	540				CRUCIBLE WT.				1		T					
10	440					21,6123	12. 337	19.4258	L(	21.2612						21.4913
15	370				DIFFERENCE PRE			,0007	`	,0009	I	,090	0.0248	0304	.0240	.0434
20	340				FURNACE	52	56	>		9		1800	0 4960	6080	4800	8680
25	320				CRUCIBLE		1									
30	300				WT. + SAMPLE	21.6149	<u>17.)382</u>	19.4265		21.2621		19.64	421.7418	19.596	22.0575	21.534>
40	280				WT, POST			·		1	]			ļ		
50	270				FURNANCE			19.4758		212612						21,5008
60	260			Į	DIFFERENCE	,002.6	1.	.000>		.0009	]					.0339
		-			VOLATILE	52	56			9		984	02960	3580	2840	6780
123	A	1	2	3	PRE-FURNACE				$  \rangle$							
	T				VOLATILE .				/			<u> </u>				
2.73.22)	) C				FIXED SOLIDS	Ø	ø	Ø		D		816	0 2000	2500	1960	1900
1284	1 R	1	2 3	4									<u></u>			
	S				COLIFORM	BACTERI				<b>IAGNET</b>				NOTES		
ST 12.					SAMPLE	COLON	lies #	/100mL	N	ILSS A1	2.4	15	INF	TEMP:		
1 2 3 4	4 D	1	2 3	4						ALSS A2				A1 pH		
	0				·					ALSS A3	2.2	12		A2 pH		
	B									RAS-3	<u> </u>			A3 pH:	6.6	
1 2 3 4	A F	1	2 3	4						RAS 4				L ËFF		
	D									WAS	1.0	25	AKA	LINITY		
040.42	<u>40</u>															
					START:							·				
					FINISH:								•			
									Į							
					QUT:				1	<i>'</i>						
									]							

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) × 1,000,000

TOTAL NITROGEN - 7.2 NITRATE - 5.43

Ámmonjo NITRIFE - O. 150

Al 5ml

I Removal  $\frac{52-7}{52} = 100 = 87\%$ 2 Primary Removal  $\frac{52-54}{52} = 100 =$ Ib/day RAW 8.34 x  $52\times283 = 1245$ Ib/day PRI. 8.34 x  $54\times283 = 1245$ Ib/day PRI. 8.34 x  $54\times283 = 1293$ Ib/day ENF. 8.34 x  $7\times2.83 = 168$ MLSS. 8.34 x .467 x 4800 = 18695SVI  $\frac{1000 \times 300}{4800} = 63 \text{ m1/g}$ CF  $\frac{4800}{2.7} = 1378 \text{ mg/l/ml}$ 

 $\frac{54 + 8 - 34 \times -467 \times 4800}{8 - 34 \times 54 \times 2.85}$  [4] DAYS

SE	TLEO		R		FAIRHAVEN C						ITIAL		10	DATE:		
Time	9	05		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF100	F3 🔀	F4 /00 R	3×	R4 5	A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE						Ì					
0	1000	<u> </u>		1	WT. + SAMPLE	21.7592	17.7382	19.4269		22.0344		21724	21.2881	19 5955	19.534	21.6411
5	640			ĺ	CRUCIBLE WT.	T,	,									
10	490	ļ				<u>21.7563</u>				22,0333	1.					21.6128
15	430				DIFFERENCE PRE	· · ·		.0004		.0014	]					,0283
20	390				FURNACE	58	50	4	1	.14		11080	5320	5820	5 <b>3</b> 80	5660
25	360				CRUCIBLE			· .			1					
30	340				WT, + SAMPLE	21.7592	17.7382	19.47.69	1	23.0347	1	21.1724	21.288,	19.3153	19.534	21.6411
40	300				WT. POST		1.1.1			_ ~				a 130		
50	290				FURNANCE	QJ,7563				20,0333						21.6187
60	290				DIFFERENCE	.0029	.002.5			.0014	1					.0724
					VOLATILE	58'	50	4	_(	14	(	5940	3100	1820	3060	A480
123	A	1	2	3	PRE-FURNACE						1			-		1
	Т				VOLATILE						<u> </u>					
27 3.02)	) C				FIXED SOLIDS	Í	Ø	Ø	1	l	1	5140	2220	4000	2220	1180
1284	R	1	2 3	3 4							1					-
	s				COLIFORM	BACTERI	A	:	M	AGNETITE	E (mg)	(L)		NOTES		
6.	<u>s c</u>				SAMPLE	COLON	IIES #	/100mL			2.3.		INF	. TEMP:	14.5	
1 2 3 4	D	1	2 3	3 4						ALSS A2 🔮				A1 pH:	7.0	
	0								N	ILSS A3 🞜	1.32	Z		A2 pH:		
	В									RAS 3				A3 pH:	6.3	
1 2 3 4	A	1	2 3	34						RAS 4	<u>4. &gt;:</u>	3		LEFF		
	D									WAS a	<u>2.53</u>	3	AKAL	INITY		
0.4 1.0 2.0	o															
					START:											
					FINISH:											
					OUT:											
									-							

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 6. // NITRATE -

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NITRITE -

I Removal  $\frac{58-4}{58} \times 100 = 9.3\%$ 7 Primary Removal 58 - 50 x 100 - 14% 16/day RAW 8.34 x 58x2.41 = 1166 16/day PRI. 8.34 x 50 \$ 2.4/ = 1005. 1b/day HFT. 8.34 x 4 x 2.4.1 = . 8.0 MLSS, 8-34 x -467 x 5280 = 20564  $\frac{\text{SVL}}{5280} = 64 \cdot \text{m1/g}$ CF <u>5280</u> = 1956 mg/1/ml SA :8.34 x .467 x 5280 20 DAYS

Al 5ml

	<u>8</u> 0			SAMPLES - VOLUME									DATE:		
	200			SAMPLES - VOLUME	INF 50	PRI 30	EFF ∕∞	F3 🗡	F4 100	R3 🖌	R4 5	A1 5	A2 5	A3 5	WAS
000	200	SSV	SSC					ý		)					
				WT. + SAMPLE	21.4984	21.3191	21.6131	/	19.4235		22 0926	19.5809	13.7644	21.7876	19,5963
740					· · · · · · · · · · · · · · · · · · ·			1		1	<u> </u>	////			//////////
00					21.4926	21.7173	21.6128		19.4212		22 031/2	19 5582	133364	21 2622	19,5668
40				DIFFERENCE PRE-	,0058	,0018	,0003	1							
00				FURNACE	116	36	3								
20				CRUCIBLE	•						// • • • -	<u>,                                    </u>	57800		
50				WT. + SAMPLE	21.4984	21.5191	21-6131		19.425		22.0926	19.5809	13.3644	21.2836	19.596>
30				WT. POST		•				1	<u>, ,,,,</u>				
				FURNANCE	21.4926	21 7173	21.6128		19.4272	ļ	22.0620	19 5618	13.7485	21.2232	19 5729
90				DIFFERENCE	.00.58	.0018	.0003		.0003		. 0306	,0131	0159	.0144	,0238
				VOLATILE	116	36	3		3						
A	1	2	3	PRE-FURNACE				1		í	10100				
Т				VOLATILE				]							•
C				FIXED SOLIDS	Ø	Ø	ĺ	ĺ	æ	$\langle$	5560	1920	2420	2200	1220
R	1	2 3	4												, , - ,
s				COLIFORM I	BACTERI	Ą	:	M	AGNETI	TE (mg	/1)		NOTES		1
C				SAMPLE	COLON	IES #/	'100mL								ĺ
D	1 .	2 3	4				·	M	LSS A2	2.82			A1 pH:	6.9	
0													A2 pH:	6.8	ĺ
₿									- RAS-S		~-~				1
A	1 ;	23	4						RAS 4	5.3	5	FINA			
D									WAS	0,8	Ď	AKAL	INITY		
0			:												•
				ISTART:											
				FINISH:											
				001.											
								l							
	00 40 00 00 00 00 00 00 00 00	20       40       20       20       20       30       20       30       20       30       20       30       20       30 <td>00     00       40     00       00     00       30     00       30     00       30     00       30     00       70</td> <td>00       0       0         90       0       0         20       0       0         30       0       0         30       0       0         30       0       0         30       0       0         30       0       0         90       0       0         90       0       0         90       0       0         90       0       0         90       0       0         8       0       0         8       0       0         8       1       2       3       4         0       0       0       0       0       0         8       1       2       3       4         0       0       0       0       0       0</td> <td>20       CRUCIBLE WI.         20       DIFFERENCE PRE-         20       CRUCIBLE         20       CRUCIBLE         30       CRUCIBLE         31       2         32       COLIFORM I         33       COLIFORM I         34       COLIFORM I         35       CRUCIBLE         34       CRUCIBLE         35       CRUCIBLE         36       CRUCIBLE         37       CRUCIBLE</td> <td>00       <td< td=""><td>00       <td< td=""><td>Do       CRUCIBLE WI.       11/926       21/1/3       21.6/28         40       DIFFERENCE PRE       .0053       .0013       .0003         20       CRUCIBLE       .0055       .0013       .0033         20       FURNANCE       .0055       .0013       .0033         20       DIFFERENCE       .0055       .0013       .0033         20       PRE-FURNACE       VOLATILE       .0055       .0013       .0033         20       Startile       FIXED SOLIDS       Ø       .0013       .0033         20       Startile       Startile       .0013       .0033       .0033         20       Startile       .0013       .0013       .0033       .0033       .0033         21       <t< td=""><td>20      </td><td>Do       CRUCIBLE W1.       1/4/926 (2) /)/32 (6/28)       (9.49)2         40       DIFFERENCE PRE       0058       0013       0003       0003         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       WT. + SAMPLE       21.4984       21.591       1.6131       19.425         30       WT. POST       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.4984       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         21       VOLATILE       1/6       3.6       3       3         7       VOLATILE       FIXED SOLIDS       Ø       Ø       Ø         8       COLIFORM BACTERIA       MLSS A3      </td><td>Difference       Difference       Presson       Presson&lt;</td><td>Do      </td><td>DO       CRUCIBLE W1.       214/926 (2) 7/3 (2) 6/28 (19.45)2       22.03/2 (9.55)2         90       DIFFERENCE PRE       0.05% (0.01%) (00.03)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       19.4325       22.0426 (9.5007)         90       WT. + SAMPLE       21.4934 (2).5191       19.4325       22.0426 (9.5007)         30       WT. POST       FURNANCE       9.4934 (2).5193       19.4325       22.0426 (9.5007)         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00003       .00003       .00003         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00</td><td>DO      </td><td>20       CRUCIBLE W1.       21/9/26 (21/7)/3 (21.5/28)       19.45/2       22.0242 (9.556) (7.534 (21.2623)         40       DIFFERENCE PRE       .0053       .0003       .0534       0.23       .0230       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202</td></t<></td></td<></td></td<></td>	00     00       40     00       00     00       30     00       30     00       30     00       30     00       70	00       0       0         90       0       0         20       0       0         30       0       0         30       0       0         30       0       0         30       0       0         30       0       0         90       0       0         90       0       0         90       0       0         90       0       0         90       0       0         8       0       0         8       0       0         8       1       2       3       4         0       0       0       0       0       0         8       1       2       3       4         0       0       0       0       0       0	20       CRUCIBLE WI.         20       DIFFERENCE PRE-         20       CRUCIBLE         20       CRUCIBLE         30       CRUCIBLE         31       2         32       COLIFORM I         33       COLIFORM I         34       COLIFORM I         35       CRUCIBLE         34       CRUCIBLE         35       CRUCIBLE         36       CRUCIBLE         37       CRUCIBLE	00       00 <td< td=""><td>00       <td< td=""><td>Do       CRUCIBLE WI.       11/926       21/1/3       21.6/28         40       DIFFERENCE PRE       .0053       .0013       .0003         20       CRUCIBLE       .0055       .0013       .0033         20       FURNANCE       .0055       .0013       .0033         20       DIFFERENCE       .0055       .0013       .0033         20       PRE-FURNACE       VOLATILE       .0055       .0013       .0033         20       Startile       FIXED SOLIDS       Ø       .0013       .0033         20       Startile       Startile       .0013       .0033       .0033         20       Startile       .0013       .0013       .0033       .0033       .0033         21       <t< td=""><td>20      </td><td>Do       CRUCIBLE W1.       1/4/926 (2) /)/32 (6/28)       (9.49)2         40       DIFFERENCE PRE       0058       0013       0003       0003         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       WT. + SAMPLE       21.4984       21.591       1.6131       19.425         30       WT. POST       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.4984       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         21       VOLATILE       1/6       3.6       3       3         7       VOLATILE       FIXED SOLIDS       Ø       Ø       Ø         8       COLIFORM BACTERIA       MLSS A3      </td><td>Difference       Difference       Presson       Presson&lt;</td><td>Do      </td><td>DO       CRUCIBLE W1.       214/926 (2) 7/3 (2) 6/28 (19.45)2       22.03/2 (9.55)2         90       DIFFERENCE PRE       0.05% (0.01%) (00.03)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       19.4325       22.0426 (9.5007)         90       WT. + SAMPLE       21.4934 (2).5191       19.4325       22.0426 (9.5007)         30       WT. POST       FURNANCE       9.4934 (2).5193       19.4325       22.0426 (9.5007)         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00003       .00003       .00003         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00</td><td>DO      </td><td>20       CRUCIBLE W1.       21/9/26 (21/7)/3 (21.5/28)       19.45/2       22.0242 (9.556) (7.534 (21.2623)         40       DIFFERENCE PRE       .0053       .0003       .0534       0.23       .0230       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202</td></t<></td></td<></td></td<>	00       00 <td< td=""><td>Do       CRUCIBLE WI.       11/926       21/1/3       21.6/28         40       DIFFERENCE PRE       .0053       .0013       .0003         20       CRUCIBLE       .0055       .0013       .0033         20       FURNANCE       .0055       .0013       .0033         20       DIFFERENCE       .0055       .0013       .0033         20       PRE-FURNACE       VOLATILE       .0055       .0013       .0033         20       Startile       FIXED SOLIDS       Ø       .0013       .0033         20       Startile       Startile       .0013       .0033       .0033         20       Startile       .0013       .0013       .0033       .0033       .0033         21       <t< td=""><td>20      </td><td>Do       CRUCIBLE W1.       1/4/926 (2) /)/32 (6/28)       (9.49)2         40       DIFFERENCE PRE       0058       0013       0003       0003         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       WT. + SAMPLE       21.4984       21.591       1.6131       19.425         30       WT. POST       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.4984       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         21       VOLATILE       1/6       3.6       3       3         7       VOLATILE       FIXED SOLIDS       Ø       Ø       Ø         8       COLIFORM BACTERIA       MLSS A3      </td><td>Difference       Difference       Presson       Presson&lt;</td><td>Do      </td><td>DO       CRUCIBLE W1.       214/926 (2) 7/3 (2) 6/28 (19.45)2       22.03/2 (9.55)2         90       DIFFERENCE PRE       0.05% (0.01%) (00.03)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       19.4325       22.0426 (9.5007)         90       WT. + SAMPLE       21.4934 (2).5191       19.4325       22.0426 (9.5007)         30       WT. POST       FURNANCE       9.4934 (2).5193       19.4325       22.0426 (9.5007)         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00003       .00003       .00003         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00</td><td>DO      </td><td>20       CRUCIBLE W1.       21/9/26 (21/7)/3 (21.5/28)       19.45/2       22.0242 (9.556) (7.534 (21.2623)         40       DIFFERENCE PRE       .0053       .0003       .0534       0.23       .0230       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202</td></t<></td></td<>	Do       CRUCIBLE WI.       11/926       21/1/3       21.6/28         40       DIFFERENCE PRE       .0053       .0013       .0003         20       CRUCIBLE       .0055       .0013       .0033         20       FURNANCE       .0055       .0013       .0033         20       DIFFERENCE       .0055       .0013       .0033         20       PRE-FURNACE       VOLATILE       .0055       .0013       .0033         20       Startile       FIXED SOLIDS       Ø       .0013       .0033         20       Startile       Startile       .0013       .0033       .0033         20       Startile       .0013       .0013       .0033       .0033       .0033         21 <t< td=""><td>20      </td><td>Do       CRUCIBLE W1.       1/4/926 (2) /)/32 (6/28)       (9.49)2         40       DIFFERENCE PRE       0058       0013       0003       0003         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       WT. + SAMPLE       21.4984       21.591       1.6131       19.425         30       WT. POST       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.4984       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         21       VOLATILE       1/6       3.6       3       3         7       VOLATILE       FIXED SOLIDS       Ø       Ø       Ø         8       COLIFORM BACTERIA       MLSS A3      </td><td>Difference       Difference       Presson       Presson&lt;</td><td>Do      </td><td>DO       CRUCIBLE W1.       214/926 (2) 7/3 (2) 6/28 (19.45)2       22.03/2 (9.55)2         90       DIFFERENCE PRE       0.05% (0.01%) (00.03)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       19.4325       22.0426 (9.5007)         90       WT. + SAMPLE       21.4934 (2).5191       19.4325       22.0426 (9.5007)         30       WT. POST       FURNANCE       9.4934 (2).5193       19.4325       22.0426 (9.5007)         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00003       .00003       .00003         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00</td><td>DO      </td><td>20       CRUCIBLE W1.       21/9/26 (21/7)/3 (21.5/28)       19.45/2       22.0242 (9.556) (7.534 (21.2623)         40       DIFFERENCE PRE       .0053       .0003       .0534       0.23       .0230       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202</td></t<>	20	Do       CRUCIBLE W1.       1/4/926 (2) /)/32 (6/28)       (9.49)2         40       DIFFERENCE PRE       0058       0013       0003       0003         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       CRUCIBLE       1/6       3.6       3       3       3         20       WT. + SAMPLE       21.4984       21.591       1.6131       19.425         30       WT. POST       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.4984       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         20       FURNANCE       21.513       2.6138       19.425         21       VOLATILE       1/6       3.6       3       3         7       VOLATILE       FIXED SOLIDS       Ø       Ø       Ø         8       COLIFORM BACTERIA       MLSS A3	Difference       Difference       Presson       Presson<	Do	DO       CRUCIBLE W1.       214/926 (2) 7/3 (2) 6/28 (19.45)2       22.03/2 (9.55)2         90       DIFFERENCE PRE       0.05% (0.01%) (00.03)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       00.03       0.05% (0.22)         90       CRUCIBLE       116 (3.6) (3.0003)       19.4325       22.0426 (9.5007)         90       WT. + SAMPLE       21.4934 (2).5191       19.4325       22.0426 (9.5007)         30       WT. POST       FURNANCE       9.4934 (2).5193       19.4325       22.0426 (9.5007)         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00003       .00003       .00003         90       DIFFERENCE       .005% (0.01%) (0.0003)       .00003       .00	DO	20       CRUCIBLE W1.       21/9/26 (21/7)/3 (21.5/28)       19.45/2       22.0242 (9.556) (7.534 (21.2623)         40       DIFFERENCE PRE       .0053       .0003       .0534       0.23       .0230       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202       .0202

4

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 7. 55 NITRATE - 5.21

Annonia NITRITE -0.563

I Removal 116 - 3 x 100 - 9 % 2 Primary Removal 116 - 36 x 100 - 69% 16/day RAW 8.34 x 116x 2. 38 = 2689 16/day PRI. 8.34 x 36×2.98 = 835 1b/day EFF. 8.34 x 3 x2.98 = 69 MLSS, 8.34 x .467 x 5080 = 19 85  $\frac{5VI}{50\times0} = 69 \cdot mi/s$ CF <u>5080</u> = 2032 mg/1/ml 54 -34 x -467 x 36 8-34 x 5080 x 2.78 24 DAYS

Al 5ml

SET	TLEO	METE	R		FAIRHAVEN C					EST	INITIAL	.s: 🖊	9	DATE:	1211	41 15
<b>T</b> :	9	:00		:	SAMPLES - VOLUME	INF 50	PRISO	EFF /00	F3 🖌	F4 /00	R3 📈	R4 5	A1 5	A2 5	A3 5	WAS 5
Time		1	ssv	SSC					$\sum$	:	$\left \right\rangle$			19.154	ł	212885
0	1000				WT. + SAMPLE	22.0371	19 551	21.7172		19 3668		17 783	3152)	4	21.63%	
5	660				CRUCIBLE WT.		[									
10	540					22.0334		21.7164		19 5659						212616
15	460	L			DIFFERENCE PRE		4			.0009				,0283		.0269
20	430				FURNACE	74	62	8		9		9580	7260	5660	5020	5380
25	390	ļ			CRUCIBLE					- 110						
30	360	ļ			WT. + SAMPLE	22.0371	19.5596	21.7172		19.5668		17.7839	21.5274	19.4545	21.6372	21.2885
40	340	ļ		ļ	WT. POST			h								
50	310				FURNANCE	22.0337				19.5659						212665
60	300				DIFFERENCE		,0026		3	_0009		,0264				,0219
					VOLATILE	68	52	8		9		5280	4240	3220	2760	4380
123	A	1	2	3	PRE-FURNACE								•			
	T				VOLATILE				[							
1.0 3.0 3.0	_				FIXED SOLIDS	6	Ø	Ø		Ø		4300	3020	2440	2260	1000
1-3-2 4	R	1	2 3	3 4												-
6.0	S				COLIFORM			:		AGNET				NOTES		
		[			SAMPLE	COLON	IES #	/100mL		ILSS A1		-	INF	TEMP:		
1234		1	2 <sup>.</sup> 3	3 4	<u> </u>					ILSS A2				A1 pH:		
*	0				50	13/4		\$ 15		ILSS A3			. <u> </u>	A2 pH:		
	B	ļ			100	14/1	60 14	1/100			- 4.20	>		A3 pH:	6.5	
1234		1	2 3	34		<u> </u>				-RAS-4				L EFF	56	1
	D									WAS	0.3	6	AKAL	INITY	20	
0.40.91.9	0															
					······································											
					START: //: 0	5										
					FINISH:	5						•				
					OUT: //://											
					11.72	~										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -4.8

NITRATE -

Ammonie, NITRITE -

X Removal 74-8 x 100 = 89% Z Primary Removal 74-52 x 100 - 30% 16/day RAW 8.34 x >4 x 20; =1278 1b/day PRI. 8.34 x 52 + 207 = 898 1b/day EFF. 8.34 x 8 / 2.0 > = 138 MLSS, 8.34 x .467 x 5020 = 19552 SVI 1000  $\pm 5020 = 13944 \pm 1/g$  $\frac{cr}{3.0} = \frac{5020}{3.0} = \frac{16}{3} \frac{mg/1/m1}{mg/1/m1}$ SA 18.34 x .467 x 5020 8.34 x 52 x 205 22 DAYS

AI 5ml

SE	TLEO	METE	R		FAIRHAVEN CO	ONTROL	DATA L	0G - BlO	MAG	TEST	INITI	ALS: 🗹	0	DATE:	1211	1115
Time	8	:55			SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3				A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE				7		- / '	· · · · ·	1	1		
0	1000				WT. + SAMPLE	10000	1 h h - 0 /		(	100 11 1.1	-	. h		1000		
5	650					19_5647	<u>17.2328</u>	21 4928		19.4276		21 7672	<u> 2/_25<i>4</i></u>	17.57/3	20.629	21.6382
10	500		 		CRUCIBLE WT.	in m			$  \rangle$		1	ير فر ا		- 10		
15	450				DIFFERENCE PRE-	<u>19.5575</u> .0072	17.7355			19.4264		21.7/24	21.2616	19 507	20,602.5	21,6119
20	100	:		i	FURNACE	144		.000/		,0012						.0263
25	360		<u> </u>		CRUCIBLE	177	46	- 7		12		9960	6760	4920	4640	5260
30	350				WT. + SAMPLE	Acces		21.4928		10.11-20		. در هر م		10 10-		a
40	330				WT. POST	19.304/	17.7.3/2	21.4728		19.12%		21.7673	21.2754	17.2713	20059	21.6382
50	300					19.5575	13 3700	nilant		19.4264		12-00	01 2500	a seco		a
60	290				DIFFERENCE	17.3325	0023	0007				- W.1378	21. 193	17.5769	20.0/19	21.6158
	A/U				VOLATILE		-			,00/2	ł	.0274	.0206	.0198	.0/38	,0224
123		~	~	~		144	46	7	<u> </u>	12		5480	4120	2960	2360	4480
123		1	2	3	PRE-FURNACE				l l		]					
20 200	T					<u> </u>			ļ		1	141776				- N/1-0
32252.	> C R		2 3	4	FIXED SOLIDS	ø	Ø	Ľ	- {	Ð	1	7980	2640	1960	1880	780
1204	S	1	2 3	4			4									1
63								:		MAGNETI	<u>TF (u</u>	ig/L)		NOTES		
1 2 3 4			2 3	4	SAMPLE	COLON		(100mL		MLSS A1	<u>d.</u>	22	INF	. TEMP:		
1 2 3 4	ŏ		د ۲	4						MLSS A2		29	ļ	A1 pH:		ļ
	В			·					╎┝	MLSS A3		34	ļ	A2 pH:		
1 2 3 4		1	2 3	4						RAS3				A3 pH:	6.6	
1 2 3 4			2 3	4	· · · · · · · ·					RAS 4						
0.37.84.									L	WAS	0.	<u>56</u>		INITY		J
0.37.07.																x.
					OTADT.											
					START:											
					FINISH:											
					OUT:											
					i				l							

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T\$S TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 9.51 NITRATE -

NITRITE -

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I Removal  $\frac{144 - 7}{144} = 100 = 95\%$ 7 Primary Removal 144 - 46 x 100 - 68% Ib/day RAW 8.34 x 144x 211 = 2534 1b/day PRI. 8.34 x 46x 2. 11 = 809 1b/day EFF. 8.34 x 7x2.11 = 123 MLSS, 8.34 x .467 x 4640 = 18072  $\frac{\text{SVL}}{4640} = \frac{75 \text{ ml/g}}{4640}$  $CF = \frac{4640}{2.7} = \frac{1}{19} \frac{mg}{mg} \frac{1}{ml}$ SA :8.34 x .467 x 4640 8.34 x 46 x 211 22 DAYS

Al 5ml

SET	TLEO	METE	R		FAIRHAVEN C							INN	FIAL	S:		DATE:	1211	01.15
Time	9	:20		:	SAMPLES - VOLUME	INF 25	PRISO	EFF/20	F3	$\boldsymbol{\times}$	F4 100	R3	$\times$	R4 5	A1 5	A2 5	A3 5	WAS 5
0		SSC 3.0		SSC	CRUCIBLE	16,6023					2],X2]							22,0601
5 10	820 690				CRUCIBLE WT.	16,5812	21.7162	19.5569			21.26/1		<u> </u>	21,6/24	21, 4922	19:42(1)	17.7365	27,0332
20	590 520				DIFFERENCE PRE- FURNACE	10211 844	,0031 62	10006	(		16			.0499	,0214	10292	,0208	.02,69 5,380
30	480 440				CRUCIBLE WT. + SAMPLE	16.6023	21,7183	19,5575		$\bigcup$	21.2229			2).(123	2],5141	19,4552	17,1523	22,0609
50	390 360 330				WT. POST FURNANCE DIFFERENCE		21,7/60 10033	19,5563			21.248							22,0397
123	A	1	2	3	VOLATILE PRE-FURNACE	10151 604	66	100 12 12	_		,0019 19		/	5,540	2,540	3,300	2,400	,0224 4,480
2,6 3,5 3,0	т	•	2	5	VOLATILE FIXED SOLIDS	844	62 4	6		$\downarrow$	16			9,980	4,380	5,840	4,160	5,380
X X X 4	R S C	1		4	COLIFORM I SAMPLE		A	: 100mL	Ē	M	AGNETI	2,	04			NOTES	14,6	
1234	D O B	1	23	_					~	MI	LSS A2 LSS A3 RAS 3	2,	,65	-		A1 pH: A2 pH; A3 pH;	6.8	
1234 0,31.623	A D O	1	2 3	4					E		RAS 4 WAS					L EFF INITY	6.7	
					START: FINISH: OUT:													

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 7,8 NITRATE - 5,6

NITRITE -

AMMONIA: 0.709

I Removal 
$$\frac{844-6}{844} = 100 = 99\%$$
  
Z Primary Removal  $\frac{844-62}{844} = 100 = 9.3\%$   
Ib/day RAM 8.34 x  $844 \times 2.15 = 15$  33  
Ib/day PRL 8.34 x  $62 \times 2.15 = 11/2$   
Ib/day EFF. 8.34 x  $6 \times 2.15 = 108$   
MLSS, 8.34 x  $-467 \times 4,160 = 16,202$   
SVI 1000 x 440 = 106 mI/g  
CF  $\frac{4,160}{4,140} = 1,387$  mg/1/m1  
SA  $\frac{-8.34 \times -467 \times 4,160}{8.34 \times 62.5}$  15 DAYS

SA<u>\*8-34</u> 8-34

Al 5ml

SET	TLEO		R		FAIRHAVEN C						INITIA	LS: 1/	ъ	DATE:	12-19	115
Time	9	10		•••	SAMPLES - VOLUME	INF 50	PRI <b>50</b>	EFF/00	F3 🖌	F4 100	R3K	R4.5	A1 5	A215		WASS
Thue	SSV	SSC	SSV	SSC	CRUCIBLE				5							
0	1000				WT. + SAMPLE	21 2920	11 262	217569		21556	. ]	10 mm	10.100	A 450	10 400	21463>
5	860			i		31.0 10	~ / o A W / )	277207		27.2767	-+	17.7152	177.10.36	10.001	10.001	[ ~ [ , [ 0 ] ]
10	680		<u> </u>		CRUCIBLE WT.	212826	21 360	21.7564		21.5748		19415	10 0900	Con Stull	16 580	21,435 3
15	580		1		DIFFERENCE PRE			.0005		-0015		0474	0235	0326	0208	.0,230
20	520		<b></b>		FURNACE	188	48	5		15						5600
25	480				CRUCIBLE								1.700	02 40	,,,,,,,	7800
30	440				WT. + SAMPLE	21.2920	21.7631	21.7569		21.5763		19.4732	19.1230	21.0075	16.6019	21.4637
40	390				WT. POST								1 11.10			
50	360				FURNANCE	21.2843				21.5748		19.4470	19.109	20989	165904	21 +416
60	340				DIFFERENCE	,0077		.0005		.0015		.0362	,0135	,0182	,0115	.0221
					VOLATILE	154	48	5		15						4420
123	A	1	2	3	PRE-FURNACE											
Ι	Т				VOLATILE					l i						
2 60 2					FIXED SOLIDS	.34	Ø	Ø	}		_{	4240	2000	8880	1860	1180
4 22-20-4		1	2 3	4	<b>F</b>				_							_
6.0	S				COLIFORM			<u>:</u>		AGNETI				NOTES		
					SAMPLE	COLON	IES #/	100mL		ILSS A1	2.1		INF	. TEMP:		
1234	_	1	23	4						ILSS A2	2.8			A1 pH:		
-	0									ILSS A3	21	2		A2 pH:		
1 2 3 4	B	1	2 3	4						RAS 3	~			A3 pH:	6.7	
1 2 3 4		1	2 3	4	· · ·					RAS 4	4.2	5				
0.3 0.8 1.	_									WAS	0.6.	5	AKAL	INITY		J
0.30.37.																
					START:											
					SIANI.											
					FINISH:		•••									
					OUT:											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5,28

NITRATE -

NITRITE -

X Removal 
$$\frac{15.4 - 5}{15.4} \ge 100 = 93\%$$
  
X Primary Removal  $\frac{154 - 48}{154} \ge 100 = 69\%$   
Ib/day RAM 8.34  $\ge 154 \times 2.16 = 2,774$   
Ib/day PRI. 8.34  $\ge 48 \times 2.16 = 865$   
Ib/day PRI. 8.34  $\ge 5 \times 2.16 = 90$   
MLSS, 8.34  $\ge .467 \ge 4/60 = 16202$   
SVI 1000  $\ge 440$  = 106  $\ge 1/8$   
CF  $\frac{4/60}{7.5} = 1541 = 90$   
MLSS  $\ge 34 \ge .467 \ge 4/60$   
SA  $\ge 34 \ge .467 \ge 4/60$   
 $\ge .34 \ge .467 \ge 4/60$   
 $\ge .34 \ge .487 \ge .16$   
(19 DAYS)

Al 5ml

SE	TLEO		R		FAIRHAVEN C						INITIA			DATE:	12.19	3115
Time		:20			SAMPLES - VOLUME	INF 50	PRI 50	EFF/00	F3X	F4 100	$R3 \times$	R4 3	A1 3	A2 5	A3 5	WAS 5
11116	SSV	SSC	ssv	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	21.4408	20.976	17 7354		21 8131		20 651)	21.514	16 613)	21.7396	19 582 3
5	800				CRUCIBLE WT.	Γ.	, 				1	1				
10	650							17 73-16		21.6113	/	20 6013	21.4911	16.5810	21.7162	19 <u>.5566</u> .026 1
15	670				DIFFERENCE PRE			,0008	1/	,0014		1.0500	10,238	2367	10237	.0261
20	500				FURNACE	114	44	<u> </u>	ļ	14		10000	4760	340	4680	5220
25	450	ļ			CRUCIBLE	a ildan	. Abro	the Arrest					. 18.50			1. cont
30 40	430				WT. + SAMPLE	21.4408	20.97 <i>6</i> 9	17.2354	<u> </u>	21.6131	}	20.6517	21.5149	16.617)	21.7376	19_5877
40 50	400				WT. POST FURNANCE	21.4.351		17 7216		21.611>			alter	1. 600	A DATE	19.5604
60	720				DIFFERENCE	0057	207742			-0014		20624	21,5002	163100	A1.1257	.0223
					VOLATILE	114	44	8	/	14		e sur	0141	1700	nada	4460
123	Ā	1	2	3	PRE-FURNACE	+ <i>"7</i>	77	<u> </u>				37.70	<u>x770</u>	7.300	1000	/////
	T		-	-	VOLATILE						}				-	
275024	c c				FIXED SOLIDS	Ľ	2	Ø	$\rightarrow$	X		4260	1820	3040	1840	760
1224	R	1	2 3	; 4					••••••••••••••••••••••••••••••••••••••							
	S				COLIFORM	BACTERI	A	:		MAGNETI				NOTES		]
2.3					SAMPLE	COLON	IIES #	/100mL		MLSS A1			ÍNF	. TEMP:		
1 2 3 4	D	1	2 3	6 4						MLSS A2				A1 pH:	2.0	ļ
	0					ļ				MLSS A3		<u> </u>		A2 pH:	6.8	-
1234	B		<u> </u>						╏┝┈	RAS 3		-		A3 pH:	6.2	
1 2 3 4		1	2 3	4	· · · ·					RAS 4	0.4			L EFF JINITY		
0.31.725					· · · · · · · · · · · · · · · · · · ·		·····			MAG	0.4	2			1	
0.07.940						1										
					START:	1										
					FINISH:				ĺ							
									Į							
					OUT:		i									
									1				-			

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5.8.5

NITRATE -

Ammonie NHRIFE-

X Removal 
$$\frac{114}{114} = \frac{8}{114} = \frac{114}{114} = \frac{93\%}{114}$$
  
X Primary Removal  $\frac{114-44}{114} = 100 = \frac{61\%}{114}$   
Ib/day RAN 8.34 =  $\frac{114}{114} \times 2.2 = 2.092$   
Ib/day PRI. 8.34 =  $\frac{44}{114} \times 2.2 = 2.092$   
Ib/day PRI. 8.34 =  $\frac{44}{114} \times 2.2 = 3.07$   
Ib/day ENF. 8.34 =  $\frac{8}{12} \times 2.2 = 147$   
MLSS, 8.34 = .467 =  $\frac{4680}{132} = \frac{13228}{1228}$   
SVI 1000 =  $\frac{430}{4680} = \frac{92}{123} = \frac{112}{12}$   
CF  $\frac{4680}{12.7} = \frac{133}{123} = \frac{112}{12}$   
SA  $\frac{8.34}{12} \times \frac{467}{144} \times \frac{4680}{12.7} = \frac{23}{123} = \frac{143}{12}$ 

A1 5mL

SET	TLEO		R		FAIRHAVEN C						INITIAI	LS: 🗸	0	DATE:	121	7115
Time	9	:20		:	SAMPLES - VOLUME	INF 50	PR1 50	EFF	F3 📐	1F4/00	R3	1R4[5	A1 5	A2 5	A3 5	WAS 5
une .	SSV	ssc	∣ssv	SSC	CRUCIBLE						)	1				
0	1000				WT. + SAMPLE	A.1135	21 4951	21,3169		20,6025	- /	21 6574	19.5788	1911543	71 5944	16.6032
5	800				CRUCIBLE WT.				1						~~~	
10	650			[		19,0994	21.4910	21.7164		20,6014		21 6114	19.5571	19.4257	215743	16.5809
15	550				DIFFERENCE PRE-	.0161	.0041	.000.5		,0011				.0286		
20	500				FURNACE	322	52	5		11				5720		
25	450				CRUCIBLE	-					1		'			
30.	420					19.11.5.5	21.4951	21.7169		20.6025		21.6574	19.5738	19.4543	21.594	16.6032
40	380				WT. POST				1							
50	350				FURNANCE			21.7164		20.6015		21.6331	195570	19-13-33	21,539	\$ 16.5860
60	330				DIFFERENCE	0111		.0005		.0010		,0243	.0118	-01.55	.0051	,0212
					VOLATILE	222	68	5	/	10				3100		
123	A	1	2	3	PRE-FURNACE				(			ľ				
1	T				VOLATILE											
23352					FIXED SOLIDS	100	14	Æ		1		4340	1980	2620	3100	1020
1284	R	1	2 3	4							,					
	S				COLIFORM			:		MAGNETI				NOTES		
6.0					SAMPLE	COLON	IES #	/100mL		MLSS A1	20		INF.	. TEMP:		
1234		1	23	4	B	0		0		MLSS A2	2.63			A1 pH:		
-	0				50	2	2	2/50		MLSS A3	1.80	7		A2 pH:		
	B				100	8	8	1100		RAS 3				A3 pH:	6.7	
1234		1	2 3	4						RAS 4	4.03		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	LEFF	2	
0.2 1.531	D			ľ						WAS	0.3	0	AKAL	INITY	71	
8. X 1. J 3.	U U															
					START: 12:50											
					FINISH: 1:00											
					OUT: 1:00											
					1.00											
									•							

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 6.31 NITRATE - 5.99

Ammonie 0.082 NITRITE -

I Removal 322 - 5 x 100 = 98% Z Primary Removal 322-82 x 100 - 75 1b/day RAW 8.34 x 322 × 2.2 = 5908 16/day PRI. 8.34 x 82x 2.2 = 150 4 1b/day EFF. 8.34 x 5 × 2.2 = 92 MLSS, 8.34 x .467 x 4120 = 16046  $\frac{\text{SVI}}{4/20} = \frac{1000 \text{ m} 4/20}{4/20} = \frac{102 \text{ m} 1/g}{102}$  $\frac{c_{\rm F}}{2.7} = \frac{1526}{1526} = \frac{1526}{100} = \frac{1}{100}$ SA :8.34 x .467 x 4/20 8.34 x 82 x 22 // DAYS

Al 5ml

SE	TLEO	METE	R		FAIRHAVEN C						INITIA			DATE:	12 13	1 15
Time	9	25		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF 00	F3 📐	F4 100	R3 🗸	[R4]5	A1 5	A2 5	A3 5	WAS 5
nine	SSV	SSC	SS∨	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	21.5762	19 5583	19 4261		21.7169		20 6350	19 1237	16 600 1	21 6322	21.5169
5	650				CRUCIBLE WT.						1		1 1.7000 7			
10	600				CRUCIBLE WI.	21,5343	19,5565	19 4256		217160		20,6019	19 1007	165504	2/6/11	21,4909
15	540				DIFFERENCE PRE	,0019	,0018	.000.5		.0009	ì			,0203		
20	470				FURNACE	38	36	5		9				4060		
25	440				CRUCIBLE	•					1					
30	400				WT. + SAMPLE	21.5762	19.558	19.4261	Į	21.7/63		20.635	19.123	16.6007	216322	21.5169
40	360				WT. POST					T	1					
50	330				FURNANCE	21.5743	19.5565	19.4256		21.7160		20.6173	19,100	16.58%	21.620)	21.4962
60	320				DIFFERENCE	-	.0018	.0005		.0009	1		,0131		0115	
					VOLATILE	38	36	5		9		3640	2620	2240		
123	A	1	2	3	PRE-FURNACE				1			T T			~~	////
1 . 1	T				VOLATILE				N.							
2.3 2.3 2.5	C				FIXED SOLIDS	-0	Í	B		Ø	Ì	3080	2060	1820	1920	1060
1234	R	1	2 3	4							-					
4.	s s				COLIFORM	BACTERI	A	:		MAGNETI	TE (m	g/L)		NOTES		
	L C				SAMPLE	COLON	IES #	(100mL		MLSS A1	2.1	3	INF	. TEMP:	15.1	
1 2 3 4	D	1	2 3	3 4						MLSS A2				A1 pH:	6.8	
•	0									MLSS A3		5		A2 pH:	6.7	
	B									-RAS-3		~~~.		A3 pH:	6.6	
1 2 3 4	A	1	2 3	3 4						RAS 4			FINA	l eff		
	D								L	WAS	0.4	9	AKAL	INITY		
0.42.52	γ́ O															-
					START:											
					FINISH:											
					OUT:											
						~										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 6.8

NITRATE -

NITRITE - 0.209 Ammoniq

Al 5ml

*\$* 

I Removal  $\frac{38 - 5}{38} = 100 = 87\%$ I Primary Removal  $\frac{38 - 36}{38} = 100 = 5\%$ Ib/day RAW 8.34 x  $38 \times 2.25 = 7/3$ Ib/day PRI. 8.34 x  $36 \times 2.25 = 676$ Ib/day EFF. 8.34 x  $5 \times 2.25 = 94$ 

. MLSS, 8-34 x -467 x 4220 = 16 436

 $\frac{\text{SVL} 1000 \times 400}{4220} = 95 \text{ ml/g}$   $CF = \frac{4220}{2.5} = \frac{1688 \text{ mg/l/ml}}{2.5}$ 

54 :8.34 x .467 x 4220 8.34 x 36 x 2.25 24 DAYS

SET	TLEO		R		FAIRHAVEN C							INITIAI	LS: 1/	0	DATE:	12 13	3115
Time	The Party of the P	55		••	SAMPLES - VOLUME	INF 60	PRI 50	EFF	F3	<u> </u>	F4 /00	R3	R4 5	A1 3	A2 5	A3	WASIS
0	1000		SS∨	SSC		21.7183	20.9775	21,4361			16.5826		19 6057	21600	21 6251	21515	19.4530
5	790 690				CRUCIBLE WT.	21.7165	20.9753	214355			16.5818	7	19.5568	21.5744	21.6114	21.4916	19.4269
15 20	500				DIFFERENCE PRE FURNACE	- ,0018 36	.0022 44	.0006		2	,0003 B		10489 9780	.0258	.0238	.0236	.0261 5220
25 30 40	430 400 360				CRUCIBLE WT. + SAMPLE	21.7/83	20.9775	21.4361			16.5876		19.6057	21.6007	21.6352	21.5152	19.4530
50	340				WT. POST FURNANCE DIFFERENCE	21.7165	20 9753			. ľ	16.5818 .0008						19.4317
123	A	1	2	3	VOLATILE PRE-FURNACE	36	44	6			8		,0266 5320	2960	,0134 2680	.0134 2680	,0713 4260
30 3223	T	•	-	Ĵ	VOLATILE FIXED SOLIDS	ø	B	Ð	4	_	Ø	4	4460	2200	2080	2040	960
<del>4 2 2 4</del> 65	R	1	2 3	4	COLIFORM SAMPLE		A	: 100mL	<u> </u>	MA	GNETI SS A1	ΓE (mg	/L)		NOTES		760
1234	D O B	1	2 3	4						ML ML	SS A2 SS A3 RAS 3	2.28	2		A1 pH: A2 pH:	6.9 6.8	
1 2 3 4	A	1	2 3	4	· · · · · · · · · · · · · · · · · · ·						RAS 4	4.4.			A3 pH: EFF INITY	6./	
<u>0.4 <i> </i>.4</u> 3.6	0				START: FINISH: OUT:												·

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 6.77 NITRATE -

Ammonia NHTRITE - 0.356

I Removal  $\frac{48-3}{48} = 100 = 94\%$ 7 Primary Removal 48-30 x 100 - 38% 1b/day RAW 8.34 x 48 x 2.45 = 981 16/day PRI. 8.34 x 30 × 2.45 = 6/3: 1b/day EFT. 8.34 x 3 x 2.45 = 61 MLSS, 8.34 x .467 x 4040 = 15 735  $\frac{5VI}{4040} = 99 \cdot m1/g$  $\frac{4040}{2.5} = \frac{1616}{16} = \frac{11}{10}$ 

SE	TTLEO	METË	R		FAIRHAVEN C								.s: 🗸		DATE:	12-18	2115
Time	9	15		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3	F4 /2	0 R.	3 X	R4 5	A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE				]			1					
0	1000				WT. + SAMPLE	21.7193	21/1221	10000		21.49		1		3200	a cond	4 ( 17774	21,3174
5	780					<u> </u>	1.7.2.74	<u> </u>			4	/	## <u>\$\$977</u>	1.7570	21.2777	x1.03A0	×1, 3/17
10	620				CRUCIBLE WT.	23.49	214759	19 6575	- 1	21491	<i>。</i>   \	<b>\</b>	22 1225	15 7722	1000	~ ~ ~ ~	21,2917
15	550				DIFFERENCE PRE		,0015			.000		╉			0241		.0257
20	490				FURNACE	48	30	3		5		Į –			4820		
25	430				CRUCIBLE					\				,,,	1	101-	J 1 / -
30	400				WT. + SAMPLE	21.7193	21.4374	19.5578		21,49	6	ł	22.09>>	17.7576	21.5994	21.6320	21.3174
40	360				WT. POST					]							
50	340				FURNANCE	21.7/69	21:4359	19.3575		21.491	9	1	22,0528	137441	21.5848	21.6198	21.2954
60	320				DIFFERENCE	.0024	.0015	.0003	1	.000)	>   _	1	0249	.0135	,0146	.0122	.0220
					VOLATILE	48	30	3					4980	2700	2920	2440	4400
123	A	1	2	3	PRE-FURNACE							١			ľ		
2.5 3.5 2.5	T				VOLATILE				_1			$\perp$					
					FIXED SOLIDS	Ø	Ø	ø	}	0		<u>{</u>	3860	1980	1900	1600	740
1284		1	23	4													
6.0	S				COLIFORM			:		MAGNE			_		NOTES		
	<b>×</b>		~ ~		SAMPLE	COLON	IES #/	(100mL		MLSS A		3	2	INF	. TEMP:		
1234	o	1	2 3	4						MLSS A		1.12	<u> </u>		A1 pH:		
	в									MLSS A		<u>,</u> G7	- ·		A2 pH:		
1 2 3 4		1	2 3	4		<u> </u>				RAS RAS		$\sim$	~~~	CINIA	A3 pH:	6.6	
. 2 9 9		,	2 3		i							37			L EFF .INITY		
0.41.0 2.0	A 🖳 I					· · · · ·				V W/		57	·				
0. 1770 344					/ <u> </u>	<u> </u>											
					START:	.L											
					FINISH:												
					OUT:												
					·												

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5 15 NITRATE -

Ammonia NITRITE - 0. 896

	SET	TLEO	METE	R		FAIRHAVEN C						T	INITI/	ALS:	· V	0	DATE:	1211	115
Time		9	36		-	SAMPLES - VOLUME	INF 50	PRI 🖌	EFF/00	F3		4 100	R3	R	45	A1 5	A2 5	A3 5	WASS
Three	•	SSV	ssc	SSV	SSC					$\left  \right\rangle$									
0		1000				WT. + SAMPLE	21.2559	A A ANNA	24 6000	/		12828	5		a and		100-00	10 000	19.4528
5		800					×1.4507	20.777	AU.0040			7.264.5	<del>{i_</del>	- 4'	1. /4/7	21.3174	16.6046	17,3007	17.73~0
10		680				CRUCIBLE WT.	21.2508	20 9349	20 Call		2	2820			A AKA	2120	The Cara	ila 6044	19.4258
15		580			1	DIFFERENCE PRE	.0051		.0006			0008	— )	) -#/	1.0770	.02.14	0274	0214	.0270
20		520				FURNACE	102	44	6			8	- 1		680	HORD	4180	4280	5400
25		480				CRUCIBLE	•			Ì							1000	10-0-	
30		450				WT. + SAMPLE	21.2559	20.970	20.6020		2/	2828	- /	19	1419	21.2794	16 GOUL	19.5869	19.4528
40		400				WT. POST	1					*****	- 1	- 22			<u> </u>	, <u>, , , , , , , , , , , , , , , , , , </u>	,,,,,,,,,
50		390				FURNANCE	212508				21	1 1820		19	1.1187	21.7648	16.591	19.574	19.4308
60		350				DIFFERENCE	.0051	,0072	,0006			0008							,0720
						VOLATILE	102	44	6	/	Í	8						2420	
12	3	A	1	2	З	PRE-FURNACE				7				71	<b>X</b>				1.1.2
	_	T				VOLATILE				(			(	<u></u>					
3.0 3.0	25	C				FIXED SOLIDS	Ð	ø	Ø	1		Ø	1	3	940	1760	1980	1860	1000
1-23	- 4	R	1	2 3	\$ 4								)		_				
		S				COLIFORM			:			GNETI					NOTES		
		C				SAMPLE	COLON	IES #/	/100mL			SS A1		98		INF	TEMP:		
1 2 3	4	D	1	2 3	\$ 4	B	0		1			<u>3S A2</u>	1.5				A1 pH:		
·		o p				50	2		150	⊢⊦		SS A3		D			A2 pH:		
1 2 3	A	B A	1	2 3	4	100	20	20	1,00			XAS 3		-	-		A3 pH:	6.7	
1 2 3	4	מ	1	2 3	) 4							RAS 4			-		EFF	10	
0.3 1.7	28	. – .					· · · · · ·			L		WAS	0.3	8			INITY	52	
0.3 1.7	n. 0					l <u> </u>													
						START:	1												
						START: 11:15													
						FINISH:													
						11:25													
						11:30													
										i i									

a

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 6.66 NITRATE - 5.40

Ammonia 0.415

2

I Removal 102 - 6 = 100 = 94% 2 Primary Removal 102 -44 x 100 - 57% 1b/day RAW 8.34 x 102 × 2.38 = 2024 1b/day PRI. 8.34 x 44×2.38 = 8/3 1b/day EFF. 8.34 x 6 × 2.38 = 119 MLSS. B.34 x .467 x 4280 = 16,670  $\frac{\text{SVL}}{4180} = 10.5 \text{ ml/g}$ CF 4280 = 17/2 mg/1/ml  $\frac{SA}{8.34 \times .467 \times 4280}$  19 DAYS

Al 5ml

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Time 9:20 : SAM	MPLES - VOLUME	INF 60	omil z.			_					DATE:		
Ime ssy ssc ssy ssc			PRISO	B## 100	F3	$ \times $	F4 100	R3	R4	5 A1 5	A2 5	A3 5	WAS 5
	CRUCIBLE			, í		<u>}</u>	6 <i>F</i> =	1	••••••••••••••••••••••••••••••••••••••				
0 1000 W	/T. + SAMPLE	217649	312849	16.582	. /		20.9759	; )	306	01 19 580	19 4483	19 119:	21.2361
5 800	RUCIBLE WT.	<u></u>									<u></u>	1 1 1 1 7 8	, , , , , , , , , , , , , , , , , , ,
10 650		21.7552	21.2823	16 5812			20.9348	> {					21.2503
	FERENCE PRE-	.0097		-0008			.0011						.0254
20 500	FURNACE	194	52	8			11		10 06	0 4160	HGHO	4020	3080
	CRUCIBLE	a VIII	A 1 26 116	· * 20 m.						-	a contra		
	WT. POST	21. 1077	<u> 71.2017</u>	16.5820			<u>20.9759</u>	·	20.65	21 19.586	19.443,	17-1173	21.2361
		213536	21 2830	16.5814			20.9250		200	1010 100	la dan	10 10	21.2563
	DIFFERENCE	.0073	.0019	0006			0009	<u> </u>					,0194
	VOLATILE	146	38	6	Į		G			2300			
123 A 1 2 3 PF	RE-FURNACE			- <b>-</b>	1				<u> </u>		1		. <u></u>
3. I I I	VOLATILE												
	IXED SOLIDS	48	14	2	1		2		464	0 1860	2120	1840	1200
	000000000000					<b></b>							
2.0 c	COLIFORM B SAMPLE			100-1		<u>M/</u>					NOTES		
1 2 3 4 D 1 2 3 4	SAWFLE	COLON		100mL			LSS A1 LSS A2	1.8		INF	. TEMP: A1 pH:		
0							LSS A3				A2 pH:		
В							RAS 3	<u> </u>			A3 pH:		
1 2 3 4 A 1 2 3 4							RAS 4	42	5	FINA			1
							WAS			AKA	INITY	56	ŀ
0.2 3.75 0													-
STA	ART:												
	ISH:												
FINI	ιоп,												
	Γ:												

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5.4

NITRATE -

Ammonia = 0.063m5/L NH3

Al 5ml

I Removal  $\frac{194 - 11}{194} = 100 = 94\%$ 2 Primary Removal 194-52 100 - 73% 16/day RAW 8.34 x 194 x 2:3. = 3 >21 1b/day PRI. 8.34 x 52 × 2.3 = 997 1b/day EFF. 8.34 x 11 × 2.3 = 2.11 MLSS, 8.34 x .467 x 4020 = 15657 SVI 1000 x 420 - 105 ml/g  $\frac{CF}{2.5} = \frac{4020}{1608 \text{ mg/l/ml}}$ 

 $\frac{-7020}{2.5} = \frac{1608 \text{ mg/l/ml}}{8.34 \text{ x} .467 \text{ x} 4020}$   $\frac{16}{8.34 \text{ x} .52 \text{ x} 2.3} = \frac{16}{16} \text{ DAYS}$ 

SE	TTLEO		R		FAIRHAVEN C	ONTROL	DATA L	OG - BIOI	MAG	TEST	INI	TIAL	S:		DATE:	11 12	5115
Time	9			:	SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3[)	< F4 /00	R3	X	R4 <b>5</b>	A1 5	A2 5	A3 5	WAS
11116	SSV	SSC	SSV	SSC	CRUCIBLE				$\rightarrow$						1		
0	1000				WT. + SAMPLE	AU1603[	21,2252	19.0978	1	16,582	5	/	ə(; 30(g	17,3817	17,7907	2027749	21,7854
5	550		[		CRUCIBLE WT.					_ <u></u>	$\pm 7$	/	• •				
10	460					20.6011	21,2825	19.0983		16.554	$\downarrow \$		21.2503	19 5661	19.425	20 921	21 7557
15	410				DIFFERENCE PRE			.0010		,0015			.0513	.02/8	,0252	,0198	.0297
20	380				FURNACE	40	54	10		1.5							5940
25 30	350 330				CRUCIBLE	00 (00)					]						) a ch
40	300				WT. + SAMPLE WT. POST	10.60.51	21.7852	19.0988		/6.582	<u>علم الم</u>		2 <u>1.3016</u>	19.5879	19.4509	20.9945	21.)854
50	290					DA 64/7	a seab	19.0988		16.5810	J	1		1	041		1.44
60	280				DIFFERENCE	10018	.0075			1001.5	1	┤─┤					21 7613
	<b>V</b> . 30			i	VOLATILE	36	30	10	- 1	15		11					,0237
123	Α	1	2	3	PRE-FURNACE		30		{-		+	+	5300	7380	2740	2100	4740
	Т				VOLATILE				{			/					
27 3.02	o K				FIXED SOLIDS	4	4	0	$\neg$	0	Ħ		4960	1980	2300	1860	1200
1-2-2-4	R	1	2 3	4							<u> </u>			- f f		7075	
6.	<  S				COLIFORM			:		MAGNET					NOTES		
	L L		~ ~		SAMPLE	COLON	IES #	'100mL		MLSS A1			•	INF	. TEMP:		
1234	DO	1	2 3	4						MLSS A2					A1 pH:	-	
	B					 				MLSS A3		00			A2 pH;		
1234		1	2 3	4						RAS 3		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	<u> </u>	<b>EINIA</b>	A3 pH:	6.6	
	D		- •	· 1	· · · · · · · · · · · · · · · · · · ·					WAS					L EFF INITY		
0.3 1.6 3.6	νōΙ											.90					
					START:		1										
					FINISH:												ν.
					OUT:												

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 7.78 NITRATE - 6.83

Ammonia NITRITE - - 9113

 $x = \frac{40 - 10}{40} = 100 = \frac{56}{6}$ Z Primary Removal  $\frac{40-54}{40} \times 100 =$ 15/day RAW 8.34 # 40 x2.>> = 924 16/day PRI. 8.34 x 54 x2.>>= 124> 16/day HFF. 8.34 x 10 x 2.7) = 2.31 . MLSS, 8.34 x .467 x 3960 = 15423 SVI 1000 x 330 - 83 m1/g 3960  $\frac{CF}{2.5} = \frac{3960}{146} = \frac{146}{1} \frac{1}{11}$ SA <u>\*8.34 x .467 x 3960</u> /2 DAYS

Al 5ml

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**#** 

SE	TTLEO		R		FAIRHAVEN C						INITIAL		0	DATE:	11 12	4115
Time	9	:00		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3	F4 100	R3 🔨	R4 5	A1 5	A2 5	A3 5	WAS
Inne	SSV	SSC	SSV	SSC					17							
0	1000	1			WT. + SAMPLE	21.6/33	19.5681	21.7571		21,2516	/	216029	16 600	20 6333	213043	19.1233
5	630	:			CRUCIBLE WT.							[], <u>,,,,,</u>	(			
10	430 3>0				GRUCIDLE WI.	21.6119	19 5659	21.7561		21,2503		21 5751	16 5813	20.6020	21 282	19.6995
15	3>0				DIFFERENCE PRE	.00 14	.0072	.0010		.0013				.0317		,0282
20	350				FURNACE	28	. 44	10		13				6340		5640
25	310				CRUCIBLE	•										
30	300				WT. + SAMPLE	21.6/33	19 5681	21.757		21.2516		21.6029	16.6029	20.6337	213043	19.1277
40	270				WT. POST							Ĩ .		[		
50	260	L				21.6119	19.5659	21.7561		21.2503		21.5888	16.5919	20,6169	212933	19.1060
60	\$50				DIFFERENCE	.0014		.0010		.0013	1	.0141	.0110	.0168	.0110	.0717
					VOLATILE	28	44	10		13		2820	2200	3360	2200	4340
123	A	1	2	3	PRE-FURNACE				1							
	Т				VOLATILE					: 						
2 452	C C				FIXED SOLIDS	X	Ø	Å		Ø		2740	2120	2980	2120	1300
1-2-2-4	1	1	2 3	4												
<u>か</u>	s				COLIFORM	· · · · · · · · · · · · · · · · · · ·		:	M	AGNETI	TE (mg	/L)		NOTES		
					SAMPLE	COLON	IES #/	100mL		ILSS A1			INF	. TEMP:		
1234		1	2 3	4	B	Ð		0		ILSS A2				A1 pH:		
-	0				50	/	/	150	M	LSS A3		5		A2 pH:		
	B			·	100	.3	3	[100		RAS 3		[		A3 pH:	6.6	
1234		1	2 3	4							5.43			LEFF		
	Ð									WAS	0.48	3	AKAL	INITY		
0.41.2.4-1	0															
							<b>u</b> r									
					START:											
					12:50											
					FINISH: 1:00											
					OUT:											•

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 9/9 NITRATE - 6.98

Ammonia N<del>itrit</del>e -0.698

Al 5ml

I Removal  $\frac{28 - 10}{28} \times 100 = 64\%$ 2 Primary Removal 28 - 44 44 x 100 -1b/day RAW 8.34 x 28 × 2.86 = 668 1b/day PRL. 8.34 x 44 x 2.86 = 1050 1b/day EFF. 8-34 x 10 × 2.86 = 239 MLSS, 8.34 x .467 x 4320 = 16 825  $\frac{\text{SVI} \ 1000 \ \text{x} \ 300}{4320} = 69 \ \text{ml/g}$  $cr = \frac{4320}{2.5} = \frac{1600 \text{ mg/1/ml}}{1.5}$ 54 :8-34 x -467 x 4320 8.34 x 44 x 2.86 = 16 DAYS

SE	TLEO				FAIRHAVEN C							.s: 🗸		DATE:	1113	3115
Time		:05		:	SAMPLES - VOLUME	INF 50	PRISO	EFF 60	F3 🔀	F4 /00	R3 🖂	R4 5	A1 5	A2 5	A3 5	WAS 5
	+	[	SSV	SSC	CRUCIBLE WT. + SAMPLE				ζ							
0	1000	<u> </u>			VVI. + SAMPLE	19.5680	19.1019	16.5813		21.6128		21.8063	20.6231	212722	21,5958	21.3121
5 10	520 410				CRUCIBLE WT.	in ter.	10000	16.5808								
15	360				DIFFERENCE PRE-	0019				R1.6119		21,7562	20.5014	21,2505	21.5755	21.2823
20	330				FURNACE	38	48	°,		9						6880
25	310				CRUCIBLE	Ť.		· /				10020	7370	73.00	-70 00	2200
30	300				WT. + SAMPLE	19.5680	19.1019	16.5817		21.6128		21.8063	20.6231	21.2722	21.5958	21.3121
40	270				WT. POST									<u> </u>		•
50	260		<u> </u>		FURNANCE			16.580		21.6119	and the second					21,2883
60	250				DIFFERENCE			.0009		.0009			· ·			.0234
			<u>.</u>	_	VOLATILE	38	48	9		9	/	5180	2340	2320	2160	4680
123		1	2	3	PRE-FURNACE				42,000						· ·	
272323	T C				VOLATILE FIXED SOLIDS	Ø	Ð	Ø		e		4840	2000	2060	1900	1200
2234	R	1	2 3	4				~	 		11	1/0 1	2000	0000	17700	(AUV
7.0	s				COLIFORM	BACTERI	A	:		AGNET	TE (ma	(L)		NOTES	;	F
					SAMPLE	COLON	IES #/	100mL		ALSS A1	2.00		INF	. TEMP;	15.6	
1234		1	23	4	B			1		ALSS A2				A1 pH;		
•	0				50	N	5 600	va l		ALSS A3	1.96			A2 pH:		
1234	B				100			1		<u>-RAS-3</u>	$\sim$	~		A3 pH:	6.6	
1 2 3 4	A	1	2 3	4		Bay	<del>7</del> 00,	ting.		RAS 4 WAS				LEFF	55	
0.40.92.5										VVAS	0.40		AKAL	INITY	57	ł
												•				
					START:	<i>.</i>										
					12:53											
					FINISH:											
					01/75											
					OUT:											
	-															

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 7.29 NITRATE - 5.53

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Amagonia NITRITE- 0.245



I Removal 38 - 9 = 100 = 76% Z Primary Removal 38 -48 1b/day RAW 8.34 x 38 × 3.15 = 998 1b/day PRI. 8.34 x 48 x 3.15 = 1261 16/day EFF. 8.34 x 9 x 3.15 = 236 MLSS, 8-34 x -467 x 4060 = 15813 SVI 1000 x 300 = 74. ml/g CF <u>4060</u> = 1504 mg/1/ml

54 :8.34 x .467 x 4060 13 DAYS

SE	TTLEO	METE	R		FAIRHAVEN C					TEST II	NITIAL	s: l	10	DATE:	11 12	2115
Time	9	:05			SAMPLES - VOLUME	INF 50	PRISO	EFF 100	F3,	F4 /00 F	र3	R4 5	A1 5	A2 5	A3 5	WAS
0	1000		ss∨	SSC	CRUCIBLE WT. + SAMPLE	19.5690	21,614	19.1005	$\rangle$	21.5769	$\rangle$					21-7891
5 10	500				CRUCIBLE WT.		21.6117	19.0946		21.5352	1	21,2503	16,5810	21 2828	20.6020	217559
15 20 25	350 330 310					.0031	.0030 60	.0009		,0015 15						,0332 6640
30 40	300				CRUCIBLE WT. + SAMPLE WT. POST	19.5690	21.6147	19-1005	$\rightarrow$	81.5767	(	1.3120	16.6061	2 <i> .30</i> 84	<u>20.6267</u>	21.3891
50 60	250				FURNANCE DIFFERENCE		21.6117 .0030	19.0996	$\rightarrow$	1.575		21,2808 .0312	16.5924	21.2945	20.6135 0132	21.7623
123	A	1	2	3	VOLATILE PRE-FURNACE	62	60	9	-{	15		6240	2740	2780	2640	5280
2) 2. 32.	, <u>с</u>		~~~~~		VOLATILE FIXED SOLIDS	ø	ø	B	$\rightarrow$	Ø		6060	2280	2340	2300	1360
),( ),(	RSC	1	2 3	6 4		BACTERI COLON		; 100mL	F	MAGNETIT	E (mg/	L)	INF	NOTES		
1234 ·	0	1	2 3	4						MLSS A2 2 MLSS A3 2	2.60			A1 pH: A2 pH:	6.9	
1234		1	2 3	4						RAS 3 RAS 4 WAS 2				A3 pH: L EFF .INITY	6-5	
0.4 2.24	40	-			START:											
					OUT:	<del></del>										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 9.23

NITRATE- 8.46



 $x \text{ Removal} = \frac{62 - 9}{62} \times 100 = 85\%$ X Primary Removal 62-60 x 100 - 3% 15/day RAW 8.34 x 62 x 2.5 = 1293 16/day PRI. 8.34 x60×2,5 = 1251 Ib/day EFF. 8.34 x 9 x 2.5 = 188 MLSS, 8-34 x .467 x 4940 = 19240 SVI 1000 x 300 - 6 / milg  $\frac{CF}{2.5} = /830 \text{ mg/l/ml}$ SA <u>\*8.34 x .467 x 4940</u> 8.34 x 60 x 2 5 15 DAYS

SET	TLEO	METE	R		FAIRHAVEN C	ONTROL	DATA L	OG - BIQ	MAC	S TEST	INITIAL	.s: V	0	DATE:	11 11	7115
Time	<u> </u>	55		•	SAMPLES - VOLUME	INF 50	PRISO	EFF 100	F3.	F4 /00	845	A13	A1 5	A8.5	WAS5	
Time	SSV	SSC	SSV	SSC	CRUCIBLE			[						1	<u>ار او </u>	
0	1000				WT. + SAMPLE	19 4295	19 100	21.7169	{	0.0.070		16 609		21.000	20.6319	:
5	550	, ,				11.1210	17.1044	<u>a</u>		- 41.0257	A1.2/70	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	141.0116	0-1. 0-200A	00.03/7	· · · · · · · · · · · · · · · · · · ·
10	450				CRUCIBLE WT.	19 412 44	19 0991	21.7162		07 0721	212500	10 500	210011	21.2612	20 (020	
15	400				DIFFERENCE PRE	A0 32	00.31	0006	- {					0970		ـــــ
20	360				FURNACE	64	62	6		5				5400		
25	B50	1		· · · · ·	CRUCIBLE		0~				14000	<u>9320</u>	1700	2700	3700	· · · · · ·
30	320				WT. + SAMPLE	19 HADK	19 1022	21.7168		22 1722	21 2140	11 hogo	1000	10000	20.6319	
40	300				WT. POST	1.74.10		AI . /100	· · ·	20,0220	<u> 1. 170</u>	10. W 12	<u> 1.0110</u>	17.9000	20.00/7	
50	290				FURNANCE	19.4264	19.0991	21.7102		120331	21 2810	16 5934	21 5908	21,2727	20,6057	
60	280				DIFFERENCE	.0032	.0031	.0006		.0007	.0330	0153	0208	.0155	0252	
					VOLATILE	64	62	6	- {	\S _	6600	2160		3100		
123	A	1	2	3	PRE-FURNACE		***		Ť		17.000	7,0-	1	<i>3100</i>	10.75	
	Т				VOLATILE				- 7							
3.0 5.0 3.0	C				FIXED SOLIDS	0	0	0	1	0	6200	2360	3240	2300	940	
X224	R	1	2 3	4		1					Up VV	W-3-0+		<u>/////////////////////////////////////</u>		
	S				COLIFORM	BACTERI	A	:	<b> </b>	MAGNET	TE (ma		1	NOTES		
8.0	C				SAMPLE	COLON	IES #	/100mL		MLSS A1			INF	TEMP:		
1 2 3 4	D	1	2 3	4					i i	MLSS A2		·		A1 pH:		
· ·	0			·						MLSS A3				A2 pH:		
	В									RAS-3				A3 pH:		
1 2 3 4	A	1	2 3	4						RAS 4	6.40		FINA		<b>v</b> .,	
	D									WAS	0.4	3		INITY		
0.4 1.236	° O															
					*****											
					START:	•										
					FINISH:											
					OUT:			·······								
					B											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 7.45 NITRATE - 7.06

Ammousia NITRITE - 0.222

A1 5m1

T Removal  $\frac{64-6}{64} = 100 = 91\%$ Z Primary Removal 64 -62 x 100 - 3% 16/day RAW 8.34 x 64 × 2.01 = 1073 16/day PRI. 8.34 x 62×201=1039 1b/day EFF. 8.34 x 6 X2.01 = 101 MLSS, 8.34 x .467 x 5400 = 21,032  $\frac{\text{SVI} \ 1000 \ \text{x} \ 320}{5400} = 59 \ \text{ml/g}$  $CF = \frac{5400}{30} = /800 \text{ mg/l/ml}$ 

5A <u>48-34 x 467 x 5400</u> 8-34 x 62 × 201 20 DAYS

BIOMAG TEST         INITIALS:         VO         DATE           ao         F3         F4         Ao         R3         R4         S         A1         S         A2         S           ao         F3         F4         Ao         R3         R4         S         A1         S         A2         S           ao         F3         F4         Ao         R3         R4         S         A1         S         A2         S           ao         F3         F4         Ao         R3         R4         S         A1         S         A2         S           ao         F3         F4         F4	A3 5 WAS 5
10 20.6020 21.6301 21 74 16 19.44	1 1
1- 10.000 21.0001 21.7770 17.72	21787020191
	10 er ev 58 22.05/1
07 20 6012 01 5741 21 7161 19 42	501261220225
	4 0237 .0266
10 20.6020 21,6301 21, 74/6 19.45	021.2838 22.059/
	1021.2710 22.0373
8 .0005 ,0282,0/37 .012	0.0128 .0218
5 5640 2740 3600	2560 4360
3560 2360 30 80	2180 960
MAGNETITE (mg/L) NOTE	
	<u>'' /6 5</u>
	56
1	
24	2502 20 6015 21.5741 21 7161 19.42 0 08 .0005 .0560 .0255 .0334 8 5 .11200 5100 6684 2.510 20.6020 21.6301 21.74/16 19.459 1.2502 20.6015 21.6019 21.7279 19.44 0008 .0005 .0282 .0137 .018

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5.31 NITRATE - 4.39

Himonic 0.089

Al 5ml

 $\frac{58-8}{58} = 100 = 86\%$ Z Primary Removal 58 - 46 x 100 - 20% 1b/day RAW 8.34 x 58 x / 99 = 963 1b/day PRI. 8.34 x 46 × 1.99 = >6.3 1b/day EFF. 8.34 x 8 x /.9.9 = 13.3 MLSS, 8.34 x -467 x 4/40 = 18 461  $\frac{5VL}{4540} = 63 \cdot m1/g$ CF 4)40 = 1580 mg/1/ml SA :8.34 x .467 x 4 40 8.34 x 46 x 1.99 24 DAYS

SET	TLEO				FAIRHAVEN C					TEST	INITIAL	.s: V	0	DATE:	11 1	7115
Time		55		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF/00	F3	F4 100						WAS 5
Time	SSV	SSC	∣ssv	SSC	CRUCIBLE				}		)					
0	1000				WT. + SAMPLE	21.2524	212031	20 3365	{	16.5813	(	216,94	21 5158	19 ALSI	19 1218	21,7438
5	790				CRUCIBLE WT.	The second	57.2021	120.11.22				<i>a<u>7.</u> 97. 77</i>		11.7.201	//./~/3	a. 1730
10	390				CRUCIBLE WI.	21.2502	21.2609	20.9751		16.5812		21575	214916	19.428	19099	21.7163
15	350				DIFFERENCE PRE	.0022		.00.04		.0005	$\neg$	.0442	.0242	,0783	.0220	.0271
20	520				FURNACE	44	44	4		5		3840	4840	5660	4400	5420
25	300				CRUCIBLE											
30	280				WT. + SAMPLE	21.2524	21.2631	20.9755		16.581		21.6194	21.5158	19.4551	19.1218	21.)438
40	270				WT. POST			. abri	)							
50 60	250				FURNANCE DIFFERENCE	21.2509	21.2609	20.7751		16.5812						21.7221
	<i>p30</i>			1	VOLATILE	.0072 44	.0022	.0004		.0005	ł	-	-			.0217
123	A	1	2	3	PRE-FURNACE	44	44	4				4500	2520	2940	2240	4340
	T	L	2	J	VOLATILE					· · ·						
25 3223	Ċ				FIXED SOLIDS	æ	8	8		101		4340	2220	2920	2160	1080
1/2 2 4	R	1	2 3	4			A#**	<u></u>				177 -	0-124	1/20	0100	1000
	S				COLIFORM	BACTERI	A	:		MAGNETI	E (ma	<u>/L</u> )	· · · · · · · · · · · · · · · · · · ·	NOTES		1
6.5	) C				SAMPLE	COLON	IES #/	100mL		MLSS A1			INF	TEMP:		
1 2 3 4	D	1	2 3	4			·			MLSS A2	2.72			A1 pH:	6.9	
. 1	0									MLSS A3	222	-		A2 pH:		
	B									RAS 3				A3 pH:	6.6	
1234	A	1	2 3	4						RAS 4				LEFF		
210624	D				· · · · · · · · · · · · · · · · · · ·			ÿ.,		WAS	0.4:	5	AKAL	INITY		
0.4 0.6 2.4	0															
					START:		-									
					START.											
					FINISH:											
					OUT:											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL)  $\times$  1,000,000

TOTAL NITROGEN - 10.6 NITRATE - 5.96

Amonia NITRHE - 0,161

Al 5ml

X Removal.  $\frac{44-4}{44} = 100 = 90$ 2 Primary Removal 44 -44 44 x 100 - 0 15/day RAW 8.34 x 44 x /98 = 72> 16/day PRI. 8.34 x 44× 1.98 = 727 1b/day RFF. 8.34 x 4 x 1.98 = 66 . ELSS, 8.34 x .467 x 4400 = 1>13> SVI 1000 x 280 - 64. ml/g CF <u>4400</u> = /630 mg/1/ml 54 - 34 x - 467 x 4400 8-34 x 44 x 198 24 DAYS

SE	TTLEO	METE	R		FAIRHAVEN CO						INITIA			DATE:	11 11	61 15
Time	9	:05		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF/@	F3	F4 /00	R3	R4 5	A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE						<u>)</u>					
0	1000				WT. + SAMPLE	22,0385	20 9773	217171		19.4265		216242	21 5142	212883	19 1210	16.6093
5	40		<u> </u>			×				7,7500					· · · · · · · · · · · · · · · · · · ·	20,00 / 2
10	450 360				CRUCIBLE WT.	22.0330	20.9749	217165		19.4256		215747	21.4912	212602	19.099	16.5810
15	330				DIFFERENCE PRE-		,0024	.0006		.0009	1	.0495	,0230	0281	0212	.0283
20	300				FURNACE	110	48	6		9						5660
25	280				CRUCIBLE	· ·									:	
30	270					<i>27.03</i> 85	20.9713	21.7171		19.4265		21.6242	21.5142	21,7883	19,1210	16.6093
40	250				WT, POST											
50	250							21.5165		19.4256	· <u> </u>	21.5991	21.5017	21 2)33	19.109	16.5862
60	240				DIFFERENCE		,0074	.0006		.0009						,0231
					VOLATILE	104	48	6		9'	}	5020	2500	3000	2280	4620
123	A	1	2	3	PRE-FURNACE											
	Т				VOLATILE							1/20			10.0-	
27 322	<u> ५ ०</u>				FIXED SOLIDS	6	0	Ø		l l		4880	2/00	2620	1960	1040
x 2 8 1	1	1	2 3	4									<u>.</u>			T
6.	5 5									MAGNET				NOTES		
			~ ~		SAMPLE	COLON		/100mL		MLSS A1				. TEMP:		
1234		1	2 3	\$ 4	3	0				MLSS A2				A1 pH:		
-	O B			ľ	50 100	68			┦┝	MLSS A3 RAS-3				A2 pH: A3 pH:		
1234	and the second sec	1	2 3	4	700	<u> </u>				RAS 4	5.0		EINIA	LEFF	6.0	
		! '	~ `	· +↑	······			·····	┨┝╌	WAS					56	
04 14 2.									╎╙		•	3		JINCL T	-0	
0-7 7-1 0.																
					START:	L,										
					10:40											
					FINISH:				1							
					10:50											
					OUT:				1							
					10:30											
					/				3							

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL)  $\times$  1,000,000

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TOTAL NITROGEN - 8.56 NITRATE - 6.12

Amoniq N<del>ITRITE</del> -0.134

X Removal \_10 - 6 x 100 - 95% 7 Primary Removal 110-48 x 100 - 56% 16/day RAW 8.34 x 110 x 2.08 = 1908 16/day PRI. 8-34 x 48 × 2.08 - 833 1b/day KUT. 8.34 x 6 x 2.08 = 104 MLSS, 8.34 x .467 x 4240 = 16514 SVI 1000 x 2)0 = 64 · m1/g  $Cr = \frac{4240}{2.5} = \frac{1696}{100} = \frac{1000}{100}$ SA :8.34 x .467 x 4240 8.34 x 48x 2.08 20 DAYS

SET	TLEO	METE	R		FAIRHAVEN C					TEST	INITIA	LS:		DATE:	1111	3115
Time	9	:05	-	:	SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3	F4/00	R3_	R4 5	A1 5	A2 5	Â3 5	WAS 5
time	SSV	SSC	SSV	SSC	CRUCIBLE				(							
0	1000				WT. + SAMPLE	21 4923	19 1019	19.4266	}	16. FB/A		22 0625	100 9962	11 375	8 71 595	21 3440
5	390								1				20,1107	*****		0.0.2.7.70
10	310				CRUCIBLE WT.	21.4910	19.0999	19,4263		16.580	1	22 0334	20 9344	212613	21.525	21.7172
15	280				DIFFERENCE PRE			.0003		.0006				.0661		
20	250				FURNACE	30	40	3		6		58 20	4260	13220	4140	5360
25	240				CRUCIBLE											1
30	830				WT. + SAMPLE	21-4925	19.1019	19.4266		16,5815	<u> </u>	22.0625	20.9962	21.3278	a <i>1.5959</i>	21.7440
40	220				WT. POST	30.00						1				
50	210				FURNANCE	31.4910				16.5809						21.7228
60	200				DIFFERENCE	.0015				-0006	1	.0152		.0363		
4 0 0				~		30	40	3		6		3040	<u>2270</u>	7260	2100	4240
123	A	1	2	3	PRE-FURNACE VOLATILE						)			1		
22 8.02.7	T C				FIXED SOLIDS	æ	ø	æ		B		2780	20110	1960	2040	1120
1/2/3/4	R	1	2 3	4			, e					4/00	0070	5760	00.70	1120
	s				COLIFORM	BACTERI	A	-	Г	MAGNETI	TE (m	9/L)		NOTES		1
4.6	C				SAMPLE	COLON		(100mL		MLSS A1	2.2		INF	. TEMP:		
1 2 3 4	D	1	2 3	4						MLSS A2				A1 pH:		
. n	0									MLSS A3				A2 pH:		
	В								[	RA <del>S</del> 3				A3 pH:	6.5	
1 2 3 4	A	1	2 3	4						RAS 4			FINA	LEFF		:
	D								L	WAS	0.4	8	AKAL	INITY	48	ļ
0.40.8 1.4	0					·										
					START:											
					FINISH:											
					FINION.											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 8. 50 NITRATE - 7.45

Amonia NITRITE - 0.683

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I Removal  $\frac{30-3}{30} = 90$ Z Primary Removal 30-40 x 100 -1b/day RAW 8.34 x 30 x 2: 3 = 575 16/day PRI. 8.34 x 40 x2 3 = >6> 1b/day EFF. 8.34 x 3 x 2.3 = 58 . MLSS, 8.34 x .467 x 4/40 = 16 124  $\frac{5VL}{400} = \frac{1000 \text{ m} 230}{4140} = 56 \text{ ml/g}$  $\frac{CF}{2.2} = \frac{4/40}{2.2} = \frac{1633 \text{ mg/l/ml}}{1633 \text{ mg/l/ml}}$  $\frac{54 \times 8.34 \times .467 \times 4/40}{8.34 \times 40 \times 23}$  21 DAYS

SE	TTLEO	METE	R		FAIRHAVEN C						ALS: $\nu$	10	DATE:	11 11	2115
Time	9	:20		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF/co	F3_	F4 /00 R3	R4 5	A1 5	A2 5	A3 5	WAS 5
0	SSV 1000		SSV	SSC		21.5781	21.20	ie Inco		20.602	16 10 10	IG JIK		02000	240005
5 10	420				CRUCIBLE WT.	215)50				20 60 19					20 9350
15 20	290 260				DIFFERENCE PRE FURNACE	-0031 62	.0024 48		1	.0005	.0462	,0199	-0332	.0224	.0255 5100
25 30	250				CRUCIBLE WT. + SAMPLE	21.5781		<u> </u>		20.6027	ſ.				21.0005
40 50	240 230				WT. POST FURNANCE			19.1002		20.6019	16.6043	19.4358	21.50%	22.0441	20.9801
60	230					.0031 62	.0024 48	.00 <i>04</i> 4		.0008 8					.02 <b>04</b> 4 <b>0</b> 80
123	א ד לי כ	1	2	3	PRE-FURNACE VOLATILE FIXED SOLIDS	Ø	æ	Ð	<u> </u>			19.40	2 (1 -	0-00	
25402	4 R 5	1	2 3	4	COLIFORM	,  _	·			MAGNETITE (n		1870	NOTES		1020
	o c	1	2 3	4	SAMPLE	COLON		/100mL		MLSS A1 2.: MLSS A2 3.0	20	INF	. TEMP: A1 pH:	17.0	
	0 B		- v	-						MLSS A3 2./			A2 pH: A3 pH:	6.8	
1234	4 A D	1	2 3	4				· ,		RAS 4 4.9 WAS 0.4			LEFF	0.0	
0.40.72.	/ 0								<b>-</b>					1	2
					START:										
					FINISH:										
					OUT:										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 3. By/L NITRATE - 6,03 m/L Ammenia = 0.06 mg/L 7.27 Ir luent NH3-N=26mg/L 20:1 RATIO

I Removal  $\frac{62-478}{62} = 100 = 94\%$ Z Primary Removal 62 - 48 x 100 - 23% 1b/day RAW 8.34 x 62 x 233 = 1205 1b/day PRI. 8.34 x 48 x 2.33 = 933 1b/day EFF. 8.34 x 4 x 2.33 = 78 MLSS, 8.34 x .467 x 4480 = 1) 449 SVI  $1000 \pm 250 = 56 \pm 1/g$ 4480 $\frac{4480}{2.5} = 1659 \text{ mg/l/ml}$ SA :8.34 x .467 x 4480 8.34 x 48 × 2.33 19 DAYS

SE	TTLEO		R		FAIRHAVEN C	ONTROL	DATA L	OG - BIO	MAG	TEST	INITIAL	LS: 🗸	0	DATE:	11 11	0115
Time		:/0		:	SAMPLES - VOLUME	INF 30	PRI 50	EFF/00	F3	F4 100				A2 5	A3 5	WAS 5
1.110	SSV	SSC	SSV	SSC	CRUCIBLE	ļ		i			)					
0	1000				WT. + SAMPLE	16.5850	21,4941	21 2616		19,1006	(	21 2906	27 0726	19 110	120 6244	21.5985
5	420				CRUCIBLE WT.						-	07.20100	<i>**</i> - 700	77,7007	40.047	01103
10	340					16.5812	21.4914	21.2611		19 1000	1	212501	22 0332	19 425)	20 6022	21.5752
15	300				DIFFERENCE PRE	,0038	.0027	-0005	$\square$	.0005		.0405	0404	.0397	.0218	,0233
20	220				FURNACE	76	54	5		6		8100	8030	7940	4360	4660
25	260				CRUCIBLE				i			1			-	
<u>30</u> 40	250	····			WT. + SAMPLE	16.5850	21.4941	21,2616		19.1006		21.2906	22.0736	19.46.54	20.6240	21.5985
<u>40</u> 50	230				WT. POST FURNANCE		austano	1101-								
60	230				DIFFERENCE		,0021	21.2613		19.1002		21.2712	22.0515	194153	20.6134	21 5805
0	<i>a</i>				VOLATILE	60		.0003		.0004	- I	-0194	,022/	.0201	30102	.0/80
123	A	1	2	3	PRE-FURNACE	60	42	3		4		3880	4420	4020	2120	3600
	Т	- •.	-	J	VOLATILE				۱.		1					
4.0 5.02.					FIXED SOLIDS	15	12.	2		2	_/	1/220	2000	2010	2240	1060
1-2-8-4		1	2 3	4		78	12.	<u> </u>		<u> </u>		TAAU	5600	9720	2090	1000
	s				COLIFORM I	BACTERI	Ą	: 1		MAGNETI	E (ma	<i>(</i> 1)		NOTES	/	
4.:	S C				SAMPLE	COLON		100mL		MLSS A1				TEMP:		
1234	D	1	23	4						MLSS A2				A1 pH:	-	
	0									MLSS A3				A2 pH:		
	B							:		RAS-3				A3 pH:	6.6	
1234		1	2 3	4	-					RAS 4				EFF		
										WAS	0.35	5	AKAL	INITY		
0.31118	5 0															
					OTADT.											
					START:			:								
	•				FINISH:			·								
					OUT:											

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TSS TESTING: (CRUCIBLE WY, + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - ノクシ NITRATE - 8. シシ

Amoni'q NITRITE- 0.069

I Removal  $\frac{76-5}{76} = 100 = 93\%$ I Primary Removal  $\frac{76-54}{76} = 100 = 29\%$ Ib/day RAM 8.34 x  $76 \times /.90 = 1204$ Ib/day PRI. 8.34 x  $54 \times 1.90 = 856$ Ib/day PRI. 8.34 x  $54 \times 1.90 = 856$ Ib/day EFF. 8.34 x  $5 \times 1.90 = 99$ MLSS, 8.34 x .467 x 4360 = 16981SVI 1000 x 250 = 57 m1/8 CF  $\frac{4360}{2.5} = 1744$  mg/1/m1

 $\frac{58.34 \times .467 \times 4360}{8.34 \times .54 \times 1.90}$  20 DAYS

5m1

<u>A1</u>

SET	TLEO		R		FAIRHAVEN CO	NTROL	DATA L	OG - BIO	MAG	TEST	INITIAL	S:	10	DATE:	1119	1115
Time	9	:10		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3	F4/00			A1 5		A3 5	WASIS
line	SSV	SSC	SSV	SSC	CRUCIBLE				T							
0	1000				WT. + SAMPLE	12 0404	20.9786	19 005		16.5815	21.5402		21605	21 2020	19 110	21.2744
5	400					<u> </u>		//////			A.1 .2700	$\vdash$	a(1,00)0	1367.3037	//.119	d1-0171
10	310					22.0322	209349	19.1000		16 5813	21.4913	)	21 574	11200	10 4259	21,2503
15	80	·	1		DIFFERENCE PRE-	,0072	.0037				.0489					.0241
	250				FURNACE	144	54	>	)		9380	$ \langle \rangle$				4830
	240				CRUCIBLE				1			$\uparrow$		1		
	240				WT. + SAMPLE	22.0404	20.9786	19.100>	$\mathbf{X}$	16.5818	21.5402	i `	21.60%	51.3239	19.448	21.2>44
	230				WT. POST				1					1	<i></i>	
	230					22.0348	20.9752	59,1000		16.5813	215179		21.5900	21.2930	19 1380	21.2560
60	220				DIFFERENCE									1	0107	
					VOLATILE							\			2140	
123	A	1	2	3	PRE-FURNACE										<u> </u>	
70 .	Т				VOLATILE											
3.0 7.022					FIXED SOLIDS				Ţ			- {				
1-2-2-4	R	1	2 3	4												
5.0	S				COLIFORM B	ACTERI. COLON		: 100mL		MAGNET	TE (mg/	L)		NOTES		
	c				SAMPLE	MLSS A1 2.74 IN					IF. TEMP: 12.4					
1234	D	1	2 3	4	B	<u> </u>		150		MLSS A2	5.56			A1 pH:		
•	0				50		MLSS A3	2.03			A2 pH: 6.8					
4 9 9 4	В				100	4		100		RAS.3		-		A3 pH:	6.6	
1 2 3 4	A	1	2 3	4	· ·					RAS 4				LEFF	1	
0.70.71.2	D O									WAS	6.43	ļ	AKAI	<u>.INITY</u>	75	
0. / 0. / I. K	0															
					START: 12-50											
					FINISH: 1:00											
					OUT:		· · · · · ·									
					11:45											
					11150											
	т	ee te	OTIM		RUCIBLE WT. + SAMP			10(T ) ()		<b>(</b>		~				

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TOTAL NITROGEN - 6 > NITRATE - 8 > NITRITE - 0 0>2

I Removal 
$$\frac{144 - 3}{144} = 100 = 95\%$$
  
Z Primary Removal  $\frac{144 - 34}{144} = 100 = 49\%$   
Ib/day RAW 8.34 x  $144 \times 1.39 = 2150$   
Ib/day PRI. 8.34 x  $74\times 1.39 = 1/05$   
Ib/day EFF. 8.34 x  $74\times 1.39 = 1/05$   
Ib/day EFF. 8.34 x  $74\times 1.39 = 105$   
MLSS, 8.34 x .467 x  $4.380 = 105$   
SVI 1000 x  $240 = 55$  ml/g  
CF  $\frac{4380}{2.2} = 1991$  mg/1/ml  
SA  $\frac{(8.34 \times .467 \times 4.380)}{8.34 \times 34 \times 1.39}$  15 DAYS

SET	TLEO		R		FAIRHAVEN C	ONTROL		.OG - BIC	MAG	TEST IN	ITIALS: V	0	DATE:	17 16	116
Time		:40			SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3	F4 /00 R			A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC							7				······································
0	1000				WT. + SAMPLE	21.5773	16 5841	22.0344		19.1013	24012	21 2908	11000	20 6266	19.4529
5	480				CRUCIBLE WT.							<i>x, x, 00</i>	41.7400	20 0203	19.130 1
10	380				CROCIBLE WI.	21,5 345	16.5816	22 0333		19.1005	20 935	21 2609	21 4914	20 6018	19 4264
15	340	ļ				1.0005	.0005	.0007		.0008					.0265
20 25	300				FURNACE	56	50	<u> </u>		8	7300	7180	7080	4940	5300
30	280						. 10	0.344						·	
40	260				WT. + SAMPLE WT. POST	21.5713	16.2819	22.0344		19.1013	21.0120	21.2968	21.5268	<u>20.6763</u>	19.4529
50	260				FURNANCE	21.5745	16 691	12 0221		19,005	20 60.1	L. M			a dese
60	260				DIFFERENCE	0078		0007	<u> </u>	0008	774	21,2772	31.5974	20.614	319.4328
	ų. <u>U</u>				VOLATILE	56	50	5		8	1017	20190	-0174	0117	10201
123	A	1	2	3	PRE-FURNACE			<u>/</u>			3400	3500	3480	2340	4020
	T				VOLATILE							ľ			
3.24.025	C				FIXED SOLIDS	ø	Ð	B	<u>}</u>	-e	3820	2380	3600	2600	1280
1-2-2-4	R	1	23	4			X				1 10 11		2000		1000
6.0	S				COLIFORM					MAGNETITE	(mg/L)	<b></b>	NOTES		
	<u>c</u>				SAMPLE	COLON	IES #/	/100mL		MLSS A1 3	3.03	INF	TEMP:	19.5	
1234	D	1	2 3	4						MLSS A2 3			A1 pH:	6.8	
•	О В								ļ	MLSS A3 2	.52		A2 pH:		
1234		1	2 3	4		ļ				RAS-3			A3 pH:	6.6	
, <b></b>	6		2 9	<b>4</b>	· · · · ·				·	RAS 4 3 WAS 0			EFF	78	
0.6 1.0 2.0	. – .									WAS D	- 36	AKAL	INITY	13	
		· · ·		ł	····										
					START:	L	I								
					FINISH:										
					OUT:										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL)  $\times$  1,000,000

TOTAL NITROGEN - 11. 5 NITRATE - 9.24 Amonia NITRITE - 0,472

Z Removal <u>56 - 56</u> x 100 - 88% 7 Primary Removal <u>56 - 50</u> x 100 - 11% 1b/day RAN 8.34 x 56 x / 98 = 925 16/day PRI. 8.34 x 50 + 1.98 = 826 1b/day EFF. 8.34 x > X 1.98= 116 MLSS, 8.34 x -467 x 4940 = 19240 SVI 1000 x 2 0 = 55 m1/g  $CF = \frac{4946}{2.5} = 1956 \text{ mg/1/ml}$ SA :8.34 x .467 x 4940 8.34 x 50 × 1.98 23 DAYS

		S	ET	TLEO					FAIRHAVEN C	ONTROL	DATA L	<u>OG - BION</u>	AG	TEST INIT	IALS: 🖌	0	DATE:	11 1 2	5115
	Tin	~~		9	35	1	:		SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3	F4 /00 R3	R4 5	A1 5			WAS
	1 111	ie	I	SSV	SSC	s	sv	SSC	CRUCIBLE										
	0	)		1000		ſ			WT. + SAMPLE	19.1505	209318	21.57.52		21,2615	an Liste	19 4155	A MAR	16 6050	21-5180
	5	i		470	1								-+-			<u>v 1.70-</u> 2	1/1./7./5	/4.00//	a/ 2/00
	1(			390		1			CRUCIBLE WT.	19.1470	209248	21.5750		21.2609	20 6014	19 4264	19 1000	16 581	21.4909
	1	5		740		Γ			DIFFERENCE PRE	.0035	.0020	,0002		-0006	.0435		.0475		
	2(			320					FURNACE	20	40	2		6					5420
	25			300		Γ			CRUCIBLE	•									
	- 30			280					WT. + SAMPLE	19.1505	20.9763	21.5752	۱.	21.2615	20.6449	19.4658	19.1475	16.6079	21.5180
	4(			260					WT. POST										
	50			<u>250</u>					FURNANCE			21.5750		21,2609	20.6250	19.4454	19.129	16.5953	214985
	60	)		750					DIFFERENCE	.0032	.0020	1 - 1	7	.0006	.0199	0204	.0223	.0126	.0195
			_						VOLATILE	64	40	2		6 /	3980	1080	4560	2520	3900
1 1	12	3		Α	1		2	3	PRE-FURNACE										
	×.			Т					VOLATILE										
3.2				<u>C</u>					FIXED SOLIDS	6	0			81	4720	3800	4940	2840	1520
T	2.	8	4	R	1	2	3	4	··										
:		4	5.0	S					COLIFORM			:		MAGNETITE (r			NOTES		
				<u></u>					SAMPLE	COLON	[!ES #/	100mL			52	INF	. TEMP:		
1	2	3	4	D	1	2	3	4							<u> </u>		A1 pH:		
·				0										MLSS A3 2.	83		A2 pH;		
	~	~		<u> </u>									L	RAS-3			A3 pH:	6.6	
1	2	5	4	A	1	2	3	4							60		LEFF		
0.6		s d	4م	D										WAS O.	25	AKAL	INITY		
0.0	<u> </u>	•7	<u>~</u>	<u>U</u>															
									OT 4 D T.										
									START:										
									FINISH:										· •.
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				• •	en ja en				ουτ:										
									001.										
									L										

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 12.0 NITRATE - 10.5

Amoniq NITRITE-0.688

I Removal  $\frac{20-2}{30} = 100 = 9)\%$ Z Primary Removal 100 - 43% 16/day RAW 8.34 x 70 × 1.96 = 1144 1b/day PRI. 8.34 x 40 x 1.96 = 654 16/day EFF. 8.34 x 2 × 1.96 = 33 MLSS, 8.34 x .467 x 5360 = 20,876 SVI 1000 x 280 = 52 ml/g  $\frac{\text{CF} = 5360}{2.7} = 1985 \text{ mg/1/m1}}$ SA <u>\*8.34 x .467 x 5360</u> 8.34 x 40 X 1.96 32 DAYS

\$ET	TLEO		R		FAIRHAVEN CO						INITI			DATE:	1/14	+115
Time		15		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3	F4 /00	R3	R4 5	A1 5	A2 5	A3 5	WAS 5
une	SSV	SSC	∣ssv	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	22 0384	20.6051	21.2521		21.4931	)	16.6405	19.1916	21.6094	19 4520	21.2926
5	480				CRUCIBLE WT.				1		7					
10	390					22.0332				21,4916						21.2611
15	350		ļ		DIFFERENCE PRE-	· -				.0015						.0315
20	320					104	64	14		15		11780	8920	6960	6180	6300
25 30	300		i		CRUCIBLE WT. + SAMPLE	22.0384	20 6051	110601	1	NI 1/07 1		11 Mala	a sale	- 1 may	10 4620	212926
40	260				WT. POST	00.0 <u>587</u>	40.00J	21.2301		21.493		15,0703	19.1710	21.007	17.1300	21-2926
50	250					22,0332	20.6019	21,250>		21.4918		16612	19 1663	21 5911	19 4383	21.2695
60	250		·		DIFFERENCE	.0052	.0032	.0014		.0015	┝╼┈┟─					.0731
					VOLATILE	104	64	14		15						4620
123	A	1	2	3	PRE-FURNACE				\ \							1
110 26 25	T				VOLATILE											
4.5 3.5 2.5		1	2 3		FIXED SOLIDS	B	đ	Ø		Ø		6/20	3940	3300	2440	1680
7284	RS	-]	2 3	4	COLIFORM		~			MACHET	TE /	- (1.)		NOTES		1
6.>	c				SAMPLE			/100mL		MAGNET MLSS A1			INE	TEMP;		
1 2 3 4	ŤĎ	1	2 3	4		001011		JOONIE		MLSS A2				A1 pH:		
l -	0									MLSS A3				A2 pH:	- Toronto and the second second	
	В									-RAS S				A3 pH:		
1 2 3 4	A	1	2 3	4	· · ·					RAS 4				L EFF	50	
	D									WAS	0.8	5	AKAL	JNITY	33	
0.3 0. ) /. 8	10															
					OTADT.											
					START:							*				
					FINISH:											
					OUT:											
						<b></b>										
					RUCIBLE WT + SAM				-							

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL)  $\times$  1,000,000

TOTAL NITROGEN - 828 NITRATE - 89

Amonia NHATTE- 0.073

I Removal  $\frac{104 - 64}{104} = 100 = 86\%$ Z Primary Removal 104-64 x 100 - 38% 16/day RAW 8.34 x 104 x 1.95 = 1591 1b/day PRI. 8.34 x 64 x 1.95 = 1040 1b/day EUR. 8.34 x 14 × 1.95 = 228 MLSS, 8.34 x .467 x 5/80 = 20 175  $\frac{\text{SVI} \ 1000 \ \pi \ 280}{5180} = 54 \ \text{ml/g}$  $\frac{CF}{2.5} = \frac{5/80}{20} = \frac{30}{2} \mod \frac{1}{mg} = \frac{1}{mg}$ 54. <u>\*8.34 x .467 x 5/80</u> 8.34 x 64 x 195 19 DAYS

SET	TLEO	METE	R		FAIRHAVEN C						INITIA	LS: V	0	DATE:	11 18	81 15
Time		20		:>0	SAMPLES - VOLUME	INF 50	PRI ᠫ	EFF /00	F3 //	F4 /00	R3	R4 5	A1 5	A2 5	A3 5	WAS
Time	ssv	SSC	SSV	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	19.1498	21.493	22 0339		21.5753		19 494	an hun	21.2808	26.60%	
5	490					<u>////</u>				1 27/22			AC.07 2.	 	1/0.00%	
10	710				CRUCIBLE WT.	19.1469	21.4909	22 0330		21.5745	•	19 4258	20 60 13	21 2499	16 581	212611
15	580				DIFFERENCE PRE	.0029	.0024	.0009		.0008				0309		
20	350				FURNACE	58	48	9		8		11720	8140	6180	5200	
25	310				CRUCIBLE						. [					
30	300			:		19.1498	21.4935	22.0339	\	21.5%	5	19.4844	20.6476	21.2308	16.602	
<u>40</u> 50	<u>58</u>				WT. POST	10	01/10-0	00 0770		21.5749	-					
60	220			~~ <u>_</u>	FURNANCE DIFFERENCE	0026	21 4407	22.0330	<u> </u>	.0008	-			21 2652		
	270		4		VOLATILE	52	48	9		8				.0156	1 · ·	· ·
123	A	1	2	3	PRE-FURNACE	52	40	<u> </u>		<u>×</u>		5540	H300	3/20	2660	
	T		~	Ť	VOLATILE				i i				:			
4.5 3.22.	c				FIXED SOLIDS	6	ø	Ø		Ø	<u> </u>	6180	ZQHO	2060	2640	
1234	R	1	2 3	4			······	. ~			/	0700	5070	3000	070	
1	S				COLIFORM	BACTERI	A	:		AGNETI	TE (m	a/L)		NOTES		ĩ
2.0	C				SAMPLE	COLON		/100mL		VILSS A1			INF	TEMP:		
1234	D	1	23	4						MLSS A2	3.2	0		A1 pH:		
	0									MLSS A3		0		A2 pH:		
	B						·			RAS-3				A3 pH:	6.6	
1234		1	23	4						RAS 4	6.0	<u>#</u>		LEFF		
0.20.92.8	D					•				WAS		-	AKAL	INITY		
					START:											
					FINISH:											
					OUT:											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 733 NITRATE - 5.06

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Amonia 0.106 NITRITE -

X Removal 
$$\frac{58-9}{58}$$
 x 100 =  $84\%$   
X Primary Removal  $\frac{58-48}{58}$  x 100 =  $17\%$   
Ib/day RAW 8.34 x  $58\times20$  =  $96\%$   
Ib/day PRI. 8.34 x  $48\times20$  =  $801$   
Ib/day PRI. 8.34 x  $48\times2.0$  =  $801$   
Ib/day EFF. 8.34 x  $9\times2.0$  =  $150$   
MLSS, 8.34 x .467 x  $5200$  =  $20253$   
SVI 1000 x  $300$  =  $58$  m1/g  
CF  $\frac{5200}{8.34}$  x  $-467$  x  $5200$  2.5 DAYS

Al 5mL

SET	TLEO				FAIRHAVEN C	ONTROL	DATA L	OG - BIOI	MAG 1	EST	INITL	ALS:		DATE:	11 18	115
Time		:15		: 7	SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3/	F4 /00						WASS
Time	SSV	ssc	ssv	SSC	CRUCIBLE	}						<u> </u>				
0	1000				WT. + SAMPLE	21.2727	20,6052	215760		21.4923		16 634	19.1311	19 4613	22 0586	
5	650				CRUCIBLE WT.				1				///			
10	520					212.505				21.4914	Į	16.5816	19 1478	19 4266	12 0340	209952
	450		N		DIFFERENCE PRE			0008	1	,0009	1	.0.534	.0233	.0347	,0246	
20	410				FURNACE	444	62	8	<u> </u>	9	<b>\</b>	10680	4660	6940	4920	
	380				CRUCIBLE	. abot					Ì					
	\$50				WT. + SAMPLE	21.0101	20.6052	21.5760	<u> </u>	21.4923	<u>\</u>	16.6350	19.1711	19.4613	22.0586	
<u>40</u> 50	330		·		WT. POST		an const		\							
	300				FURNANCE DIFFERENCE	21.2584				21.4914		16.6079	19 1587	19.4435	22.0458	
	700			ł.,	VOLATILE		0028			.0009	ļ			,0178		
123	Â	1	2	3		286	56	8		7	}	5420	2480	3560	2560	
1 4 3	A T		2	്	PRE-FURNACE VOLATILE				1							
2.3 4.02.3					FIXED SOLIDS	158	6	ø		Ø	<u> </u>		1100	7700	0210	
1-2-3-4	R	1	2 3	4		190	0			N	{	9260	2180	3380	2360	
	s	•			COLIFORM	BACTERI	Δ			AGNETI	TE	a/L )		NOTES	_	ſ
6.5	Ċ				SAMPLE	COLON		100mL		WLSS A1				TEMP:		
1 2 3 4	D	1	2 3	4	ß	2				MLSS A2			11.41	A1 pH:		
-	0				50	5	5	150		MLSS A3				A2 pH:	6.8	
	В				100			1,00		RAS 3				A3 pH:	6.7	
1234	A	1	2 3	4		, í				RAS 4	4.6	6	FINA	LEFF		
	D			i						WAS			AKAL		71	
0.40.61.9	0															
								:								
					START:											
					1:00											
					FINISH:											
					1:15											
					OUT:											
					RUCIBLE WT + SAM											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 4.6.3 NITRATE - 3.06

Amonia .058

I Removal  $\frac{444-8}{444} = 100 = 98$ 7 Primary Removal 444-67 x 100 - 86 15/day RAW 8.34 x 444 x 2.0.3 = 751> 1b/day PRI. 8.34 x 62 × 2.03 = 1049 1b/day ETF. 8.34 x 8 x 2.03 > 135 MLSS, 8.34 x .467 x 4920 = 19 162 SVI 1000 x 350 - 7/ ml/g  $CF = \frac{4/920}{2.5} = \frac{822 \text{ mg/l/ml}}{1000}$  $\frac{54 + 8.34 \times .467 \times 4920}{8.34 \times 62 \times 203}$  /8 DAYS

		METE	:R		FAIRHAVEN C	DNTROL	DATA L	<u> 0G - BlO</u>	MAG 1	TEST	INITIAL	.S:		DATE:	1013	0115
Time		:/0			SAMPLES - VOLUME	INF SE	PRI 60	EFF 100	F3	F4 100	R3	R4 5	A1 5			WAS
0	SSV 1000		SS∨	SSC		2. (		10 10.	The second s				_			
5	440					20.6053	22.0351	16.5824		21.2514	<u> </u>	21.6339	21.5182	19.1881	19.4.57	
10	350				CRUCIBLE WT.	20 6018	22 0224	16.5812		21.2500	/	215348	21 4916	10 11/22	10 470	20.9747
15	310				DIFFERENCE PRE	.0035	,002-3	.0012	<u> </u>	.0014		0590	.0267	,0409	.0257	2-111/
20	R90				FURNACE	70	46	12		14	1			8,180		
25	270				CRUCIBLE		,				1					
30	250				WT. + SAMPLE	20.6053	22.0357	16.5824		21.2514		21.6333	21,5181	<u>/9.  </u> 381	19.4520	
40	240				WT. POST			. A care			1	_				_
50 60	230			1	FURNANCE DIFFERENCE	20.6018	<u> </u>			21.2500				19_163		7
	14.50				VOLATILE	70	.0023	.0012	(	14	1,			,0204		
123	A	1	2	3	PRE-FURNACE	10	46	12		77	<u> </u>	5660	2760	4080	2670	
' <u>~</u> `	T	•	£n.	Ŭ	VOLATILE				a Li		1					
2.5 4.32					FIXED SOLIDS	ê	ø	æ		B	1	6140	2580	4100	2620	
1234	R	1	2 3	4										*// • •	<i>o G p c c</i>	
	S				COLIFORM	<b>BACTERI</b>	A .	:		MAGNETI	TE (mg	/L)		NOTES		
6.0					SAMPLE	COLON	IES #/	100mL		MLSS A1			INF	. TEMP:		
1234	-	1	2 3	4						MLSS A2		<b>/</b>		A1 pH:	6.9	
•	0			:						MLSS A3	2.69			A2 pH:		
1 2 3 4	B	1	2 3	4						RAS 3				A3 pH:	<u>6.5</u>	
1 2 3 4		1	2 3	4	·					RAS 4	0.2	2		L EFF		
0.50.9 2.5					·····	  ,								IINI I I		
	Ŭ															
					START:	L										
					FINISH:											
					OUT:											

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 10 . 1

NITRATE - 7.63

Amonia 0,15%

 $Z \text{ Removal} = \frac{70 - 12}{70} = 83\%$ 2 Primary Removal 70-46 x 100 - 34 % 15/day RAW 8.34 x 70 × 2.16 = 1261 16/day PRI. 8.34 x 46 × 2.16 = 829 16/day EFF. 8.34 x 12×2.16 = 2.16 MLSE, 8.34 x .467 x 5/40 = 20 019  $\frac{\text{SVI} \ 1000 \ \text{m} \ 250}{5140} = 49 \ \text{ml/g}}{1000}$ CF <u>5140</u> = 2056 mg/1/ml SA 34 x 467 x 5140 8.34 x 46 × 2 16 24 DAYS

SET	TLEO	METE	R		FAIRHAVEN CO					TEST II	NITIALS:	. V	10	DATE:	10 12	9115
Time	9	:30		:	SAMPLES - VOLUME	INF 50	PRI 50	EFFLOO	F3]	F4 /20 1	R3, R	45	A1 5		A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	19,4360	21.5778	16 58 B	1	19.1012	/ 12	1.0409	21.2796	217470	20.623	21.5237
5	360				CRUCIBLE WT.			-			7					
10	300					19.4265				19.0998						21.4916
15	260				DIFFERENCE PRE-		1	,0007	1	.0014			.0185			7.
20	240				FURNACE	190	60	7		14	1	220	3700	6140	4420	6420
25	240		ļ			19.1300	21.5770	16.5818		19.1012	1 2/	0409	21.2796	21.7870	20.6232	6420 21.5237
<u> </u>	220				WT. + SAMPLE WT. POST				{							Ø1.3007
	200				FURNANCE	19 4276	21.5750	16.5811		19 0999	1 2	10108	212203	21 7-22	20 612	21.4999
60	200				DIFFERENCE	,0084	0028	.000 >	$\rightarrow$	.0013		0301				.0238
	20-2			· · · · · ·	VOLATILE	168	56	> 1		/3	1 1	•				4760
123	A	1	. 2	3	PRE-FURNACE							<del>.</del>	- <b>*</b>			
1 1 1 1 2 2 2 2	T	:					[		<u> </u>							
2) 3,022	-				FIXED SOLIDS	22	4	B	1		1 7	200	1840	3180	2120	1660
7234	R	1	2 3	4								_				
70	S	-			COLIFORM					MAGNETIT				NOTES		
1 2 3 4		1	2 3		SAMPLE	COLON	<u>IIES #/</u>	1 <b>00m</b> L		MLSS A1	2.65	_	INF.	TEMP:		
1 2 3 4	Ö	8	2 3	4						MLSS A2 . MLSS A3 -		-		A1 pH: A2 pH;		-
	в									RAS 3			FIN	AL EFF		
1 2 3 4		1	2 3	4						RAS 4		- I - I		ALINITY		
	D										0.69		140			1
0.4 1.3 3.1	ο								<b>.</b>			Ň				
												· ·	S	EPTAG	E	
					START:								Fa	irhaven		
													Matt	apoisett		
					FINISH:					•				Marion		
													· · · · · · · · · · · · · · · · · · ·	chester	La construction of the later of	
					OUT:								A			
														TOTAL		
	т	99 TE		a in	RUCIBLE WT + SAM						000.000					

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN - 5.36 NITRATE - 3.89

NITRITE~

Amonia AlkALINITY - 0.09

 $I \text{ Removal} = \frac{190 - 7}{190} = 100 = 96\%$ 2 Primary Removal 190-60 x 100 - 68% 16/day BAN 8.34 x 190 × 2.54 = 4025 16/day PRI. 8.34 x 60 x2.54 = 1271 15/day LTF. 8.34 x > x2.54 = 148 MISS, 8.34 x .467 x 4420 = 17215 SVI 1000 x 220 50 ml/g  $CF = \frac{4420}{22} = 2009 mg/1/m1$ SA 48.34 x .467 x 4420 8.34 x 60 x 2.54 14 DAYS

SET	TLEO				FAIRHAVEN C	ONTROL	DATA L	0G - BIO	MAG TI	EST		.S:	10	DATE:	10 12	\$11.5
Time		35		:	SAMPLES - VOLUME	INF SO	PRI 50	EFF <i>joo</i>	F3	F4 100	R3	R45				WHAS 5
1 mile	ssv	SSC	SSV	SSC	CRUCIBLE											
0	1000				WT. + SAMPLE	20.6034	21578	16 5828		19.4267		19 1512	20.996	21.7454	21 783)	24-
5	400				CRUCIBLE WT,						(	1			<u> </u>	
10	310					20 6012	21.5745	16 5811	(	19.4259		19.0990	20.9747	2) 7/64	212608	21.3553
15	280				DIFFERENCE PRE-	,0022	,0028	,0017		,0003	1	.0522	.0220	,0290	.0229	
20	250				FURNACE	44	56	1.15	/	8	í	10440	4400	5800	4580	
25	240				CRUCIBLE	(					)					
30	230				WT. + SAMPLE	20.6034	2 <u>1.5773</u>	16.5878		19.4257	i,	19-1512	20.996>	21.7454	21.283)	
40	220				WT. POST						1					
50	220				FURNANCE	20.60 12			· \	19.4259				21.7315		
60	220				DIFFERENCE	.0022		0014		.0003	1			,0139		
					VOLATILE	44	56	14		8		4780	2120	2780	2200	
123	Α	1	. 2	3	PRE-FURNACE				****		(			, , , , , , , , , , , , , , , , , , , ,		
	Т				VOLATILE				/							
22 3022	C				FIXED SOLIDS	Ľ	Ø	3	1	0	}	5660	2280	3020	2380	
1284	R	1	2 3	4					ه ا							_
5.5	S			[	COLIFORM			:	M	AGNETT	ſE (mg	/L)		NOTES		
þ	C				SAMPLE	COLON	IES #/	100mL		LSS A1			INF	. TEMP:		
1 2 3 4	D	1	23	4						ILSS A2				A1 pH:	6.9	
•	0				· .				Ň	LSS A3	2.23			A2 pH:		
	В									RAS-3	<u> </u>	·	FIN	IAL EFF		
1234	A	1	23	4						RAS 4	1		AK/	ALINITY	7/	
	D									WAS	5!33					-
0.2133.3	0															
														SEPTAG	E	
					START:								Fá	airhaven		
													Mati	apoisett		
					FINISH:									Marion		
														ochester		
					OUT;								A	cushnet		
														TOTAL		
																-

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) × 1,000,000

TOTAL NITROGEN - 9.23 NITRATE - 8.31

Ammonia 0.258 ALKALINITY-71

I Removal  $\frac{44 - 1}{44} = 100 = 61\%$ Z Primary Removal - 44 - 56 x 100 -1b/day RAW 8.34 x 44×1.98 = >2> 16/day PRI. 8.34 x 56.× / 98 = 92-5 1b/day EFF. 8.34 x 1) x 1.98= 281 MLSS, 8.34 x .467 x 4580 = 1 338 $\frac{5VI}{4580} = \frac{1000 \times 230}{4580} = 50 \text{ mL/g}$ CT <u>4580</u> **\*20**82 mg/1/ml SA <u>\*8.34 x 467 x 4580</u> 19 DAYS

No Return Due to Switching Tanks 333 - 334

G •							<u> OG - BIO</u>				NITIA					10 15	7115
	25		0	SAMPLES - VOLUME	INF 50	PRI 50	EFF <i>j00</i>	F <b>F</b> /1	0 F4	1	R3 <u>5</u>	R4	A	15	A2 5	A3 5	WAS 5
ssv	SSC	SSV	SSC	CRUCIBLE					1		1						
1000				WT. + SAMPLE	21.2859	19 1500	22 6343	2149	2				24	0.5077	21 2614	15.7431	19.5979
160								-									
20				CRUCIBLE WI.	21.2824	19.1473	22 0334	2149	5		16 8	5	3 2	0.172	31,259	17.734	19.5576
10				DIFFERENCE PRE	.0035	.0027	.0009	,001	5	7							
00				FURNACE	70	54	9	16			(		1	940	2100	1520	8040
00																	
100				WT. + SAMPLE	21.2891	19.1500	22.0343	21.493	li .	1	/		20	0.3072	21.2614	17. 7431	19.5978
00				WT. POST							1						
90				FURNANCE	21.2823	19.1474	220334	21.491									
20		_		DIFFERENCE			.0009	.001	8		1	1		0050			
				VOLATILE	68	52	9	16					1	1000	1140	840	5540
A	1	. 2	3	PRE-FURNACE					1		1	Ń				1	
Т				VOLATILE					1	ŀ	(	, î					
c				FIXED SOLIDS	2	2	D	ø			1		2	940	960	680	2500
R	1	2 3	3 4								¥						
s				COLIFORM	BACTERI	A	:		MAGN	IETIT	E (m	g/L)			NOTES		1
c				SAMPLE	COLON	IES #	/100mL							INF.	TEMP:	18.1	1
D	1	2 3	) 4					1 Г	MLSS	A2	0.8	22					1
0								1 [	MLSS	A3	0.5	9			A2 pH:	6.9	1
B								1 F	RA	8-3			I [	FIN	AL EFF		
A	1	2 3	3 4					1 Г	RA	<del>S</del> -4				AKA	ALINITY	61	
D								1 [	V	/AS	1.6	3	-				-
0								1 -					-				
				·	1			1						S	EPTAG	Ë	1
				START:	<u> </u>	·····		1						Fa	airhaven		1
														Matt	apoisett		
				FINISH:				1							Marion		
													Ē	Ro	chester	1	1
				OUT:			· · ·	1						A	cushnet	:	1
															TOTAL		1
	000 60 20 00 00 00 00 00 00 00 00 00 00 00 00	000 160 20 00 00 00 00 00 00 00 00 0	000 60 20 00 20 00 00 00 00 00 00 0	000	000       WT. + SAMPLE         160       CRUCIBLE WT.         20       DIFFERENCE PRE         20       CRUCIBLE         20       COLIFORM         21       23         4       COLIFORM         5       CRUCIFORM         6       CRUCIFORM         7       START:         7       START:         7       START:	000       WT. + SAMPLE       2/.3359         20       CRUCIBLE WT.       21.2824         20       DIFFERENCE PRE       .0035         20       CRUCIBLE       7.0         20       CRUCIATILE       6.8         20       STARTILE       FIXED SOLIDS         21       23       4       COLIFORM BACTERI         21       23       4       COLIFORM BACTERI         20       START:       START:       FINISH:	000	000       WT. + SAMPLE       2/.3359       19.1500       22.034/3         20       CRUCIBLE WT.       21.2334/19.14/33       22.0334/3         20       DIFFERENCE PRE       .0035       .0035       .0009         20       CRUCIBLE       70       54       9         20       WT. + SAMPLE       2/.2859       19.1500       22.0347         20       WT. + SAMPLE       2/.2859       19.1500       22.0347         20       WT. POST       YOLATILE       68       52       9         20       VOLATILE       68       52       9       9         20       VOLATILE       SAMPLE       20.034       9       9         21       23       4       COLIFORM BACTERIA       1       1       100mL         31       2       3       4       Image: SAMPLE       Image: SAMPLE       1       100mL         36       SAMPLE       <	000       WT. + SAMPLE       2/.3359       19.1500       22.0374       21.493         20       CRUCIBLE WT.       21.23234       19.1473       22.0334       21.493         20       DIFFERENCE PRE       .0035       .0037       .0009       .0019         20       CRUCIBLE       7.0       5.44       9       16         20       CRUCIBLE       VT. + SAMPLE       21.2837       19.1500       22.0343       21.493         20       CRUCIBLE       VOLATIBLE       7.0       5.44       9       16         20       CRUCIBLE       VT. + SAMPLE       21.2837       19.192       0334       21.493         20       VT. + SAMPLE       21.2837       19.1500       22.0343       21.493         20       VT. POST       FURNACE       7.0       5.60       20.034       21.3334       21.493         20       DIFFERENCE       .0034       .0026       .0009       .0017         20       VOLATILE       S       .0034       .0026       .0019       .0017         21       23       4       COLIFORM BACTERIA	000       WT. + SAMPLE       2/.3359       19.1500.22 c37.32/.4931         100       CRUCIBLE WT.       21.3834/19.1500.22 c37.321.4931       20.3374 21.4915         100       DIFFERENCE PRE       .0035       .0009       .0016         100       CRUCIBLE       VT. + SAMPLE       21.3834/19.1473       22.03374 21.4915         100       CRUCIBLE       VT. + SAMPLE       21.3834/19.14931       00.9016         100       CRUCIBLE       VT. + SAMPLE       21.3834/19.1500       22.0343 21.4931         100       CRUCIBLE       VT. + SAMPLE       21.3834/19.1500       22.0343 21.4931         100       VT. POST       FURNANCE       21.3834/19.14931       00.0009       .0016         100       DIFFERENCE       .0034/1020       .0009       .0016       VOLATILE         110       PRE-FURNACE       VOLATILE       VOLATILE       VOLATILE       VOLATILE         110       SAMPLE       COLIFORM BACTERIA       MAGN       MLSS         111       213       4       VOLATILE       VOLATILE       VOLATILE         111       213       4       VOLATILE       VOLATILE       VOLATILE         111       213       4       VOLATILE       VOLATILE       VOL	000       WT. + SAMPLE       21.2359       19.150022       034321/49.15         1/20       CRUCIBLE WT.       21.2324       19.1473       22.0334       21.49.15         1/20       DIFFERENCE PRE       0035       0035       0009       0016         20       CRUCIBLE       VI.       21.2324       19.1473       22.0334       21.49.15         1/20       DIFFERENCE PRE       0035       0035       0009       0016         20       CRUCIBLE       VI.       19.1473       22.03473       21.4931         20       CRUCIBLE       VI.       9.050       22.03473       21.4931         20       VI.       POST       19.1500       22.03473       21.4931         20       FURNANCE       21.2935       19.1742       21.0334       21.4931         20       FURNANCE       20.0347       10.334       21.4931         20       FURNANCE       20.0345       19.1742       21.0334       21.4931         20       FURNANCE       20.3455       19.1742       21.0334       21.4931         20       FIXED SOLIDS       2       2       2       2       2         21       SAMPLE       COLIFORM BACTERIA <td>000       WT. + SAMPLE       2/.2359       19.150022.0374.21/4921         20       CRUCIBLE WT.       21.2824       19.1473       22.0334       21/4915       16.581         20       DIFFERENCE PRE       00.35       .0009       .0016       .0009       .0016         20       CRUCIBLE       YO       54       9       16       .0016       .0009       .0016         20       CRUCIBLE       YO       54       9       16       .0016</td> <td>000       WT. + SAMPLE       2/.3359       19.1500.22 0374.32/.4931         1/20       CRUCIBLE WT.       21.2824/.9.1473.22.0334.21.4935       16.58152         1/20       DIFFERENCE PRE       .0035       .009       .0009       .0016         1/20       CRUCIBLE       7.0       544.9       16       .009       .0016         1/20       CRUCIBLE       7.0       544.9       16       .009       .0016         1/20       CRUCIBLE       0.035       .009       .0016       .0017       .0017         1/20       CRUCIBLE       1.2824/.9.149.19.1500       22.02473.21.4931       .0016       .0016         1/20       CRUCIBLE       1.28347.19.1500       22.02473.21.4931       .0016       .0016         1/20       WT. + SAMPLE       21.28347.19.1500       22.0373.21.4931       .0016       .0016         1/20       WT. POST       FURNANCE       .00347.0036       .0029       .0016       .0016         1/20       DIFFERENCE       .00347.00346       .00347.0036       .0016       .0016       .0016         1/20       VOLATILE       .00347.00346       .0029       .0016       .0016       .0016         1/20       2.3.4       COLIFORM BACTER</td> <td>000       WT. + SAMPLE       2/3359       19.1500       22.0314       2/49.1       2         20       CRUCIBLE WT.       21.2324       19.1473       22.0334       21.4915       16.5814       3         20       DIFFERENCE PRE       0035       0009       0016       1       1       16       1         20       CRUCIBLE       VOLATILE       0.35       0029       0016       1       1       2       16       1       1       2       16       1       16       1       1       2       16       1       1       16       1       1       16       1       16       1       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16       <td< td=""><td>000       WT. + SAMPLE       2/.3359       19.1500       20.2373       21.4931       20.3572         20       CRUCIBLE WT.       21.3334       19.1473       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5915       20.3092         20       CRUCIBLE       7.035       20.392       20.099       .0016       19.400         20       WT. + SAMPLE       21.2359       19.1432       20.343       21.4931       20.3022         20       WT. + SAMPLE       21.2355       19.1432       20.343       21.4931       20.3022         20       WT. POST       70.324       21.4935       14.4931       20.3022       20.3022         20       DIFFERENCE       20.324       .0029       .0016       .0036       .0029       .0016       .0036         20       VOLATILE       6.9034       .0026       .0029       .0016       .0036       .0016       .0036         20       VOLATILE       SAMPLE       COLIFORM BACTERIA      </td><td>000         WT. + SAMPLE         2/.3456/19.1500.22.03/3.21/45.1         20.35/2.21.36/4           20         CRUCIBLE WT.         21.2324/19.14/3.2.0334/21.45.15         30.39.21.326           20         DIFFERENCE PRE         .0033         .0029         .0016         .0095         .0039         .0039         .0039         .0039         .0039         .0039         .0036         .0039</td><td>000         WT. + SAMPLE         1/3359         19.160021         21.4821         20.3572         21.307         13.232         13.232         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.1421         21.335         13.325</td></td<></td>	000       WT. + SAMPLE       2/.2359       19.150022.0374.21/4921         20       CRUCIBLE WT.       21.2824       19.1473       22.0334       21/4915       16.581         20       DIFFERENCE PRE       00.35       .0009       .0016       .0009       .0016         20       CRUCIBLE       YO       54       9       16       .0016       .0009       .0016         20       CRUCIBLE       YO       54       9       16       .0016	000       WT. + SAMPLE       2/.3359       19.1500.22 0374.32/.4931         1/20       CRUCIBLE WT.       21.2824/.9.1473.22.0334.21.4935       16.58152         1/20       DIFFERENCE PRE       .0035       .009       .0009       .0016         1/20       CRUCIBLE       7.0       544.9       16       .009       .0016         1/20       CRUCIBLE       7.0       544.9       16       .009       .0016         1/20       CRUCIBLE       0.035       .009       .0016       .0017       .0017         1/20       CRUCIBLE       1.2824/.9.149.19.1500       22.02473.21.4931       .0016       .0016         1/20       CRUCIBLE       1.28347.19.1500       22.02473.21.4931       .0016       .0016         1/20       WT. + SAMPLE       21.28347.19.1500       22.0373.21.4931       .0016       .0016         1/20       WT. POST       FURNANCE       .00347.0036       .0029       .0016       .0016         1/20       DIFFERENCE       .00347.00346       .00347.0036       .0016       .0016       .0016         1/20       VOLATILE       .00347.00346       .0029       .0016       .0016       .0016         1/20       2.3.4       COLIFORM BACTER	000       WT. + SAMPLE       2/3359       19.1500       22.0314       2/49.1       2         20       CRUCIBLE WT.       21.2324       19.1473       22.0334       21.4915       16.5814       3         20       DIFFERENCE PRE       0035       0009       0016       1       1       16       1         20       CRUCIBLE       VOLATILE       0.35       0029       0016       1       1       2       16       1       1       2       16       1       16       1       1       2       16       1       1       16       1       1       16       1       16       1       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16       1       16 <td< td=""><td>000       WT. + SAMPLE       2/.3359       19.1500       20.2373       21.4931       20.3572         20       CRUCIBLE WT.       21.3334       19.1473       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5915       20.3092         20       CRUCIBLE       7.035       20.392       20.099       .0016       19.400         20       WT. + SAMPLE       21.2359       19.1432       20.343       21.4931       20.3022         20       WT. + SAMPLE       21.2355       19.1432       20.343       21.4931       20.3022         20       WT. POST       70.324       21.4935       14.4931       20.3022       20.3022         20       DIFFERENCE       20.324       .0029       .0016       .0036       .0029       .0016       .0036         20       VOLATILE       6.9034       .0026       .0029       .0016       .0036       .0016       .0036         20       VOLATILE       SAMPLE       COLIFORM BACTERIA      </td><td>000         WT. + SAMPLE         2/.3456/19.1500.22.03/3.21/45.1         20.35/2.21.36/4           20         CRUCIBLE WT.         21.2324/19.14/3.2.0334/21.45.15         30.39.21.326           20         DIFFERENCE PRE         .0033         .0029         .0016         .0095         .0039         .0039         .0039         .0039         .0039         .0039         .0036         .0039</td><td>000         WT. + SAMPLE         1/3359         19.160021         21.4821         20.3572         21.307         13.232         13.232         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.1421         21.335         13.325</td></td<>	000       WT. + SAMPLE       2/.3359       19.1500       20.2373       21.4931       20.3572         20       CRUCIBLE WT.       21.3334       19.1473       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5815       30.392         20       DIFFERENCE PRE       20.335       20.327       20.334       21.4915       16.5915       20.3092         20       CRUCIBLE       7.035       20.392       20.099       .0016       19.400         20       WT. + SAMPLE       21.2359       19.1432       20.343       21.4931       20.3022         20       WT. + SAMPLE       21.2355       19.1432       20.343       21.4931       20.3022         20       WT. POST       70.324       21.4935       14.4931       20.3022       20.3022         20       DIFFERENCE       20.324       .0029       .0016       .0036       .0029       .0016       .0036         20       VOLATILE       6.9034       .0026       .0029       .0016       .0036       .0016       .0036         20       VOLATILE       SAMPLE       COLIFORM BACTERIA	000         WT. + SAMPLE         2/.3456/19.1500.22.03/3.21/45.1         20.35/2.21.36/4           20         CRUCIBLE WT.         21.2324/19.14/3.2.0334/21.45.15         30.39.21.326           20         DIFFERENCE PRE         .0033         .0029         .0016         .0095         .0039         .0039         .0039         .0039         .0039         .0039         .0036         .0039	000         WT. + SAMPLE         1/3359         19.160021         21.4821         20.3572         21.307         13.232         13.232         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.160         21.3324         19.1421         21.335         13.325

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

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TOTAL NITROGEN - 12.3 NITRATE - 61

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Z Removal 70 - 9 x 100 - 87% 7 Primary Removal - -54 x 100 = 23% 1b/day RAW 8.34 x >0×=/82 = 1063 15/day PRI. 8.34 x 54 x /.82 = 820. Ib/day ENT. 8.34 = 9 × 1.82 = 13) MLSS, 8.34 x .467 x 1520 = 5920  $\frac{\text{SVI}}{1520} = \frac{1000 \text{ m}}{1520} = 66 \text{ ml/g}$  $CF = \frac{1520}{(1-0)} = \frac{1520 \text{ mg/l/ml}}{520 \text{ mg/l/ml}}$ SA -8-34 x -467 x /520 8-34 x 54 x 182 - 7 DAYS

SE	ITLEO	METE	R		FAIRHAVEN C						INITIAL			DATE:	10 12	5115
Time	9	27		:	SAMPLES - VOLUME	INF 50	PRISO	EFF/20	F3 /20	F4	R3 5	R4	A1 5	A2 5	A3 5	WAS 5
0	SSV 1000	•		SSC	CRUCIBLE WT. + SAMPLE	zo. 99.25	21,4392	21.7171	19, 1005		19,6157		21,28/7	21.135[	19.4472	21,7837
5 10	370				CRUCIBLE WT.	20,9751	21.4355	21.7163	19.0999		19,5112		21.2/29	21.611.5	19,420	21,7560
15 20	260				DIFFERENCE PRE FURNACE	148	<u>74</u>	8	6		10495 9.900		4.160	4,820	4,200	.0277 5,540
25 30	2020				VALLE DOOT	20.985				+ 7	19.6157		_			21, 7837
40 50 60	2012				WT. POST FURNANCE DIFFERENCE	20.9756	21/13/1	21,7162	17.197	4 /	19,5939 10218	ļ				21,7132 :02.05
123		1	. 2	3	VOLATILE PRE-FURNACE	138	62	9	9		4,360					4,100
2.0 4.0 2.1	Т	I	. 2	3	VOLATILE FIXED SOLIDS	148 70	74 12	8	6		9,900 5.540					5,540
1-2-3 4	R	1	2 3	34	······							·····				
5.0	S C				COLIFORM SAMPLE	BACTERI COLON		: /100mL		MLSS A	<b>FITE (mg/</b> 1 ス, <i>45</i>		INF	NOTES		
1234 ·	0	•	2 3	34	0 100	8		3/100		MLSS A	2 4,27 3 1,63	3		A1 pH: A2 pH:	6.8	
1 2 3 4		1	2 3	34	150	2		2/50		RAS				AL EFF		
0.1 0,6 1,	0 0								╎└	VV AX	5 0.6-	्र ।	<b></b>			
					START: 12 ; 45 FINISH:		<b>L</b>						F	SEPTAG airhaven tapoisett Marion		
					OUT: 1:00								Boom to a subscription of the subscription of	ochester Acushnet		
					//:00	-110	~		1					TOTAL		]

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

I Removal 148-8 x 100 = 95% 2 Primery Removal 148-74 100 - 50% 16/day RAW 8.34 x 148 x 1.84 = 2271 15/day PRI. 8.34 x 74 x 1.84 = 11 36 15/dey KTT. 8.34 x 8 × 1.84 = 123 MLSS, 8.34 x .467 x 4,200 = 16,358 SVI 1000 x 220 = 52 · m1/g  $CT = \frac{4,200}{2,0} = 2,100 mg/1/ml$ BA +8.34 x 467 x 4,200 14 DAYS

Al 5ml 4,160

SET	TLEO	METE	R		FAIRHAVEN C						INITIAL		VO	DATE:		
Time	9	<u> </u>		;0	SAMPLES - VOLUME	INF 50	PRISO	EFF	F3 / 40	F4	R3 5	R4	A1 5	A2 5	A3 5	WAS 5
	ssv	SŠC	SS∨	SSC	CRUCIBLE							Ì				
0	1000	·			WT. + SAMPLE	21,2848	21.6150	20. 1025	21 3133		21.4760	. }	21.2834	19.465	20 99%	21.3396
- 5	350				CRUCIBLE WT.					1		f			A.S.	
10	280					21 24.20	21.646	20,6015	21.3165	- /	21,4359		2126/3	19 4264	20 4350	21,7564
15	240				DIFFERENCE PRE	,0022	.0034		.0012	ļ	.0401	ļ	.0221	,0393	.0726	.0232
20	220				FURNACE	44	68	10	12	)	8020		4420	7860	4520	4640
25	200				CRUCIBLE					1						
30	200				WT. + SAMPLE	21.2848	21.6150	20.6023	21.717		21.4760		21.2834	19.4657	20.99%	21.3396
40	190				WT. POST							7				
50	190				FURNANCE			20.6015			21.4592	- (	212736	19.449;	20 9875	21.7630
60	190				DIFFERENCE	.0077		.0010	.00/2	ļ	.0163	)	.0098	0165	.0098	,0166
					VOLATILE	44	64	10	12		3360	1	1960	3300	1960	3320
123	A	1	. 2	3	PRE-FURNACE							/				
	Τ.				VOLATILE					<u> </u>						
22 32 20	C				FIXED SOLIDS	B	4	Ĺ	B		4660	· /	2460	4560	2.560	1320
1-2-3 4	R	1	2 3	34	,							_				-
4.0	S				COLIFORM						TITE (mg/			NOTES		
	C				SAMPLE	COLON	IJES #	/100mL		LSS A			INF	. TEMP:		
1 2 3 4		1	2 3	\$ 4						<u>.SS A</u>				A1 pH:		
•	0								M	SS A				A2 pH:		
	B										3 4.80			VAL EFF		
1234	1 **	1	2 3	34					[	RAS-		_	AK	ALINITY		]
1	D						<u> </u>			WA	5 0.6	2				
0.40.60.8	0												2			
													-	SEPTAG		
					START:									airhaven		
													Mat	tapoisett		
					FINISH:									Marion	Summer of the second	
														ochester		ļ
					OUT:								A	\cushnet	1	1
									l					TOTAL		J

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

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 NITRATE -

NITRITE -

X Removal 44 -10 x 100 - 77% 2 Primary Removal 44. -68 x 100 -1b/day RAW 8.34 x 44 x 1:89 = 694 16/day PRI. 8.34 x 688 /.89 = 10 72 15/day EFF. 8.34 x 10 % 1.89 = 158 MLSS, 8.34 x .467 x 4520 = 17604  $\frac{\text{SVI}}{4430} = 44 \text{ ml/s}$ CT <u>4520</u> \* 2260 mg/1/ml 54 -8.34 x .467 x 45.20 = 16 DAYS

	SET	TLEO		R			FAIRHAVEN C							<u>S:</u>	10	DATE:	10 B.	21 15
Time e		9	00		2	.2	SAMPLES - VOLUME	INF 50	PRI 50	EFF100	F3 /00	F4	R3 5	R4	A1 5	A2 5	A3 5	WAS
Time		SSV	ssc	SS	vIs	ssc	CRUCIBLE							Þ				
0		1000			╈		WT. + SAMPLE	21.7188	19.4281	21,2616	21.7571	{	19,2033	(	21.329	920.99%	20 625	21.4944
5		330					CRUCIBLE WT.							. ]				
10		260						21.7166					19,1478	[				21.4667
15.		220					DIFFERENCE PRE		0020	.0004	.0006	\	.0.555	[		2.0225		
20		210					FURNACE	44	40	4	L.6		11100	ļ	9440	4500	4720	5540
25		200					CRUCIBLE					/		1				
30		190					WT. + SAMPLE	21.7188	19.4281	21.2616	<u>21.257/</u>		19.2033		21.329	20.997	<u>2ao. 67.55</u>	5 <u>21.4944</u>
40		190					WT. POST									d. en.		
50		190		<b> </b>	_	]	FURNANCE	21.7166	19 1261			<u> </u>	19.1799	<u>'</u>		120,707	20.614	21-4748
60		190					DIFFERENCE	.0072	10	-0004	_	Ì	.0234	۱	.0210	1	5.0107	
							VOLATILE	44	40	4	6		4680		4200	2100	2140	3920
12	3	A	1	, 2		3	PRE-FURNACE					/						
		T					VOLATILE			ļ				[				L
<u>4522</u> XX3	22	C			_		FIXED SOLIDS	2º	ê	Ø	Ø		6420	· {	5240	2400	2580	1620
723	4		1	2	3	4	<u>^</u>		-					_				7
6.0		S					COLIFORM						ETITE (mg/			NOTES		
-		C			_		SAMPLE	COLON	IES #	/100mL		LSS				TEMP:		
123	4	D	1	2	3	4		<u> </u>					A2 2.80				6.8	4
•		0											A3 2.8:			A2 pH:		-
1 2 3	4	B	1	2	3			<u> </u>			▮ ⊨	RAE	36.80	·		NAL EFF		
123	4	A		2	3	4		1			╡ ┝──	-			A	ALINITY		1
		D								<u></u>		W/	AS 1.02					
0.2 0.6	1.0						· · · · · · · · · · · · · · · · · · ·									OEDTA-		7
							START:	<u> </u>			4					SEPTAC airhaver		-
							START									ttapoiset	_!	-
							FINISH:	······			1				1Via	Marior		-
							E INIGIL.				ţ					ochester	_	-
							OUT:				1					Acushne		1
																TOTAL		1
											1					10176	<u>- I</u>	J.

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) × 1,000,000

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NITRATE -

NITRITE -



I Removal  $\frac{44-4}{44} = 100 = 91\%$ Z Primary Removal 44-40 - 9% 1b/day BAW 8-34 x 44 x 1:99 = 730 16/day PRI. 8.34 x 40×1.99 = 664 16/day EFF. 8.34 x 4 x 1.9.9 = .66 MLSS, 8.34 = 467 = 4320 = 18383  $\frac{5VI}{422} = 40 \text{ ml/g}$  $CF = \frac{4320}{22} = 2145 mg/1/ml$ 

SA -8-34 x -467 x 4/20 8.34 x 40 x / 99 = 28 DAYS

SET	TLEO		R		FAIRHAVEN CO								10	DATE:	10 12	1115
Time	9	30		:	SAMPLES - VOLUME	INF 50	PRI 5	EFF /00	F3 100	F4.	R3 5	R4.	A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC			1									
0	1000				WT. + SAMPLE	19,1302	217198	21 4261	209/5		R1.3334	.	21.282	419.449:	30 Ez):	21.2923
5	330									1				1	AU	
10	250				CRUCIBLE WT.	19-1422	21316	214359	20 9750		21,282	ł	217563	19 4200	20 602	212618
15	220		:		DIFFERENCE PRE-	.0025	.0028	.0002	,0009	1	.0509	Ì		10227		.0309
· 20	210				FURNACE	50	56	2	9		10180	ļ		4540		
25	200				CRUCIBLE					1		Í				
30	190				WT. + SAMPLE	19.1502	21.7198	21-4361	20.979		21.3339	j j	21.7824	19.4495	20.6272	21.292>
40	190	÷.			WT. POST		[			7		1	1			
50	190				FURNANCE	19.1477	217170	21.435	20 9750	6	2/3/38		21.774	19.4395	20.6163	21.2703
60	190				DIFFERENCE	.0075	.0028	.0002	.0009		,0201		.0110	.0100	,0109	.0224
· · ·					VOLATILE	30	56	ス	9		4020	1	2200	2000	2180	4480
123	A	1	. 2	3	PRE-FURNACE				······	)		(	1			
	т				VOLATILE							<u>&gt;</u>				
2.5 2.0 2.5	1 c				FIXED SOLIDS	Ð	6	ø	e	Ţ	6160	-7	2980	2540	2820	1700
123A	1 R	1	2 3	3 4								•				·
	S				COLIFORM	BACTERI	A	:	[ ] M	AGNI	ETITE (mg/	L)		NOTES		
5.0	C				SAMPLE	COLON	IES #	100mL	M	LSS	A1 3.46		INF	. TEMP:	18.9	
1 2 3 4	D	1	2 3	3 4					M	LSS .	A2 2.92			A1 pH:	6.9	
•	0					[			M	LSS.	A3 3.20			A2 pH:		
	В										\$3 6.60			IAL EFF		
1 2 3 4	A	1	2 3	3 4	-					RAS			AK	ALINITY	62	
	D									Ŵ,	AS 0.95					•
0.2 0.9 1.4	4 o															
						1	·····							SEPTAG	Ε	
					START:								Fa	airhaven		
								-					Mat	tapoisett		
					FINISH:									Marion	:	
													R	ochester		
					OUT:								A	cushnet		
														TOTAL		
					······································											-

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE ~

NITRITE -

 $x \text{ Removal} = \frac{50-2}{50} \times 100 = 96\%$ Z Primary Removal 50 -56 x 100 -1b/day RAW 8.34 x 50 x / 98 = 826 Ib/day PRI. 8.34 x 56 x 1.98 = 925 15/day EFF. 8.34 x 2 x 1.98 = 33 MLSS, 8.34 x .467 x 5000 = 19 474 . SVI 1000 x 190 = 38 ml/g  $\frac{CF}{2.5} = 2000 \, \text{mg/1/ml}$ SA :8.34 x .467 x.5000 8.34 x 56 x 1.98 21 DAYS

SE	TTLEO				FAIRHAVEN C						INITIAL	<b>\$</b> :	VO	DATE:	10 12	0115
Time		00		2,0	SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3/00	F4,	R3 5	R4,	A1 5			WAS 5
1 Ulie	SSV	SSC	SSV	ssc	CRUCIBLE							Ì				
0	1000				WT. + SAMPLE	20.9809	20.604	21.7569	212616		213449		21.474	21.2385	19 1678	19.4526
5	340				CRUCIBLE WT.							. /			ľ	
10	2)0							<u>21.7563</u>	212607		21.2830		21 1/351	21.7164	19.1433	19.4266
15	240			ļ	DIFFERENCE PRE	1,0000	.0030		1 . <b>'</b>		.0619		.0389	,0221	0206	.0260
20	210				FURNACE	116	60	6	9	1	12380	<u> </u>	7780	4420	4120	5200
<u>25</u> 30	200						0	AL NACA			at milt	ļ		1.1-07	- 40	10 1626
40	190				WT. + SAMPLE WT. POST	20.9809	20.604)	21. 1967	21.2616	{	21.3449		21.4713	21.7382	19. 1678	19.4536
50	180				FURNANCE	209356	20 619	21.7563	21 260	Í	21,3200		7160	11 5296	IA ICA	19:4352
60	1				DIFFERENCE	.0053	0028	,0006	.0009	<u> </u>	.0349		.0165	0095	0085	.0174
				1	VOLATILE	106	56	6	9		4980					3480
123	A	1	. 2	3	PRE-FURNACE	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			<u> </u>	Ť		î		1/00		
	Ţ				VOLATILE					}		ļ				
40 2220	) C				FIXED SOLIDS	10	4	0	0	) 	7400	- /	4480	2520	2380	120
1-2-3 4	1 R	1	2 3	34		<i>4</i>								•		_
6.5	S			:	COLIFORM			<u> </u>			TITE (mg/			NOTES		
1 2 3 4		4	~ ~		SAMPLE	COLON	IES #	/100mL			1 4 > 5		INF	TEMP:		
1 2 3 4	D	1	2 3	\$4							22.39			A1 pH:		-
-	в			:	·						13 2.54 3 7 30			A2 pH:		
1 2 3 4		1	2 3	3 4		l <u></u>	·····			RAS				VAL EFF ALINITY		
		•		, ,							S 1.01	_		ALINIT		]
0.51.) 3.	١ō										w //					
<u>B</u>					·····	· · · · · · · · · · · · · · · · · · ·								SEPTAG	Ē	1
					START:	•							F	airhaven	1	1
													Mat	tapoisett		1
					FINISH:									Marion	<u> </u>	
							<u> </u>							ochester		
					OUT:								· · · · · /	cushnet		-
														TOTAL		1

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

NITRATE -

NITRITE -

ALKALINITY -

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I Removal  $\frac{11.6 - 6}{11.6} = 95\%$ Z Primary Removal 116 -60 x 100 - 48% 1b/day RAW 8.34 x //6 x 2:0 = 1935 1b/day PRI. 8.34 x 60 x 2.0 2 /001 16/day EFF. 8.34 x 6 x 2.0. 2 100 MLSS, 8.34 x .467 x 4120 = 16046 SVI 1000 x 200 = 49 ml/g  $\frac{CF}{20} = \frac{4120}{200} = 2060 \text{ mg/1/ml}$ 5A 18.34 x .467 x 4/20 - 16 DAYS

SET	TLEO	METE	R		FAIRHAVEN C							.S:		DATE:	10 TH	1115
Time	9	05		:	SAMPLES - VOLUME	INF 30	PRI <i>30</i>	EFF/@	F3 /10	F4	R3 5	R4	A1 5	A2 5	A3 5	WAS 5
1	SSV	SSC	SSV	SSC	CRUCIBLE					l l		$\left  \right\rangle$				
0	1000				WT. + SAMPLE	21.4416	21 7642	19 4270	20 9769		21,3044	$\langle \rangle$	21 7696	213051	20 623	19 1318
5	350			<u> </u>				<u> </u>						<u> </u>	A	<u> </u>
10	300				CRUCIBLE WT.	21.4355	21.7556	19.4259	20 974		21,2607		21.716	21 22	20 601	19.1482
15	250				DIFFERENCE PRE	,0061		.00 //			.0492	1				.0236
	230				FURNACE	122	52	11	10		8840			4480		
25	210				CRUCIBLE	21.4416				1	21.3049		71.7696	21-3051	20.6239	19.1718
30	200				WT. + SAMPLE	21.4361	21.7561	19 4265	209752	1	21.2868	/				19,551
40	190	·			WT. POST	.0055		20005	1000>	/	.0181		,0218	.0095	.0095	,0167
50	190				FURNANCE	110	42	5	7		3620					3340
60	190	<u> </u>			DIFFERENCE					Į		and the second	ł			
					VOLATILE											
123	A	1	. 2	3	PRE-FURNACE					$\rangle$						
	Т			·	VOLATILE											
502.225	C				FIXED SOLIDS	12	10	6	3	ζ.	5220		6220	2580	2580	1380
123 X	R	1	2 3	4												
5.0	S				COLIFORM			:			TITE (mg/			NOTES		
_	<u>c</u>				SAMPLE	COLON	IES #/	100mL		LSS A			INF.	TEMP:		
1234		1	2 3	4	B	0				LSS A				A1 pH:	6.8	
	<u>0</u>				50	2		2/50	M	LSS A				A2 pH:		
1 2 3 4	В	1	2 3		100	0				RAS		5		AL EFF		
1 2 3 4	A	4	2 3	4	4					RAS-			AK/	ALINITY	63	
0	D				· · · · · · · · · · · · · · · · · · ·					WA	S 8.6	8				
0.2 1.5 3.0	0															
					<u></u>									EPTAG		
					START: 12:55	•								irhaven		
					FINISH:								Matt	apoisett		
					FINISH: 1:10									Marion		
					OUT:									chester		
					12:50								<u> </u>			
					11.30								L	TOTAL		

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

NITRATE -

NITRITE -

 $I \text{Removal} = \frac{122 - 11}{122} \pm 100 = 91\%$ 2 Primary Removal 122-52 x 100 - 50% 15/day RAW 8.34 x /22 x 2.06 = 2096 16/day PRI. 8.34 x 52 × 2.06 = 893 : 16/day EFF. 8.34 x /1 × 2.06 = 189 MLSS, 8.34 x .467 x 4480 = 17 449 SVI 1000  $\pm 200 = 45 \cdot \pm 1/g$  $CF = \frac{4480}{2.5} = 1992 mg/1/ml.$ 54 <u>\*8.34 x 467 x 4480</u> 8.34 x 52 × 2 06 20 DAYS

SET	TLEO		R		FAIRHAVEN C						INITIAL	S:	VO	DATE:	10 11	5115
Time	10	45		20	SAMPLES - VOLUME	INF 50	PRI 50	EFF 100	F3 /00	F4,	R3 5	R4]	A1 5	A2 5	A3 5	WAS 5
Time	Issv	SSC	SSV	SSC	CRUCIBLE		-			Y		Ŋ		1		
0	1000				WT. + SAMPLE	215767	21.4384	20.6026	20.9365		21.3/24		21.7878	19,14,96	217769	213020
5	390				CRUCIBLE WT.									1		
	300					21.5752	214363	20 6022	20.9758	,	21.2611		21.7168	19.4271	21.7567	21,2830
	250			L	DIFFERENCE PRE	2100,5	,0021	.0004	,0007		,05B		1.0310	,0215	.0202	.0190
	230				FURNACE	30	42	4	1 >		10260		14200	4300	4040	3800
	200				CRUCIBLE	la con										
30	190				WT. + SAMPLE	21-5767	21.4349	20.6026	20.9765	1	2/3/24	]	21.7878	19.4480	21.7769	21.3020
40	180				WT. POST					(						
50	180				FURNANCE	81.5752				<u>} \</u>	21.290		21.279	19 1375	215667	212836
60	180				DIFFERENCE	,0015	.0021		,000 >	}	0212		.0299	.0111	.0102	.0144
·					VOLATILE	30	42	4	2		4340	1	5980	2220	2040	2880
123	A	1	. 2	3	PRE-FURNACE					1						
	T				VOLATILE											
6.7 2.0 20	C				FIXED SOLIDS	2	К	D	Ø	(	5920	- {	8220	2080	200 D	920
1-2-3 4	R	1	2 3	4											·	
5.0	S				COLIFORM			:	M/	AGNE	TITE (mg/	L)		NOTES		
1	C				SAMPLE	COLON	IES #	/100mL		LSS /			INF	. TEMP:	19.2	
128K	D	1	2 3	4					M	LSS	2 2.50			A1 pH:	6.7	
	0			·					M	LSS /	13 2.34			A2 pH:	6.7	
	В									RAS	3 5.96		FIN	VAL EFF		
1 2 3 4	A	1	2 3	4						RAS	-4		AK	ALINITY		
	D									- WA	S 0.61					•
0.11.728	0															
														SEPTAG	E	
					START:								F	airhaven		
													Mat	tapoisett		
					FINISH:									Marion		
						<u></u>							R	ochester		
					OUT:								A	cushnet		
														TOTAL		
									•							

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

NITRATE ~

NITRITE -

ALKALINITY -

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 $\frac{30-4}{30} = \frac{30}{30} = \frac{30}{5}$ Z Primary Removal 30 - 42 = 100 -1b/day RAW 8.34 x 30 x2.32 = 580 16/day PRI. 8.34 x 42 x 232 = 813 1b/day EVF. 8.34 x 4x232 = >> MLSS, 8-34 x -467 x 4040 = 15735 SVI 1000 x 190 = 47 m1/g  $\frac{CF}{2.6} = \frac{4646}{2020} = 2020 \text{ mg/1/m1},$ SA :8.34 x .467 x 40.40 B.34 x 492 X 237 /9 DAYS

SE	TLEO		R		FAIRHAVEN C							10	DATE:	10 11	5115
Time	9	20		2.0	SAMPLES - VOLUME	INF 50	PRISO	EFF 100	F3 /00 F4	R3 5	R4	A1 5	A2 5	A3 5	WAS 5
111100	SSV	SSC	SSV	' ssc	CRUCIBLE					)					
0	1000				WT. + SAMPLE	21.7592	19.429	211249	216121	20.6434	/	22 0684	217450	212803	209868
5	450									1 1 20	1	24,	<u> </u>		14.3 400
10	250				CRUCIBLE WT.	\$1.7567	19 436	271 1258	216115	20 6015		27 034	21.3163	21 2613	20 9749
15	280				DIFFERENCE PRE	,0025	0029	0011	.0016	_0424		.0336	.0258	0191	,0119
20	240				FURNACE	50	58	11	16	8480					2380
25	210	ŀ			CRUCIBLE			<u> </u>		1					
30	200				WT. + SAMPLE	21.7592	19.4291	21.4369	21.6131	20.6439	/	22.0684	21,7125	212803	20.9868
40	180				WT. POST		1	[					· · · · · · · · · · · · · · · · · · ·		
50	170				FURNANCE	21,7567		214358	216115	20.62)1		22.0546	21.7318	21,2722	20.9383
60	170				DIFFERENCE	.0075	.0029	.00 11	,0016	,0168		.0138	,0107	.0081	.0081
					VOLATILE	50	58	11	/6	3360		2760	2140	1620	1620
123	A	1	. 2	3	PRE-FURNACE						1		1		
	T				VOLATILE					)					
272520	C   C				FIXED SOLIDS	0	I.C	Ø	Ð	1 5120	1	B960	3020	2200	760
1-2-3 4	1 R	1	2 3	34											-
11.	S				COLIFORM			:		NETITE (mg			NOTES		
40	C				SAMPLE	COLON	IIES #	/100mL		5 A1 <i>3.</i> 8		INF	. TEMP:		
1234	_	1	2 3	3 4						SA2 3.2				6.80	
•	0									5 A3 2.28				6.62	
	В									AS 3 5.50	2		IAL EFF	1	
1234		1	2 3	34						AS-4		AK	ALINITY		
0 . 7	D									NAS 0.6	5				
0.71.80.3	0														
													SEPTAG		
					START:							5	airhaven		
												Mat	tapoisett		
					FINISH:								Marion		ļ
													ochester		
					OUT:								cushnet		ļ
													TOTAL		1

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

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TOTAL NITROGEN -

NITRATE -

NITRITE -

ALKALINITY ~

.

 $x \text{ Removal} = \frac{50 - 11}{50} \times 100 = \frac{38}{8}$ 2 Primary Removal 50 - 58 1b/day RAW 8-34 x 50 x 2.22 = 926 16/day PRI. 8.34 x 58x 2.22 = 10 74 Ib/day EFF. 8.34 x 11 x 2.22 = 204 MLSS, 8-34 x -467 x 3820 = 148)8  $\frac{5VI_{1000 \pm 200}}{3820} = 52 \text{ ml/g}$  $Cr = \frac{3820}{2.0} = /9/0 = g/1/ml$ 54 <u>98.34 x 467 x 3820</u> 8.34 x 58 × 222 - 14 DAYS

SET	TLEO	METE	R		FAIRHAVEN C						INITIAL		20			4115
Time	9	05		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF100	F3 100 F	-4	R3 5	R4	A1 5	A2 5	A3 5	WAS
Tane	SSV	SSC	SSV	SSC	CRUCIBLE					$\sum$		$\gamma$				
0	1000				WT. + SAMPLE	21.7223	21.6149	210076	19.4280	(	212911	$\sum$	22.0865	21 7829	21 4539	20,6133
5	520						[				, in the second se	1				
10	400					21.7166	21.6124	21.0069	19.4269		21.2614					20.6020
	330				DIFFERENCE PRE	.005>	0025	,000%	.00 11'	Т	1029>					.0153
20	280				FURNACE	114	50	2	11		5940		10540	5240	3520	3060
25	240				CRUCIBLE					T	81.2911					
30	220					21.7223	21.6149	21.0076	19.4280	1	21.2794		22.086	21.7829	21.1539	20.61)3
40	190				WT, POST						10117	1				
50	180				FURNANCE	217176	21 6126	21.0069	19 4268				22.065	21.7726	21.4463	206032
60	071				DIFFERENCE	.0047		.0005	0011	)	2340		.0210	.0103	-0076	.0 101
					VOLATILE	94	46	2	11		2.570	1	4200	2060	1520	2020
123	Α	1	. 2	3	PRE-FURNACE		,			T						
	Т			i	VOLATILE					. (						
5,02.520	С				FIXED SOLIDS	20	4	Ð	Ø	)	3600	· (	6340	3180	2000	1040
1-2-3 A	[ R	1	2 3	4					_							_
2.5	S			ĺ	COLIFORM	BACTERI		:	MA	GNET	TTE (mg/	Ľ)		NOTES		
	C				SAMPLE	COLON	IES #	/100mL	ML,	SS A1		9	INF	. TEMP:	19.1	
1 2 3 4	D	1	2 3	4						SS A2				A1 pH:		
-	0										3 2.16			A2 pH:	6.6	
	в									RAS		-	FIN	JAL EFF		
1 2 3 4	A	1	2 3	4						RAS	1	:	AK	ALINITY	80	
	D									WAS	5 0.64	L				-
0.12.5 0.6	† 0												,			
														SEPTAG	E	]
					START:				1				F	airhaven		]
													Mat	tapoisett		]
					FINISH:				1					Marion		
													R	ochester		
					OUT:								A	cushnet		
														TOTAL		
									-							-

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

ALKALINITY ~

.

 $I \text{ Removal} = \frac{1.4 - 5}{1.4} \pm 100 = 94\%$ 2 Primary Removal 114-50 x 100 - 56% 10/day RAW 8.34 x 114 x 2.3 > = 2253 16/day PRI. 8-34 x 50 x 2.3 > = 988 1b/day EFT. 8.34 x > x 2.3 > = 138 . MLSS. 8.34 x .467 x 3520 = 13 709  $\frac{5VI}{3520} = 63 \text{ ml/g}$ 

 $\frac{GF}{2.0} = 1.60 \text{ mg/l/ml}$ 54 -34 x -467 x 3520 8.34 x 50 x 2.35 14 DAYS

SET	TLEO		R		FAIRHAVEN C	ONTROL	DATAL	OG - BIC	MAG TI	EST		INITIAL	.S:		DATE:	10 11	3115
Time		10		1.5	SAMPLES - VOLUME	INF 50	PRI 30	EFF /CC	F3 /00	F4	┟───	R3 5	-R <b>4</b>	A1 3	A2 5	TAJ	WAS 5
	SSV	SSC	SSV	SSC	CRUCIBLE						r T		T				
0	1000				WT. + SAMPLE	20,6034	217196	216156	20.9794		\ b	1.2916		22 06	2 18 442	01932	21.4526
5	800				CRUCIBLE WT,	1		1			<u>וררו</u>	<i>y</i>	- í		<u></u>	0-1.1.100	al
	520					20.6011	21 4163	216122	20.9758			21.261		2203	419.426	21 750	21.4358
	430				DIFFERENCE PRE	.0063	.0033	.0034				.0299	Ť	1027	1 .0 16	0156	.0162
	360				FURNACE	126	66	34	36			5980			2 3220		
	320				CRUCIBLE	20 (0)				1			1				
	280				WT. + SAMPLE	20.6074	21.7196	21.6155	20.9794		2	1.2916		22.06	2 19.443	421.3723	21.4520
	230		<u>.</u>		WI.POST				<b>i</b> .						1		1
	200	· ·			FURNANCE	20.6014				5	6	<u>2/2)83</u>		22.04	<u>3`}   9_</u> 435	1217649	21.4410
60	190			·	DIFFERENCE	.0060	.0033	,0078	.0029	1	.	0133	1	.012	5.0079	0075	.0110
					VOLATILE								J				
123	A	1	. 2	3	PRE-FURNACE	120	33	28	20		.			0.000		1600	2200
2.5 1.5 1.5	T C				VOLATILE				29		F	2660			1580		
1 2 3 4	R	1	2 3	4	FIXED SOLIDS	6	0	6	2	1		3320	<u> </u> }	2920	1640	1620	1040
	s		2 0	-	COLIFORM	DACTEDI	A		1 1 14			·····					2
2.7	c				SAMPLE	COLON		/10 <b>0</b> mL				E (mg/			NOTES		
1 2 3 4	D	1	2 3	4	B			TOVILL		_	A1	<u>2.7%</u> 1.62	2		F. TEMP		
	ō	•	- *	-	50	0		150				1.60				6.30	
	в			1	100	Ĥ		1100				3.25			NAL EFF	6.60	
1 2 3 4	A	1	2 3	4	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	······		// 00			\$4	<u>~~</u>			KALINITY	An	
	D											0.63	7			11/2	
0.2 1.5 2.6	ο								<b>K</b> annan			0.00	,				
															SEPTAG	\$F	1
					START:										airhaver		
					1:30										ittapoiset		
					FINISH:										Marior		
					1:40										Rochester		
					OUT:										Acushne		
					12:40										TOTAL		
				•										·			

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

I Removal 126 - 34 x 100 - 3% Z Primary Removal 126 -66 x 100 = 48% 1b/day BAW 8.34 x /26 x 2.57 = 2701 16/day PRI. 8.34 x 66 x 2.5 > = 1415. 16/day EVE 8.34 x 34 x 2.57 = 729 MLSS, 8-34 x .467 x 3/20= 12,151. SVI 1000 x 280 = 90 ml/g  $\frac{CF}{1.5} = 2080 \cdot \frac{mg}{mg} \frac{1}{mI}$ SA :8.34 x .467 x 3/20 9 DAYS

SE	TTLEO	METE	R	·	FAIRHAVEN C						INITIAL			DATE:		9115
Time	10	20		:	SAMPLES - VOLUME	INF 50	PRISO	EFF 100	F3 /00	F4 🔀	R3 5	R4)	A1 5	A2 5	A3 5	WAS 5
	1000	· · · ·	SSV	SSC		217590	21,2645	22.0340	17.7441		19.4604	t ]	20.3/69	19.5755	21.508	20.9967
5 10	940 3×0				CRUCIBLE WT.	21,7556	21,2613	22 0330	12,2361	í	19.4257		30.2964	19 5578	21,4909	20 9749
15 20	830				DIFFERENCE PRE FURNACE	.0034 68	.0032 64	,0010 10	80		.034> 6940					.0218 4360
25 30 40	740 670 620				CRUCIBLE WT. + SAMPLE WT. POST	21.7590	21.264	27.0340	17.844)		19.1604		20.3119	19.5798	<u>21.50</u> 85	20.9963
50 50	480				FURNANCE DIFFERENCE	21.7556 0034	0037	22.0330	17.7390 .0051		19.4438 .0166		20.306)			20.9823 .0144
123	A	1	, 2	3	VOLATILE PRE-FURNACE	68	64	10	51		3320		2040	•	, r	2880
20 20 21 X 2 3 A		1	2 3	3 4	VOLATILE FIXED SOLIDS	8	0	D	29		3620		2060	1780	1720	1480
7 Z 3 A 4,0	R S C		2 3	, 4	COLIFORM SAMPLE			: /100mL		AGNET	TTE (mg/ 1 /_ 96		INF	NOTES		
1234 ·	D O B	1	2 3	3 4						ILSS A ILSS A RAS (	2 1.2	3	FIN	A1 pH: A2 pH: JAL EFF	6.8	
1234 0.20.41.8	D	1	2 3	\$4	· · · · · · · · · · · · · · · · · · ·					RAS-	4			ALINITY		J
0.20-11.2					START:				:				F	SEPTAG airhaven tapoisett		
					FINISH:								R	Marion ochester		
					OUT:								<u> </u>	Cushnet TOTAL		l

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

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NITRATE -

NITRITE -

I Removal <u>68 - 10</u> x 100 = 85% I Primary Removal 68-64 100 - 6%. 16/day RAW 8.34 x 68 x 2.4 = 1361 16/day PRI. 8.34 x 64x2.4= 1281. 16/day EFF. 8.34 x 10 x 2.4 = 200 . MISS, 8-34 = .467 = 3520 = 13709. SVI 1000 x 600 - 190 mI/g  $cr = \frac{3520}{2.2} = 1600 \text{ mg/l/ml}$ 5A <u>78.34 x .467 x 3520</u> 8.34 x 64× 2.4 // DAYS

SE	TTLEO		R		FAIRHAVEN C						INITIAL			DATE:		
Time	9	10		:	SAMPLES - VOLUME	INF 50	PRI 50	EFF /00	F3 /00	F4	R3 5		A1 5	A2 5	A3 5	WAS 51
0	SSV 1000	<u> </u>	SSV	SSC		21.2567 21.2507	21.4373	21-6129	21,983		19.181	19.12	19,598	21,596	16.605	$X_{\circ}$
5	960				CRUCIBLE WT.	<u>×1.4507</u>	7 <u>,4354</u>	21.612	41.08047		<u> </u>	17.1012	1736.	21.3152	16.58/6	<u>ai.7467</u>
10	900								[							
15	850				DIFFERENCE PRE			.0008	0006					,0215		
20	810				FURNACE	120	38	8	6		6800	5360	4300	1300	4700	
25	770				CRUCIBLE											
30	700				WT. + SAMPLE	21.2567	21.437	21.6/29	21.2830		19.1817	19.1780	19.580	21.5967	16.6051	
40	1000				WT. POST											
50	910				FURNANCE	21.2509	21.4354	21.6121	21994		19,1647	19,1144	19,5769	21.5856	16,5893	
60	250				DIFFERENCE	,00.58	.0019	.0008	.0006		.0970	.0136	,0111	,0111	.0 158	
				-	VOLATILE	116	38	8	6		3400	2720	2220	2220	3160	
123	A   T	1	. 2	3	PRE-FURNACE VOLATILE											
30252					FIXED SOLIDS	4	0	0	0		3400	2640	2080	2080	1540	
م 3 <i>محرم</i> د	HR	1	2 3	3 4												
45	S				COLIFORM			:			ETITE (mg/			NOTES		
-	C				SAMPLE	COLON	IES #/	(100mL		ILSS /			INF	. TEMP:		
1234	t D	1	2 3	3 4						ILSS /				A1 pH:	6.9	
•	0									·	A3 <i>1.86</i>			A2 pH:	6.8	
	В								<u>.</u>		33 2.65	-	FIN	IAL EFF	<b>N</b> -	
1234	A	1	2 3	3 4						RAS			AK,	ALINITY	70	
	D									- WA	AS 0.99					-
0.20.74	d O															
						[			1					SEPTAG	Ë	
					START:		-		1				F	airhaven		
													Mat	tapoisett		
					FINISH:				]					Marion		
													R	ochester		
					OUT:				1				A	cushnet		
														TOTAL		
																•

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL)  $\times$  1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

 $x \text{ Removal} = \frac{120 - 8}{120} \times 100 = 93\%$ Z Primary Removal 120 - 38 x 100 - 68%. 16/day RAW 8.34 x /20 x23 - 2302 15/day PRI. 8.34 x 38 22.3 = 729 16/day ETT. 8.34 x 8 82.3 = 153 MLSS. 8.34 x .467 x 4300 = 16 748 SVI 1000 - 700 = /63 · m1/g  $CI = \frac{4300}{2.5} = 1)20 \text{ mg/1/ml}$ SA :8.34 x .467 x 4300 8.34 x 38 x 2.3 22 DAYS

Al 5ml ·

									Balking.				
\$ET	ITLEO				FAIRHAVEN C					INITIALS: U	/0 DAT	E: 101	7115
Time		35		22	SAMPLES - VOLUME	INF 50	PRI 50	EFF/00	F325.F4	R3 5 R4	A1 5 A2	5 A3 5	WAS
	SSV	SSC	SSV	ssc	CRUCIBLE				- 1				
0	1000				WT. + SAMPLE	21 2834	19 568	19 100	21.6464	21,2862	19.1711 21.1	123 21 692	
5	910						1				11111212		
10	880				CRUCIBLE WI.	21,2824	19 5651	19.0991	21.6124	2/2505	19 1422214	169 21 575	And the second
15	820				DIFFERENCE PRE	_0050	,0032	.0012	.0340	.0354	.0736 .019		
20	780				FURNACE	100	64	12	1360 1	7080	4720 368	04620	
25	740				CRUCIBLE								
30	590				WT. + SAMPLE	21.2874	19.5683	19-1003	21.6464	21.2862	19.1711 21.44	39 21, 398	
40	650				WT. POST								
50	560				FURNANCE	81.2824				21.267	19.157621.4		2
60	490		i		DIFFERENCE	,0050				.0 185	.0135 .010		
					VOLATILE	100	6.4	12	728	3700	2700 2100	2580	
123	A	1	, <b>2</b>	3	PRE-FURNACE	į							
201122													
3.0 2.2 2.2		1	2 3	4	FIXED SOLIDS	ø	Ð	Ð	632 1	3380	2020 158	0 2040	
	ŝ	1	2 3	4	COLIFORM		Δ				L NOT	= 0	1
6.0	c			,	SAMPLE	COLON		100mL	MLSS	ETITE (mg/L)			-
1 2 3 4		1	2 3	4	OAMIFLE			TOUTIL	MLSS		INF, TEN		
1. 2 4	ō	'	2 9	-					MLSS	* : = 1		H: 6.9 H: 6.7	
	B	•								S3 2.85	FINALE		
1 2 3 4		1	2 3	4	· · · · · · · · · · · · · · · · · · ·				RA			TY //3	ł
	D				:					ASF.	- Alvaunt		
0.50.4 4.3	o												
f											SEPT	AGE	1
					START:				1		Fairhav		
											Mattapois		1
					FINISH:				1		Mari		1
									]		Roches	ter	1
					OUT:				1		Acushi		] .
											TOT	AL.	]

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TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

I Removal  $\frac{100 - 12}{100} = 48\%$ Z Primary Removal 100 - 64 x 100 - 36%. 16/day RAW 8.34 x 100 = 2:44 = 2035 1b/day PRI. 8.34 x 64 = 2.44 = 1302 15/day KUY. 8.34 x 12 = 2.44 = 244 . MLSS, 8.34 x .467 x 4629 = 17 993  $\frac{5VI}{4620} = 149 \text{ ml/g}$  $CE = \frac{4620}{2.2} = 2/00 mg/1/ml$ 54 :8.34 x .467 x 4620 8.34 x 64 x 2.44 14 DAYS

SET	TLEO	METE	R		FAIRHAVEN C						INITIAL			DATE:		
Time	9	10		22	SAMPLES - VOLUME	INF 50	PRI 50	EFF/00	F3 /00	F4	R3 5	R4	A1 5	A2 5	A3 5	WAS 5
Time	SSV	SSC	SSV	SSC	CRUCIBLE	21.2660	22.0357	20.2937	19.1278	• )	16,622.4		21.510	321.7715	19.50	20.6300
0	1000			· · · ·	WT. + SAMPLE	21.2603				, (	16.5816	۱				20 6014
5	900						<u> </u>	<u> </u>	1 1000	ħ	18.000			-1		A
10	830				CRUCIBLE WT.					U.		[				
15	750				DIFFERENCE PRE	,0052	.0025	.0017	.0012	V	,0403		,0186	.0157	.0154	.0286
20	676				FURNACE	104	50	17	12		8160		3720	3140	3080	5720
25	600				CRUCIBLE							\ \			4	
30	550					21.2660	22.0351	<u>20 2987</u>	19.427	5	16.6724		5103 (kg	321-7/15	19.572	20.6300
40	440				WT. POST			Ι.		ł				4-1-7		
50	350				FURNANCE	21.2610				<u> </u>	15,6022	]				20.6109
60	₿∞.				DIFFERENCE	- 00.50	,0021	.00  3		1	,0202	į				.0191
					VOLATILE	100	42	13	12	<b> </b>	4040		1920	1640	1620	3820
123	A	1	2	0	PRE-FURNACE					ł		/				
2.11.922	T										4/20	/	1000	1100	2010	10.00
	C R	1	2 3	3 4	FIXED SOLIDS	4	8	4	0	J	4120	Ę	1800	1500	1400	1700
1 2 3 4	S	'	~ `	· •	COLIFORM		Δ	•			TITE (mg/		<b></b>	NOTES		1
55	c				SAMPLE	COLON		100mL			1 1.40	<u>-/</u>	INF	TEMP:		
YZZA	D	1	2 3	3 4				TOOTHE			21.10	-		A1 pH:		
	Ō										31.14			A2 pH:		
	В										33.2		FI	VAL EFF		
1 2 3 4	A	1	2 3	3 4						RAS			AK	ALINITY		
	D				····					WA	S 0.74	4				•
0.71.73.4	0															_
														SEPTAG	E	
					START:								F	airhaven		
													Ma	tapoisett		
					FINISH:									Marion		
														ochester		
					OUT:								/	<u>\cushnet</u>		
														TOTAL		l

TSS TESTING: (CRUCIBLE WT. + SAMPLE - CRUICIBLE WT.) / VOLUME (mL) x 1,000,000

TOTAL NITROGEN -

NITRATE -

NITRITE -

% Removal 104-17 × 100= 84% % Pri Removal 104-50 × 100 = 52% 10/Day Ran 8.34 × 104 ×2.58 = 2238 " Pri 8.34 × 50 × 2.58 = 1076 11 EFF 8.34×17 \$2.58=366 MLSS 8.34 X.46> X 3080 = 11996 · · · · · SVI 1000×550 179 mbg  $CF = \frac{3080}{2.2} = 1400 \text{ myll/ml}$ 

SA 8.34 × 46) × 3080 11 Days 8.34 × 50 × 2.58 11 Days

. ..... ► 1
 ► 1
 ► 2
 ► 3

		SETT	LEOME	TER		FAIRHAN	EN CON	TROL DA	TA LOG	· INITI	ALS	10	DAT	E: 10 1 4	5:115
TIME	9:22	:		SAMPLES	-	INF 50	AJ 5ml	PRI 50	EFF /00	F3 100	F4			R4 5m1	
	SSV 55	c ssv	SSC	CRUCIBLE						٤	1			<u> </u>	
σ	1000			WT. + SAM	PLE					. ,		)		$\{\cdot\}$	· .
5	900			CRUCIBLE		21.2649	22.0446	21.7580	21.4918	19.5579	. /	· ·	19.472	a . /	20,30
10	820			WT.		21,2607	22 0335	217561	21.4911	19.5574	• . (*	· ·	19.4260		20.296
15	740			DIFFEREN	ICE.	:0042	.0131	.0025	.0007	.0005		•	.0467	-	.0/30
20	660 .			· PRE-FURN		a4	acin.	50	>	H.			9340	$  \rangle$	2600
25	590 .			CRUCIBLE	-	12. 2140	22.0466	21.7586	21.4918	19.5579			19.4729		20.309
30	520		_	<u>WT. + SAM</u>	PLE ·	21.2011									· ·
40	410			WT. POS	 Т	brack	22 0390	21:7561	21.4911	19.55.74			19.4486		20,30
50	360	- <u>  .</u>		· FURNACI	<u> </u>	1			· · ·						
60	290	- Lini-		DIFFEREN		,0012	0076.	.0025	.0007	.0.005	$\Box$		.0243		.00%
2	3   4	12	3	VOLATIL	E	82.	1520	50		5	•	L	4860	}	1460
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10       120       WT. + SAMPLE       21.26320.3052       16.5936       19.4344       21.3564       22.0925         10       110       WT. POST       FURNACE       21.2610 20.3010       16.5976       19.4266       21.3557       22.0653         10       110       DIFFERENCE       2025       0042       0014       0008       0007       0.2722         2       3       1       2.3       2.3       1.2       3       0.014       0008       0007       0.2722         10       10       12       3       VOLATILE       100       840       56       8       7       5440         20       3       4       8       1.2       3       4       62.80       1       62.80         20       3       4       8       1.2       3       4       5440       5440       5440         20       5       00       0       1       62.80       1       62.80       1       62.80       1       16.5976       16.5976       16.5976       17.400       16.5986       10.907       10.717       10.717       10.717       10.717       10.717       10.717       10.717       10.717       10.717	.0		·			· .	··· ·			100	15	60 1	56	8	5				]/_/	120			1710
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D       3       4       R       1.2       3       4       R       1.2       3       4       FIXED SQLIDS       62.30			Τļ				·				<u> </u>		~~		· .		7		1		· ·	1	840
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B     SAMPLE     COLONIES     #/100ml     GROOP       2     3     A     1     2     3     A       78     3.0     0     AMOEBOIDS     A       RESIDUAL CL2     AMOEBOIDS     A       TIME     FLOW     LEVEL       Image: plant     FLAGELLATES       Image: plant     FREE       Image:	之	0	č				FIXE	D SQL	IDS ·							•	. )		<u> </u>	 		)	<u></u>
B     SAMPLE     COLONIES     #/100ml     GROOP       2     3     A     1     2     3     A       78     3.0     0     AMOEBOIDS     A       RESIDUAL CL2     AMOEBOIDS     A       TIME     FLOW     LEVEL       Image: plant     FLAGELLATES       Image: plant     FREE       Image:	RIF	1114	D I	2	3 4				A		Α.					IISM				·	• *	NOT	S
18 3.0 0     AI ph       RESIDUAL CL 2     A2 ph       TIME     FLOW       LEVEL     FLAGELLATES       Plant     FREE       SEPTA       FREE       SWIMMING       CILIATES       STALKED       Marion			ĕ				SAMP	<u> </u>	<u></u> CO	LONIES		<u>#/10</u>	0m]	GR	OUP			·····		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	· · · 、		
18 3.0 0     AI ph       RESIDUAL CL <sub>2</sub> AI ph       TIME     FLOW       LEVEL     FLAGELLATES       Plant     SEPTA       FREE     Fairhaven-       SWIMMING     Mattapoise       STALKED     Marion-	~ ~		6 I	2	34		······································		-	·····		<u> </u>		ÁMOFBO		ι <sub>τ</sub> β					INF.	. TEM	e <u>20</u> .
TIME     FLOW     LEVEL       i     plant       i     i <td>1.8</td> <td>3.0</td> <td><u>Ö</u></td> <td></td> <td><u> </u></td> <td></td> <td></td> <td></td> <td></td> <td>· · · · · · · · · · · · · · · · · · ·</td> <td>· · · · · · · · · · · · · · · · · · ·</td> <td></td> <td></td> <td>1,</td> <td>5</td> <td>15</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>6.5</td>	1.8	3.0	<u>Ö</u>		<u> </u>					· · · · · · · · · · · · · · · · · · ·	· · · · · · · · · · · · · · · · · · ·			1,	5	15							6.5
IIME     FLOW     LEVEL       i     plant       i     plant <td< td=""><td></td><td></td><td></td><td></td><td></td><td></td><td>·</td><td>-</td><td></td><td>•</td><td></td><td>····</td><td></td><td></td><td></td><td></td><td>2</td><td></td><td></td><td></td><td></td><td>•</td><td>6.3</td></td<>							·	-		•		····					2					•	6.3
SEPTA SEPTA FREE SWIMMING CILIATES Mattapoise Marion-	IIME			LEY	/CL	-11				· · · · · · · · · · · · · · · · · · ·				FLAGEL	LATES	5 Ø	27			· .	<b>AZ</b> p	h	<u></u>
FREE SWIMMING Mattapoise	:		aut		· · · · · ·	-							•	,	• •					1		SEPT	AGE
STALKED Marion-					·				_					FREE	2		, ,				Fairl	haver	
STALKED Marion-					<u> </u>			<b>.</b>				· · · ·		SWIMMIN	١Ġ	N.				•	•		· .
	:			_					_					- <u> </u>		1. A. C.		•			Matt	apois	sect-
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avg. Rochester			<u>avg</u> 2 S	. <u>.</u>			FINISH	· ·								SRA				- 1	Koch	este	· ·
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OUT: WORMS'					•		OUT:			· ·		•		WORMS			0			· .		·	total

	· · · · · · · · · · · · · · · · · · ·	SETTLEOME	TER		FAIRHAY	EN CON	TROL DA	TA LOG	· INITI	ALS	1.1	D DA	TE: 10	11	115
IME	9:20	:1.5	SAMPLES		INF 25	A3 5ml	PRI 25	EFF 100	F3 100	F4			1 R4	•	
·····	SSV SSC	SSV SSC	. CRUCIBLE						< .	1	F)				
0	1000		WT. + SAMI	PLE 					•		]	'-		$\langle \cdot \rangle$	
5	800		CRUCIBLE		71.2621	21.3069	22.0376	16.5819	21.3179	. ·		21.75	12 .	)	19.437
0	550		WT.	•	21.2618			16.5809			Ľ.	21.755	7	1	19.426
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20 25 ·	390 .		PRE-FURN		.12	2460	64	10	355		<u> .                                    </u>	300	_	$\underline{\cdot}$	2180
30	300		CRUCIBLE WT. + SAMI		2/2/2/	21.3069	22.0346	16.581	21.3179	, ·		21,75>	2	)	19.437
40	240					1	· ·	1.						ĺ	
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50	180		DIFFEREN		,0003	.0070	.0016	-0010	,0179	-		,00.11	1-1		,0064
2		23	VOLATILE		12.	1400	64	10	179		/	220		•	1280
1.5 12 3	<u>1.5 c</u> 3 4 R 1.	234	PRE-FURN		.0	1060	ø	Ó	176			. 80			900
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RII	7/14 8 1	2 3 4		FORM I	BACTERIA	· · · ·		MICROO	RGANISM	<u> </u>	<u>{</u>	- <b>-</b>			
	<u> </u>		SAMPLE -	COL	ONIES	#/10	0ml		DUP .				<u> </u>	NOTE	.5 .
2 3		2 3 4	·		•	· · ·			(.)	:			2017		20.4
20	RESIDUAL	<u> </u>			•			АМОЕВО	DS Fit		•		1.		
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:	plant					·	······································		in A	53		•	A2. pl	'n	6.4
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		· · · · · · · · · · · · · · · · · · ·				<u> </u>		FREE SWIMMING	3	<u>}</u>			Fairh	aven	<b></b>
:		-	·	·			· · · ·	CILIATES	- And				Matta	pois	ett-
<u>:</u>								<b>ŞTALKED</b>	¥.S					1	· .
	avg.		START:					CILIATES		X.		•••.••	Mario	<u>n</u>	
	H 2 S		FINISH:				·	*	AS.				Roche	ster	-
			•				•	ROTIFERS	and the second	ti l	•				:
	•		OUT:	;				WORMS'		<u>ч</u>			Acush	net-	
									6-2	۶		•		£	otal

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